



## Selected fields of application for FactSage- Modelling in nonferrous metallurgy

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# IME – Research in nonferrous metallurgy

## General

Institute of RWTH Aachen University  
30 Researchers, 30 technical/administrative staff  
30 BSc- and 20 MSc-thesis per year  
> 500 publications since 1999

## Recycling-Metallurgy

Process development and Scale Up  
Pyro- and Hydrometallurgy  
Minimization of emissions, waste material recycling

## Process technology for metallic materials

Vacuum metallurgy  
Purification of metals and alloys  
Nano powders

## Services and consulting

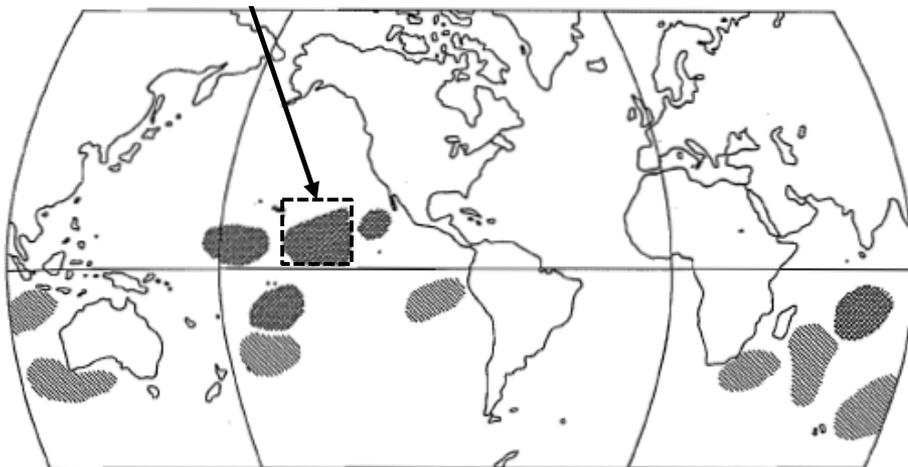


# Study I: Smelting and carbothermic reduction of manganese nodules

## Goals:

- Simulation of ocean nodule smelting
- Approximation of the liquidus temperature of the molten slag
- Influence of  $\text{SiO}_2$  content on the liquidus temperature
- Simulation of the carbothermic metal reduction from liquid slag  
→ Can Mn and Fe content be separated from metal values (Ni, Cu, Co, Mo, V)?

Nodule occurrence with  
current research licenses



5 cm

# Study I: Smelting and carbothermic reduction of manganese nodules

## Model simplifications:

- All metals in ocean nodules occur as simple oxides (see table below)
- Oxides of P, Ba and Sr are not considered, since the slag solution database (FToxid) does not contain data
- 15 component system, elements < 500 ppm are not considered
- Influence of the atmosphere during smelting is omitted

## Reality:

- Metals occur as complex oxidic, hydroxidic, carbonate or phosphate minerals (e.g.  $\text{Na}_4\text{Mn}_{14}\text{O}_{27} \cdot 21\text{H}_2\text{O}$ )
- Approximately 0.7 wt.-% P+Ba+Sr in ocean nodules
- Nodules contain nearly all elements of the periodic table
- Smelting in an open electric arc furnace

## Metal oxides considered in model [wt.-%] of 100%

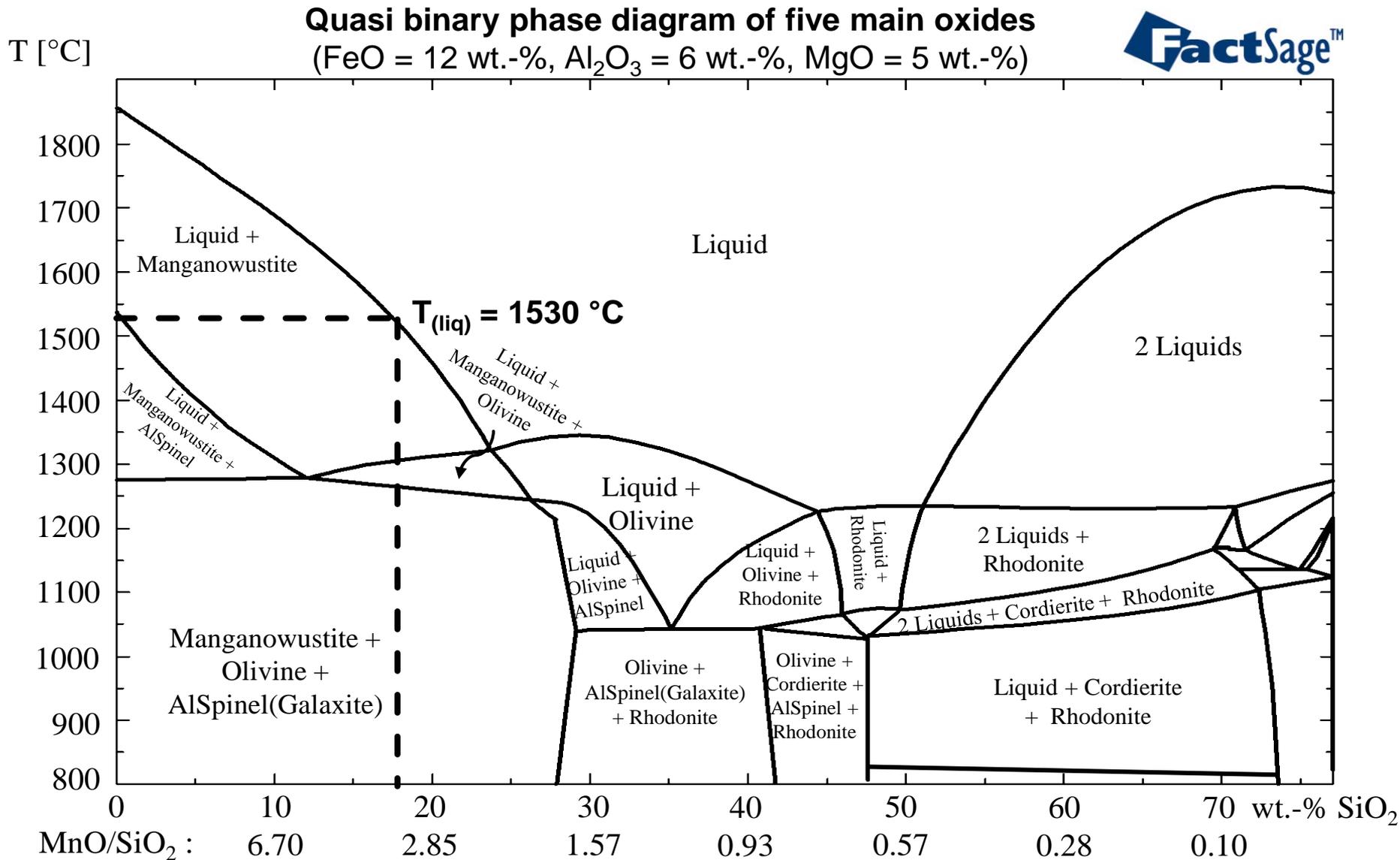
Average of 206 BGR samples → heavy fluctuation in composition

MnO	SiO <sub>2</sub>	FeO	Al <sub>2</sub> O <sub>3</sub>	MgO	Na <sub>2</sub> O	CaO	NiO	CuO	K <sub>2</sub> O	TiO <sub>2</sub>	CoO	ZnO	V <sub>2</sub> O <sub>5</sub>	MoO <sub>3</sub>
51.2	16.1	10.1	5.44	4.05	3.47	2.88	2.19	1.86	1.50	0.54	0.27	0.24	0.13	0.12

## Databases:

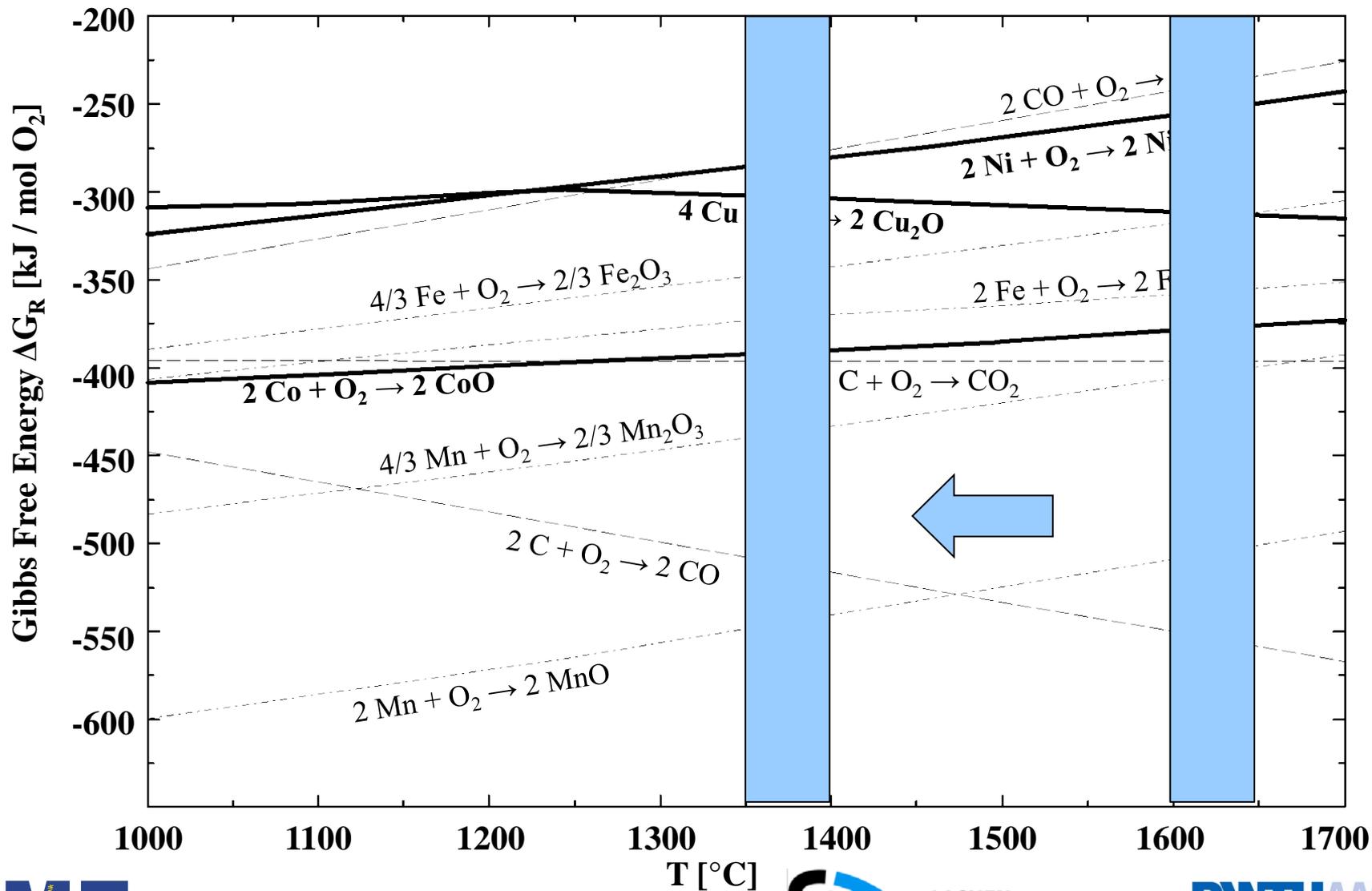
- FactPS
- FToxid (liquid slag and solid solutions)
- SGTE (liquid alloy)

# Study I: Smelting and carbothermic reduction of manganese nodules



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Activity adjusted Ellingham diagram  
(activities of oxides in slag from equilb model)



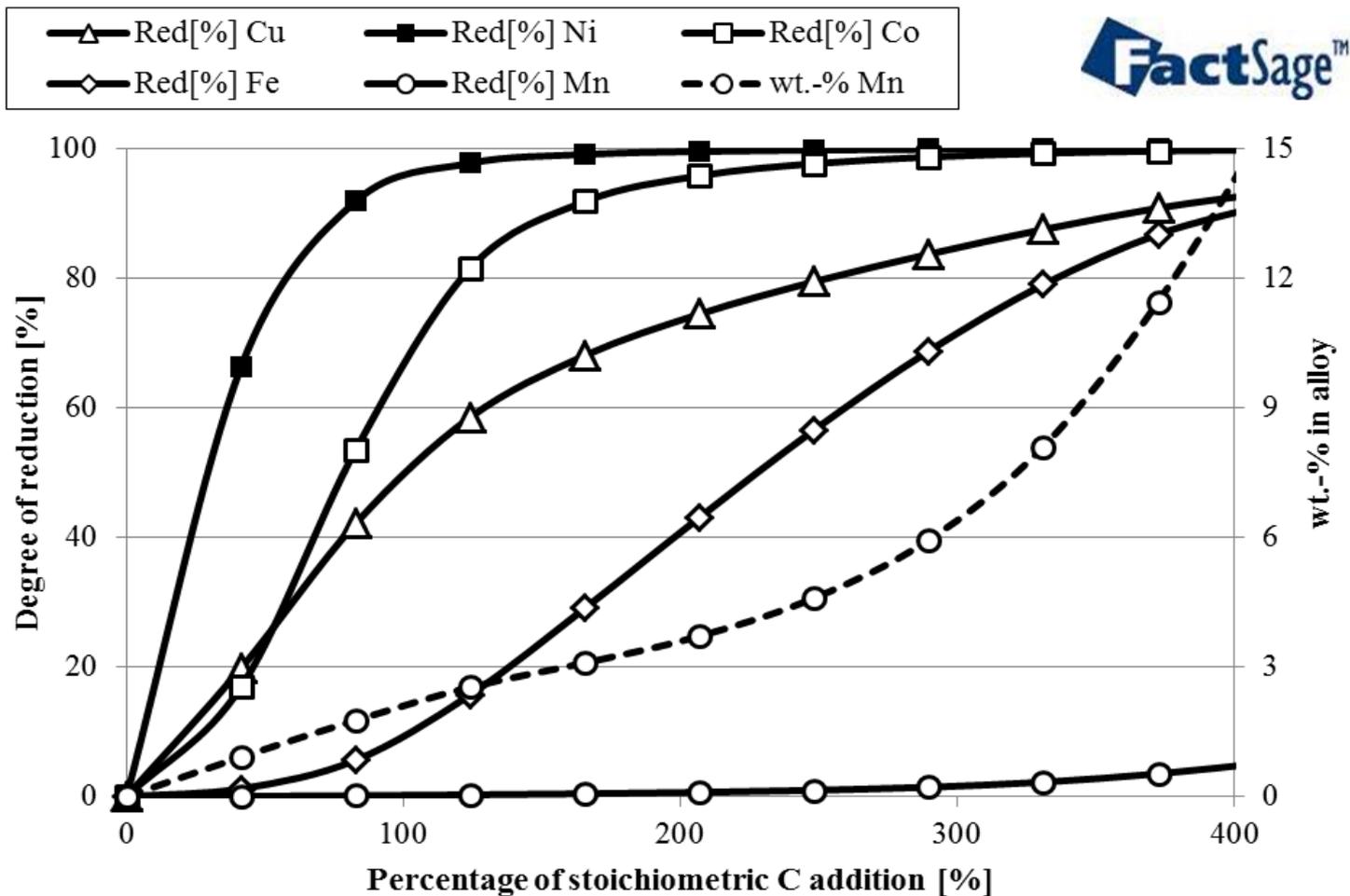
# Study I: Smelting and carbothermic reduction of manganese nodules

## Equilib model of metal reduction

No SiO<sub>2</sub> addition

MnO/SiO<sub>2</sub> = 3.2

→ T = 1650 °C



# Study I: Smelting and carbothermic reduction of manganese nodules

## Equilib model of metal reduction

High SiO<sub>2</sub> addition → 351.54 g/kg SiO<sub>2</sub>

MnO/SiO<sub>2</sub> = 1

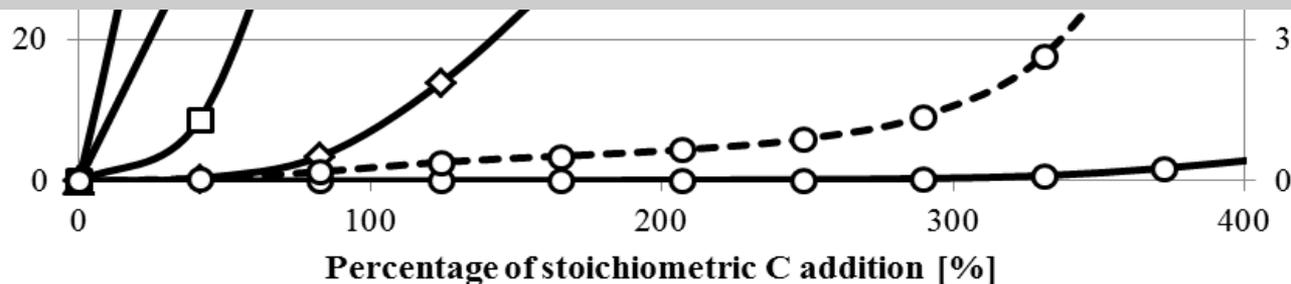
→ T = 1400 °C

### Results:

- SiO<sub>2</sub> addition decreases liquidus temperature significantly
- Metal reduction may be carried out at lower temperature
- Mn reduction becomes thermodynamically adverse
- Fe reduction cannot be avoided thermodynamically

### Key points from model for experiments:

- MnO/SiO<sub>2</sub> ratio should be between 1.5 and 1
- Control of reduction is critical to attain low Mn-content in alloy
- Complete separation of Mn in slag is improbable because of the reduction of Mn<sub>2</sub>O<sub>3</sub>
- Trade-off between undesired Fe reduction and valuable metal recovery is necessary



# Study I: Smelting and carbothermic reduction of manganese nodules



5 cm

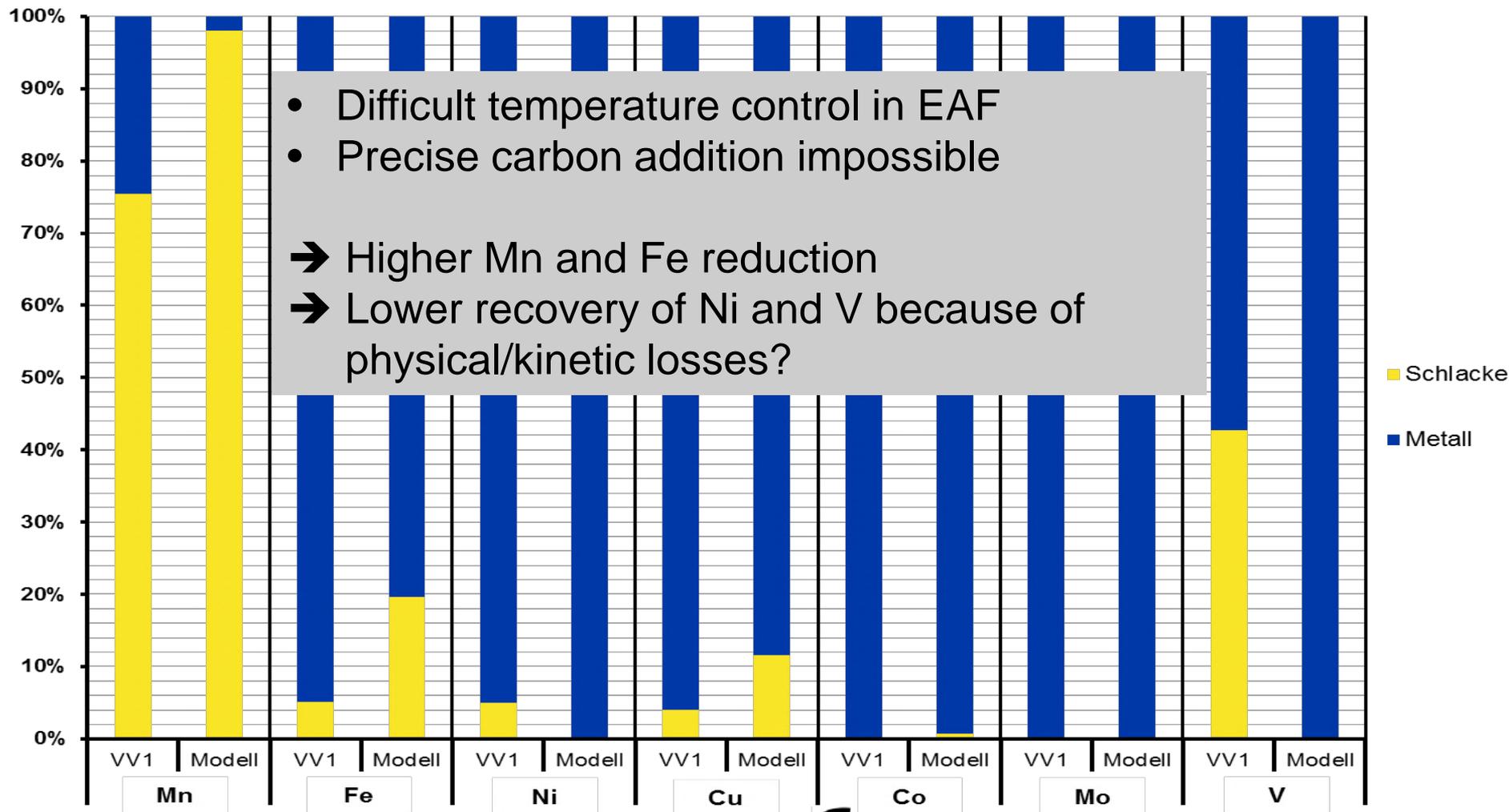


# Study I: Smelting and carbothermic reduction of manganese nodules

## Comparison of model and experiments:

No silica addition ~1650 °C

### Phase distribution comparison

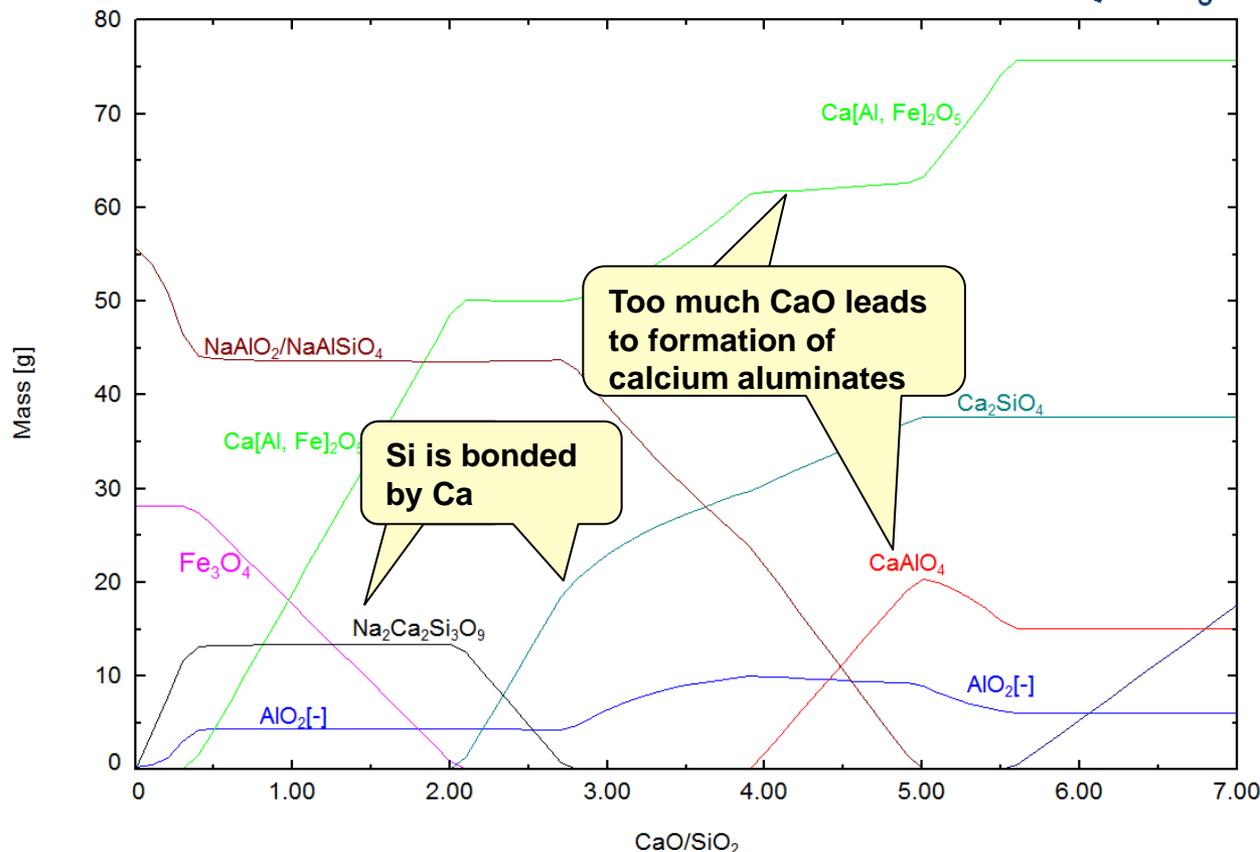


# Study II: Recovery of valuable metals Al and Fe from red mud



Al-solubility depending on the CaO/SiO<sub>2</sub>-ratio

100 g RM, 1 l at 250°C and 200 g/l NaOH (150 g/l Na<sub>2</sub>O)



**Approach:**  
Recovery of  
process with

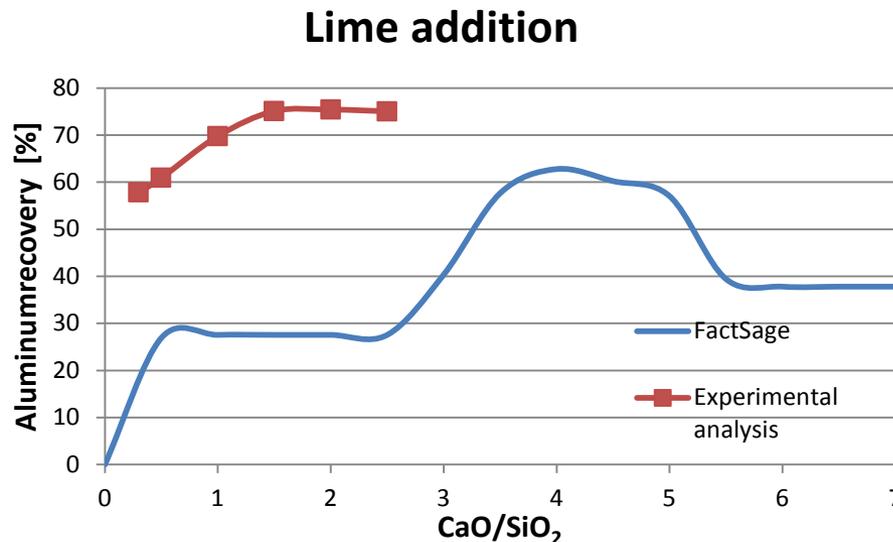
**Goal:**  
The recovery

the Bayer

# Study II: Comparison of FactSage and experiments

Maximum recovery in FactSage at 64% for CaO/SiO<sub>2</sub> of 4

Experiments verify the trend of significantly higher recoveries:



## Problem:

- FactSage -> Equilibrium calculation
  - Reality
    - ➔ existence of other phases (Al(OH)<sub>3</sub>)
    - ➔ 250°C slow kinetics for equilibrium
- ➔ Delayed recovery increase and plateau at CaO/SiO<sub>2</sub> ~1.5 and higher recoveries through readily soluble Al(OH)<sub>3</sub>

## Future approach:

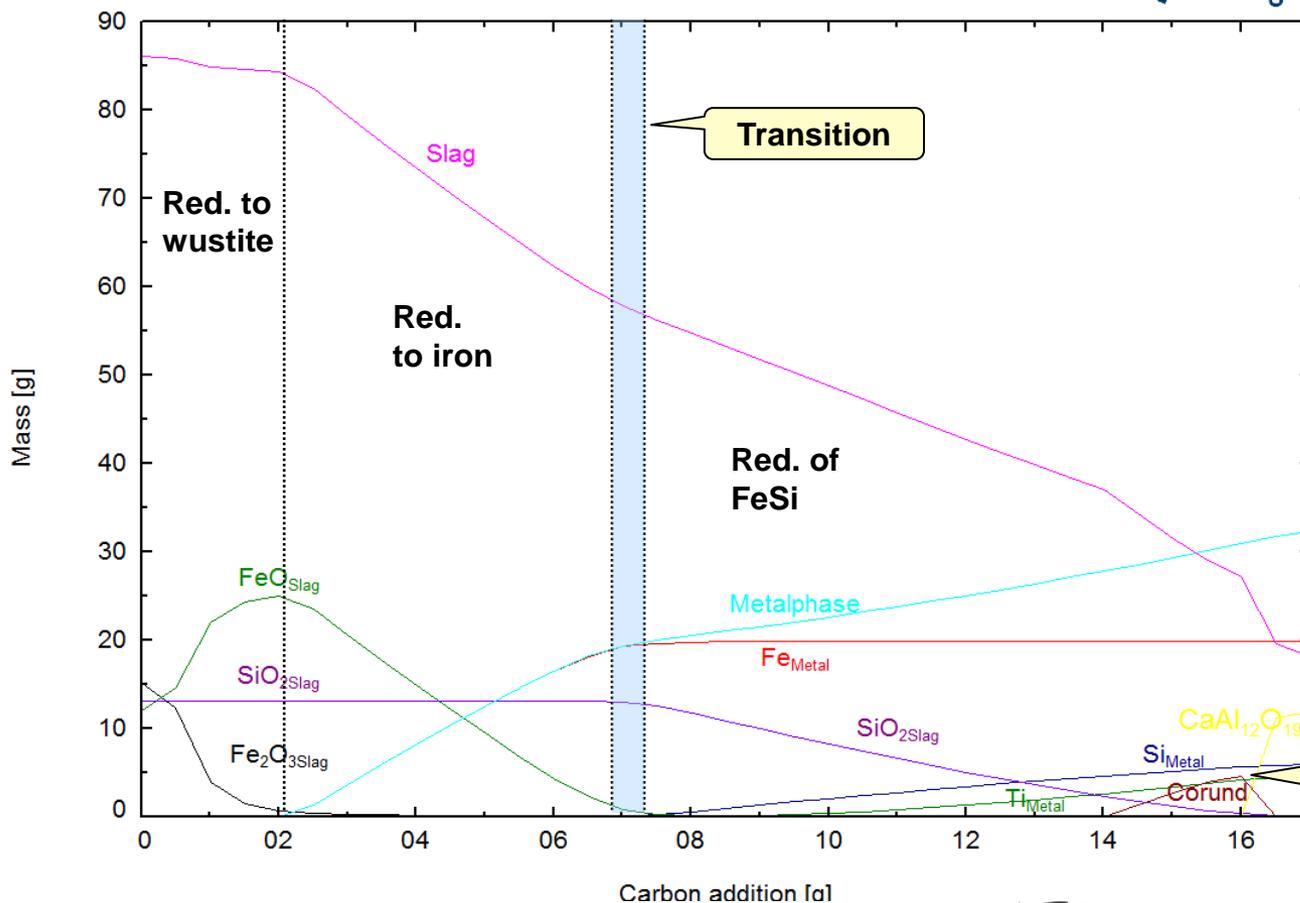
Preheating of the experimental mixture at 900°C to reach equilibrium and subsequent leaching

# Study II: New approach: Si-separation in electric arc furnace (EAF)

- Recovery of iron and silicon through carbothermic reduction
  - Enrichment of (soluble) Al in slag
- Avoiding the necessity for massive landfills for Red Mud (~ 100M t per year)

## Effect of carbon addition on smelting of red mud

referred to 100 g RM at 1800°C



Recovery of iron at a carbon addition of 75 g/kg red mud

Recovery of Fe<sub>18</sub>Si<sub>16</sub>Ti at a carbon addition of 165 g/kg red mud

Reduction of Ti and precipitation of first solid phases

# Study II: Comparison of FactSage and experiments (Fe Reduction)

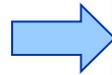
## “Selective” iron reduction at 1600°C

Slight hyperstoichiometric carbon addition (9 instead of 7 g/100g RM and CaO addition of 3.5 g/100g RM)

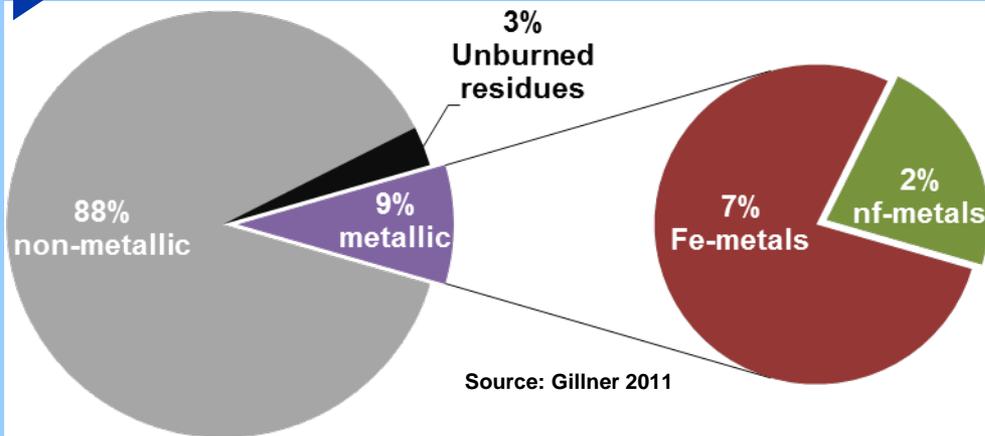
Metal [wt.-%]	Fe	C	Si	Ti	Al
FactSage	90,7	2,7	4,4	0,2	0,002
Experiment	93,7	4,4	0,04	0,2	0,000

Slag [wt.-%]	Al <sub>2</sub> O <sub>3</sub>	SiO <sub>2</sub>	CaO	Na <sub>2</sub> O	TiO <sub>2</sub>	Fe <sub>2</sub> O <sub>3</sub>
FactSage	49,2	19,4	13,2	8,3	11,7	0,02
Experiment	47,8	22,7	11,5	9,4	13,6	0,7

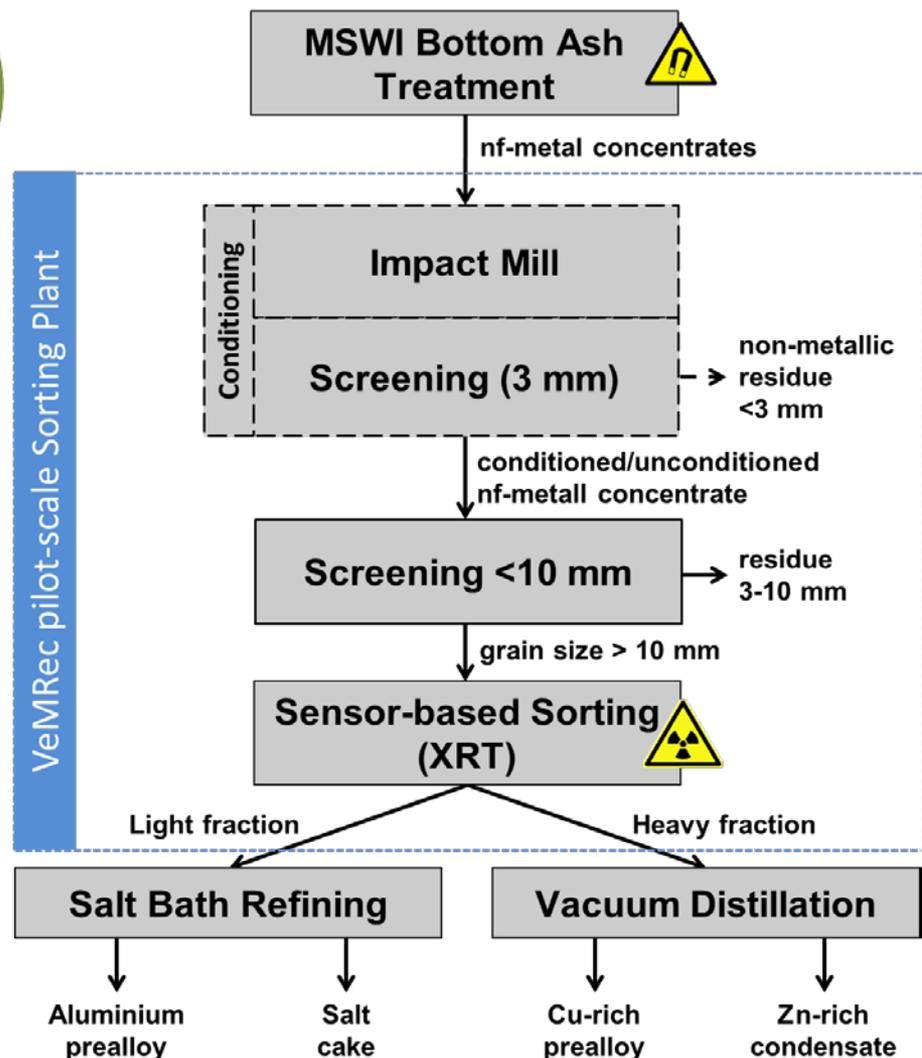
- **Si-equilibrium not reached**
- **Slag composition is in very good accordance with calculated model**



# Study III: Non-ferrous(nf) metal recycling from MSWI bottom ash



1. Separation of nf-metals by conventional MSWI bottom ash treatment
2. Sensor-based Sorting of nf-metal concentrates for the production of light and heavy metal fractions
3. Development of metallurgical evaluation methods, e.g.



# Study III: Non-ferrous(nf) metal recycling from MSWI bottom ash



**Light fraction  
10-40 mm  
conditioned**

**Heavy fraction  
10-40 mm  
conditioned**



# Study III: Metallurgical evaluation of nf-metal fractions

Treatment of light fraction through salt refining is relatively basic

→ High Al containing alloy (> 90 wt.-%)

Treatment of heavy fraction much more challenging

→ High Al, Si, Fe content which is undesired in metal

→ Zn distillation as first step

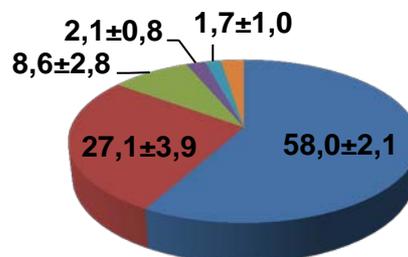
mech. conditioned heavy metal fraction 10-40 mm

**Vacuum distillation**

67,2 ± 2,7 %  
Metallic

29,5 ± 1,9 %  
Condensate  
(70 – 85% Zn)

3,2 ± 1,5 %  
Non-metallics



■ Cu  
■ Al  
■ Fe  
■ Cr  
■ Ni  
■ others

- Contamination with light metals, stainless steel and non-metallics critical for heavy metal recycling

Average Composition of the waste's heavy fraction [wt.-%]

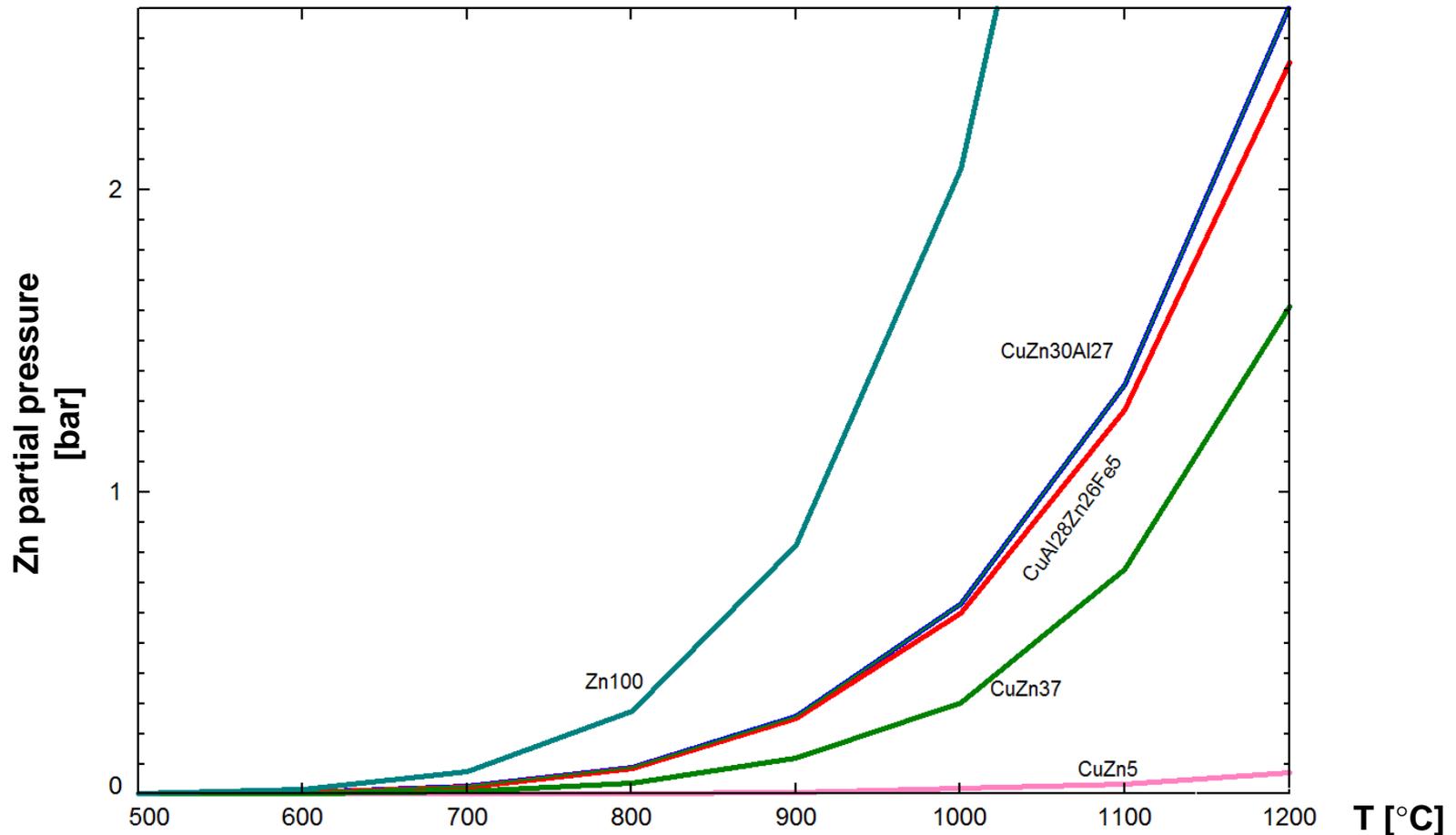
Cu	Zn	Al	Pb	Fe
37.7 ± 4	19.6 ± 5	25.7 ± 2	0.85 ± 0.5	8.33 ± 5

Si	Ni	Cr	Mn
1.48 ± 0.2	1.8 ± 1.5	2.05 ± 1.7	0.38 ± 0.2

## For the recycling of heavy metal fraction:

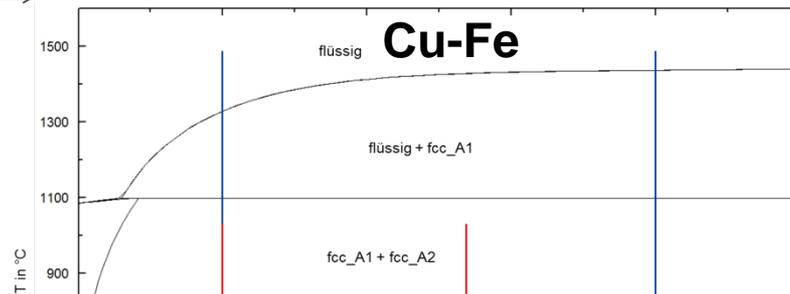
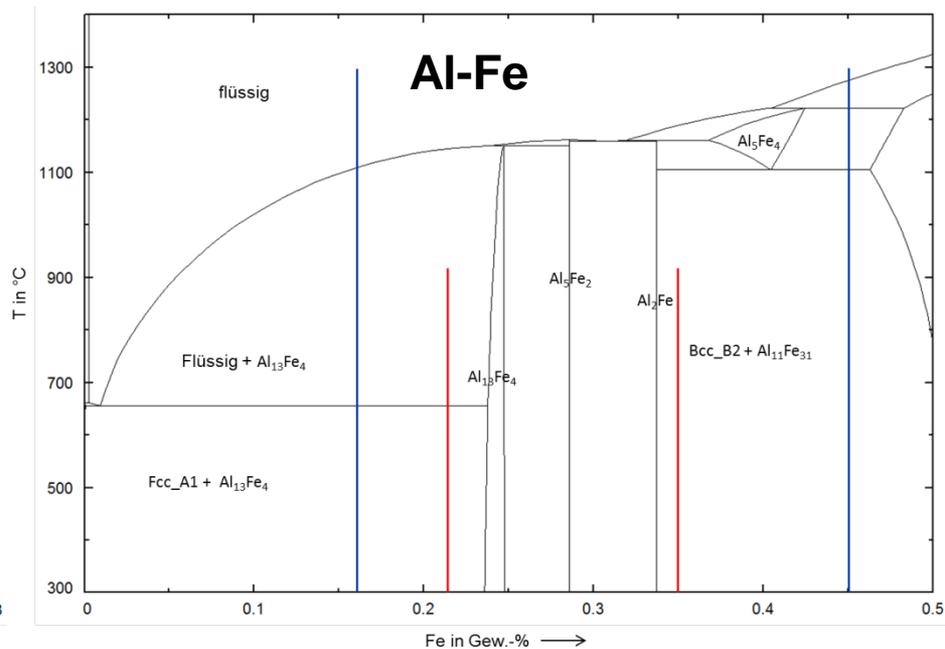
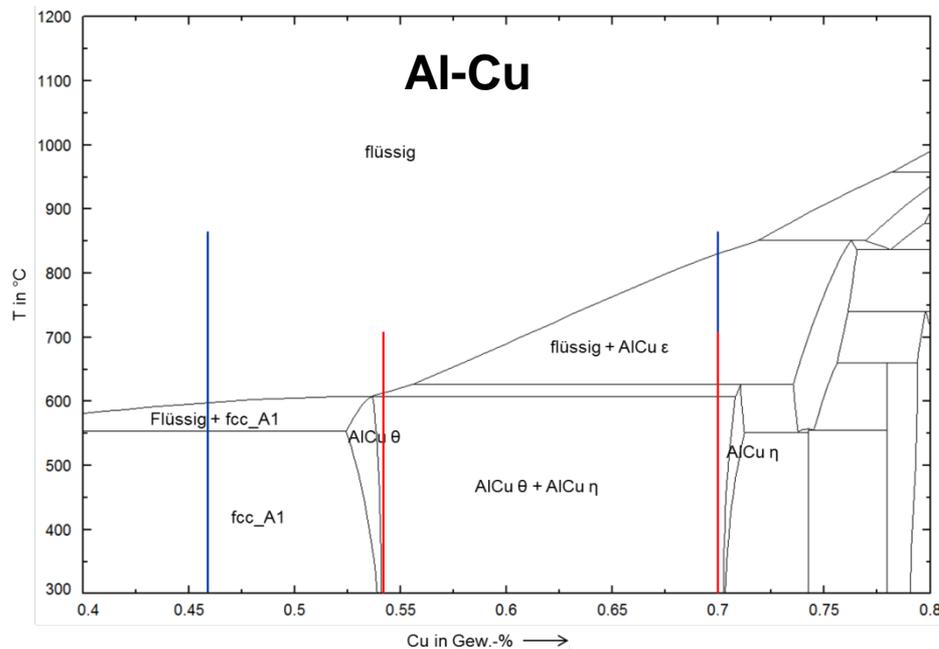
- Evaluation of vapour pressure for Zn and Zn-containing alloys with complex composition
- Calculation of binary phase diagrams for the identification of possible (intermetallic) product phases in the Cu-rich prealloy
- Selective oxidation of ignoble accompanying elements in de-zinc metal by different oxidation agents

# Study III: Vapour pressure of alloys



- Zinc partial pressure changes with the activity of zinc, which is higher for Cu-Zn-Al and Cu-Zn-Al-Fe than for Cu-Zn systems (SGPS-SGTE)

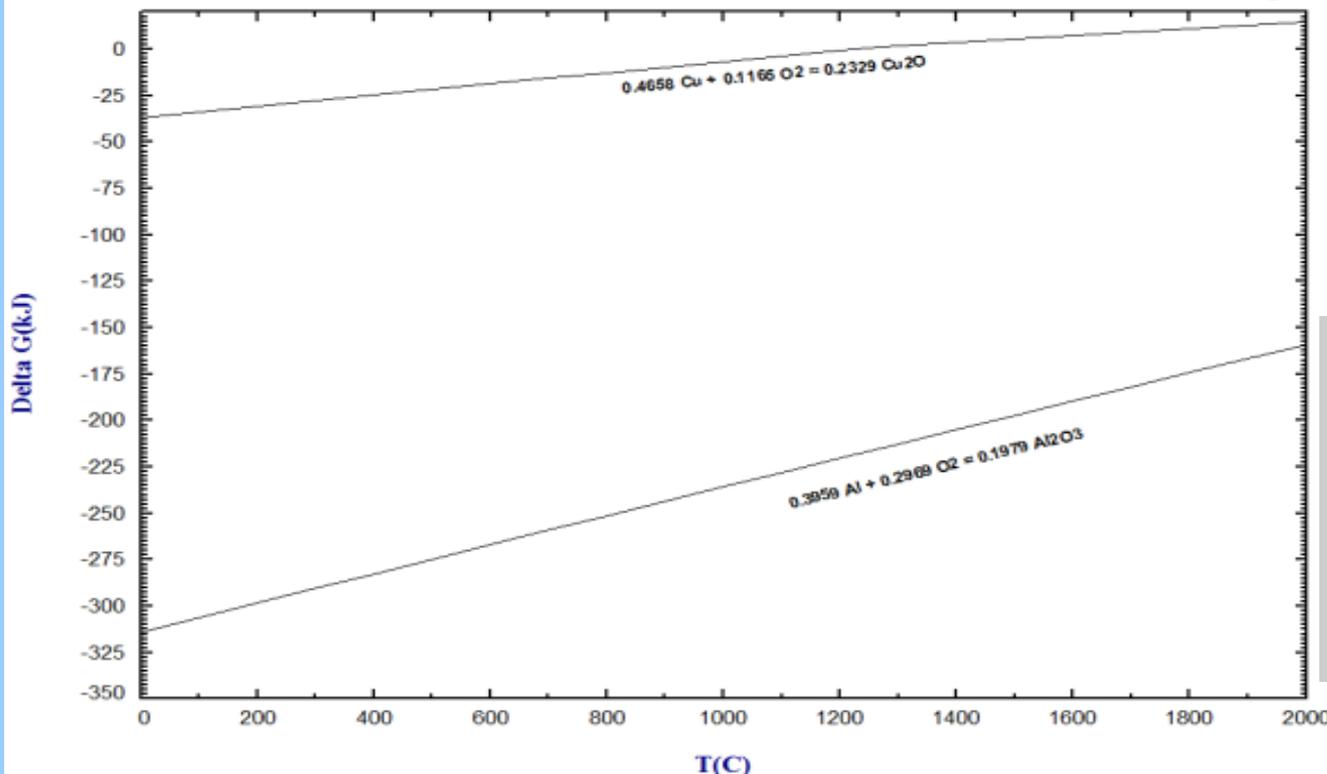
# Study III: Binary edges of de-zinced heavy metal



- Binary edges indicate, that intermetallics are predominant for Al-Cu and Al-Fe system, while demixing is typical for Cu-Fe system (FScopp-SGTE)

## Study III: Activity-fitted Ellingham-diagrams for oxidative treatment

1. Calculation of activities for the composition in de-zincd heavy metal in equilibrium at 1300 °C
2. Compilation of activity-fitted Ellingham-diagrams for the estimation of the selectivity of oxidative treatment



### Future research:

Selective Oxidation of Al and Si in metal through use of a high  $\text{Cu}_2\text{O}$  containing slag

# Summary and outlook

## FactSage Modelling is very helpful in our research:

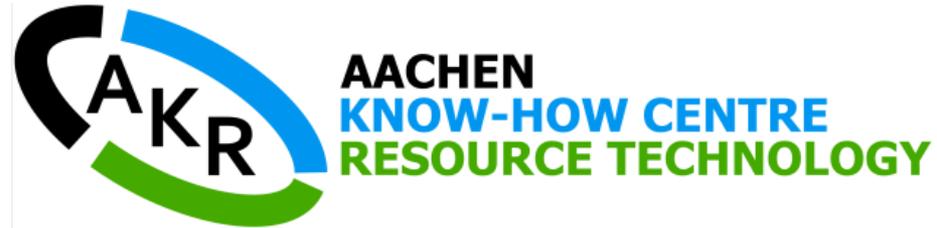
- Theoretical support of experimental results
- Feasibility checking of an idea without or in addition to experiments
- Quick verification of a new approaches / ideas

## Future / additional research involving FactSage:

- Modelling of aluminothermic metal production
- Simulation of different salt compositions for aluminum recycling
- Liquid salt electrolysis of REE

## “Need to have / nice to have” additions to FactSage:

- Rare Earth Element databases:
  - slags with REE-oxides → further addition to FToxid
  - other chemical REE-species (e.g. carbides)
  - additional data for phase diagrams
- Database involving the combustion of organic materials (simulation of pyrolysis of different wastes)
- System Ti-Al-O in contact with different slag systems (e.g.  $\text{CaF}_2$ - $\text{CaO}$ - $\text{Ca}$ ) for TiAl deoxidation in ESR



**Thank you for your attention!**