

# ISO-VISCOSITY CURVES FOR CaO-SiO<sub>2</sub>-Al<sub>2</sub>O<sub>3</sub>-MgO STEELMAKING SLAGS AT 1500°C

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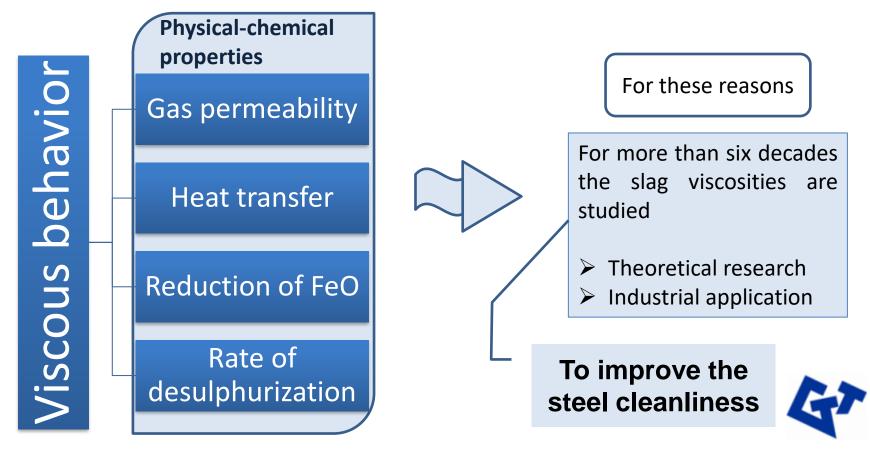
## **Summary**

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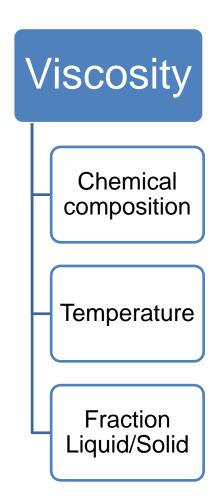


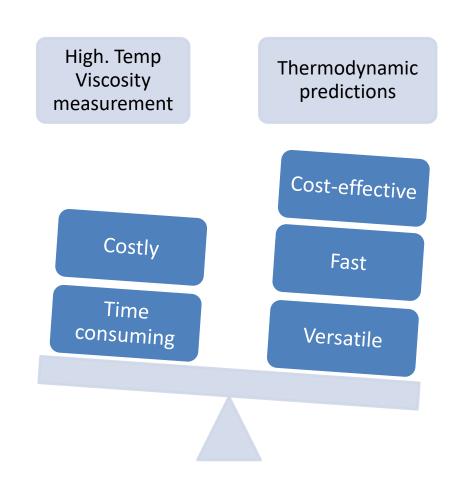


Why study the viscous behavior of the steelmaking slags?



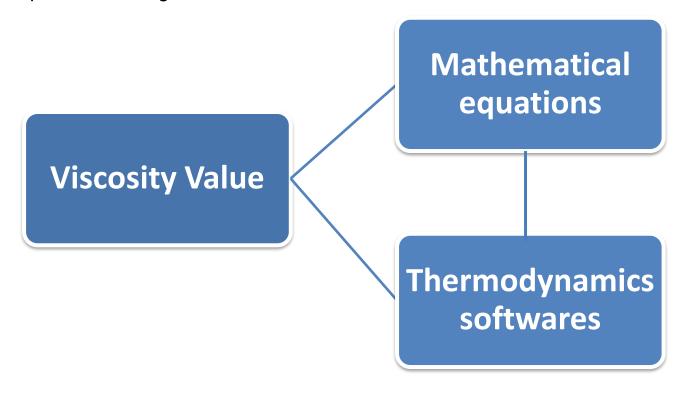








• For thermodynamic predictions it is possible to apply mathematical models or thermodynamic softwares to obtain viscosities for a given range of chemical composition and temperature of slags.



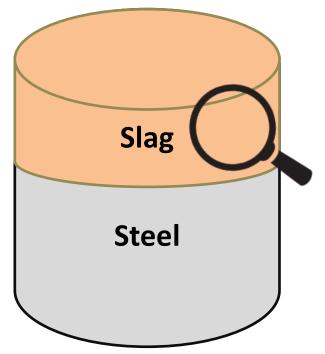




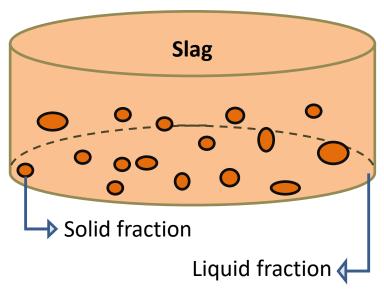
• As known, steelmaking slags in high temperatures presents two-phase melt, Phase Mixture, in which it contains a liquid fraction and a solid fraction.

 The steelmaking slags, at secondary refining, conventionally contains CaO, SiO<sub>2</sub>, Al<sub>2</sub>O<sub>3</sub>, MgO,

(CSAM System);





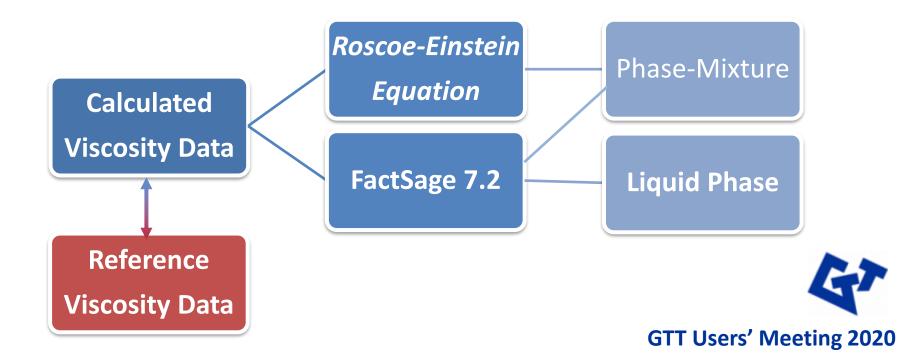


Solid particles hamper the viscosity measurements in the Phase Mixture.





- The aim of the present work is to apply a mathematical model and thermodynamic software, *FactSage 7.2*, to the Phase Mixture and thermodynamic software to the Liquid Phase, *FactSage 7.2*, to obtain the slags viscosities in <u>CSAM system</u>, for a given temperature of <u>1500°C</u> and within a range of chemical composition of slags.
- And calculate the convergence of the experimental data, collected in the literature, with a calculated data.





## **DEVELOPMENT - Experimental X calculated**

 In order to verify the accuracy of the FactSage 7.2 software in the system CSAM, experimental viscosity data were collected through published works

System	Author	Method	Crucible	Data
	Machin,1945	Oscillating	Pt	5
	Machin, 1948	Oscillating	Pt	43
SiO <sub>2</sub> -Al <sub>2</sub> O <sub>3</sub> -CaO	Machin, 1952	Oscillating	Pt	16
Data: 90	Machin, 1954	Oscillating	Pt	12
	Kozakevitch, 1954	Rotating cylinder	Mo/W	12
	Pengcheng, 2016	Rotating cylinder	Мо	2
	Machin,1945	Oscillating	Pt	15
	Machin, 1952	Oscillating	Pt	48
	Machin,1954	Oscillating	Pt	32
	Hoffman,1959	-	-	10
SiO2-Al2O3-CaO-MgO	Kozakevitch, 1966	Rotating cylinder	Mo/W	3
Data:152	Kowalski,1995	-	-	21
	Saito,2003	Rotating cylinder	Pt/Rh	3
	Kim,2010	Rotating cylinder	Pt/Rh	4
	Song,2011	Rotating cylinder	Mo	6
	Pengcheng, 2016	Rotating cylinder	Мо	10
Total Data				242





Hoffman, 1959

Kowalski,1995

Saito, 2003

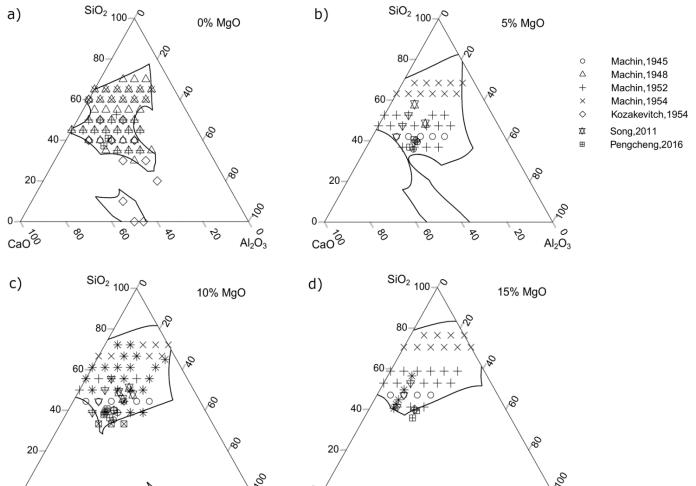
Kim,2010

Liquid phase

Kozakevitch, 1966

## **DEVELOPMENT - Experimental X calculated**

CaO S



CaO S

 $Al_2O_3$ 

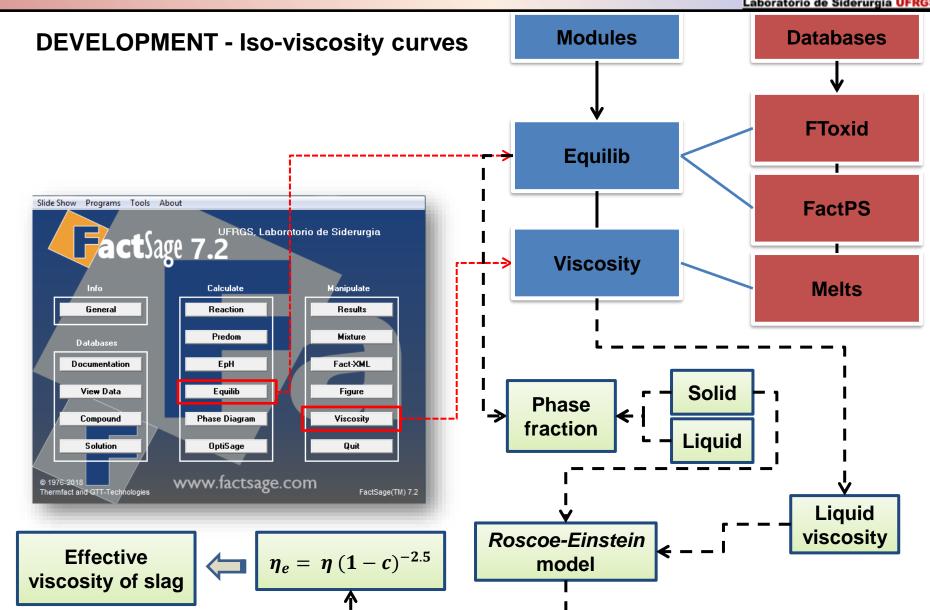
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 $Al_2O_3$ 



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# **DEVELOPMENT - Iso-viscosity curves**

• Composition ranges of calculated slags in the viscosity database (mass%).

System	Phase	MgO	SiO <sub>2</sub>	Al <sub>2</sub> O <sub>3</sub>	CaO	Calculated Data
SiO <sub>2</sub> –Al <sub>2</sub> O <sub>3</sub> –CaO–MgO Data: <b>5976</b>	Liquid	0	0 - 76	0 - 54	6 - 60	535
	Mixture	0	0 - 43	0 - 77	23 - 100	902
	Liquid	5	0 - 78	0 - 60	0 - 54	814
	Mixture	5	0 - 42	0 - 65	29 - 95	666
	Liquid	10	0 - 80	0 - 58	0 - 52	632
	Mixture	10	0 - 46	0 - 67	12 - 90	1025
	Liquid	15	32 - 70	0 - 36	0 - 44	608
	Mixture	15	0 - 40	0 - 56	28 - 85	794





#### **DEVELOPMENT - Iso-viscosity curves**

• In order to verify the convergence between the *FactSage* calculations and the reference viscosity data, for each slag composition, it was evaluated by the difference between measured and calculated viscosity value:

$$\delta_i = \frac{\eta_{Reference} - \eta_{FactSage}}{\eta_{Reference}}$$

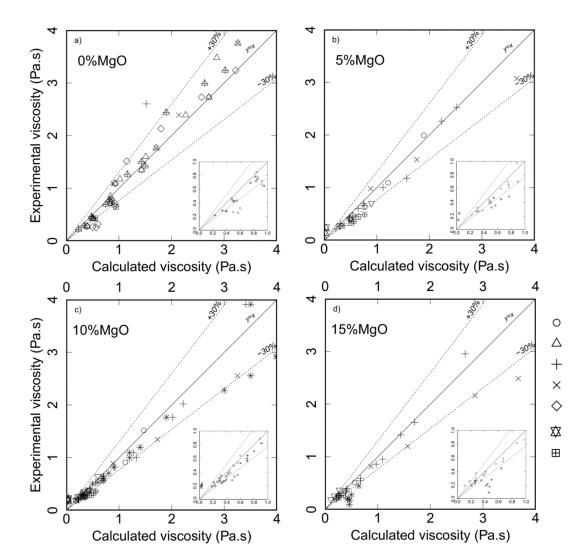
• A performance analysis of the reference source on viscosity  $(\eta)$  calculations through FactSage was evaluated by average relative error,  $\Delta$ , for N measurements of viscosity.

$$\Delta = \frac{1}{N} \sum_{i=1}^{N} \delta_i \times 100\%$$





## **RESULTS AND DISCUSSION - Convergence data**



According with Literature, the viscosity measurements values may differ from recommended values by an average of ± 30%.

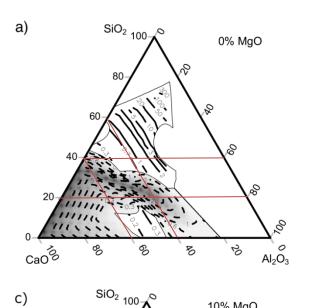
Machin,1945	$\nabla$	Hoffman,1959
Machin,1948	$\boxtimes$	Kozakevitch,1966
Machin,1952	*	Kowalski,1995
Machin,1954	$\Phi$	Saito,2003
Kozakevitch,1954	$\oplus$	Kim,2010

Song,2011 Pengcheng,2016





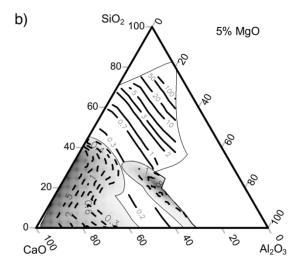
## **RESULTS AND DISCUSSION - Iso-viscosity curves**

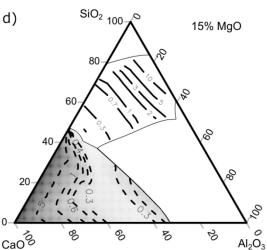


10% MgO

c)

CaO





- MgO typically as a network "modifier"
- CaO

Liquid Phase: viscosity

decrease

Phase Mixture:

"double effect"

Melilite

Liquid phase

Phase mixture

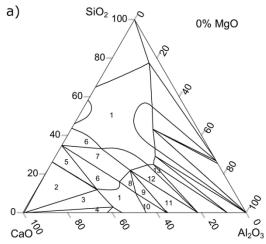
Liquid Fraction 0 0.1 0.2 0.3 0.4 0.5 0.6 0.7 0.8 0.9 1

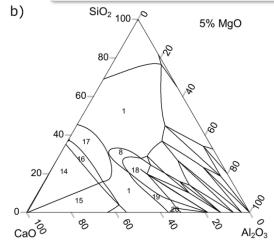


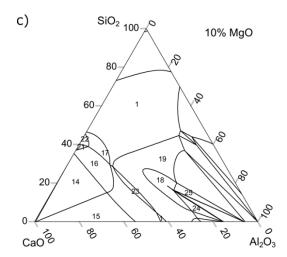
# **RESULTS AND DISCUSSION - Iso-viscosity curves**

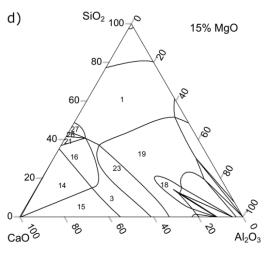


## Melilite $((Ca_2(Al,Mg,Fe^{2+})(Si,Al)_2O_7)$





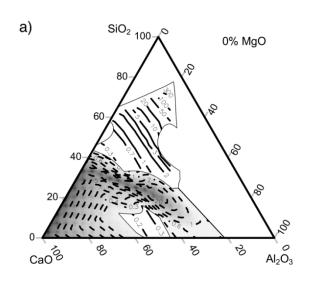


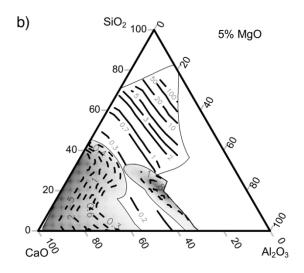


- Slag-liq
- 2 Ca{3}SiO{5} + Monoxide + Slag-liq
- 3 Monoxide + Slag-liq
- 4 Ca{3}Al{2}O{6} + Monoxide + Slag-liq
- 5 Ca{2}SiO{4}(s3) + Ca{3}SiO{5} + Slag-liq
- Ca{2}SiO{4}(s3) + Slag-liq
- 7 Ca{2}SiO{4}(s3) + Melilite + Slag-liq
  - Melilite + Slag-liq
- CaAl{2}O{4} + Melilite + Slag-liq
- 0 CaAl{2}O{4} + Slag-liq
- 11 CaAl{2}O{4} + CaAl{4}O{7} + Melilite
- 12 CaAl{4}O{7} + Melilite + Slag-liq
- 3 CaAl{4}O{7} + Slag-liq
- 14 Monoxide + Monoxide#2 + Slag-liq + a-(Ca,Sr)2SiO4
- 15 Monoxide + Monoxide#2 + Slag-liq
- 16 Monoxide + Slag-liq + a-(Ca,Sr)2SiO4
- 17 Slag-liq + a-(Ca,Sr)2SiO4
- 18 Melilite + Slag-liq + Spinel
- 19 Slag-liq + Spinel
- 20 CaAl{2}O{4}+ Slag-liq + Spinel
- 21 Ca{3}MgSi{2}O{8} + Monoxide + Slag-liq + a-(Ca,Sr)2SiO4
- 2 Ca{3}MgSi{2}O{8} + Slag-liq + a-(Ca,Sr)2SiO4
- 23 Monoxide + Slag-liq + Spinel
- 24 CaAl{4}O{7} + Melilite + Slag-liq + Spinel
- CaMg{2}Al{1}{6}O{2}{7} + Melilite + Slag-liq + Spinel
- Ca{3}MgSi{2}O{8} + Monoxide + Slag-liq
- 27 Ca{3}MgSi{2}O{8} + Slag-liq

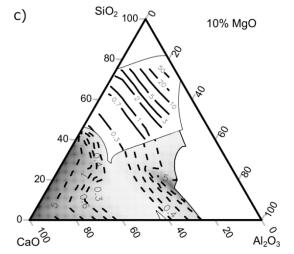


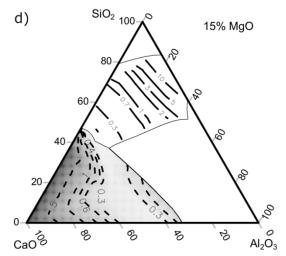
# **RESULTS AND DISCUSSION - Iso-viscosity curves**





 Increase of SiO<sub>2</sub>
 Liquid Phase showed an expressive increase in the slag viscosity.





Liquid phasePhase mixture

Liquid Fraction
0 0.1 0.2 0.3 0.4 0.5 0.6 0.7 0.8 0.9 1



#### **CONCLUSIONS**

- The viscosities calculated through chemical compositions of the literature were generally within the acceptable range of relative error compared to the literature (up to 30%).
- By the analysis proposed it is possible to visualize that the effect of the MgO content decreases the viscosity in the Liquid Phase.
- The effect of the CaO oxide for the Phase Mixture showed a double effect. Initially a
  reduction in viscosity subsequently, tends to increase viscosity. However in Liquid Phase
  tends to decrease the viscosity.
- The *FactSage 7.2* showed to be very promising for the creation of quarteternary systems with iso-viscosity curves.





## **Acknowlegments**









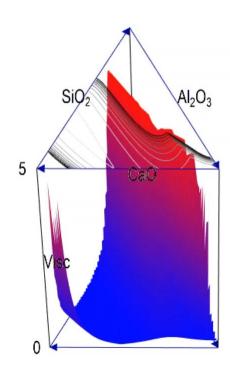
#### **Next steps**

Influence

Several temperatures [1500-1700°C]

Oxides (FeO, TiO<sub>2</sub>, MgO)

CaO-SiO<sub>2</sub>-Al<sub>2</sub>O<sub>3</sub> system (%mass) at 1600°C





-0.1 -0