

# Modelling non-ferrous processes and the importance of the gas phase

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**InsPyro**



# 5 years InsPyro: references

## Lead



## Zinc



## Steel



## Foundry

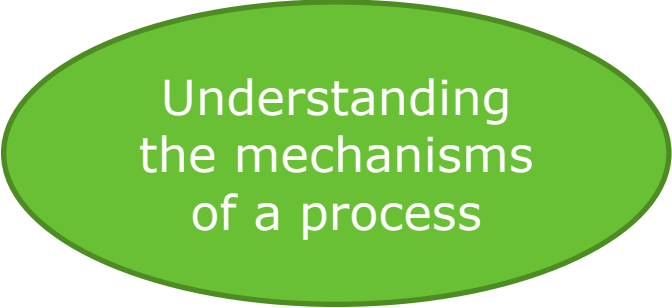


## Various




# InsPyro approach

= Knowledge centered approach



Understanding  
the mechanisms  
of a process

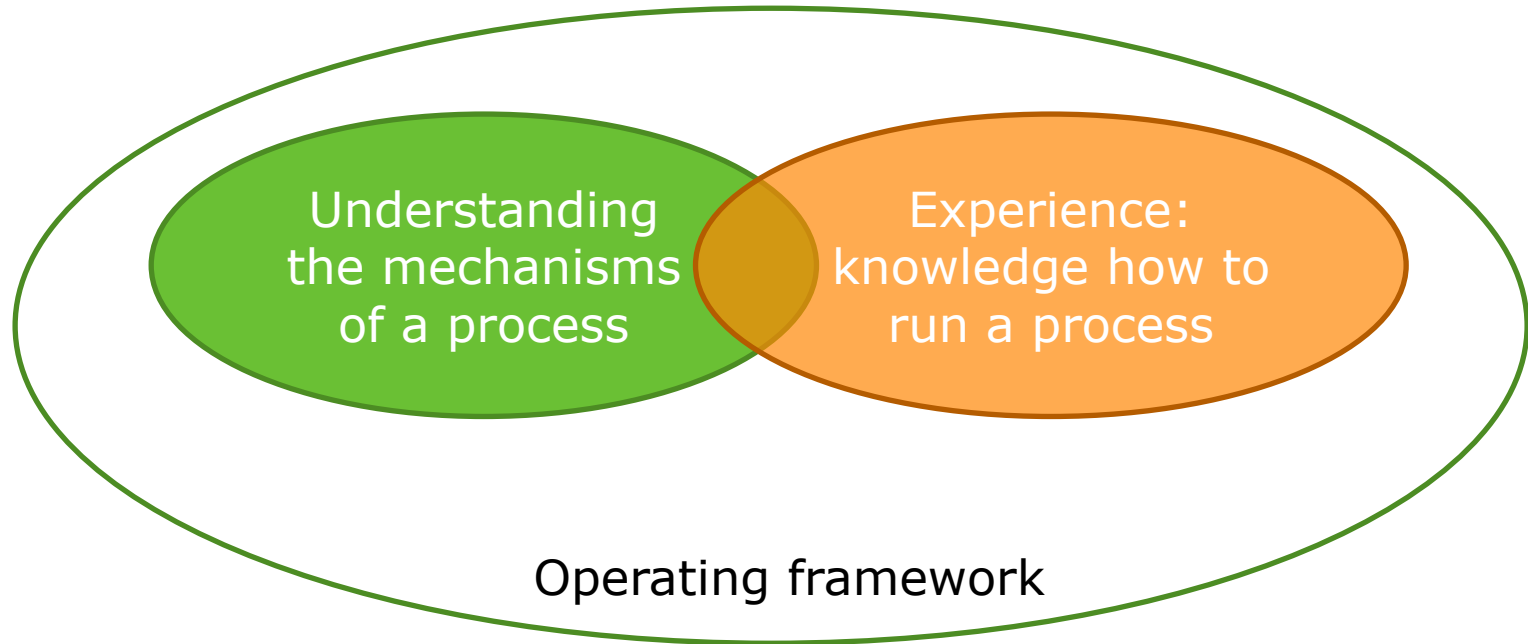
- Useful to run a process
- Control depends on model
- Changes are based on physics, thermodynamics...
- Mechanisms get unraveled
- Transferrable



Experience:  
knowledge how to  
run a process

- Essential to run a process
- Control depends on individual
- Changes based on trial and error
- Mechanisms unclear
- Experience transfer is difficult

# InsPyro approach



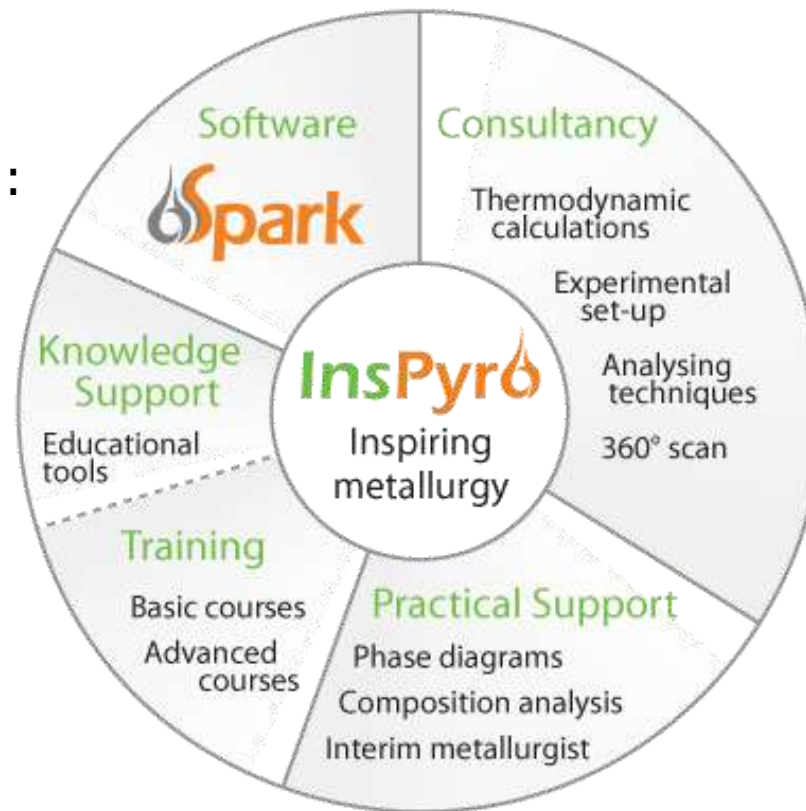
# Knowledge management

- Knowledge in the heads of people is the most readily applicable, but the most volatile:
  - People leave, retire, are on holiday
  - Intuition and feelings may be working most of the time, but may never be thoroughly checked/understood
- Need to develop concepts which are more easily transferable:
  - Define rule of thumb based on mechanisms
  - Actual process model can be useful for complex interactions
  - Summaries, concepts, hypotheses can already be much more tangible than feelings, and can be validated
  - Provide a basis for decision making, experimenting, education of operators

# Mission: « Inspiring Metallurgy »

InsPyro improves existing high-temperature processes  
develops new sustainable processes

Full circle approach:



# Process development

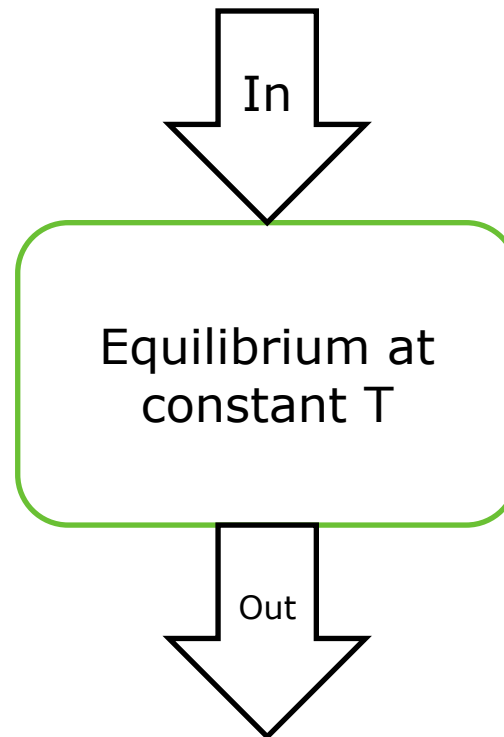
- Stepwise process:
  1. Concept from literature or experience
  2. Process model to define expected working area
  3. Lab or pilot scale experiments
  4. Validate process model
  5. Scale-up or adjustments
- Nobody will develop a new process without a model
- Yet we run several existing processes without an explicit model

# Process improvement

- Similar approach as for development
  - Literature review
  - Advantage: also process data available
  - Construct process model
  - Verify process model with experience
  - Define conditions which are expected to improve the process
  - Use process as test facility



# Simple process model



Mainly a mass balance with an indication of heat requirements for one operating point

No need to model all possible reactions!

# Integrated in charge calculation



**CHARGE CALCULATION FOR LEAD RECYCLING (SIMPLIFIED)**

**InsPyro**

Selection of raw materials	Amount (kg)	Water content	Dry weight	Composition of dry fraction										Mass balance			
				Pb	Fe	Sb	Ca	Si	Al	Na	S	O	C	organics	Pb	Fe	
Paste	1000	8.0%	920	90.0%								3.0%	7.0%			828	0
Plates	1000	2.0%	980	97.5%		1.0%						0.5%	0.5%		0.5%	956	0
Coke	25		25				0.5%	1.0%	1.0%						95.0%	0	0
Lime	5		5				71.5%						28.5%			0	0
Iron turnings	70		70	100.0%												0	70
Soda ash	20		20								43.4%		45.0%	11.0%		0	0

**Model estimation: using thermodynamic calculations**

Temperature: 1100 °C      Heat need/input: DEMO kWh      Recalculate

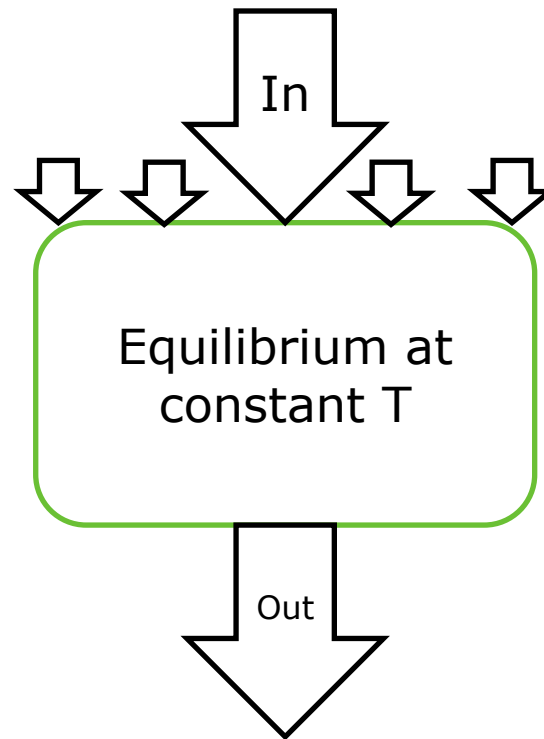
Ready

Total weight (kg)		Solid phases:			
Bullion	1738	Pb	Sb	S	O
		99.1%	0.6%	0.32%	0.00%
Slag	14	CaO	SiO2	FeOx	Na2O
		32.8%	37.4%	3.9%	22.5%
					Na2SO4
					0.2%
					PbO
					0.1%
					Al2O3
					3.1%
					...
Matte	159	Fe	S	O	Na
		40.7%	16.2%	7.3%	3.8%
					Pb
					32.0%
Gas	100	SO2			
		0.04 kg			
Other phases	8	kg Fe excess	kg C excess		
		0 kg	0 kg		

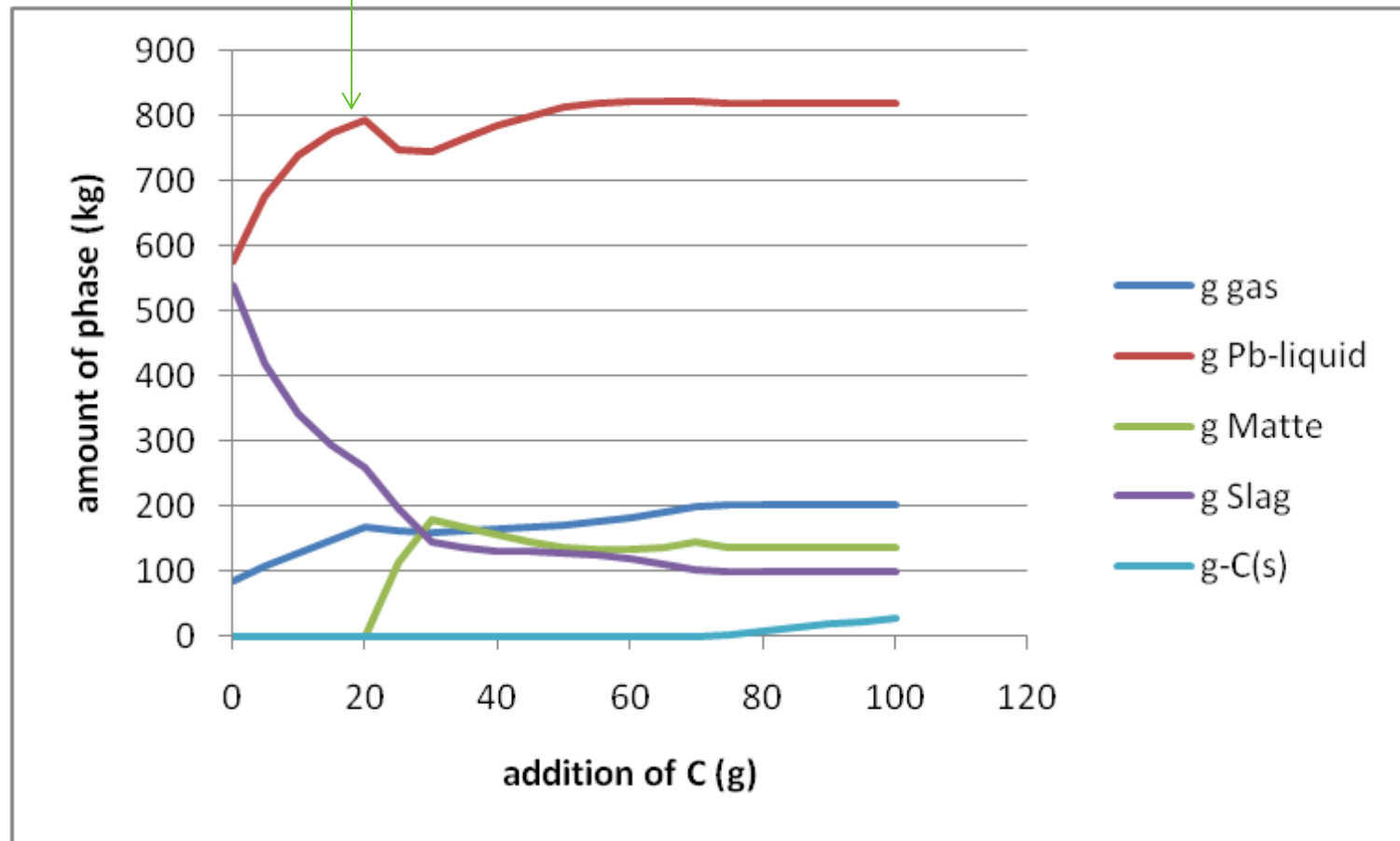
Composition of raw materials		Analysis dry fraction										
Raw material name	Water fraction	Pb	Fe	Sb	Ca	Si	Al	Na	S	O	C	organics
Plates	2%	97.5%		1.0%					0.5%	0.5%		0.5%
Paste	8%	90.0%							3.0%	7.0%		
Cable strippings		90.0%	5.0%									5.0%
Lead ingots		99.9%		0.1%								

# Stepwise simple process model



# Process modelling – Pb recycling

- Effect of carbon on Pb recycling with CaO-FeO/Fe<sub>2</sub>O<sub>3</sub>-SiO<sub>2</sub> slag
- High Pb(l) at low reduction, but S-rich and PbS(g) losses



# More advanced process model

- Take into account non-equilibrium effects
  - Assume that only a part of the system reaches equilibrium
- Different operating points in a process
  - Split the model for different zones

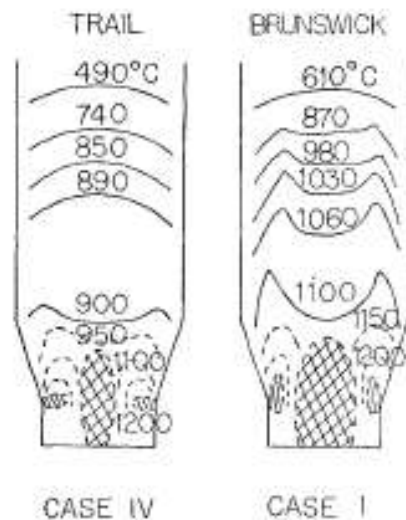


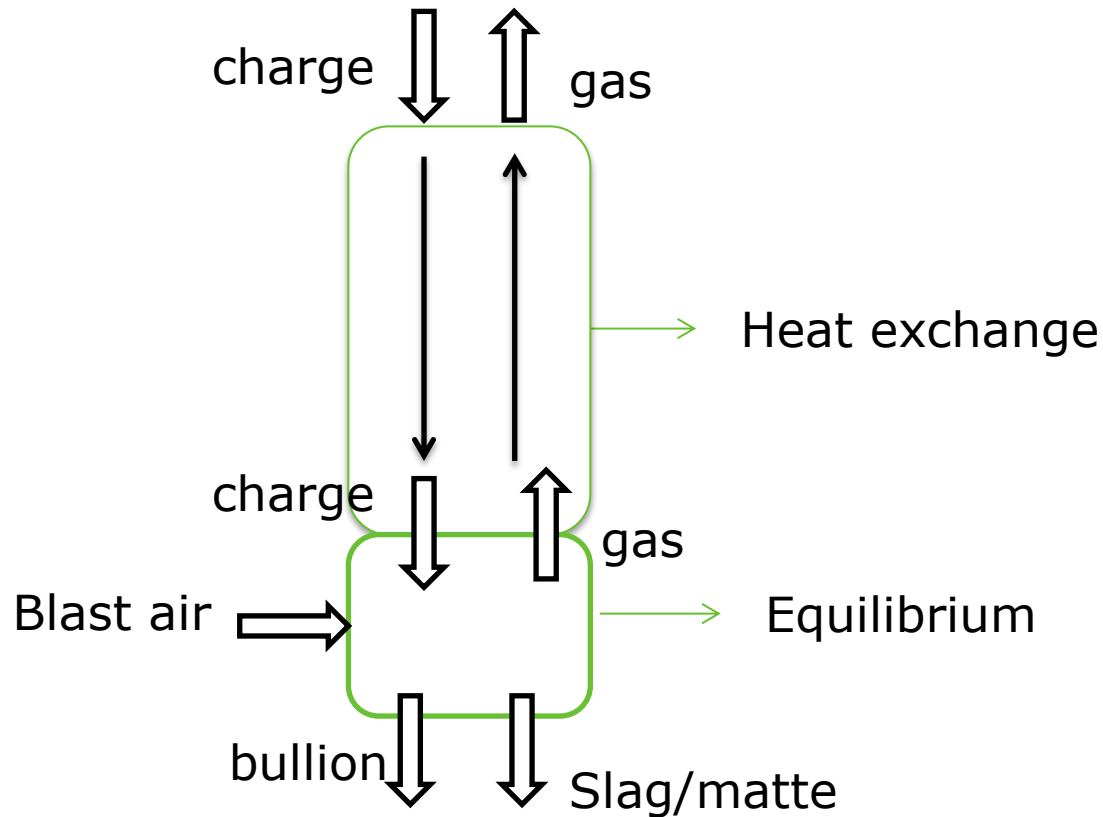
Fig. 13—Proposed isotherms and "dead man" in lead blast furnaces  
Legend: — calculated isotherms, - - - visualized isotherms.

Not a single operational point, but the conditions change continuously over the height of the blast furnace

- Kinetics limit reactions in cold zone
- Equilibrium can be assumed in hot part

**Source:** Chao, Met. Trans.B, 1981

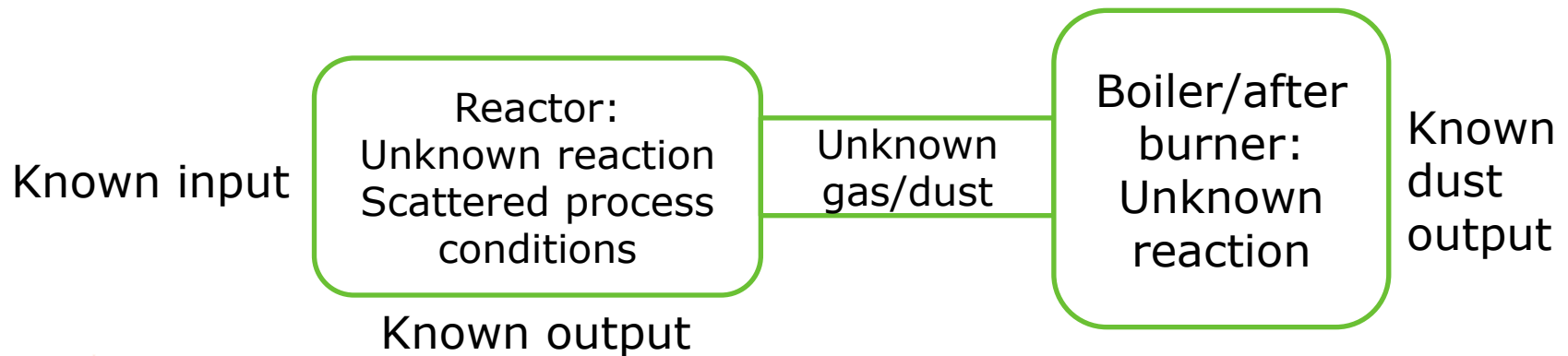
# More advanced process model



Especially the heat balance gets more realistic by implementing preheating

# Advantages of a model

- For a continuously running high-temperature plant
  - Noise causes scatter on process data, so difficult to learn from these data
  - Data over a year basically gives few average working points, despite measuring every second/hour/day
  - Experiments can be risky or expensive, certainly time consuming
  - Additional data can be collected at a single point in time but a framework is needed to do the interpretation



# Experimental set-ups

- Lab scale can give very relevant information, but not process information
- Ask a very well defined subquestion
  - Measure solubility of a certain element in slag
  - Find melting point of a matte
  - Reductive power of carbon materials
  - Maximum separation efficiency of a dross
  - Evaporation losses upon holding at high T for certain time
  - ...



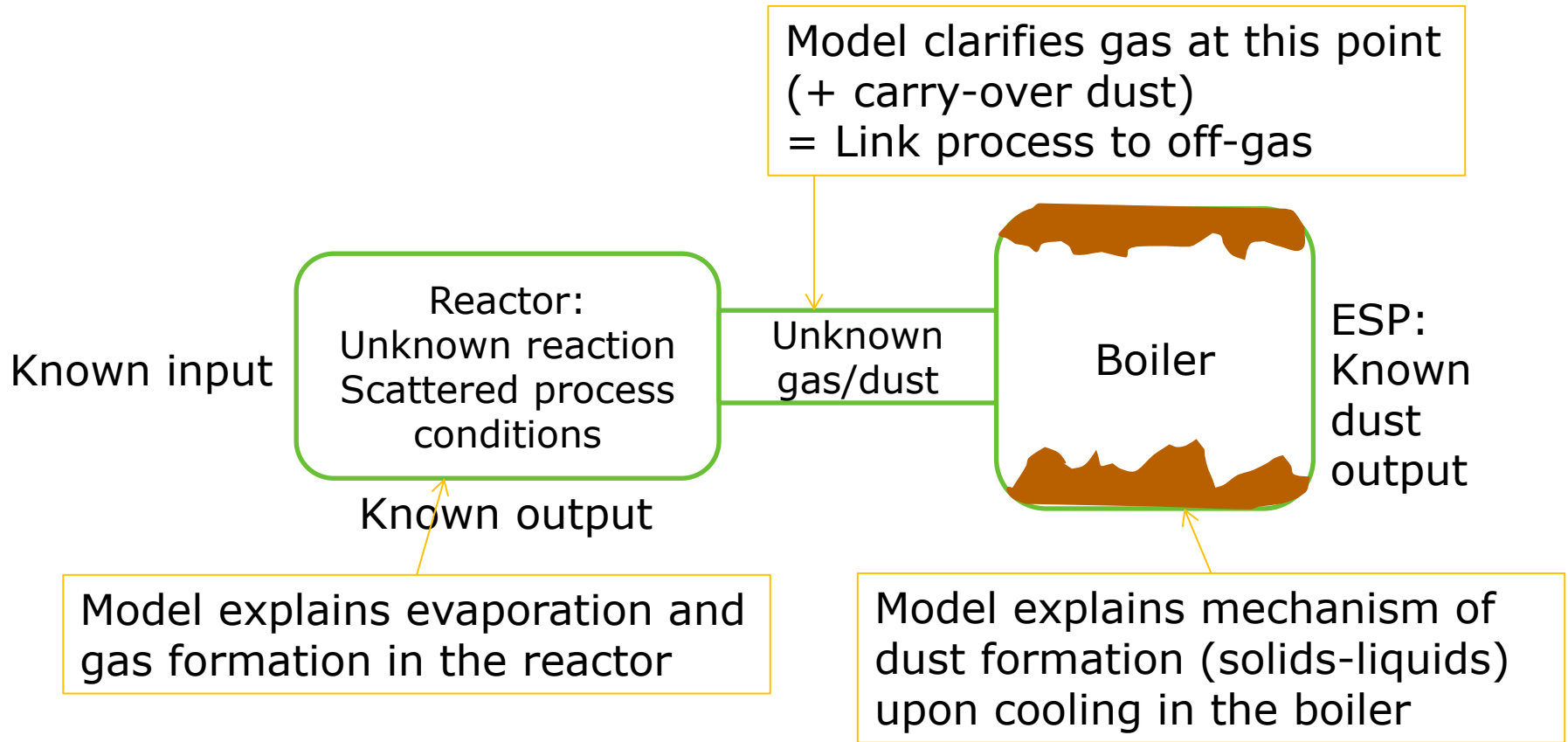


# **EXAMPLES OF THE ADVANTAGES OF A MODEL**

# Accretion formation

- First step: characterizing the accretion
- Second step: validate with framework and look for solutions
  - Define hypothesis for accretion formation mechanism
  - Can the compounds be avoided by changing the process conditions?
    - Temperature
    - Atmosphere
    - Additions
  - Is the accretion inevitable with the current mix, but linked to certain raw materials?

# Accretion formation



# Changing raw materials

- Can they be treated similarly as known materials?
  1. Characterization: not only composition but also phase structure
  2. Feeding into model
  3. Literature may give additional guidelines



# Refining process optimisation

- How close is the refining process to the thermodynamic optimum?
  - Additions
  - Final purity of the lead
  - Temperature
- 1. Analysis of the dross
  - Formed phases
  - Lead losses: entrapped or chemically bound
- 2. Verification with thermodynamic model
  - Effect of input composition
  - Influence of temperature
- 3. Define optimisation opportunities



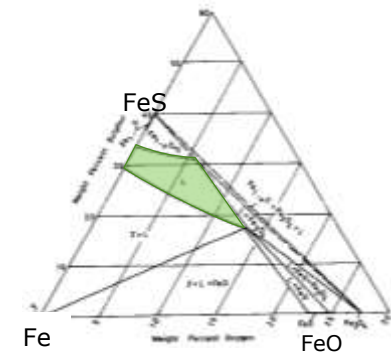
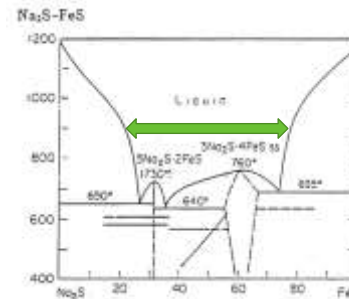
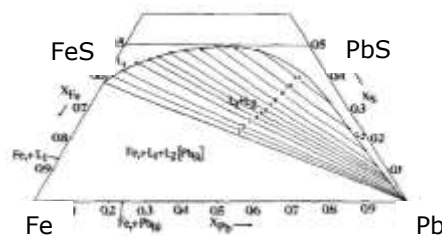
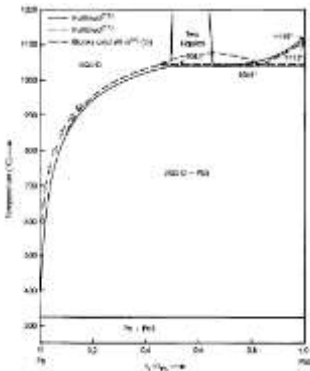
# Not everything fits in a single model

- The first version of a model can not explain everything
  - Kinetics
    - Heating time (linked to enthalpy, but also shape etc.)
    - Reaction time (mixing, settling,...)
  - Undescribed thermodynamics (compounds, rare elements)
- All these aspects can also be modelled, but require a much larger effort
  - CFD
  - Empirical models based on lots of data
  - Thermodynamic database construction
  - Link to materials properties

Open to  
partnerships!

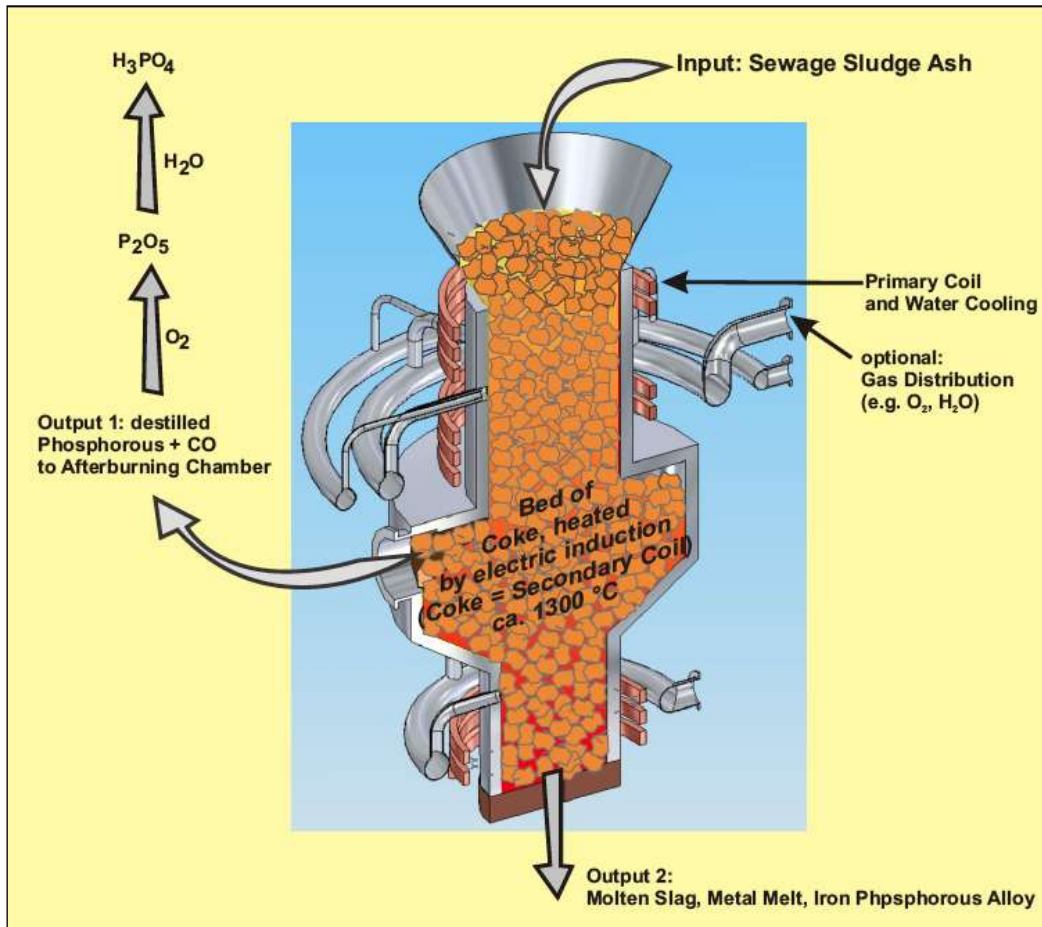
# Thermodynamics of the matte

- InsPyro has constructed a model for the matte:
  - Pb-Fe-S-O-Na system at sulphur rich side
  - Diagrams in literature are limited and several interactions have to be “guesstimated”
  - See presentation GTT2013



# Gas phase: e.g. RecoPhos model

- Fuming reactor (reduction and evaporation of P)

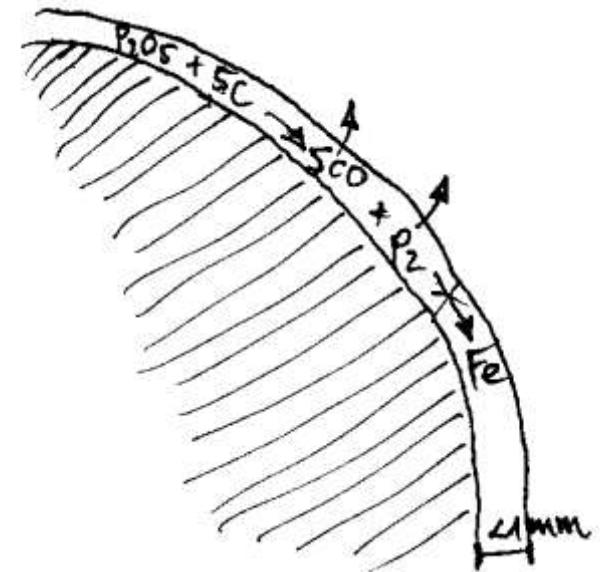
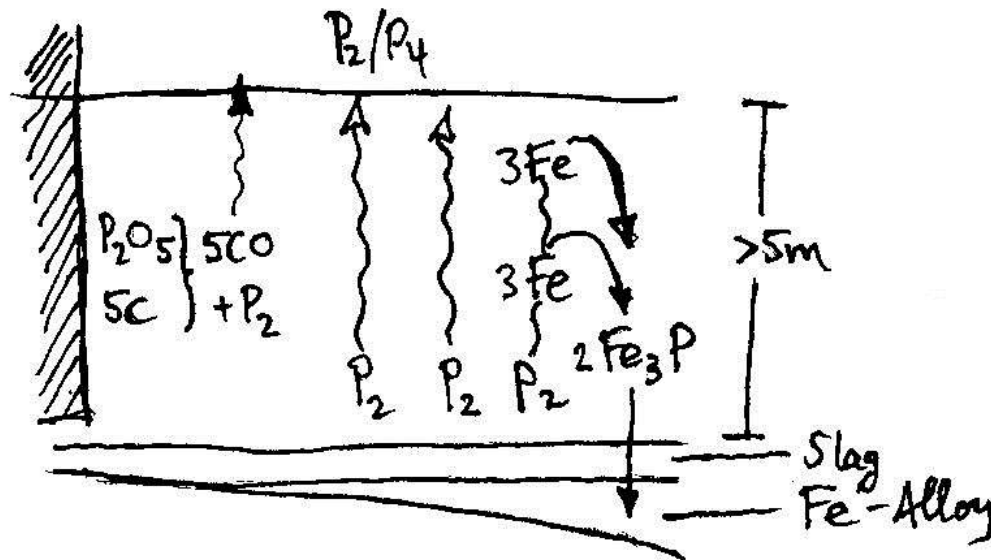


SCOPE newsletter/TPT website



# Questions in the RecoPhos process

- Will the thin-film reaction make a difference?
  - Reduction of P to gas phase before combination with Fe?



H. Raupenstrauch, ProcessNet

# Questions in the RecoPhos process

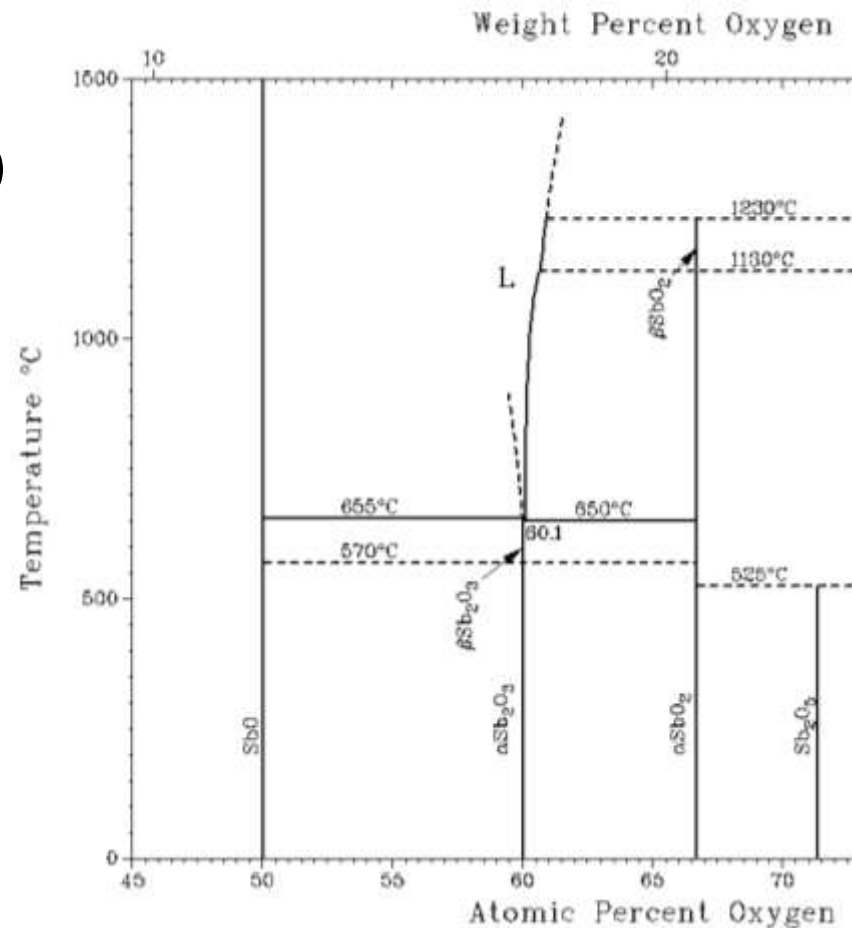
- How will the heavy metals behave?
  - Compounds in gas phase vs. activity in slag/metal
- Can we steer the slag:
  - Optimal viscosity
  - Lower/higher melting temperature
  - Higher P yield
  - Some phase diagram optimisation with  $P_2O_5$

# Thermodynamics of the gas phase

- Also in other processes, lots of evaporation occurs
  - Of course  $\text{SO}_2$ ,  $\text{CO}$ ...
  - Also impurities  $\text{As}$ ,  $\text{Cd}$ ,...
  - And the main metal, certainly in case of  $\text{Pb}$
  - Interaction to form volatile chlorides, oxides, sulphides...
    - E.g. vapour pressure of lead
  - On cooling, complex compounds
    - E.g. sulphates, arsenates, chlorides

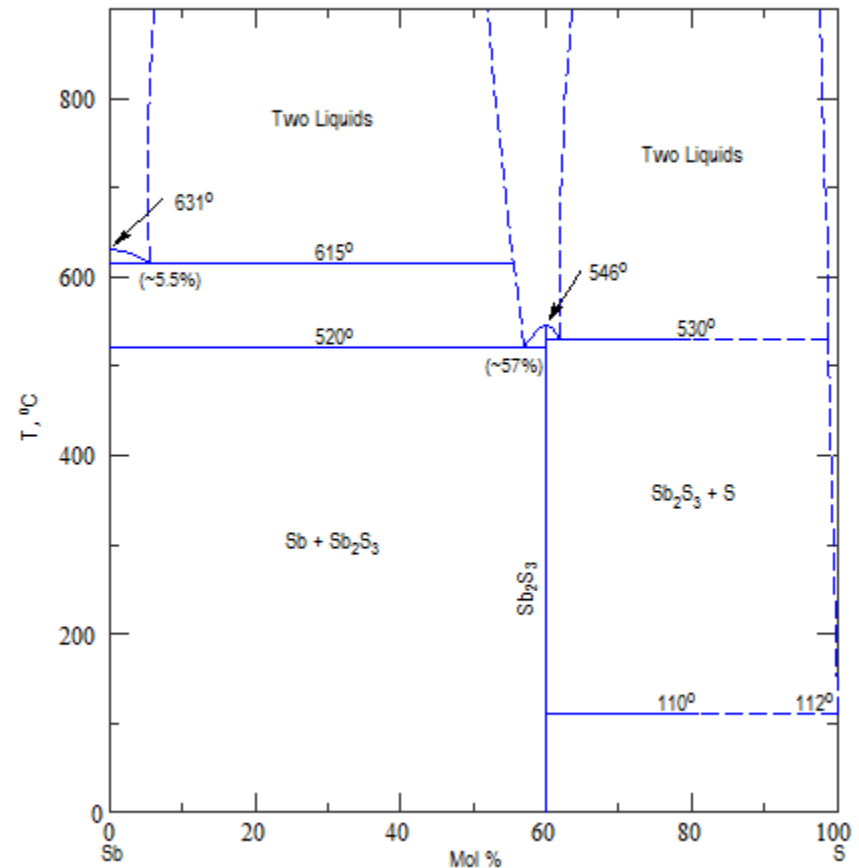
# The case of Sb

- $\text{Sb}_2\text{O}_3$ , a stable oxide known to sublime as  $\text{Sb}_4\text{O}_6$
- FactSage 6.2:
  - Melting at  $656^\circ\text{C}$
  - Evaporation at  $2467^\circ\text{C}$  ( $\text{Sb} + \text{O}_2$ )
- FactSage 6.3/4:
  - Melting at  $655^\circ\text{C}$
  - Dissociation at  $748/763^\circ\text{C}$  to  $\text{SbO}(\text{g}) + \text{SbO}_2(\text{s})$
  - Full evaporation at  $998^\circ\text{C}$  ( $\text{SbO} + \text{O}_2$ )
- Wikipedia:
  - Melting at  $650^\circ\text{C}$
  - Sublimation at  $1425^\circ\text{C}$



# The curious case of Sb

- Stibnite,  $\text{Sb}_2\text{S}_3$ , a known stable sulphide mineral
  - FactSage 6.2:  
melting at  $550^\circ\text{C}$ ,  
boiling at  $1534$  ( $\text{Sb}_2 + \text{S}_2$ )
  - FactSage 6.3:  
melting at  $550^\circ\text{C}$ ,  
sublimation at  $556^\circ\text{C}$   
( $\text{Sb}_2\text{S}_4 + \text{Sb}_4\text{S}_3$ )
  - FactSage 6.4:  
sublimation at  $103^\circ\text{C}$   
( $\text{Sb}_2\text{S}_3$ )
  - Phase diagram: well...



# Conclusions

- Modelling provide a framework for problem solving and fits well in a long term knowledge management strategy
- Apart from condensed phases, the gas phase is an integral part of a metallurgical process and need to be modelled with appropriate attention