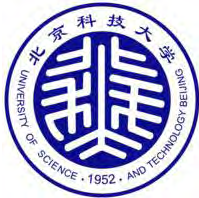


# Modification of inclusion composition in steel during secondary metallurgical ladle treatment



A comprehensive process simulation model



Qifeng Shu\*, Piotr R. Scheller\*\*

\*Beijing University of Science and Technology, China

\*\* Freiberg University of Mining and Technology

09596 Freiberg, Germany

[scheller\\_piotr@web.de](mailto:scheller_piotr@web.de)

# Contents

- Introduction
  - processes during ladle treatment
- Fluid dynamics in a steel treatment ladle (plant trials)
- Layout of the model for the prediction of inclusion composition
- Thermodynamic and kinetic factors
- Model simulations
  - effect of ladle slag
  - effect of ladle lining
  - effect of inclusion separation
- Validation of the model in the industrial process
- Parameter study (effect of slag composition and lining material)



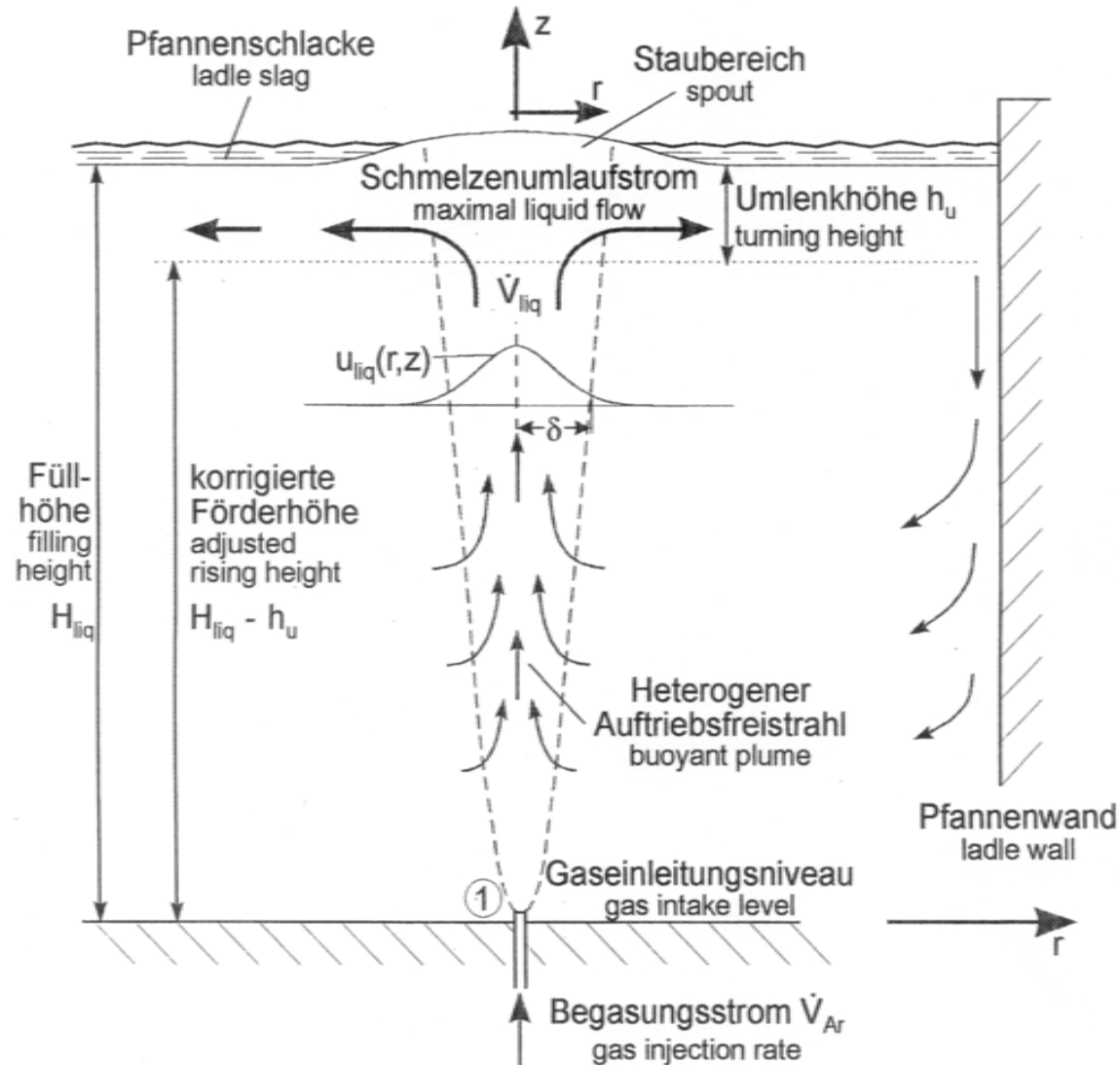
## Tasks in the ladle metallurgy:

- adjustment of chemical comp.
- adjustment of temperature
- separation of inclusions
- ....

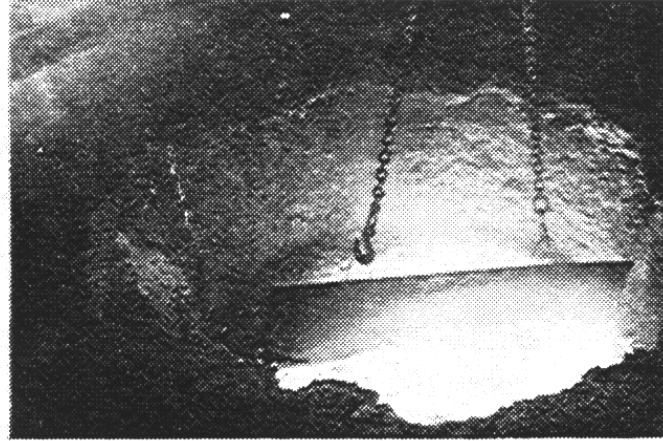
### **Intention:**

to develop the robust model predicting the inclusion composition and amount which can be used on line in the process

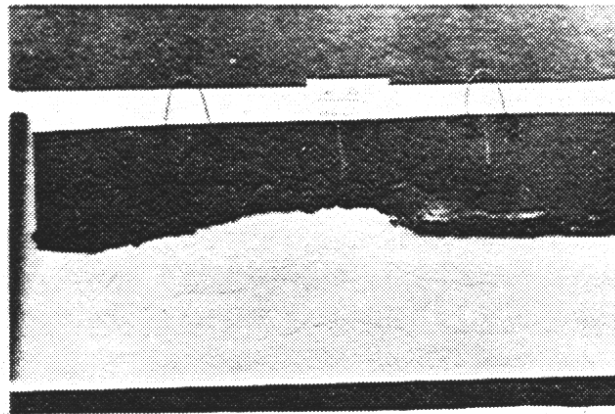
# Sketch of the buoyant plume flow pattern



# Industrial experiments, 30 t ladle



a) spout profile measuring

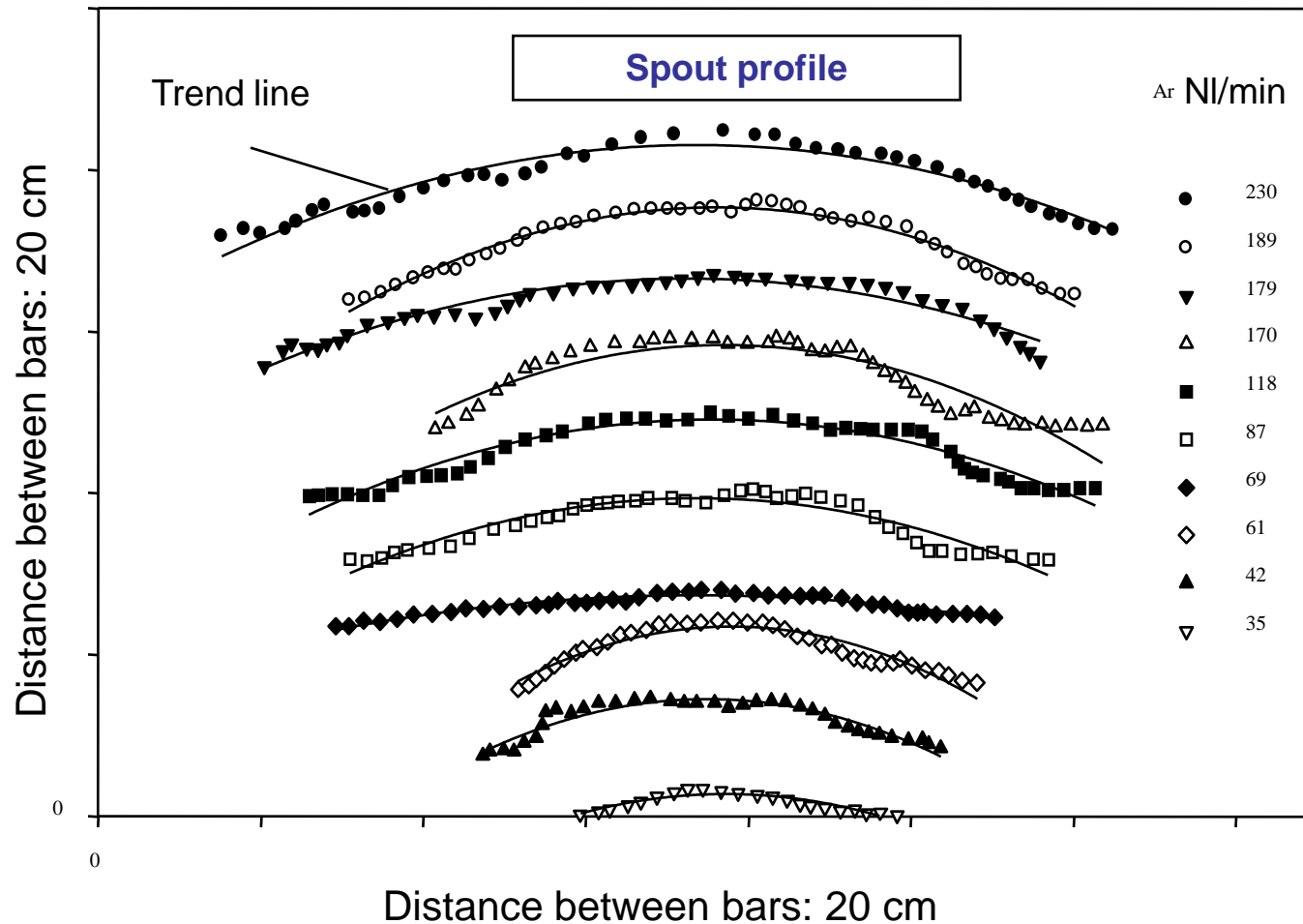


b) plate after melting procedure

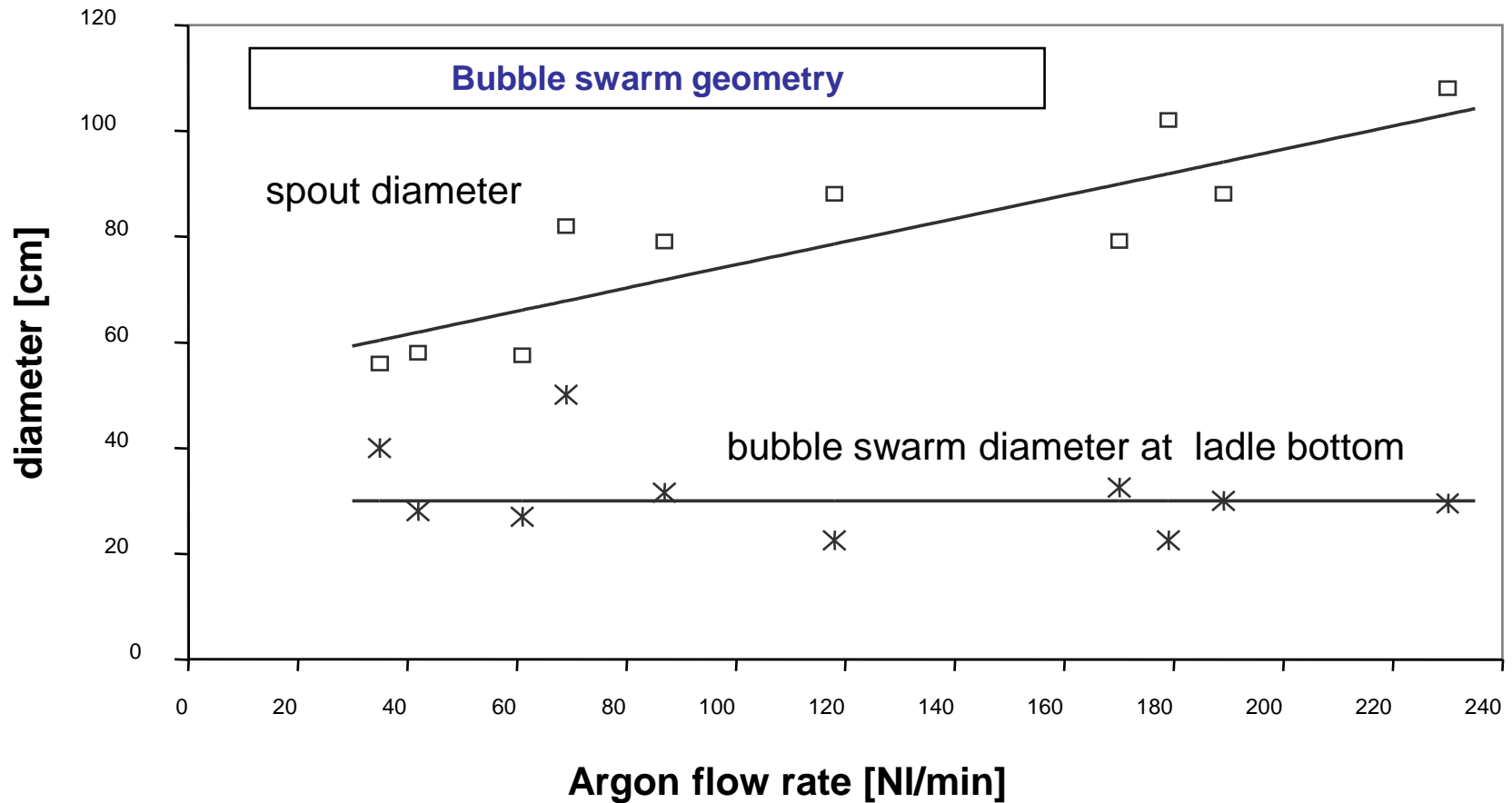
E. Steinmetz, and P.R. Scheller, *Stahl und Eisen*, 1987, no. 9, p. 57-65



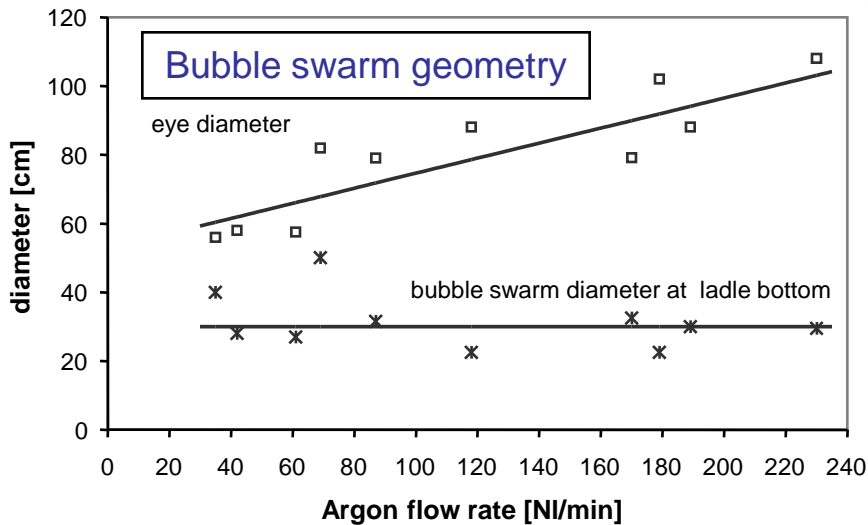
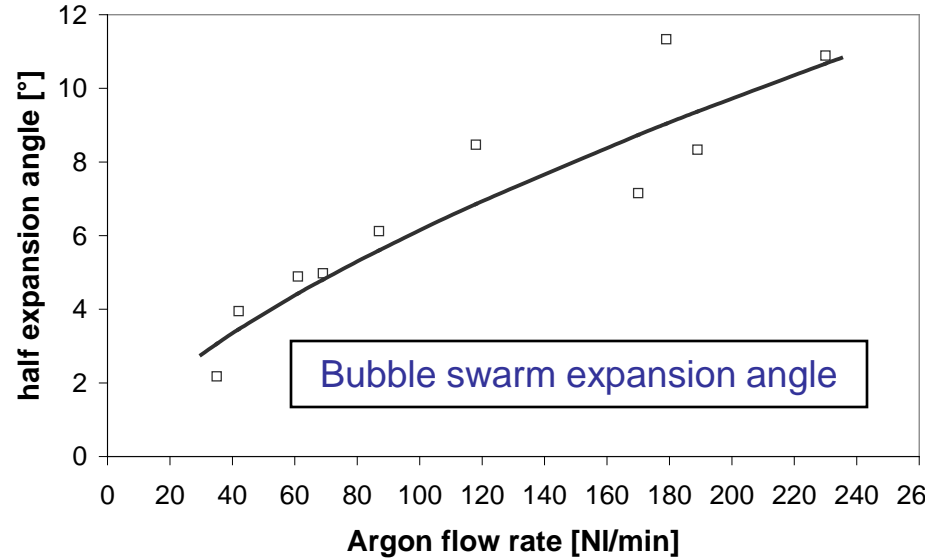
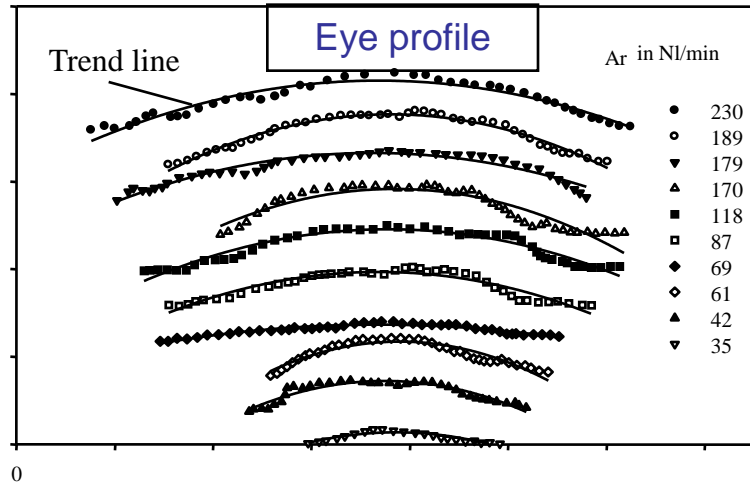
# Spout and bubble swarm geometry in 30t melts



# Spout and bubble swarm geometry in 30t melts

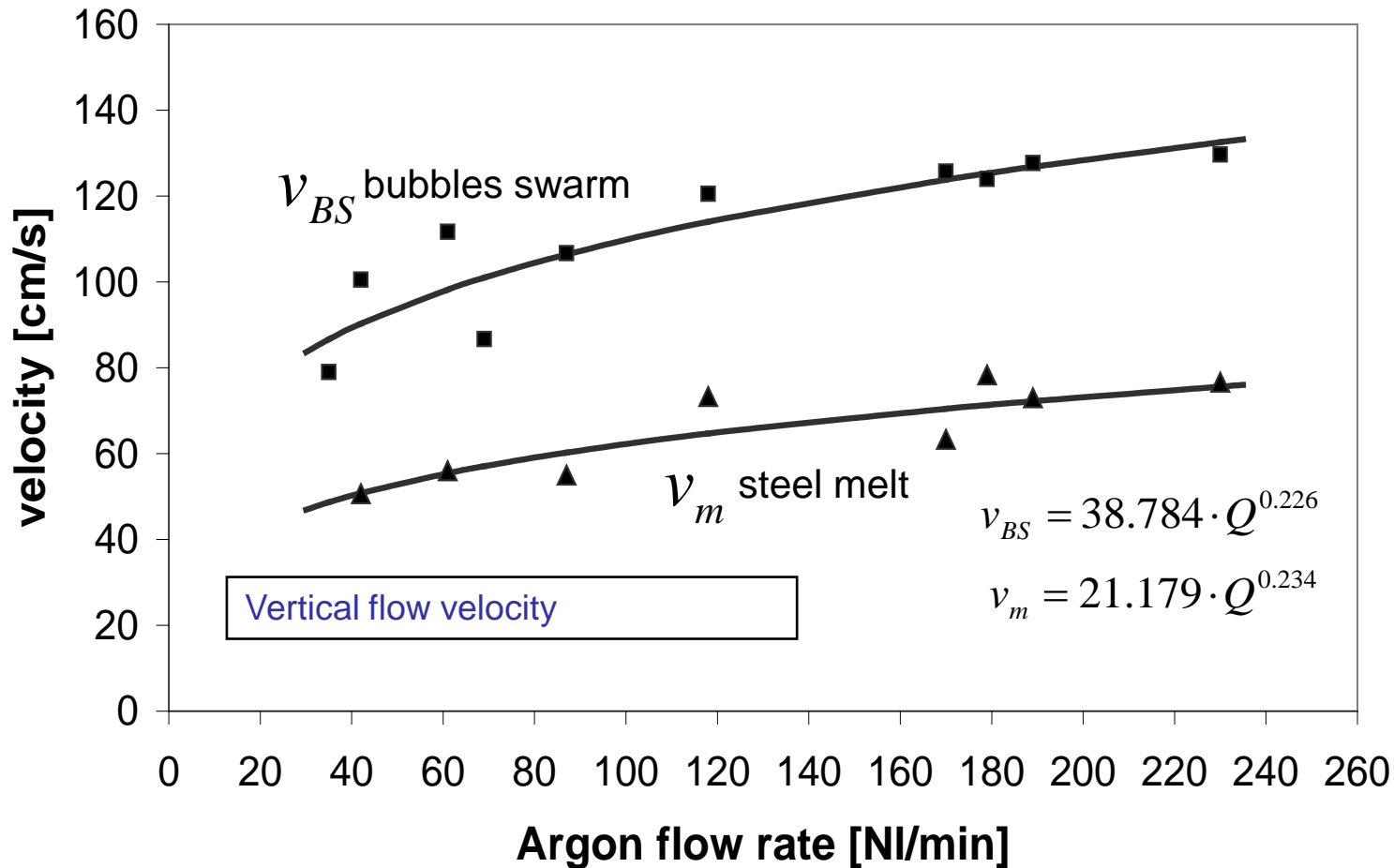


# Eye and bubble swarm geometry in 30t melts

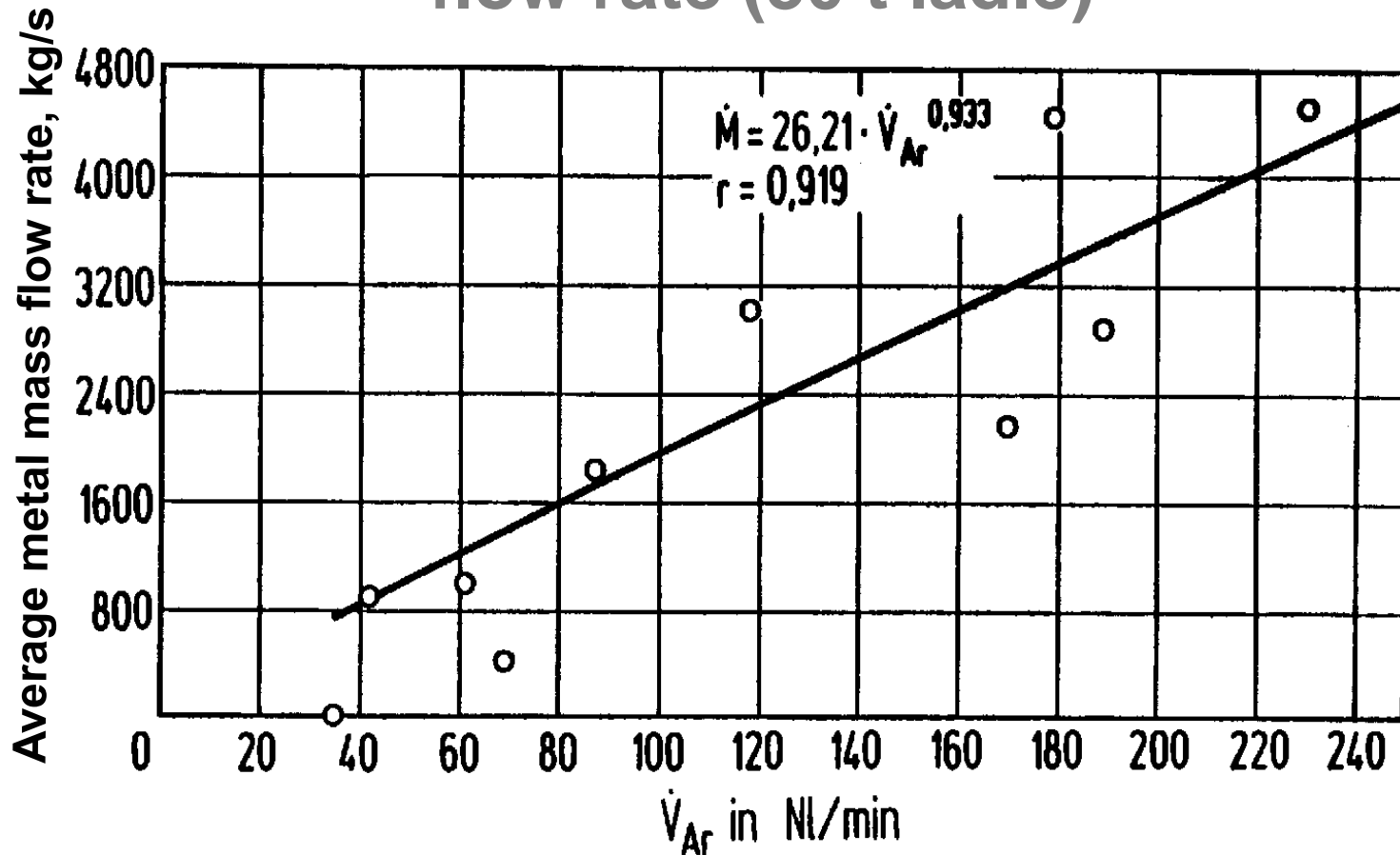




# Ascending velocity of bubbles and of steel in the centre of the swarm, 30t melts



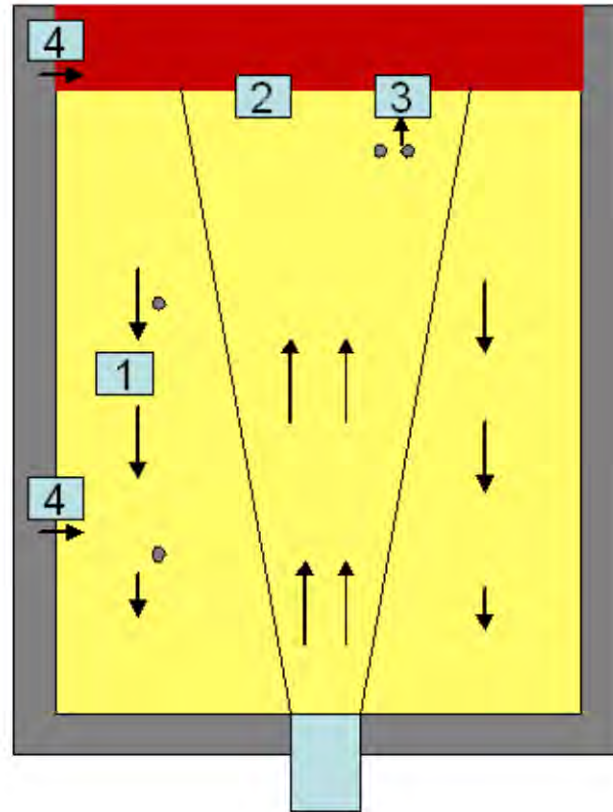
# The average metal mass flow rate near the bath surface depending on Ar-gas flow rate (30 t ladle)



# **A comprehensive model for inclusion composition in gas-stirred ladle**



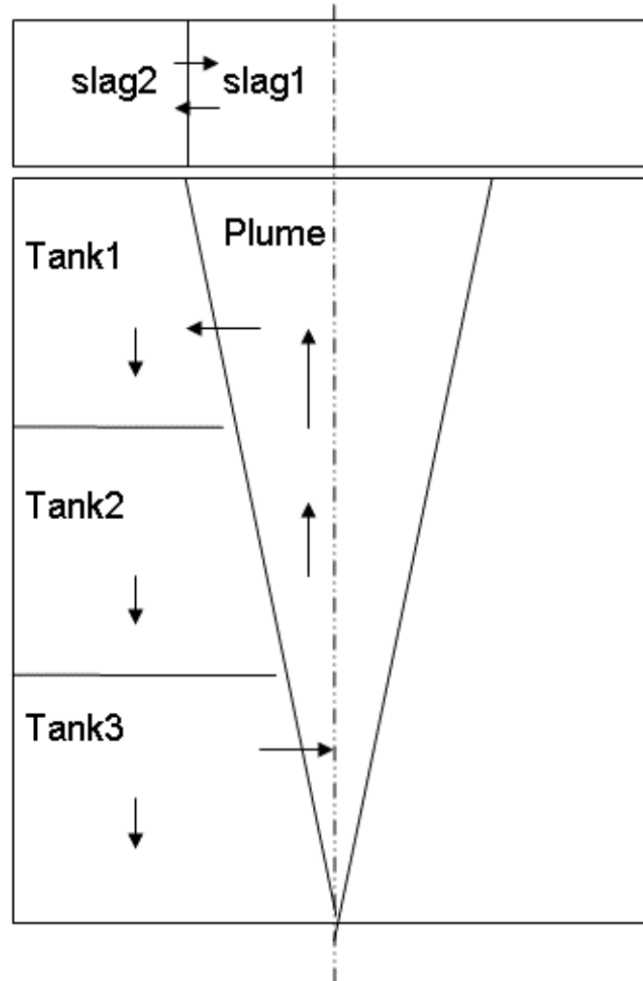
# Model Description



Process parameters influencing inclusion evolution in gas stirred ladle:  
1: Mixing in the ladle, 2: Slag-Metal reaction; 3: Inclusion separation;  
4: Lining interaction with steel and slag

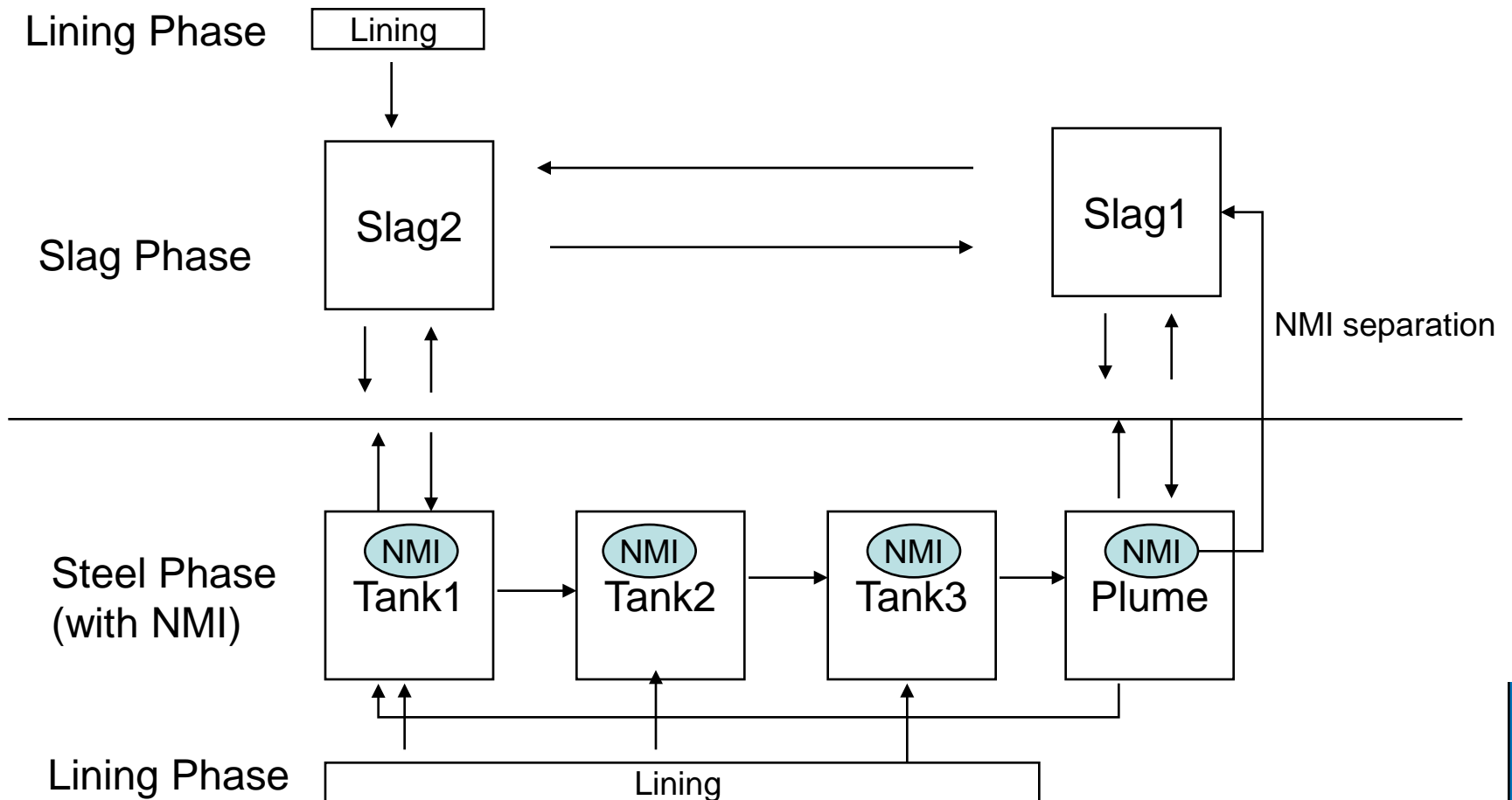
# Model Description

Schema of the tanks for calculation of mixing



# Model Description

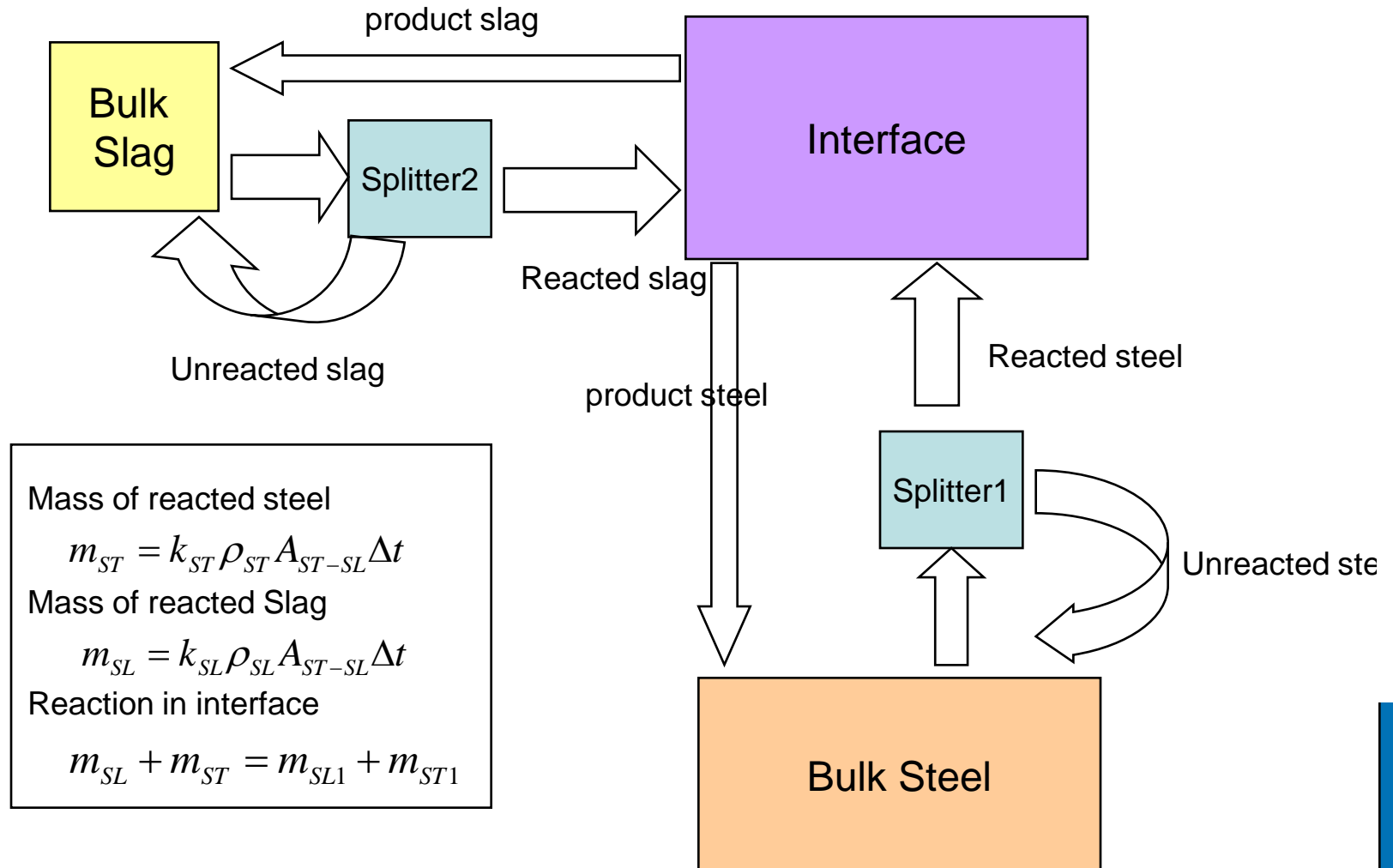
## Schema of the model





# Model Description

## Schema for slag-metal reaction



# Model Description

## Model tools



- SimuSage used as process simulation tool
  - Various basic unit operation components in SimuSage used:
    - chemical reactor,
    - mixer,
    - splitter,
    - iterator, ...



- FactSage database to acquire thermodynamic data of various phase. (Steel, Slag, Inclusions, Lining refractory)

# Local thermodynamic equilibria

- Thermodynamic equilibrium between steel and inclusions in each tank;
- Thermodynamic equilibrium between slag and steel at the slag-steel interface;
- Thermodynamic equilibrium between steel and dissolved lining material.

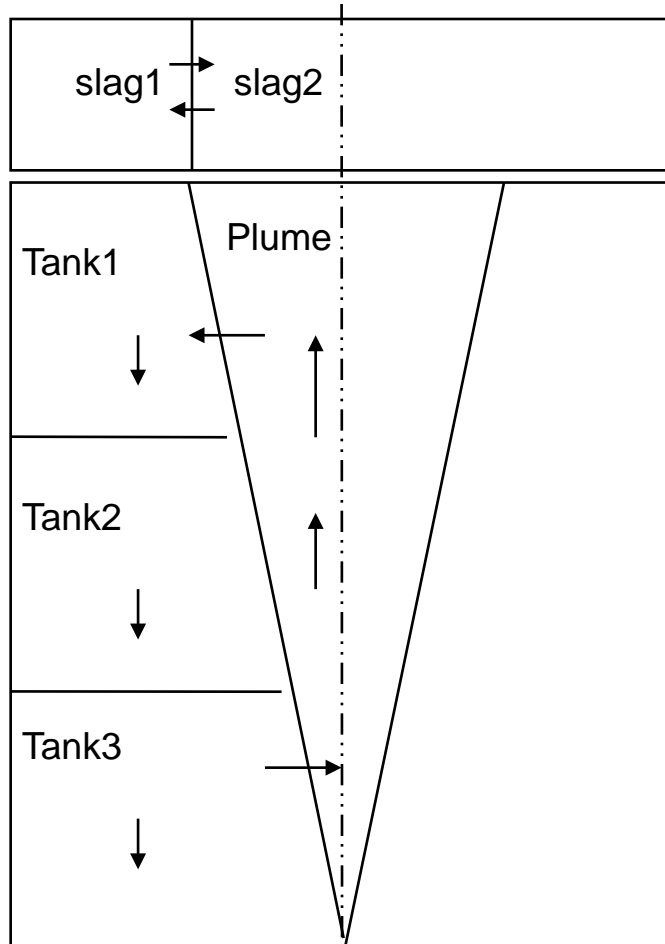
## Kinetic parameter

- Based on measurements in the industrial process:  
fluid dynamic, mixing, mass transfer coefficients, lining dissolution, separation of NMI



# Model Description

## The mixing in gas stirred ladle



- Tank1,2,3 with same height
- Diameter of plume is set as  $\frac{1}{2}$  of ladle diameter (larger than real value)
- tracer concentration in tank N at time t:

$$C(N,t) = \frac{C(N,t-\Delta t)(M(N) - r_M \Delta t) + C(N-1,t-\Delta t)(r_M \Delta t)}{M(N)}$$

where

$C(N,t)$  are concentration in tank N at time t,

$M(N)$  is the mass of tank N and  $r_M$  is the mass recirculation rate (obtained from industrial trials).



# Model Description

## Industrial data for model validation

Steel and slag mass	Steel: 210000Kg, Slag: 2500Kg
Chemical composition of steel before treatment (starting values)	C: 0.11%; Mn:0.90%; Cr: 0.24%; Mo:0.12%; V: 0.007%;Ti: 0.002%
Chemical composition of slag before treatment (starting values)	CaO: 54%; SiO <sub>2</sub> : 12%; Al <sub>2</sub> O <sub>3</sub> :22%; MgO: 8%. CaF <sub>2</sub> : 4%
Deoxidation regime	1) Si 600Kg Al 150Kg. 2) Al 130Kg 3)CaSi treatment:

## Model parameters used for calculation

Recirculation rates (industrial data)	2800 kg/s (for medium Ar flow rate)
Mass transfer coefficients	Steel side: $K_{ST}=0.002\text{m/s}$ , Slag side: $K_{SL}=0.001\text{m/s}$ .
Lining (MgO-C) dissolution rates (industrial data)	For contact with steel: $0.0005\text{kg}/(\text{m}^2.\text{s})$ For contact with slag: $0.001\text{kg}/(\text{m}^2.\text{s})$
Bath temperature (derived from industrial trials)	Decrease with time (C.E. Grip, 77th Steelmaking conference proceedings 1994) $T = 1650 - 0.144t/60 - 8.689\sqrt{t/60}$



# Model Description

**Three steps of simulation were made according to model development:**

Model 1: Ladle mixing and slag-metal reaction were taken into account

Model 2: Apart from ladle mixing and slag-metal reaction, lining dissolution into steel and into slag was further modeled

Model 3: Apart from ladle mixing, slag-metal reaction and lining dissolution, inclusion separation was also taken in consideration (separation rate depending on nature of inclusions and process development)

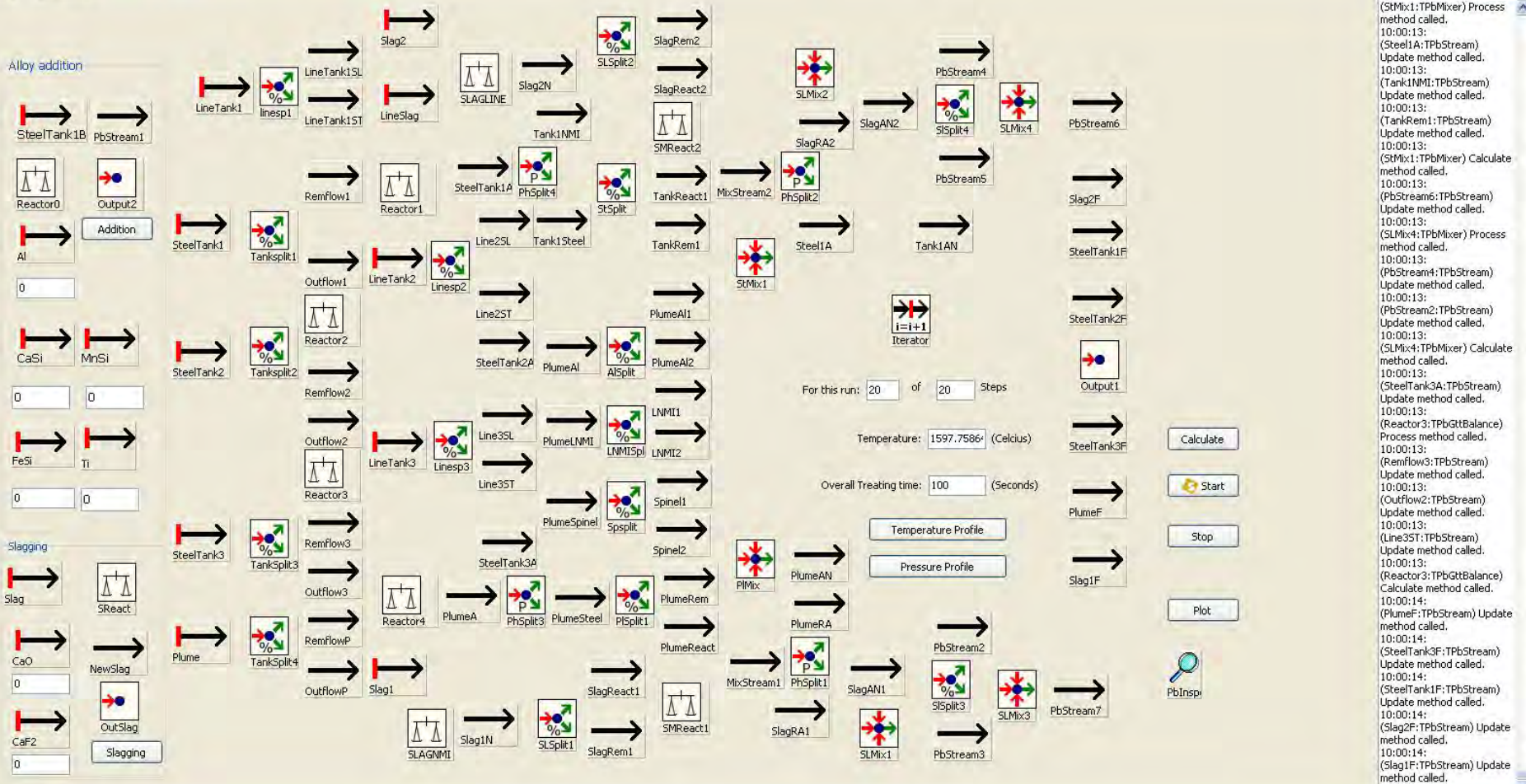




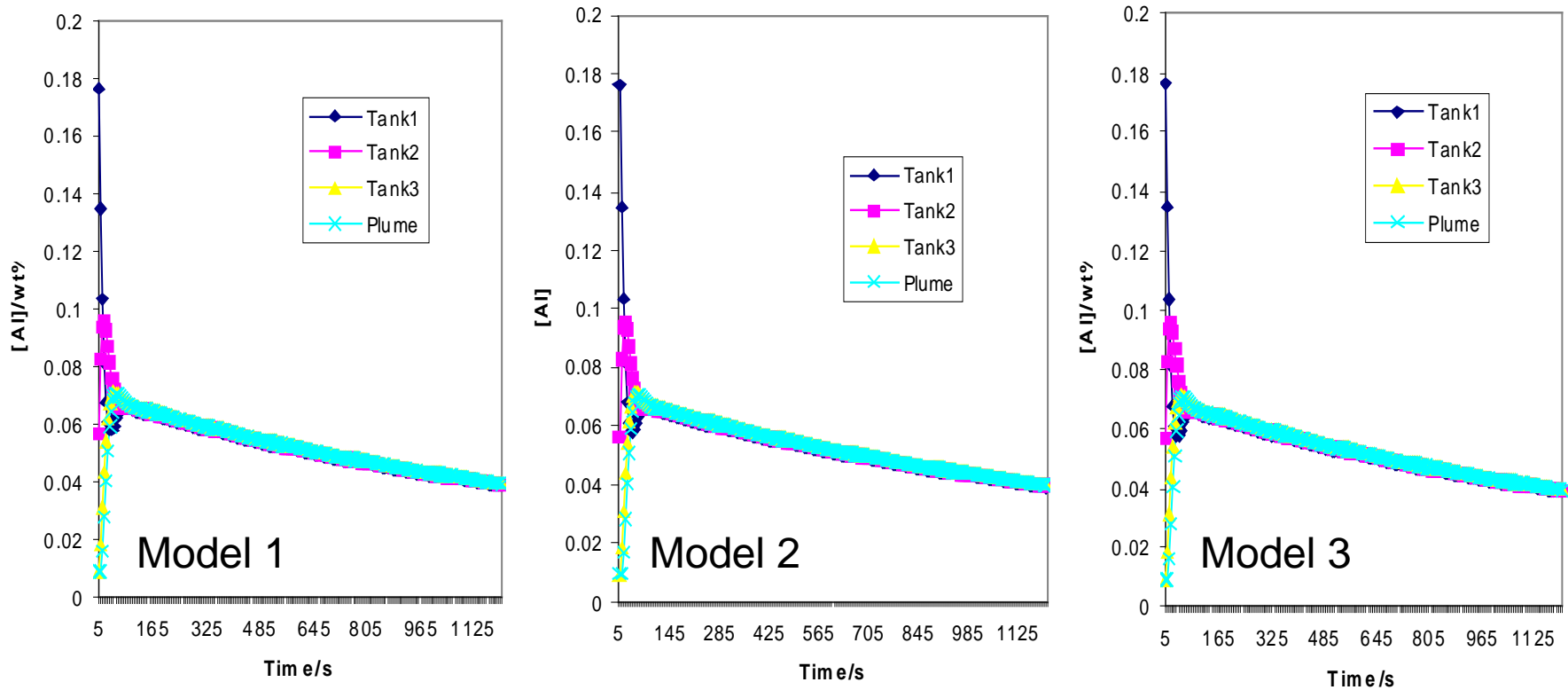
# Model Description

Simulation for inclusions in ladle v. 0.16

Settings Sgt materials

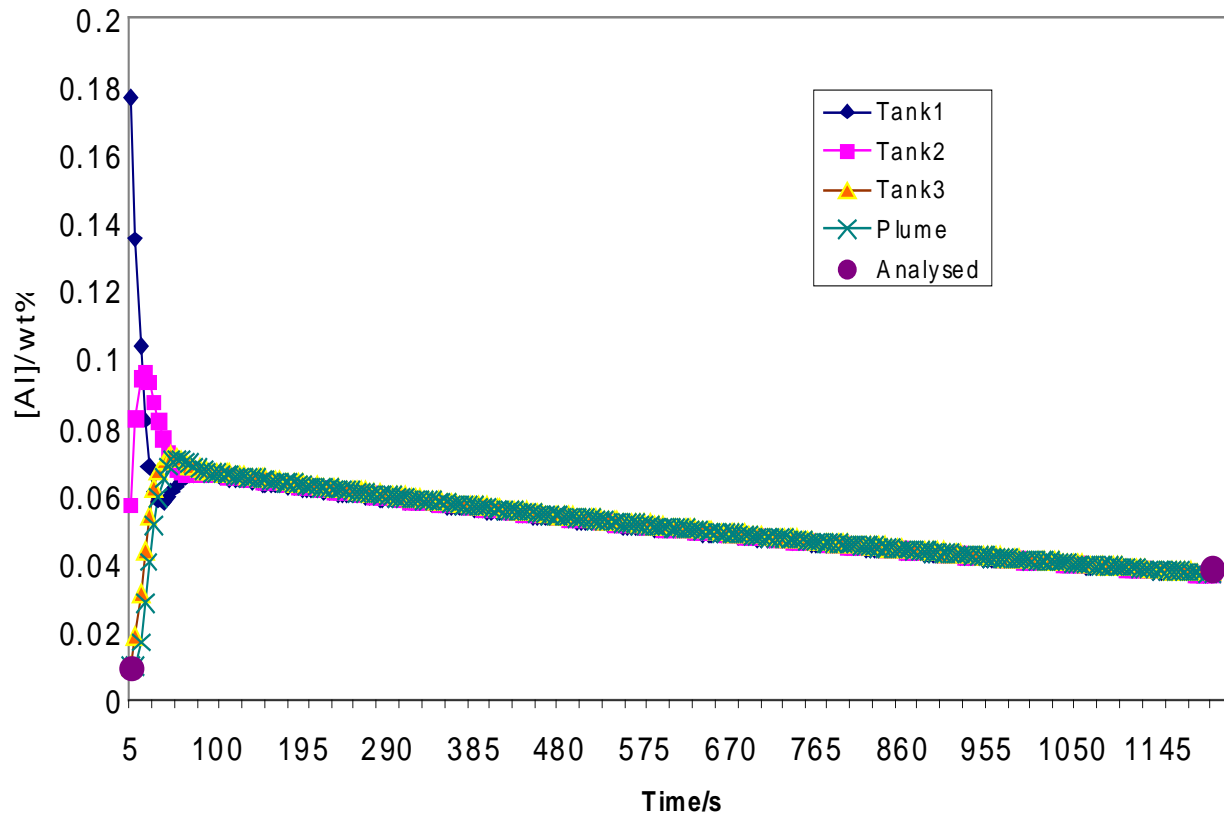


# Model Validation



Evolution of aluminum content [Al] in steel during ladle treatment calculated by different models

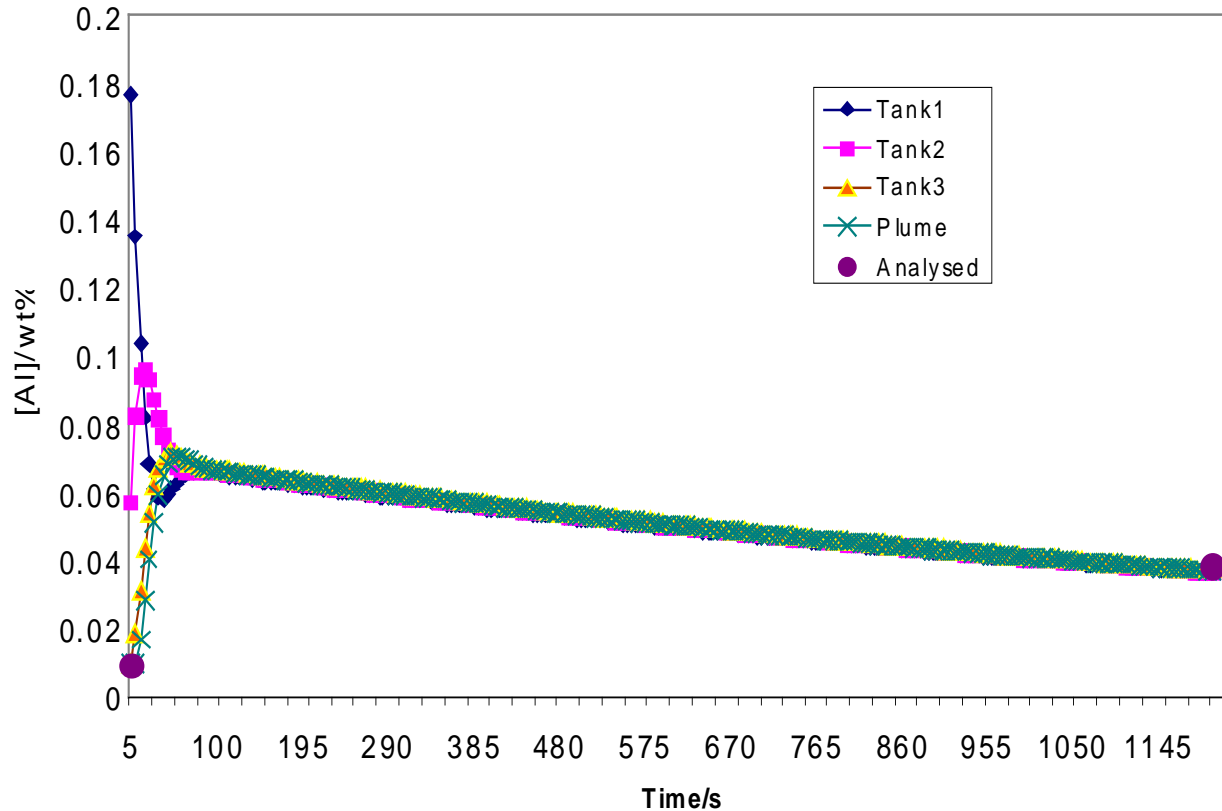
# Model Validation



Comparison between calculated [Al] and industrial analysed [Al] during ladle treatment



# Model Validation

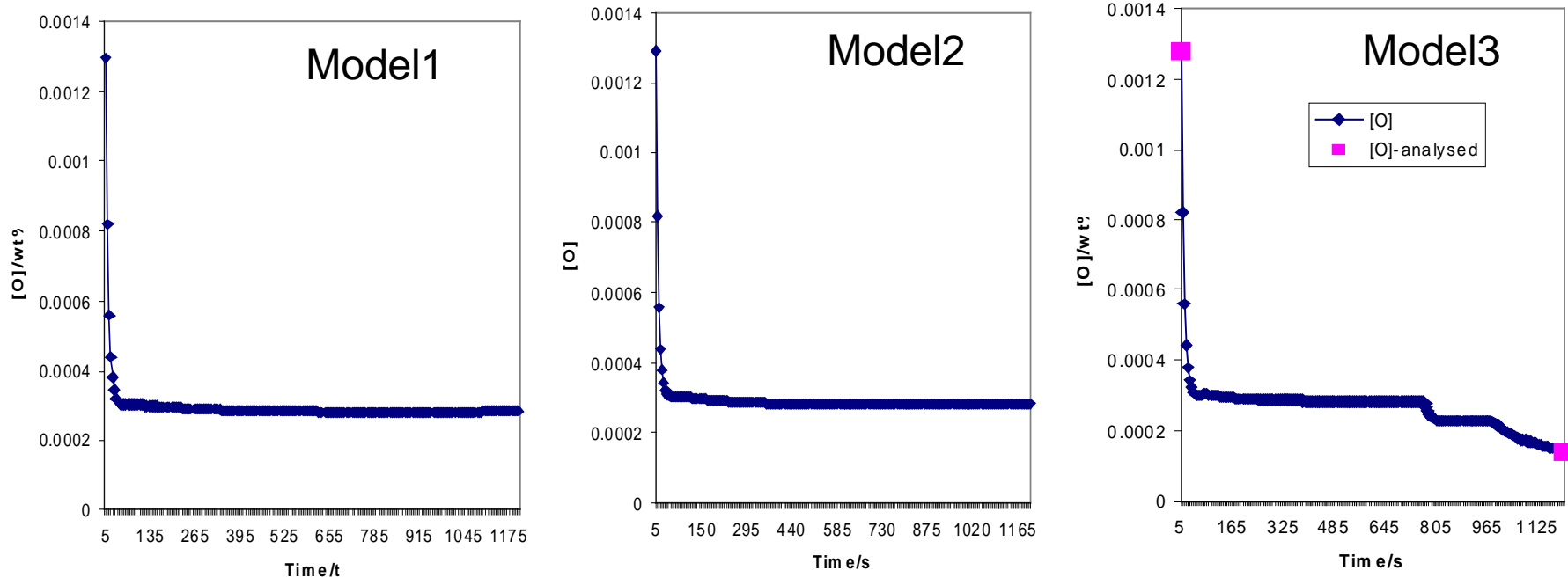


Comparison between calculated [Al] and industrial analysed [Al] during ladle treatment

→ Ladle mixing and slag-metal reaction are dominant factors for [Al] evolution.



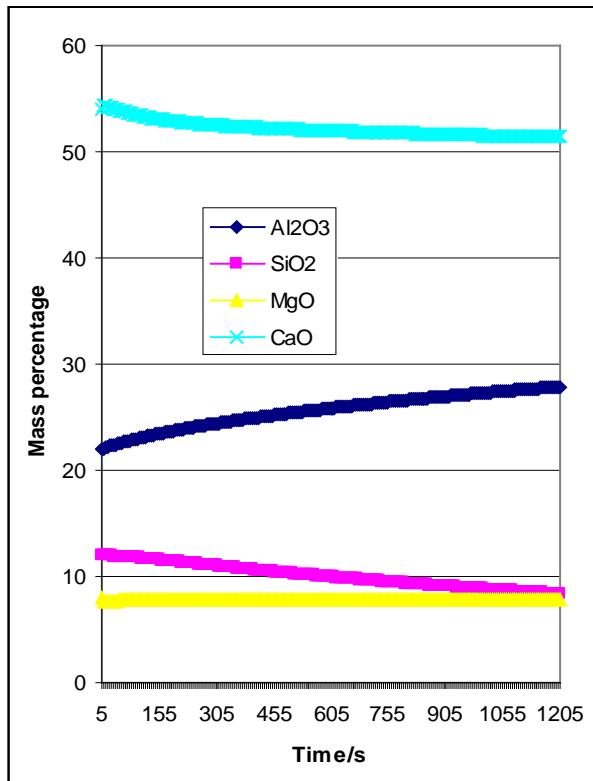
# Model Validation



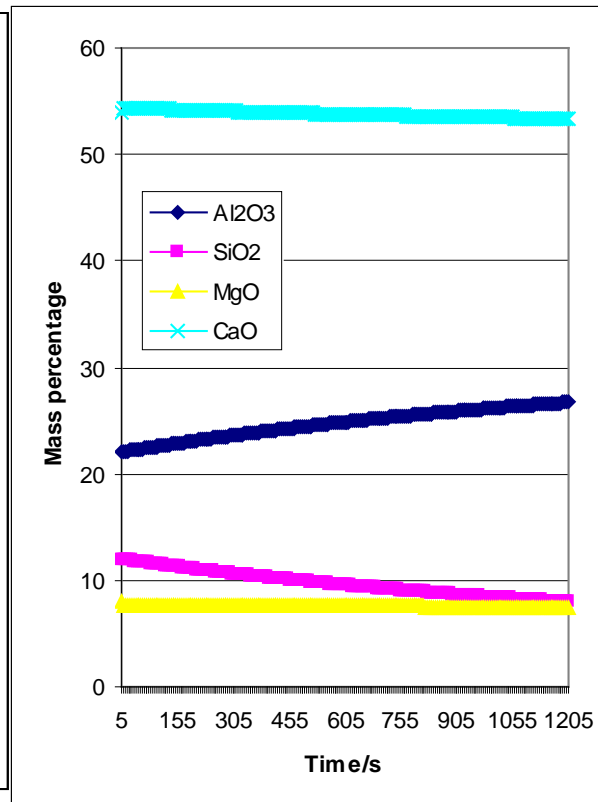
Evolution of oxygen activity  $a[\text{O}]$  in steel during ladle treatment calculated by different models

Model 3: Agree well with industrial analysed data. The first drop is due to deoxidation of Al. The other drops could be connected with the separation and modification of inclusion.

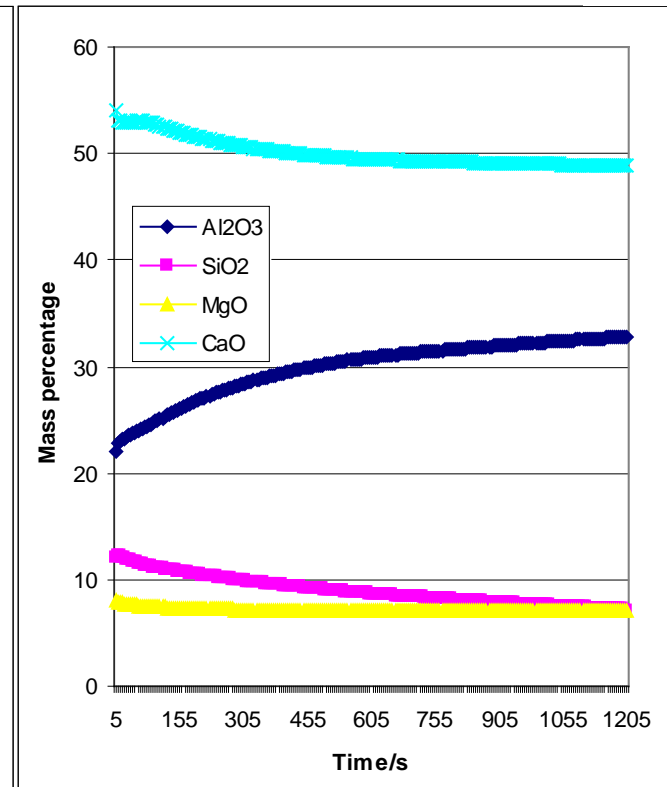
# Model Validation



Model 1



Model 2

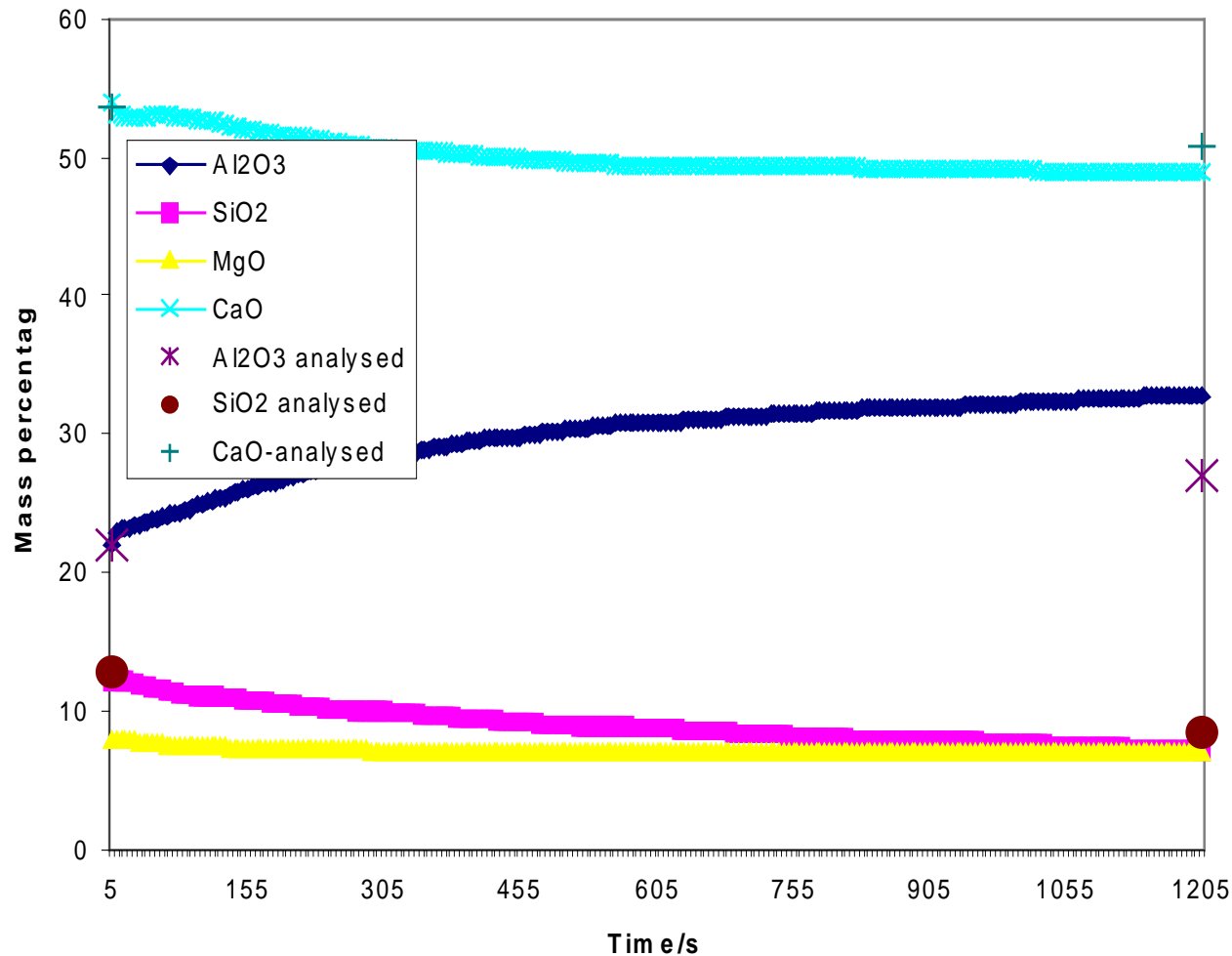


Model 3

The content of Al<sub>2</sub>O<sub>3</sub> by Model 3 increase more than the values by Model 1 and 2 due to the separation of Al<sub>2</sub>O<sub>3</sub> into slag



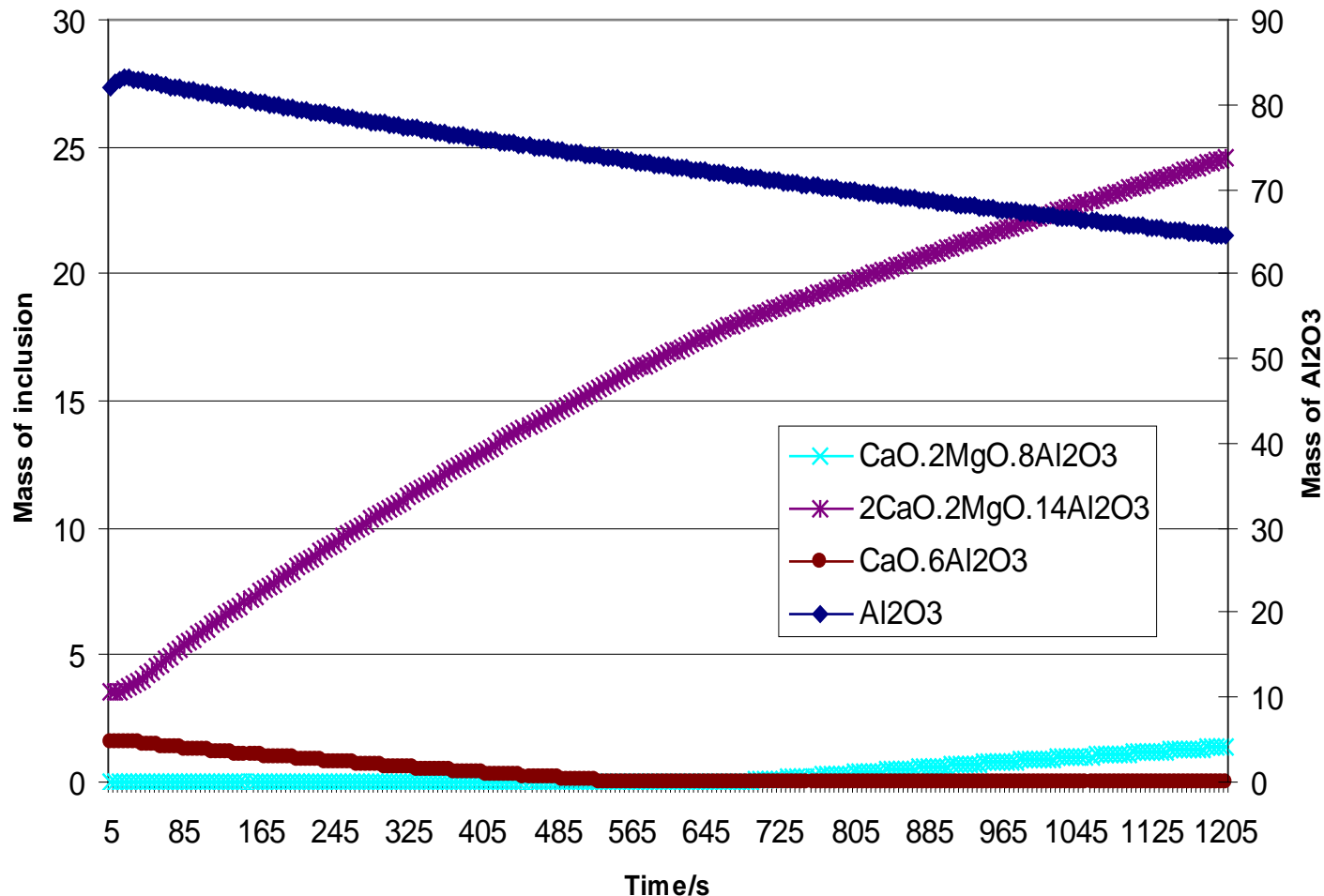
# Model Validation



Comparison between calculated chemical composition of slag (Model 3) and industrial analysed compositions during ladle treatment

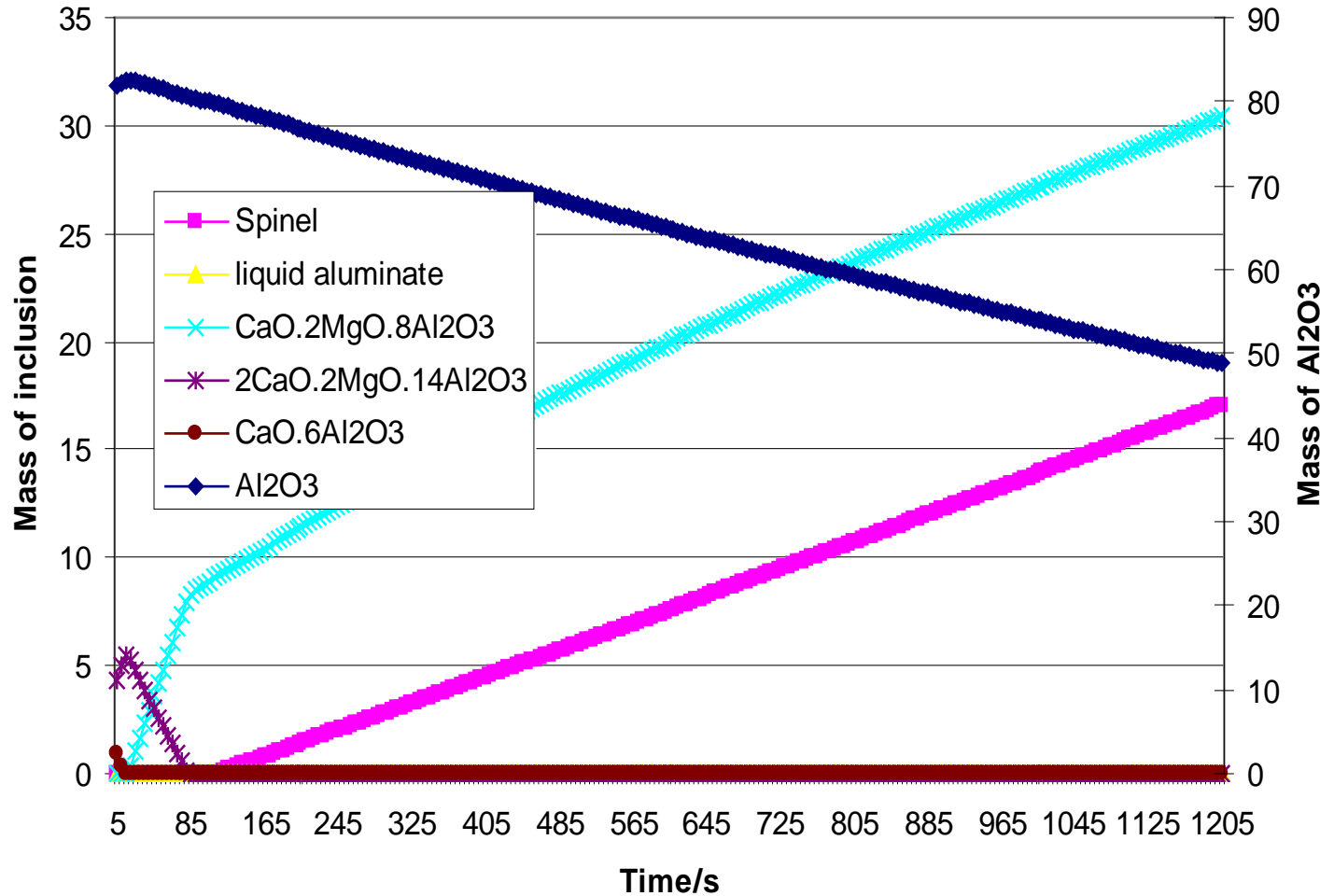


# Model 1: the evolution of inclusion with time (before CaSi treatment)



Major inclusions are alumina,  $\text{CaO} \cdot 2\text{MgO} \cdot 8\text{Al}_2\text{O}_3$  and  $2\text{CaO} \cdot 2\text{MgO} \cdot 14\text{Al}_2\text{O}_3$

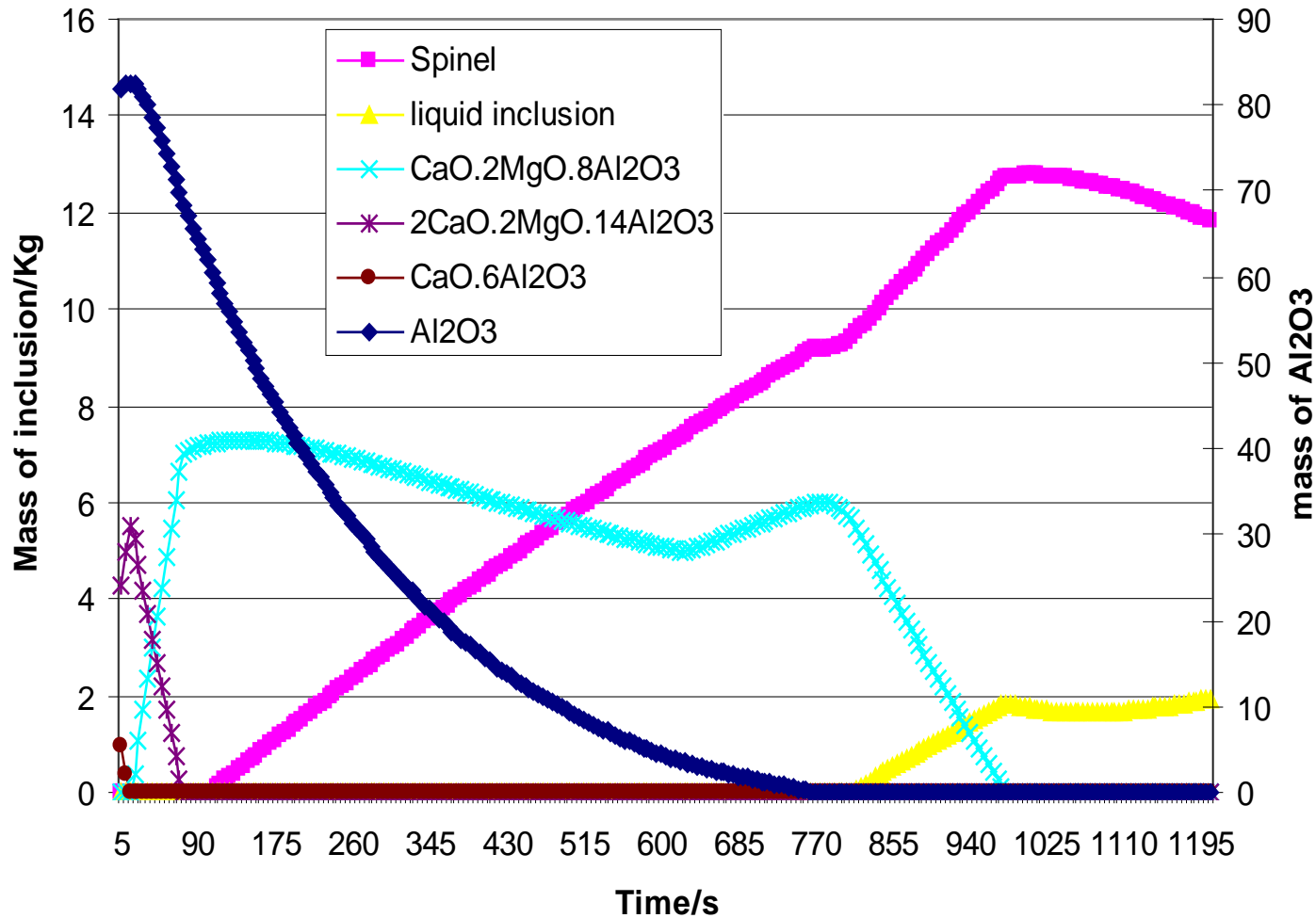
# Model 2: the evolution of inclusion with time (before CaSi treatment)



Major inclusions are alumina, spinel, CaO.2MgO.8Al<sub>2</sub>O<sub>3</sub>. Final inclusion are alumina, spinel and CaO.2MgO.8Al<sub>2</sub>O<sub>3</sub>



# Model 3: the evolution of inclusion with time (before CaSi treatment)



Major inclusions are alumina, spinel, CaO.2MgO.8Al<sub>2</sub>O<sub>3</sub>. Final inclusion are spinel and some liquid aluminate

# Model Validation

## Inclusions after CaSi treatment:

- **Model 1:** liquid aluminates,  $\text{CaO} \cdot 2\text{MgO} \cdot 8\text{Al}_2\text{O}_3$  and  $\text{CaO} \cdot 2\text{Al}_2\text{O}_3$
- **Model 2:** liquid aluminates and  $\text{CaO} \cdot 2\text{MgO} \cdot 8\text{Al}_2\text{O}_3$
- **Model 3:** liquid aluminates and CaS

Process step	Analyzed inclusions	Calculated Inclusions (Model 1)	Calculated Inclusions (Model 2)	Calculated Inclusions (Model 3)
Arrival at ladle treatment station	A C D	A C	A C	A C
Before CaSi treatment	B A C	A C	A B C	B A C
Departure ladle	C E	C	C	E C

A: Alumina; B: Spinel; C: Calcium aluminate; D: Manganese silicate; E: Calcium sulphide

Inclusions are listed by the amount decrease order.

The calculated inclusions by model 3 before and after CaSi treatment are consistent with inclusion found in industrial sample.



# Model Validation - conclusion

The best fit with the industrial measurements delivers

## **MODEL 3**

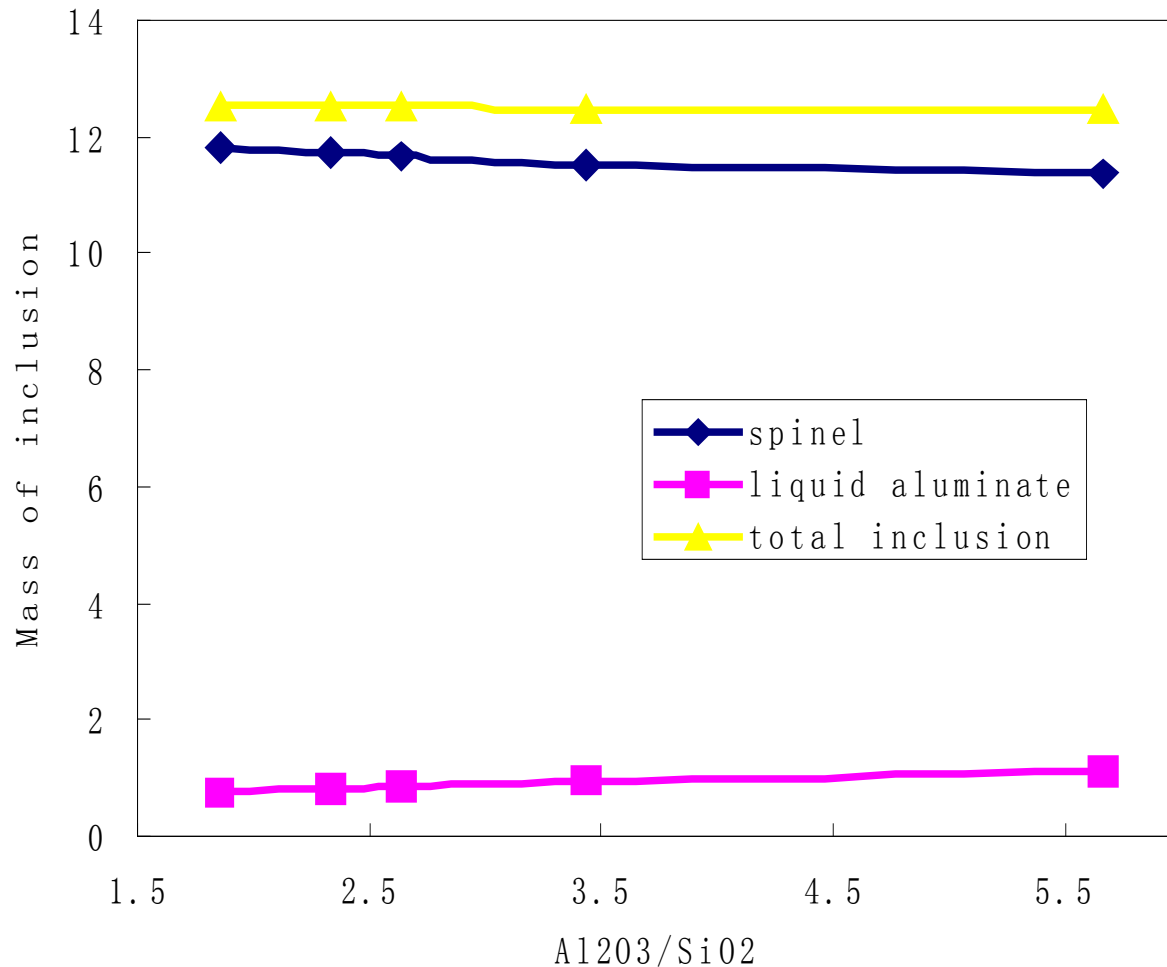
Further calculations – only using Model 3

**-PARAMETER STUDY-**



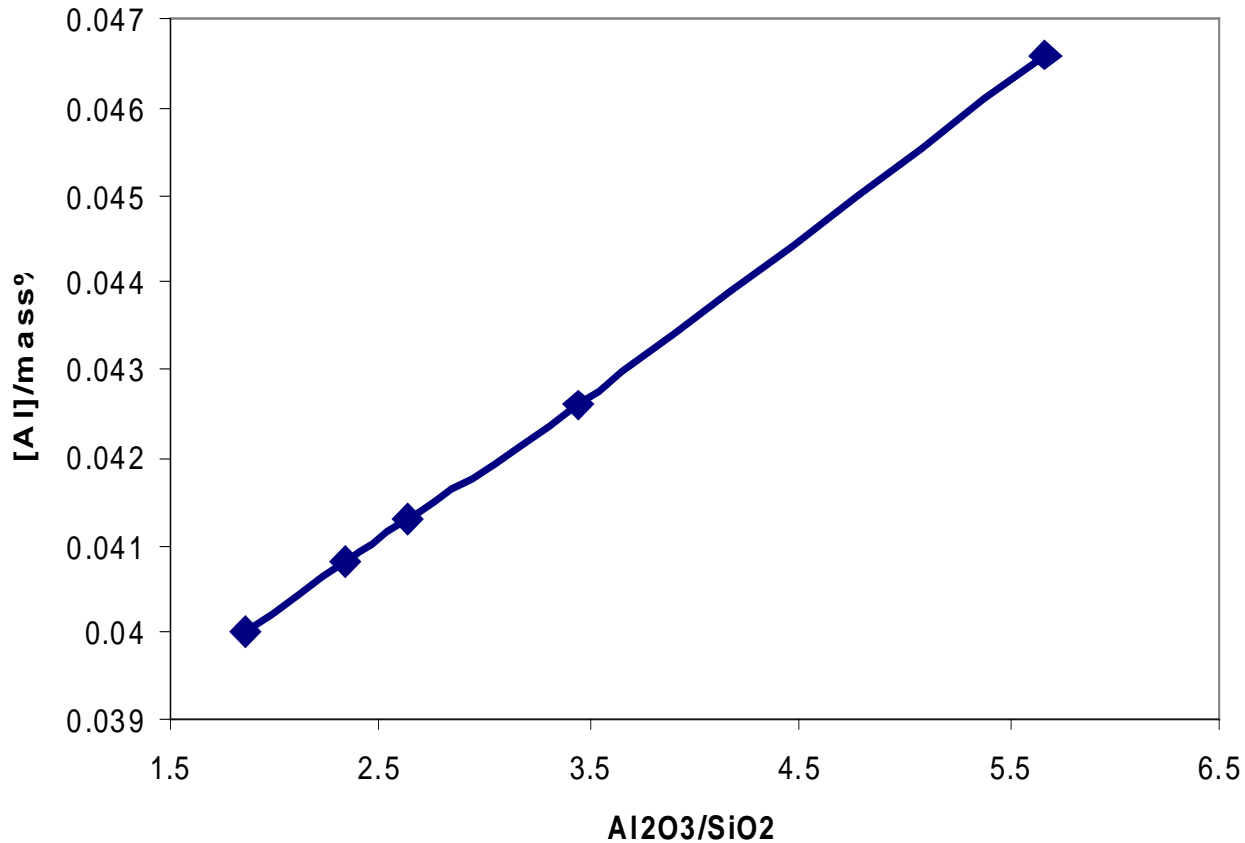
# Effect of Slag Composition

Mass of inclusions as functions of  $\text{Al}_2\text{O}_3/\text{SiO}_2$  ratio  
(all other industrial and model parameter are unchanged)



# Effect of Slag Composition

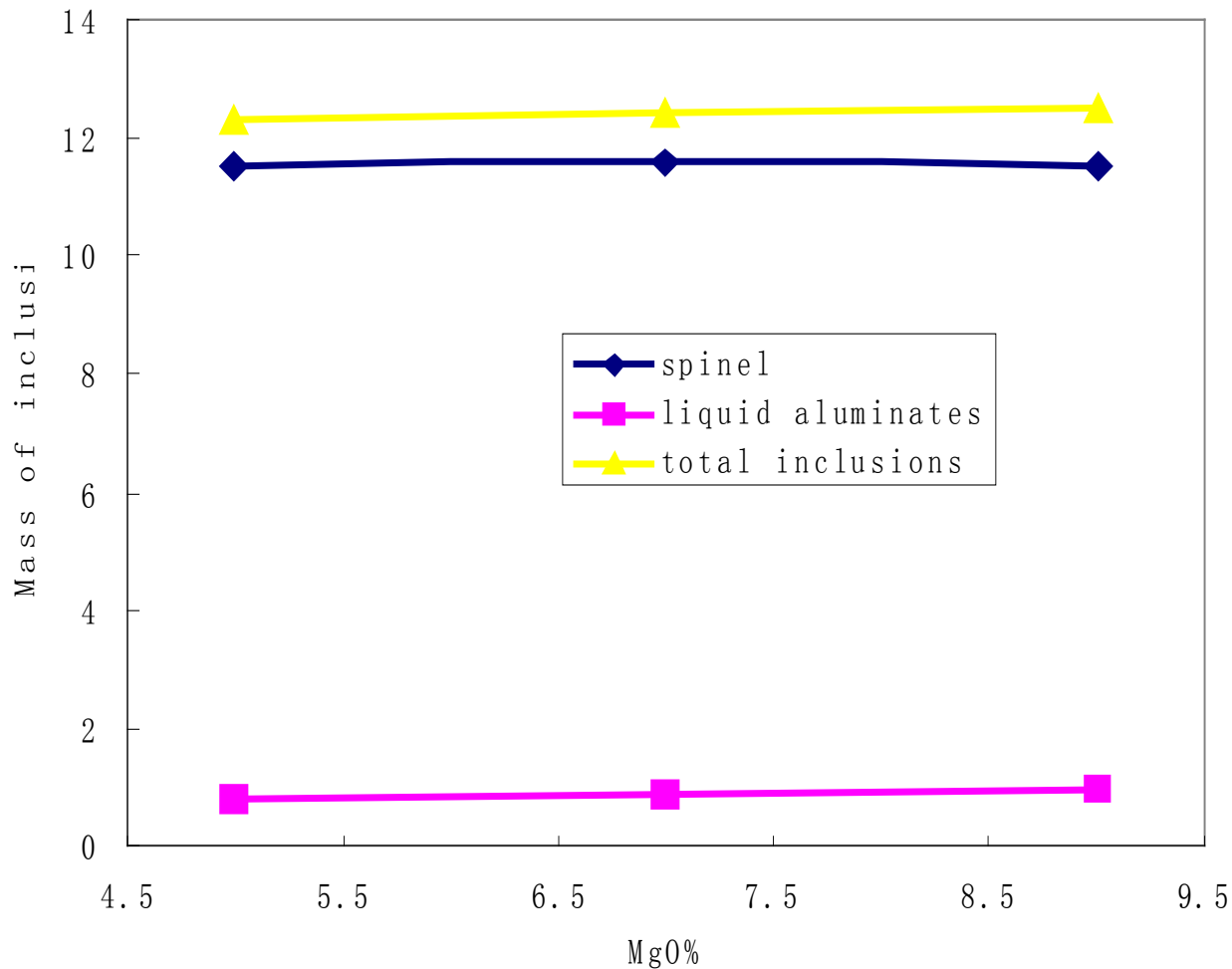
Aluminum concentration in steel as a function of  $\text{Al}_2\text{O}_3/\text{SiO}_2$  ratio in slag  
(all other industrial and model parameter are unchanged)





# Effect of Slag Composition

Mass of inclusions as functions of MgO% in slag  
(all other industrial and model parameter are unchanged)



# Effect of Lining Material

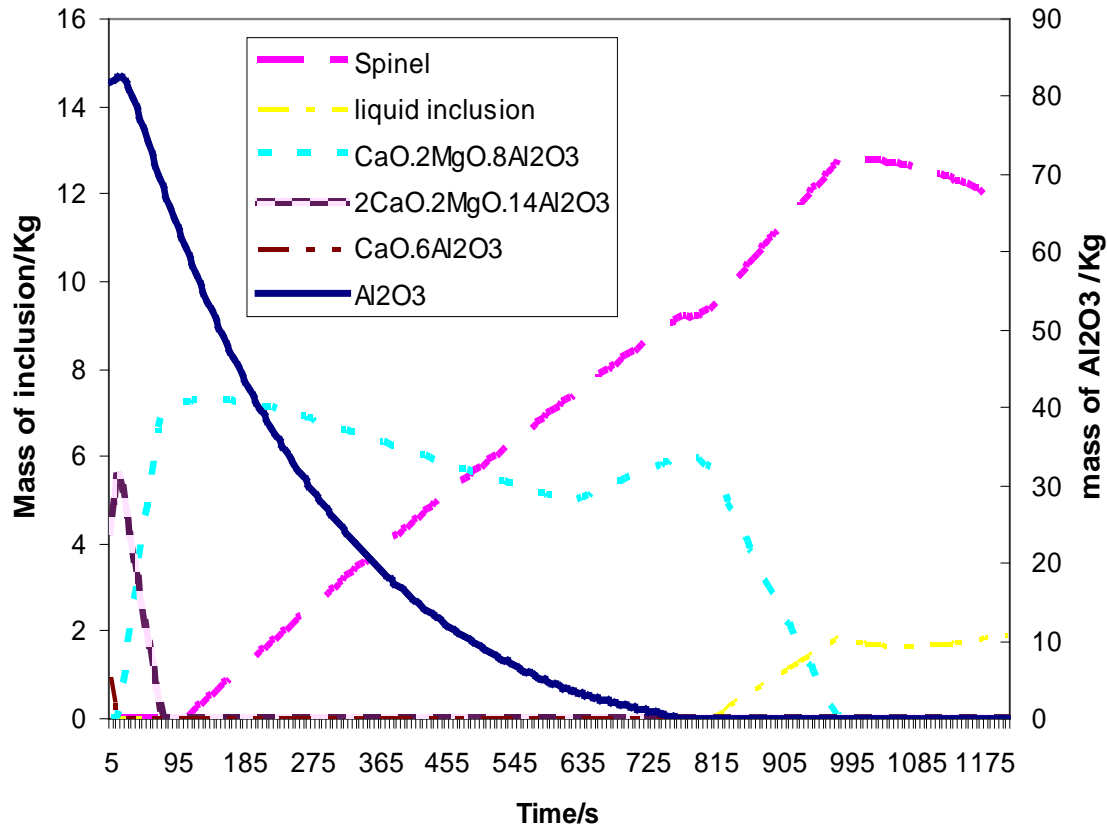
Composition of ladle lining refractory used in the model calculation

Refractory type	$\text{Al}_2\text{O}_3$	Dolomite	MgO-C
Composition (wt%)	$\text{Al}_2\text{O}_3$ : 92% MgO: 8%	CaO: 60% MgO: 40%	MgO: 95% C: 5%



# Effect of Lining Material

## Inclusion evolution in ladle with MgO-C lining

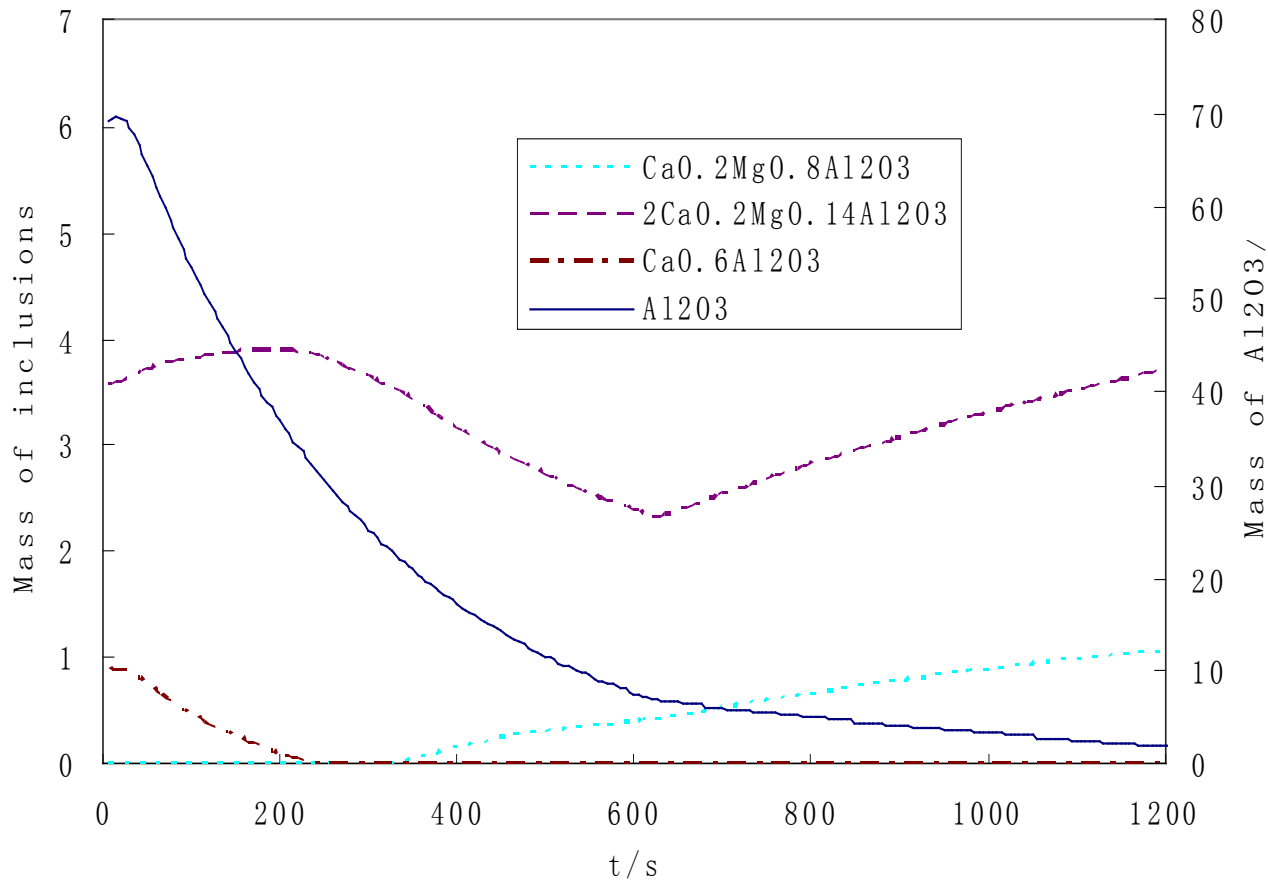


→ final inclusions: Mg-Al spinels and liquid inclusions



# Effect of Lining Material

## Inclusion evolution in ladle with $\text{Al}_2\text{O}_3$ lining

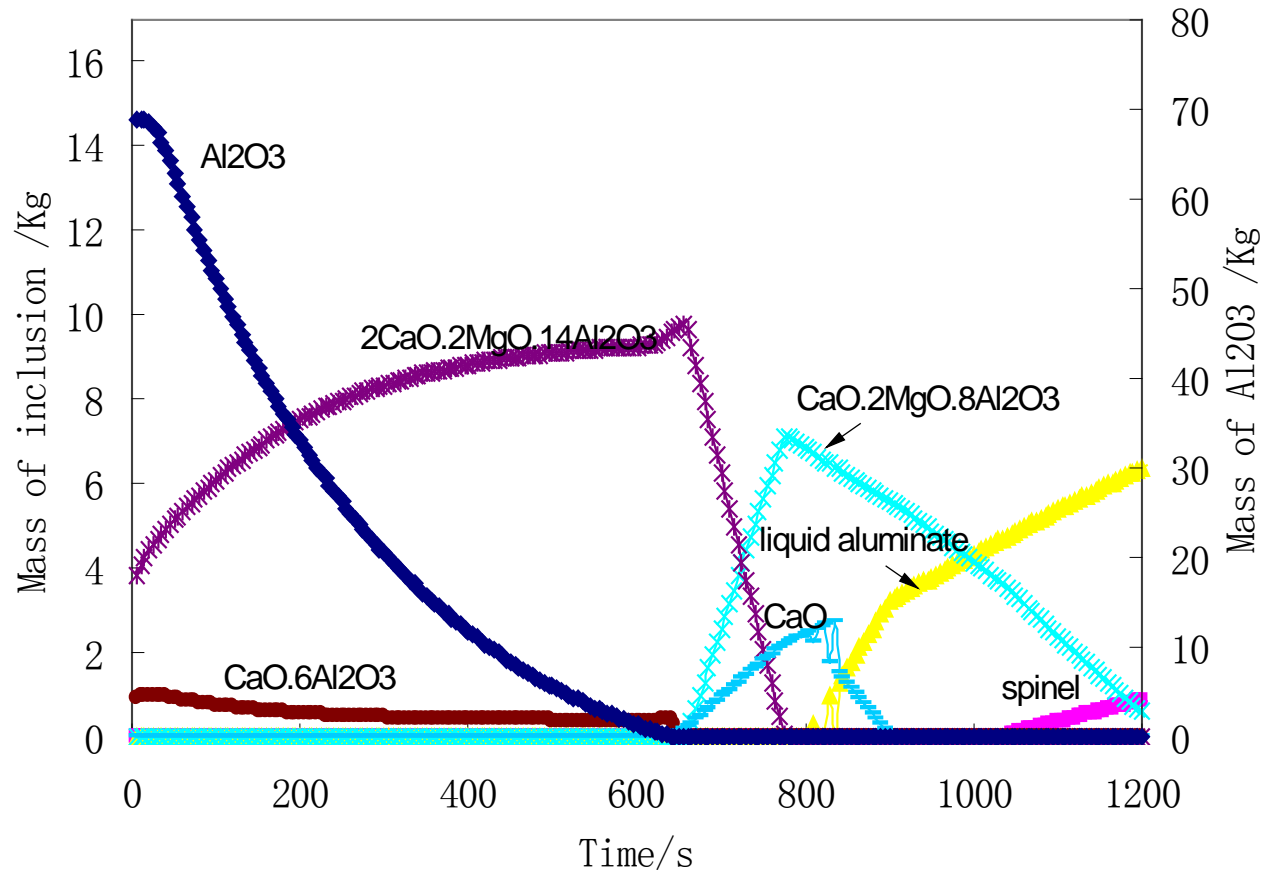


→ **final inclusions:** alumina reach inclusions and solid alumina;  
compared to MgO-C lining: no Mg-Al spinels



# Effect of Lining Material

## Inclusion evolution in ladle with **dolomite** lining



→ **final inclusions:** liquid aluminates and minor aluminates and Mg-Al spinels; dolomite lining supports the transformation of solid aluminates, spinel into liquid aluminates (by dissolution of Ca into steel and slag)

# Use for process assistance

The screenshot shows a software window titled "Change Composition" with two main sections: "Steel" and "Slag".

**Steel Section:**

[C]	0.39939%	[Al]	0.25009%
[Si]	2098367	[Ca]	2.275900 ppm
[Mg]	6.80966%	[Mn]	0.39914%
[Cr]	4.98954%	[O]	50.02711 ppm
[Ni]	0	[S]	0
[Ti]	0	[Mo]	1.25736
[V]	0.91608		

Name: NEWSTEEL

Select Steels: STEEL\_

**Slag Section:**

Al <sub>2</sub> O <sub>3</sub> %	36.986%	MgO%	9.4835%
CaO%	49.741%	SiO <sub>2</sub> %	3.7847%
CaF <sub>2</sub> %	0	FeO%	0.0010%
MnO%	0.0018%		

Name: NEWSLAG

Select Slags: SLAG\_

Temperature: 1600

Interface for input of steel and slag composition – during the process



# Use for process assistance

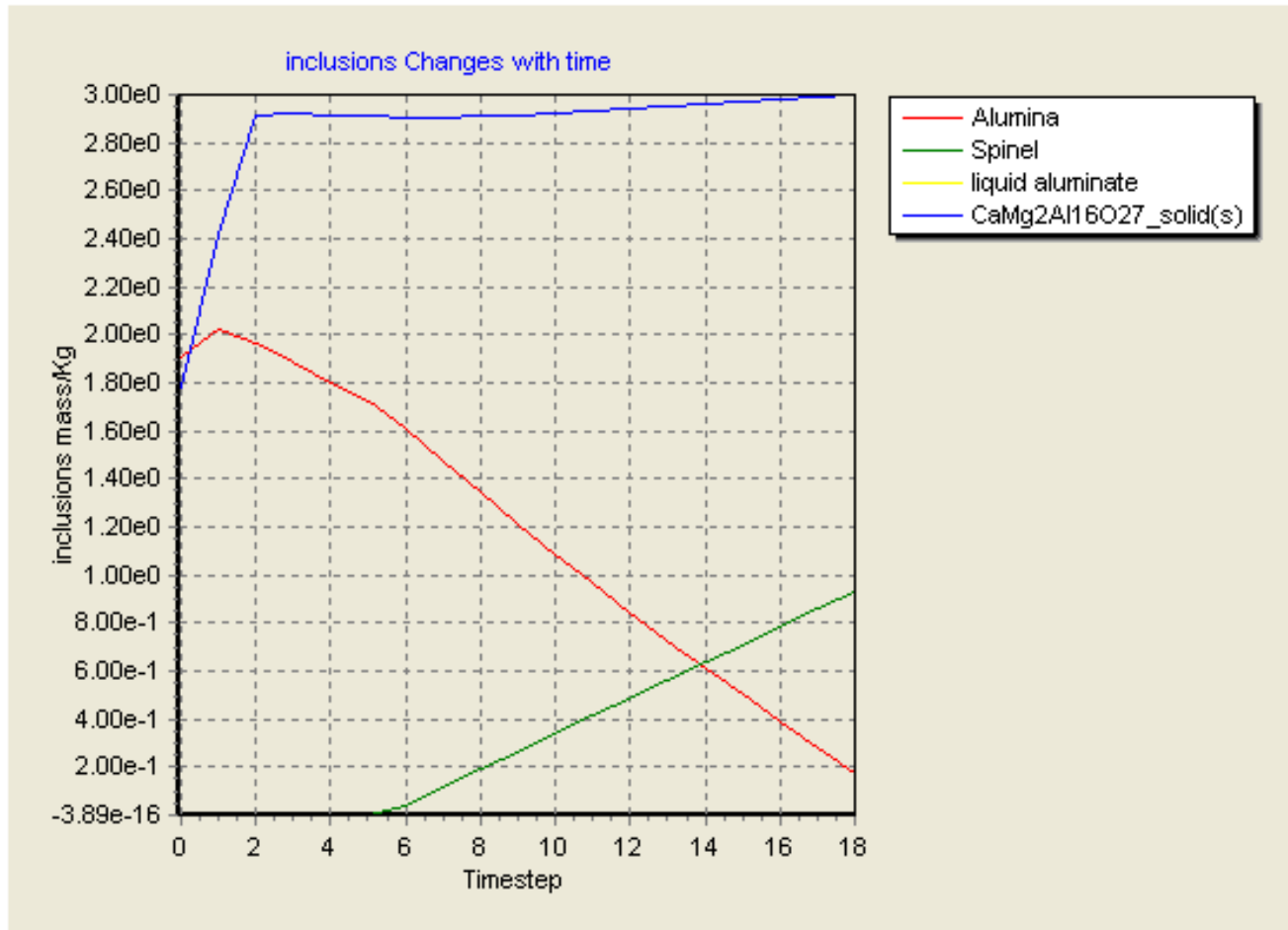
**Setting parameters dialog**

Mass transfer coefficient of steel (m/s)	<input type="text" value="0.002"/>	Steel mass (Kg)	<input type="text" value="180000"/>
Mass transfer coefficient of slag (m/s)	<input type="text" value="0.001"/>	Slag mass (Kg)	<input type="text" value="2500"/>
Dissolution rates of slag /(kg/m2/s)	<input type="text" value="0.001"/>	Ladle diameter(m)	<input type="text" value="3,2"/>
Dissolution rates of steel /(kg/m2/s)	<input type="text" value="0.0005"/>	Initial temperature TI (Celsius)	<input type="text" value="1600"/>
Separation rates for alumina Before 10 min	<input type="text" value="0.20"/>	Temperature decreasing coefficient	
After 10min	<input type="text" value="0.05"/>	KTLine (C/min)	<input type="text" value="0.028"/>
Separation rates for spinel	<input type="text" value="0.03"/>	KTRoot (C/min <sup>0.5</sup> )	<input type="text" value="1.7"/>
Separation rates for liquid inclusion	<input type="text" value="0.05"/>	Formula: T=TI-KTLine*t-KTRoot*sqrt(t)	
Time for one step/s	<input type="text" value="5"/>	Recirculate rates for steel( kg/step)	<input type="text" value="0.8"/> (0-1) of plume tank
		Recirculate rates for slag( kg/step)	<input type="text" value="0.6"/> (0-1) of slag1 tank

Interface for setting model and process parameters



# Use for process assistance



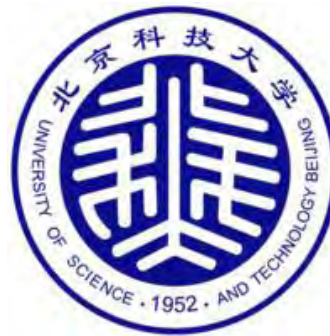
Plot module (on line) for simulation results



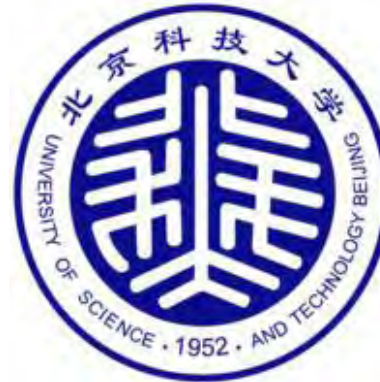


# Conclusions

- A comprehensive model for inclusion development in gas-stirred ladle was established by taking mixing, slag-steel reaction, inclusion separation and lining wear and dissolution into consideration
- The effects of slag composition and nature of lining refractory on the inclusion evolution were also investigated. The slag composition in the range investigated has a small effect on the inclusion evolution, while ladle refractory could have important effects. The strongest effect has the separation of inclusions
- The comparisons between calculated and industrial data show that the present model can predict inclusion evolution consistent with industrial practice



# Thank You



Contact:

Piotr R.Scheller  
scheller\_piotr@web.de

