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Coupling Gibbs Energy and Viscosity Modelling

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Introduction & Motivation



- Measurement of viscosity is of significant importance, however, it can not supply all data encountered in related industries.
- Modelling of viscosity is a promising approach to solve this problem.



Definition of Viscosity



L. Forsbacka: Doctoral thesis, TKK, 2007.

$$\tau = \frac{F}{A} = \eta \cdot \frac{dv}{d\ell}$$

η : dynamic viscosity, Pa·s

- Viscosity: internal fluid friction
- The fluid is sandwiched between two suspending parallel plates in a liquid.
- The viscosity is described by the shear stress that suppresses the relative movement of the two suspending parallel plates.



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Viscosity Model I

| System | Associate Species |
|---|---|
| SiO ₂ | Si ₂ O ₄ |
| Al ₂ O ₃ | Al ₂ O ₃ |
| CaO | Ca ₂ O ₂ |
| MgO | Mg ₂ O ₂ |
| SiO ₂ -Al ₂ O ₃ | Si ₂ Al ₆ O ₁₃ |
| SiO ₂ -CaO | $CaSiO_3$ and Ca_2SiO_4 |
| SiO ₂ -MgO | SiMgO ₃ and Si ₂ Mg ₄ O ₈ |
| Al ₂ O ₃ -CaO | CaAl ₂ O ₄ |
| Al ₂ O ₃ -MgO | Al ₄ Mg ₂ O ₈ |
| SiO ₂ -Al ₂ O ₃ -CaO | Ca ₂ Si ₄ Al ₄ O ₁₆ |
| SiO ₂ -Al ₂ O ₃ -MgO | Si ₅ Al ₄ Mg ₂ O ₁₈ |
| SiO ₂ -CaO-MgO | |
| Al ₂ O ₃ -CaO-MgO | |
| SiO ₂ -Al ₂ O ₃ -CaO-MgO | |



 Associate species model is employed to predict the slag structure, which can be presented by the relative concentrations of each associate species.



Viscosity Model II

$$G = \sum_{i} X_{i} \cdot G_{i}^{o} + R \cdot T \cdot \sum_{i} X_{i} \cdot \ln X_{i} + G^{ex}$$

where: subscript i represents i-th associate species in solution; X_i is the mole fraction; G_i^{o} is the Gibbs energy of the pure i-th associate species; G^{ex} is the excess Gibbs energy to summarize all other contributions to the Gibbs energy except for the entropy contribution.



Associated Solution Theory



Viscosity Model III

GactSage"



K. Hack, T. Jantzen: 12th Annual Workshop, GTT, Herzogenrath, 2010.



Viscosity Model IV

Arrhenius model (modified)

$$\ln \eta = \sum_{i=1}^{N} X_{i} \cdot \ln \eta_{i} = X_{SiO_{2}} \cdot \ln \eta_{SiO_{2}} + \sum_{i=1}^{N-1} X_{i} \cdot (A_{i} + \frac{B_{i}}{T})$$

$$\ln \eta_{SiO_2} = [A_{SiO_{2,\,Small}} + A_{SiO_{2,\,Intermediate}} \cdot (X_{SiO_2})^{m} + A_{SiO_{2,\,Iarge}} \cdot (X_{SiO_2})^{n}]$$

$$+\frac{[B_{SiO_{2, small}}+B_{SiO_{2, intermediate}} \cdot (X_{SiO_{2}})^{m} + B_{SiO_{2, large}} \cdot (X_{SiO_{2}})^{n}]}{T}$$

where: X_i is the molar fraction of structural unit i; A_i and B_i are fitting parameters of structural unit i.



T. Nentwig: Doctoral thesis, RWTH Aachen, 2011.

Fig. 3

| Q _n - | Associate species | | | |
|------------------|--|---|---|--|
| groups | SiO ₂ -Al ₂ O ₃ | SiO ₂ -CaO | SiO ₂ -MgO | |
| Q ₀ | Al ₈ Si ₂ O ₁₆ | Ca ₈ Si ₂ O ₁₂ | Mg ₈ Si ₂ O ₁₂ | |
| Q ₁ | Al ₆ Si ₂ O ₁₃ | Ca ₆ Si ₂ O ₁₀ | Mg ₆ Si ₂ O ₁₀ | |
| Q ₂ | Al ₄ Si ₂ O ₁₀ | Ca ₄ Si ₂ O ₈ | Mg ₄ Si ₂ O ₈ | |
| Q ₃ | Al ₂ Si ₂ O ₇ | Ca ₂ Si ₂ O ₆ | Mg ₂ Si ₂ O ₆ | |
| Q_4 | | Si ₂ O ₄ | | |



Optimization Process I





Optimization Process II



| | System | No. of available literature | No. of total experimental points | No. of reliable experimental points | |
|---|---|-----------------------------------|--|---|--|
|) | SiO ₂ | 19 | 326 | 239 | |
| | Al ₂ O ₃ | 4 | 58 | 36 | |
| | CaO | | | | |
| | MgO | | | | |
| | SiO ₂ -Al ₂ O ₃ | 4 | 109 | 73 | |
| | SiO ₂ -CaO | 34 | 518 | 308 | |
| | SiO ₂ -MgO | 4 | 73 | 36 | |
| | Al ₂ O ₃ -CaO | 22 | 285 | 136 | |
| | Al ₂ O ₃ -MgO | | | | |
| | CaO-MgO | | | | |
| | SiO ₂ -Al ₂ O ₃ -CaO | 82 | 4226 | 1964 | |
| | SiO ₂ -Al ₂ O ₃ -MgO | 26 | 1309 | 379 | |
| | SiO ₂ -CaO-MgO | 29 | 656 | 262 | |
| | Al ₂ O ₃ -CaO-MgO | 4 | 58 | 23 | |
| | SiO ₂ -Al ₂ O ₃ -CaO-MgO | 91 | 4913 | 1430 | |



Optimization Process III



The influence of **experimental data** and **extrapolation** of other related systems on the optimization of model parameters is assumed to be **equal**. 'Ideal Point Approach' is employed to achieve this goal.

Ideal Point Approach

• Ideal points f⁰:

$$f_i^0 = \frac{1}{N} \cdot \sum_{j=1}^N \left| \ln \eta_{j,\text{cal}} - \ln \eta_{j,\text{exp}} \right|$$

Evaluation function f(x):

$$f(x) = \sqrt{\sum_{i=1}^{N} (f_i(x) - f_i^0)^2}$$



Optimization Process IV



| Associate | Arrhenius model parameters | | | |
|---|----------------------------|----------------|------------|----|
| species | A _i | B _i | m | n |
| SiO _{2,large} | 0.093421 | 17.4248 | | 44 |
| SiO _{2,intermediate} | 9.015518 | 29.64266 | 3 | |
| SiO _{2,small} Al ₂ O ₃ CaO | -11.1009 | 24.04727 | ·27 :06 | |
| | -8.34598 12.24 | 12.24506 | | |
| | -2.86872 | 6.34E-07 | | |
| MgO | -8.52174 | 10.69859 | | |
| Si ₂ Al ₆ O ₁₃ | -36.5656 | 50.60674 | | |
| $CaSiO_3$ Ca_2SiO_4 $SiMgO_3$ $SiMg_2O_4$ | -12.5291 | 19.71572 | | |
| | -9.21692 | 13.32073 | | |
| | -15.2726 | 26.24836 | | |
| | -8.04222 | 10.4456 | | |
| CaAl ₂ O ₄ | -19.4109 | 35.71868 | | |
| Al ₂ MgO ₄ | -5.52128 | 10.91831 | | |
| CaSi ₂ Al ₂ O ₈ | -15.4246 | 40.86163 | | |
| Si ₅ Al ₄ Mg ₂ O ₁₈ | -24.138 | 56.37161 | | |



SiO2



14/21



SiO₂-Al₂O₃







Al₂O₃-CaO







SiO₂-Al₂O₃-CaO





Al₂O₃-CaO-MgO





SiO₂-Al₂O₃-CaO-MgO





Conclusion & Outlook

Conclusions:

- A new structurally-based viscosity model has been developed, for fully liquid system SiO₂-Al₂O₃-CaO-MgO and its subsystems.
- A good agreement between experimental data and model predictions within experimental error has been achieved, by using only one set of model parameters.

Outlook:

- Re-optimizing the model parameters of the system SiO₂-Al₂O₃-Na₂O-K₂O (developed by my previous colleague: Thomas Nentwig)
- Combining these two systems to develop the model parameters of the system SiO₂-Al₂O₃-CaO-MgO-Na₂O-K₂O.
- Introducing new components like FeO/Fe₂O₃ and P₂O₅ to form a higher system.
- Measuring viscosity in unknown region to validate the present model.

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Thank you for your attention!