

PHASE FIELD MODELING OF ISOTHERMAL SLAG CRYSTALLIZATION

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GTT - TECHNOLOGIES



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Outline

- Introduction
 - ▣ Research framework and organization
- Concepts of phase field modeling
- Slag specific properties in the model
 - ▣ Thermodynamic data
 - ▣ Stoichiometric phases
 - ▣ Facet interfaces
 - ▣ Redox equilibria
- Case studies (simulation results)
- Conclusions

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Goal and framework of this research

□ Problem statement

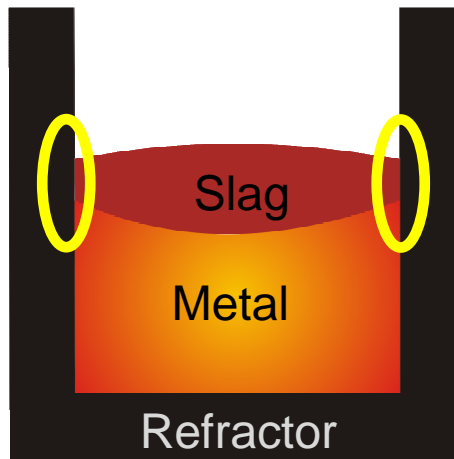
- Microstructure evolution of metallurgical slags controls many aspects of pyrometallurgical processes
 - e.g. freeze lining, refractory wear, tapping and cooling

□ Goals

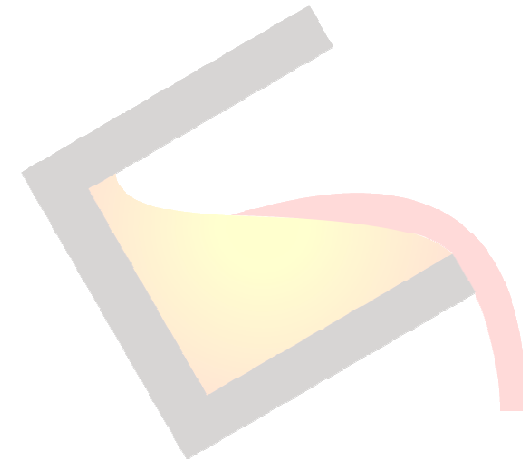
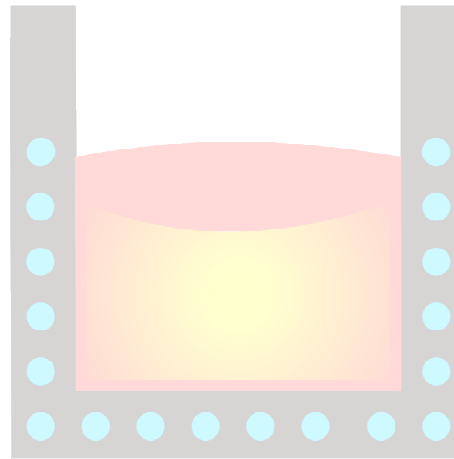
- Develop a multiphase and multicomponent model to simulate microstructure evolution in slags
- Perform necessary high temperature experiments
 - ... to compare with the model
 - ... to supply data for the model

Microstructure evolution in slags

- Process slag in contact with furnace refractories
- Freeze lining formed by solidification of process slag
- Tapping slag at high temperature and cooling down

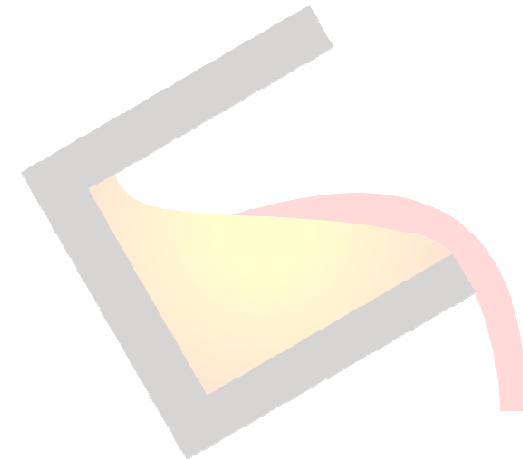
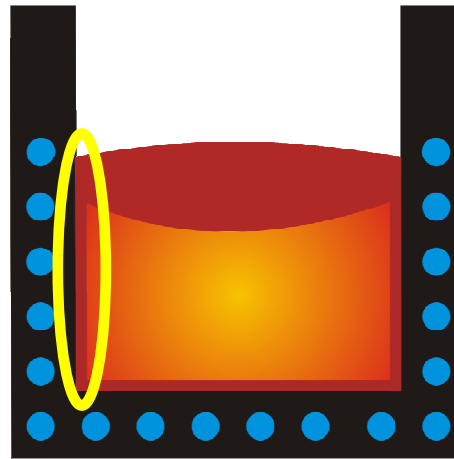
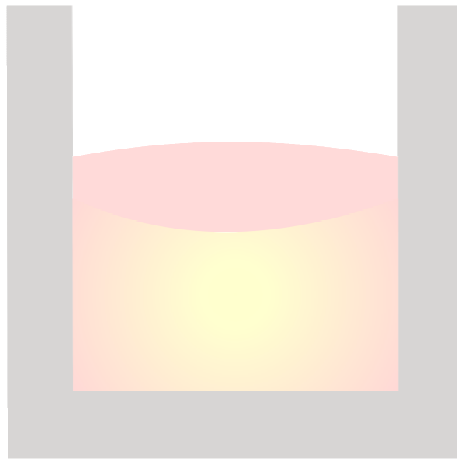


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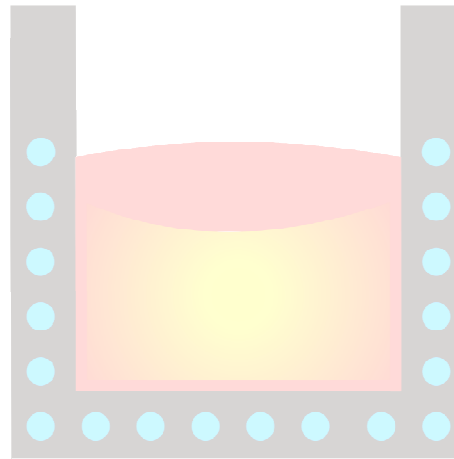
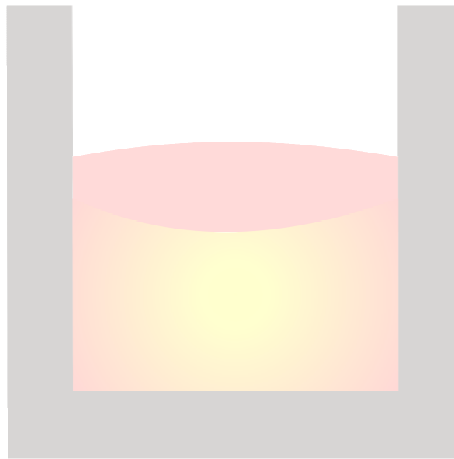
Microstructure evolution in slags

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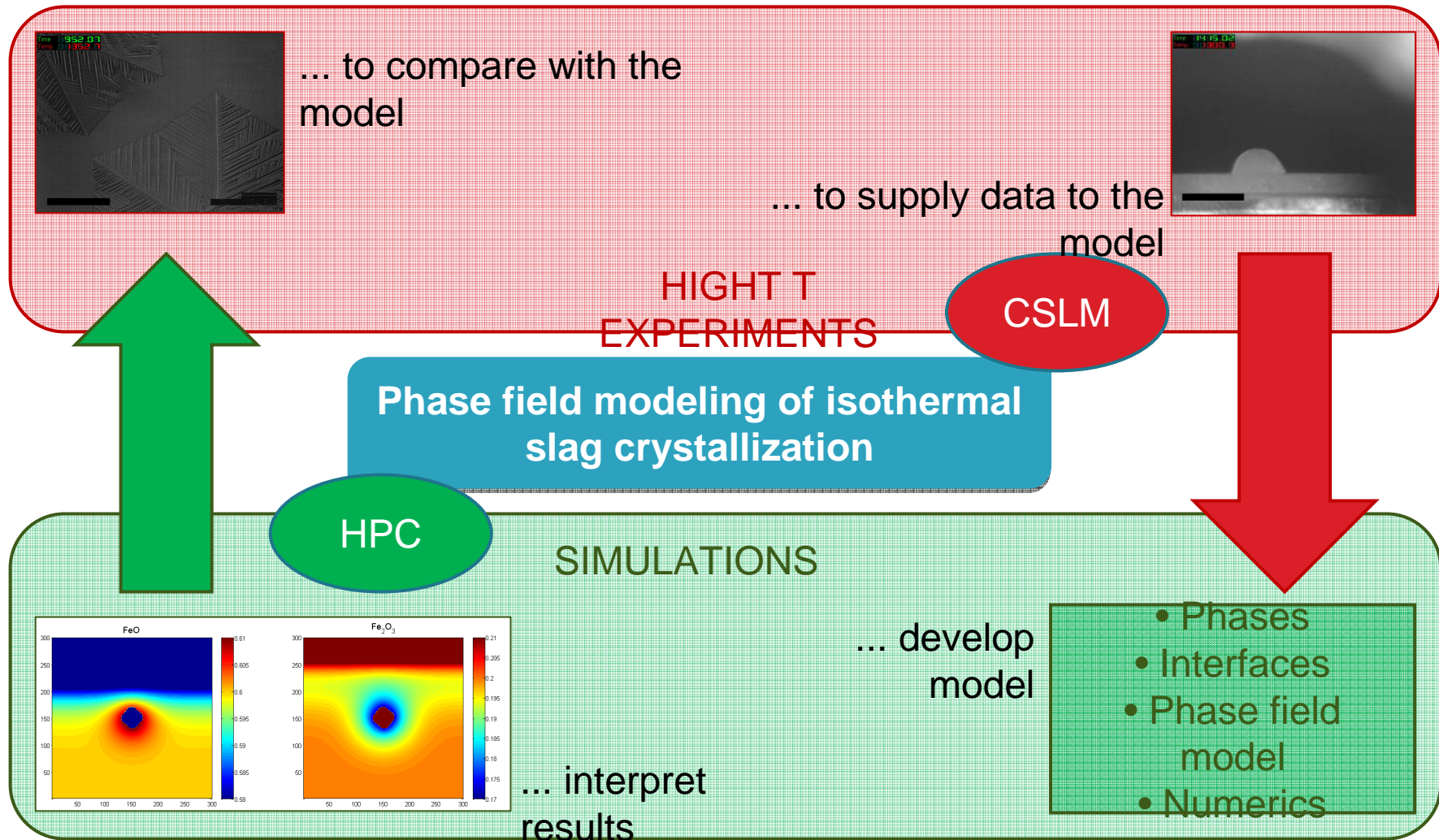


Microstructure evolution in slags

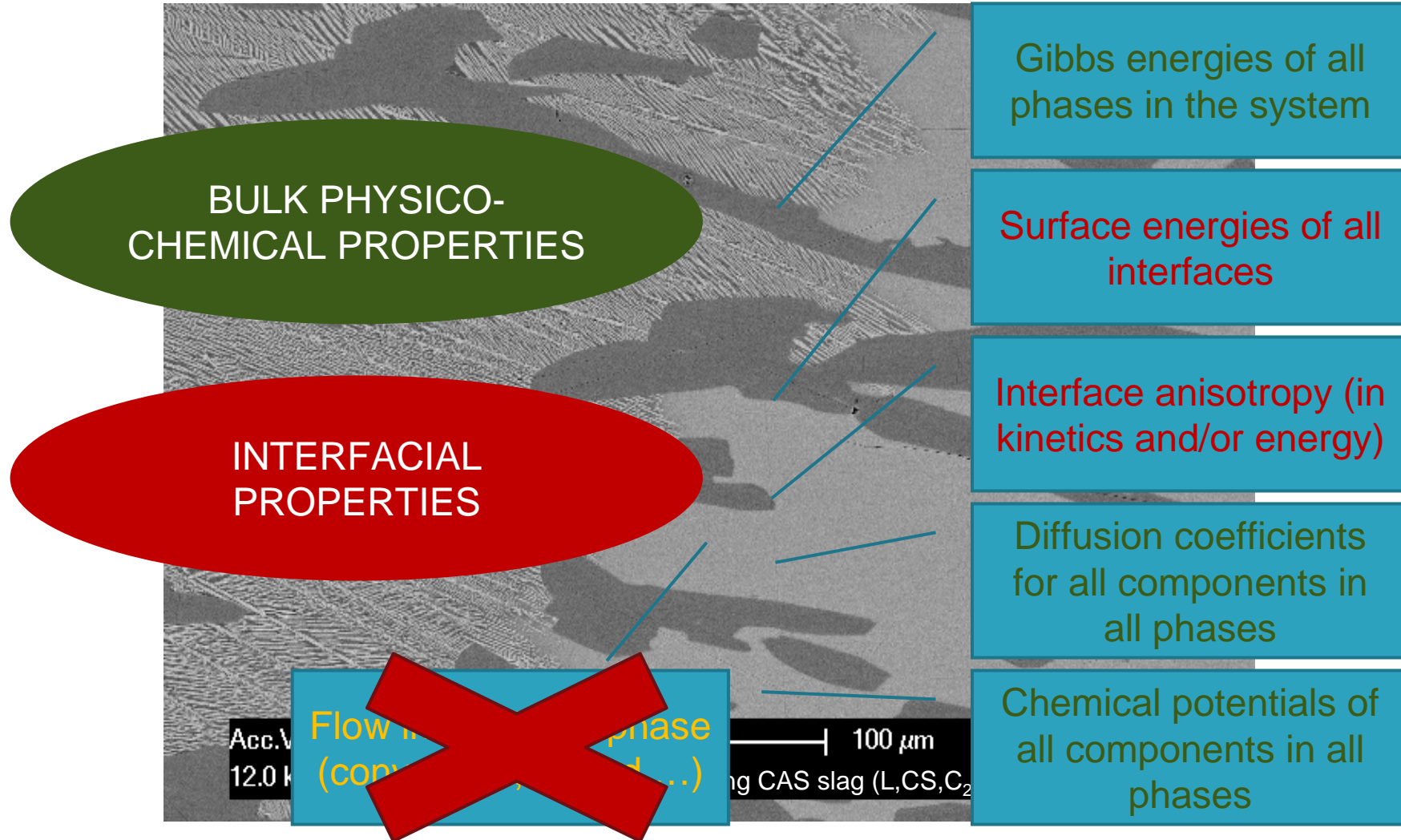
- Process slag in contact with furnace refractories
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Organization of the research



Modeled physical phenomena



Investigated slag systems



- 4-component system
 - ▣ Ca-Al-Si-O
- 3-component if oxides are assumed to diffuse
 - ▣ CaO
 - ▣ Al₂O₃
 - ▣ SiO₂



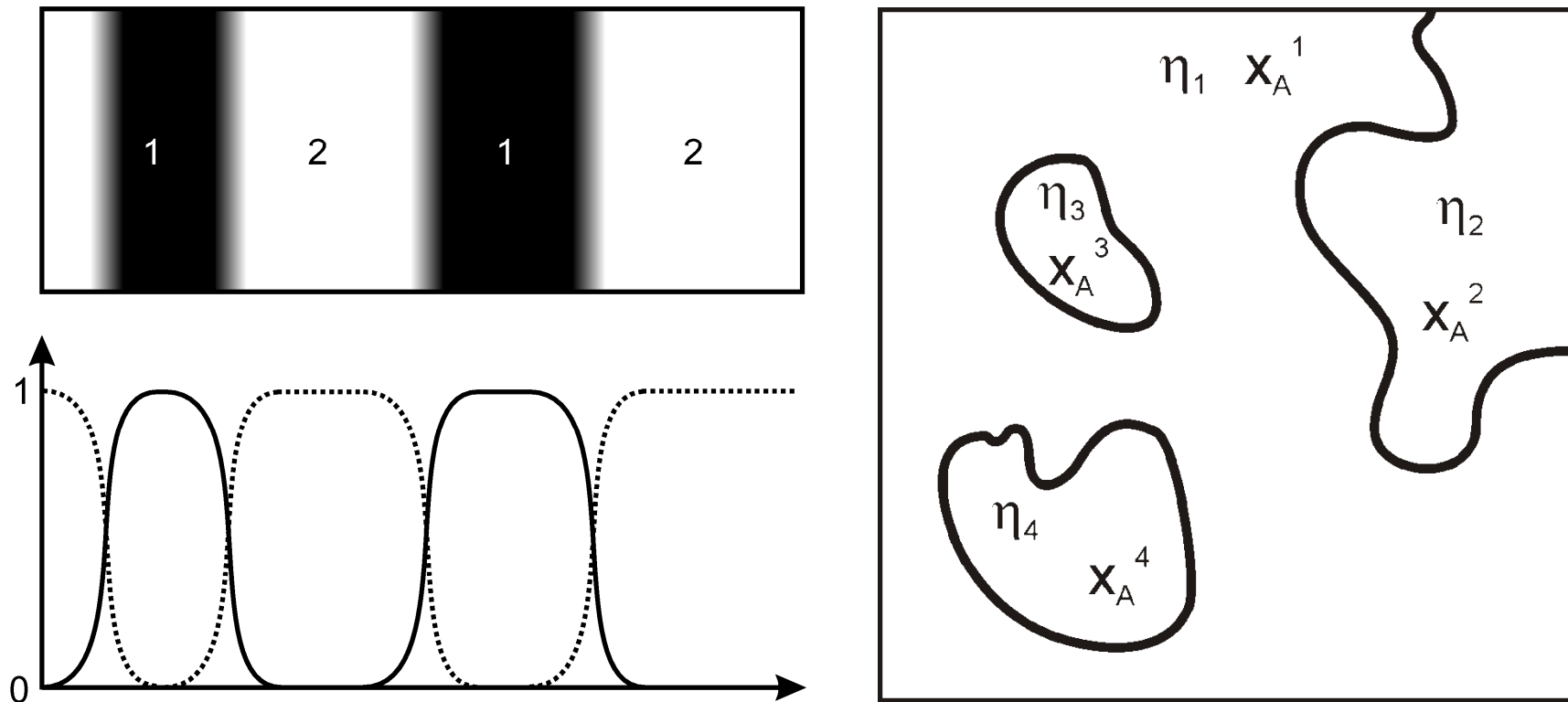
- 3-component system
 - ▣ Fe-Si-O
- Transition to FeO and Fe₂O₃ to study redox
 - ▣ FeO (Fe²⁺)
 - ▣ Fe₂O₃ (Fe³⁺)
 - ▣ SiO₂

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Concepts of phase field modeling

- Diffuse interfaces between different phases can treat arbitrary interface shapes



Microstructural evolution

- System of p phases and c components
- Phase fields evolve by energy minimization:

$$\frac{\partial \eta_i}{\partial t} = -L \frac{\delta}{\delta \eta_i} \left(\int_V \left(mf_0 + \frac{K}{2} \sum_{r=1}^p |\nabla \eta_r|^2 + f_{chem} \right) dV \right)$$

- **Interfacial energy** (Double well and gradient term)
 - **Chemical energy** (Gibbs energies of phases)
- Diffusion equation for every component:

$$\frac{\partial x_k}{\partial t} = \nabla \cdot \left(\sum_{i=1}^p \phi_i \sum_{r=1}^{c-1} M_{rk}^i \nabla \tilde{\mu}_r^i \right) \quad \tilde{\mu}_r^i = \mu_r^i - \mu_{SiO_2}^i$$

Thermodynamic equilibrium

- Local (volumetric) chemical energy is calculated as:

$$f_{chem} = \sum_{i=1}^p \phi_i f^i$$

- Equality of diffusion potentials of c-1 components in p phases:

$$\tilde{\mu}_1^i = \dots = \tilde{\mu}_k^i = \dots = \tilde{\mu}_{c-1}^i \quad i = 1..p$$

- Mass balance to link phase concentrations to x_k :

$$x_k = \sum_{i=1}^p \phi_i x_k^i \quad k = 1..c-1$$

- Set of equations is solved for phase concentrations x_k^i

Kim SG, Kim WT, Suzuki T, Physical Review E 60(6), 1999
Eiken J, Bottger B, Steinbach I, Physical Review E 73(6), 2006

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Thermodynamic data of slags

- The phase field model uses:
 - ▣ Gibbs energies of all phases (solid and liquid)
 - $f_i(\mathbf{x}_k, T)$ depends on local composition and temperature
 - 2nd order Taylor expansion for local approximation
 - ▣ Diffusion potentials of all components
 - $\mu_k(\mathbf{x}_k, T)$ depends on local composition and temperature
 - Second derivative of Gibbs energies
- This data can be calculated using ChemApp
 - ▣ Converting c chemical potentials into $c-1$ diffusion potentials
 - ▣ Carefully assess and use reference states for

2nd order Taylor approximation

- Gibbs energy of phase i is approximated by:

$$\hat{f}^i = \sum_{k=1}^{c-1} \left(\frac{A_{kk}^i}{2} (x_k^i - \hat{x}_k^i) + \sum_{l \neq k} A_{kl}^i (x_k^i - \hat{x}_k^i)(x_l^i - \hat{x}_l^i) + B_k^i (x_k^i - \hat{x}_k^i) \right) + C^i$$

$$A_{kl}^i = \frac{\partial^2 f^i}{\partial x_k^i \partial x_l^i} \quad B_k^i = \frac{\partial f^i}{\partial x_k^i} = \tilde{\mu}_k^i \quad C^i = f^i$$

- **A**, **B** and **C** are retrieved by ChemApp and stored in an array to load in the phase field code
- Diffusion potentials are linear in concentrations, which greatly reduces computational effort

ChemApp calls (liquid phase)

□ Gibbs energy

- ▣ call tqgetr('GM', 0, 0, F, noerr)

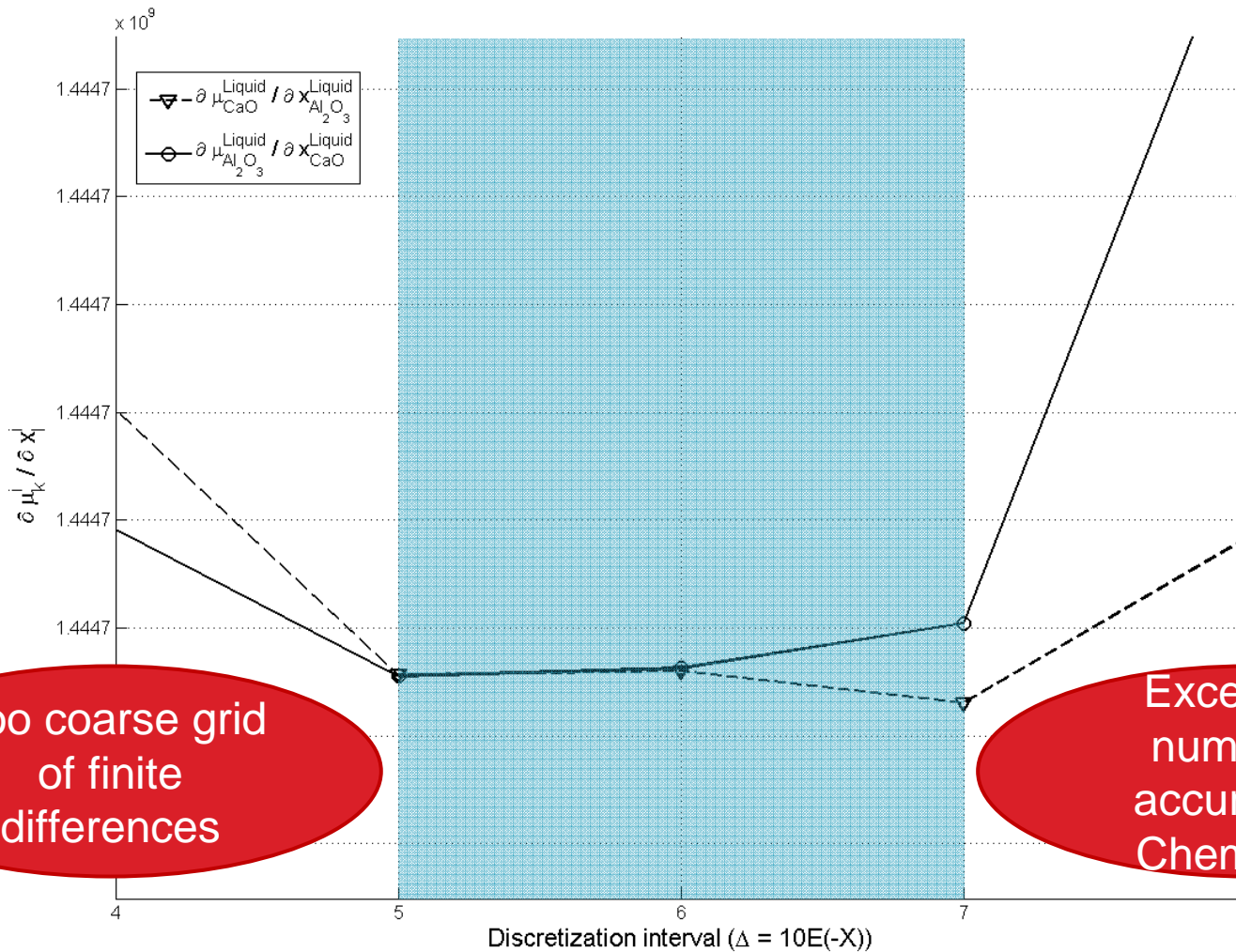
□ Diffusion potential of CaO

- ▣ G_SiO2_0 and G_CaO_0 (*standard states in liquid at certain T*)
- ▣ call tqgetr('MU', i_liquid, i_SiO2, mu_SiO2, noerr)
mu_SiO2 = G_SiO2_0 + mu_SiO2
- ▣ call tqgetr('MU', i_liquid, i_CaO, mu_CaO, noerr)
mu_CaO = ((G_CaO_0 + mu_CaO) - mu_SiO2)/Vm

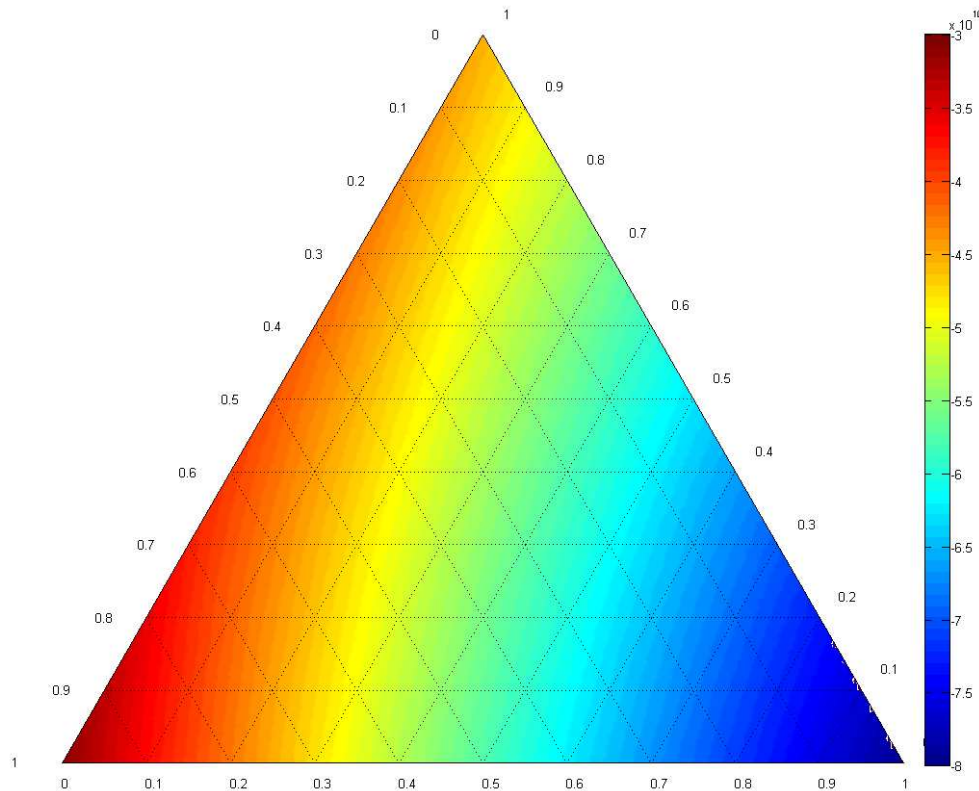
□ Second derivative of Gibbs energy

- ▣ call tqsetc('IA ', i_liquid, i_CaO, x_CaO±dr, numcon, noerr)
- ▣ **dmu_dCaO = (mu2-mu1)/(2.dθ*dr)/Vm**

Numerical determination of $d\mu/dx$



Gibbs energy of liquid



- All phases suspended
- Liquid phase is entered
- Stored in an array with $\Delta = 0.001$ spacing
- Locally approximated with 2nd order Taylor expansion

□ First derivatives

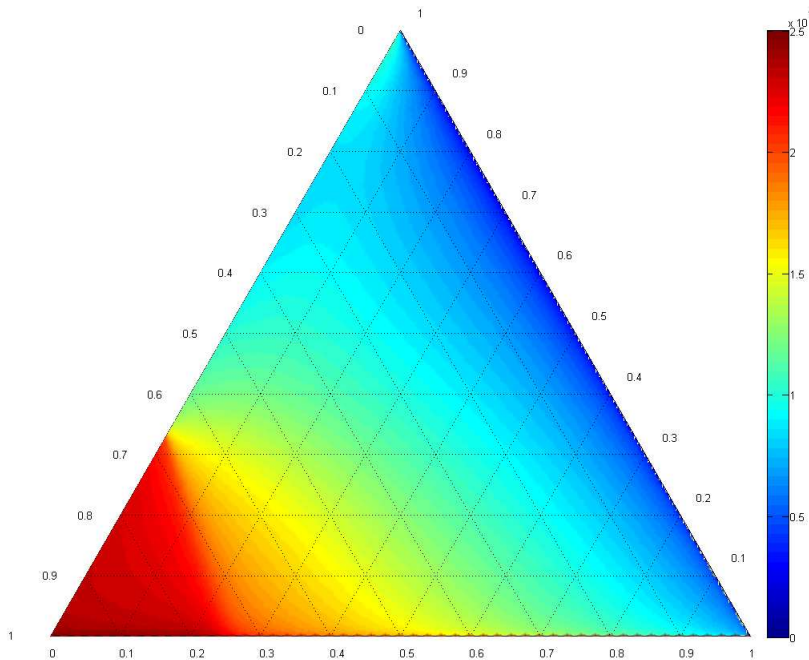
□ Second derivatives

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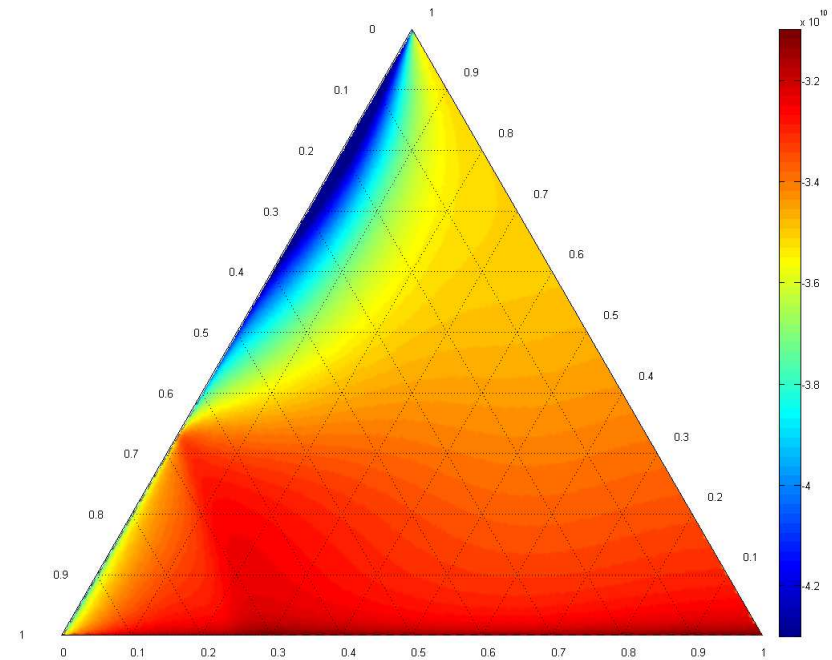
Diffusion potentials in liquid

$$\tilde{\mu}_{CaO}^{liquid} = \mu_{CaO}^{liquid} - \mu_{SiO_2}^{liquid}$$

$$\tilde{\mu}_{Al_2O_3}^{liquid} = \mu_{Al_2O_3}^{liquid} - \mu_{Al_2O_3}^{liquid}$$

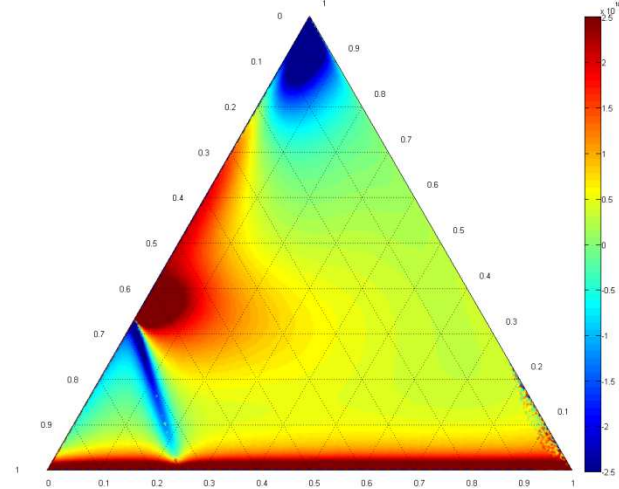
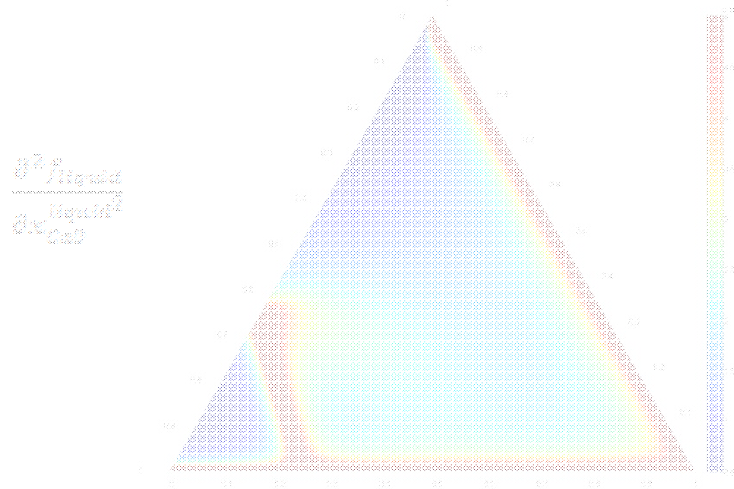


$$\frac{\partial f_{liquid}}{\partial x_{CaO}}$$

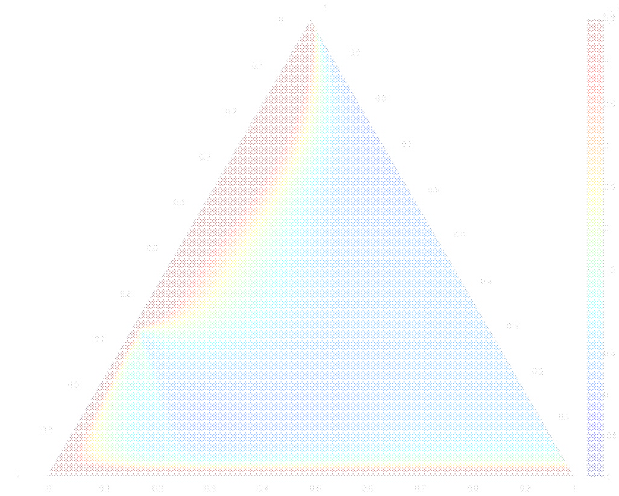
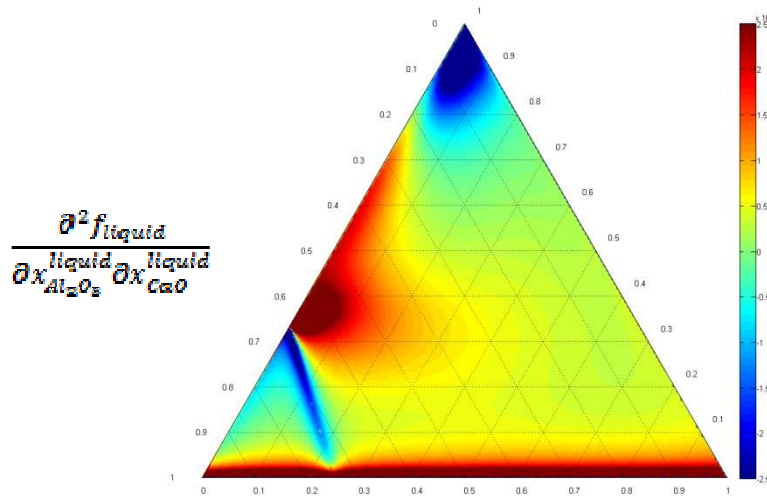


$$\frac{\partial f_{liquid}}{\partial x_{Al_2O_3}}$$

second derivative of Gibbs energy



$$\frac{\partial^2 f_{liquid}}{\partial x_{CaO} \partial x_{Al_2O_3}}$$



$$\frac{\partial^2 f_{liquid}}{\partial x_{Al_2O_3}}$$

Stoichiometric phases in slags

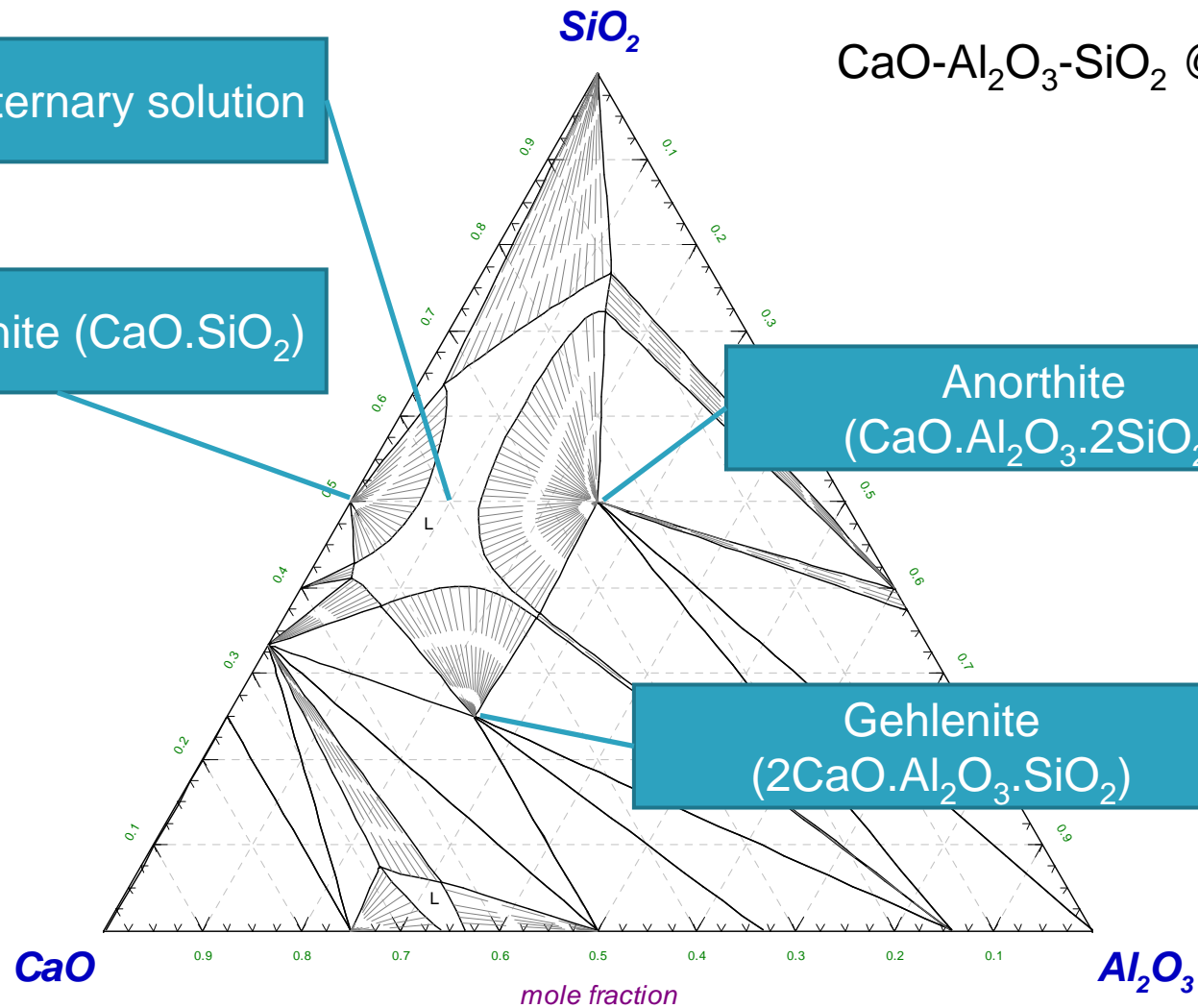
Liquid is ternary solution

Wollastonite ($\text{CaO} \cdot \text{SiO}_2$)

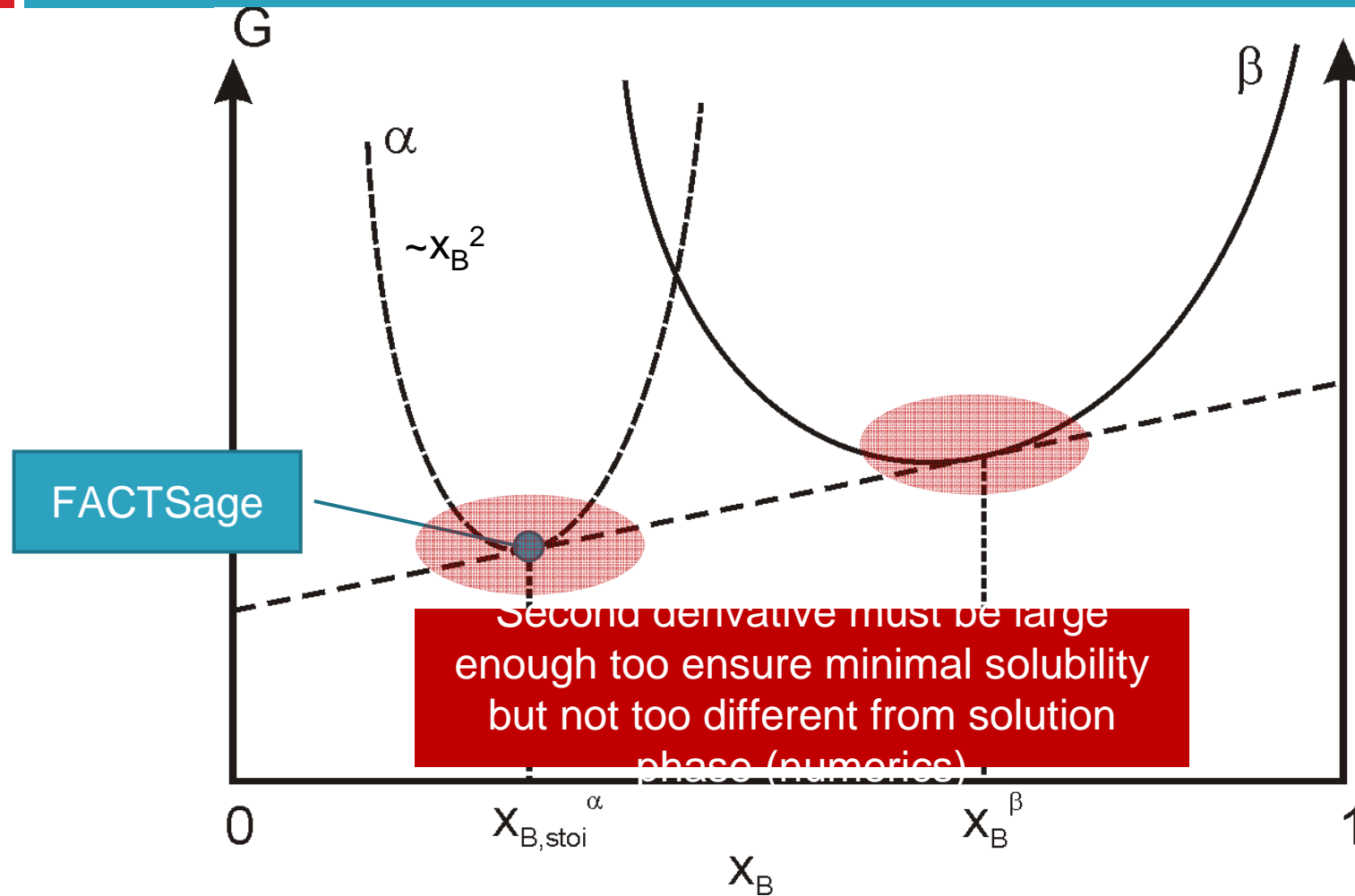
$\text{CaO-Al}_2\text{O}_3\text{-SiO}_2$ @ 1400°C

Anorthite
($\text{CaO} \cdot \text{Al}_2\text{O}_3 \cdot 2\text{SiO}_2$)

Gehlenite
($2\text{CaO} \cdot \text{Al}_2\text{O}_3 \cdot \text{SiO}_2$)



Stoichiometric phases (binary version)



Hu SY, Murray J, Weiland H, Liu ZK, Chen LQ, CALPHAD

31(2), 2007

DIFFUSION MATRIX OF $42\text{CaO}-10\text{Al}_2\text{O}_3-48\text{SiO}_2$

- Kinetic coefficients in diffusion equations can be determined by literature data and ChemApp
- Diffusion equation for component k :

$$\frac{\partial x_k}{\partial t} = \nabla \cdot \left(\sum_{i=1}^p \phi_i \sum_{r=1}^{k-1} M_{rk}^i \nabla \tilde{\mu}_r^i \right)$$

- **M** matrix relates to interdiffusion matrix **D**:

$$\begin{bmatrix} M_{11} & M_{12} \\ M_{21} & M_{22} \end{bmatrix} = \begin{bmatrix} D_{11} & D_{12} \\ D_{21} & D_{22} \end{bmatrix} \cdot \begin{bmatrix} \frac{\partial \tilde{\mu}_1}{\partial x_1} & \frac{\partial \tilde{\mu}_1}{\partial x_2} \\ \frac{\partial \tilde{\mu}_2}{\partial x_1} & \frac{\partial \tilde{\mu}_2}{\partial x_2} \end{bmatrix}^{-1}$$

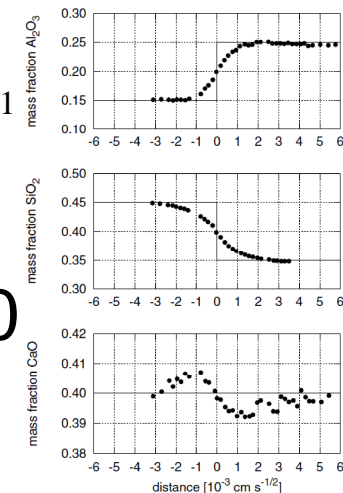
MODE
LITERATU
CHEMAPP

DIFFUSION MATRIX OF $42\text{CaO}-10\text{Al}_2\text{O}_3-48\text{SiO}_2$

- Interdiffusion matrix **D** at 1350°C
Sugawara et al., Met. Trans. 8B, 1977, 605

Uphill diffusion!

$$\begin{bmatrix} D_{\text{CaO}-\text{CaO}} & D_{\text{CaO}-\text{Al}_2\text{O}_3} \\ D_{\text{CaO}-\text{Al}_2\text{O}_3} & D_{\text{Al}_2\text{O}_3-\text{Al}_2\text{O}_3} \end{bmatrix} = \begin{bmatrix} 8.734 & -2.464 \\ -3.948 & 5.977 \end{bmatrix} \cdot 10^{-11}$$



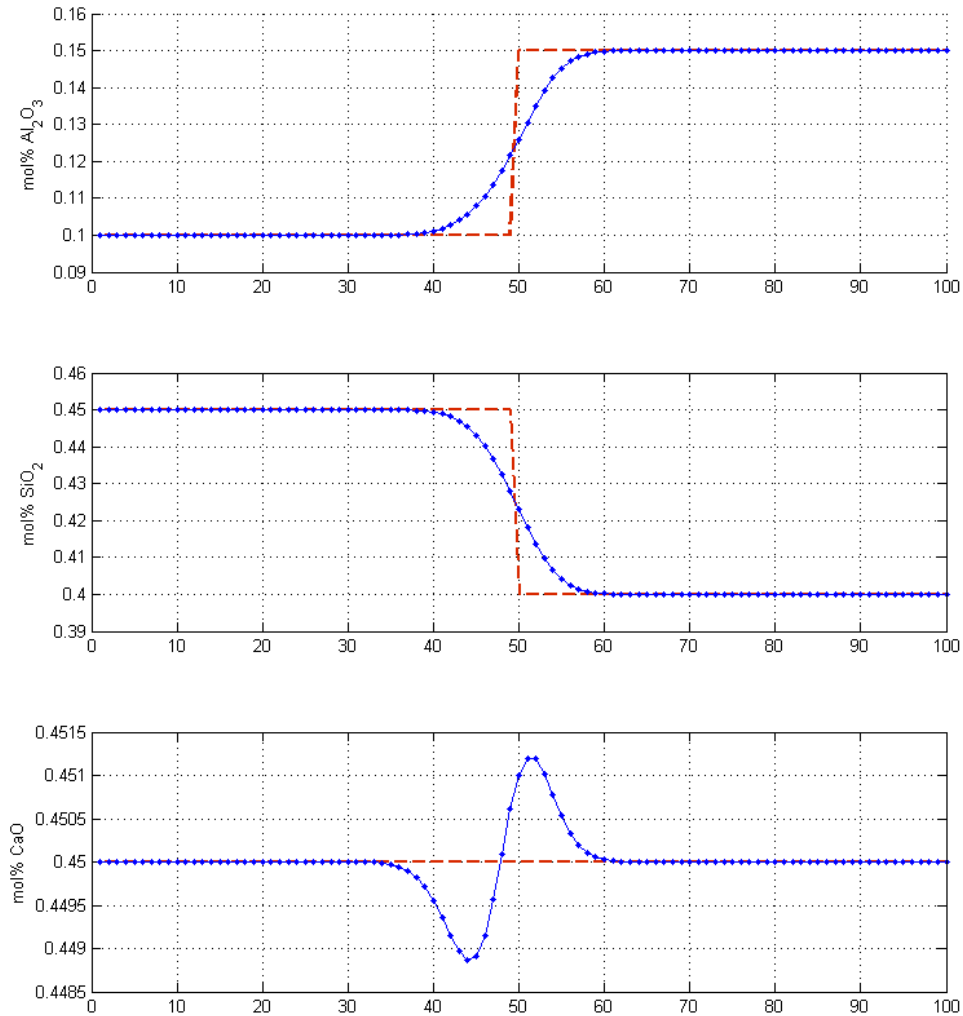
- Thermodynamic factors matrix **G** at 1350
ChemApp

$$\begin{bmatrix} \frac{\partial \tilde{\mu}_1}{\partial x_1} & \frac{\partial \tilde{\mu}_1}{\partial x_2} \\ \frac{\partial \tilde{\mu}_2}{\partial x_1} & \frac{\partial \tilde{\mu}_2}{\partial x_2} \end{bmatrix} = \begin{bmatrix} 1.375 & 1.420 \\ 1.420 & 4.307 \end{bmatrix} \cdot 10^{10}$$

- Resulting **M** matrix for the model can now be calculated

Op naar diffusie in $\text{CaO} / \text{Al}_2\text{O}_3$

SiO_2

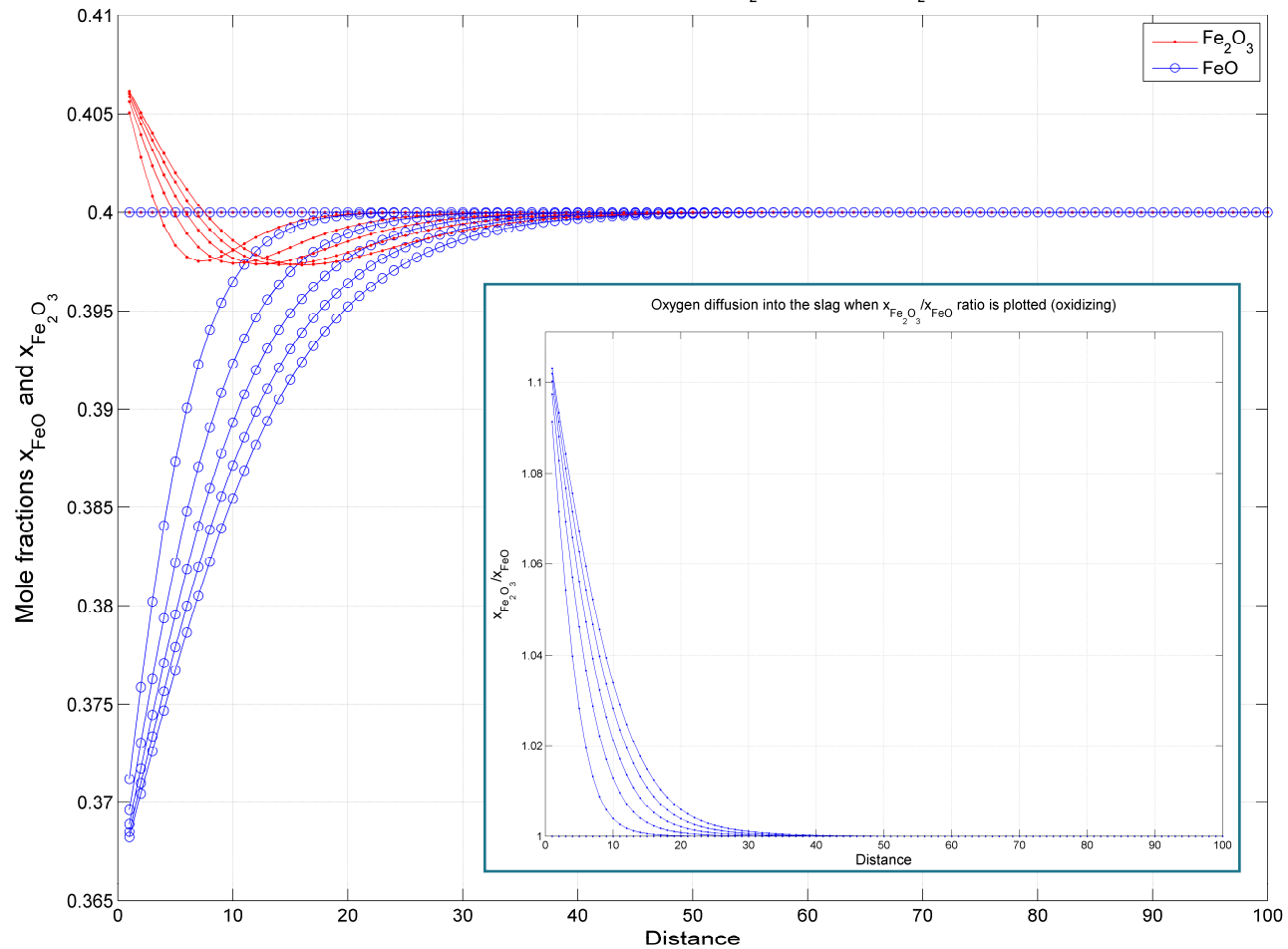


Redox Equilibria of Multivalent cations

- Oxygen dependent system
 - FeO-Fe₂O₃-SiO₂
- Open systems with at least one boundary in contact with O₂ atmosphere (with fixed p_{O_2})
- Assumptions made regarding to redox reactions
 - Redox equilibria are locally always in equilibrium
 - Fe³⁺ / Fe²⁺ is a direct measure for local oxygen potential
 - O₂ can only diffuse into the slag by changing the local multivalent composition
- Special boundary condition to preserve Fe but not O

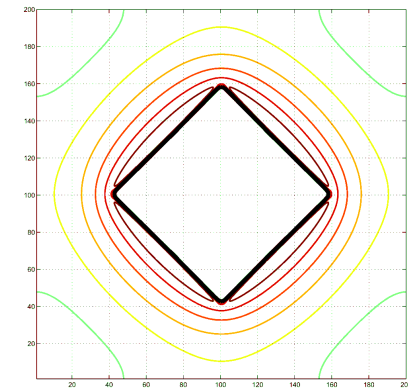
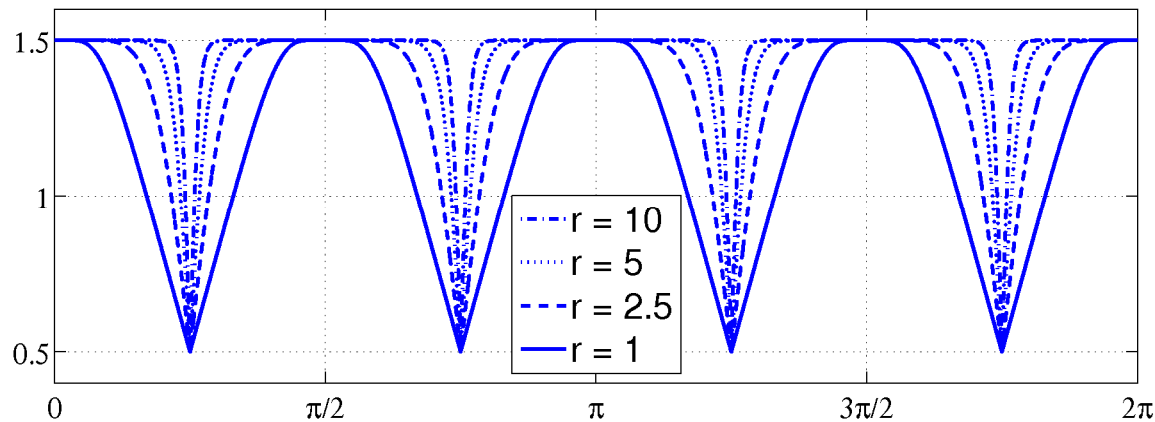
DIFFUSION OF Fe_2O_3 AND FeO (1500°C)

Oxidation of $\text{FeO-Fe}_2\text{O}_3\text{-SiO}_2$ with $p_{\text{O}_2} = 0.5$ while $p_{\text{O}_2, \text{init}} = 0.296$



Faceted growth of minerals

- Conditions for a faceted interface:
 - ▣ Interface controlled growth (diffusion is faster)
 - ▣ Interface mobility is heavily dependent on orientation



- *Tanh* type function has physical meaning (Burton-Cabrera-Frank)

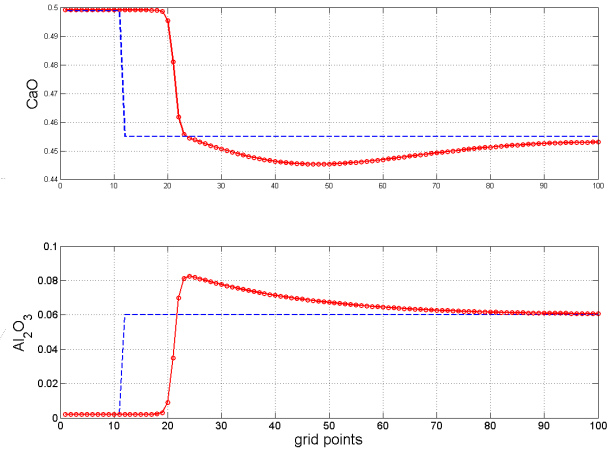
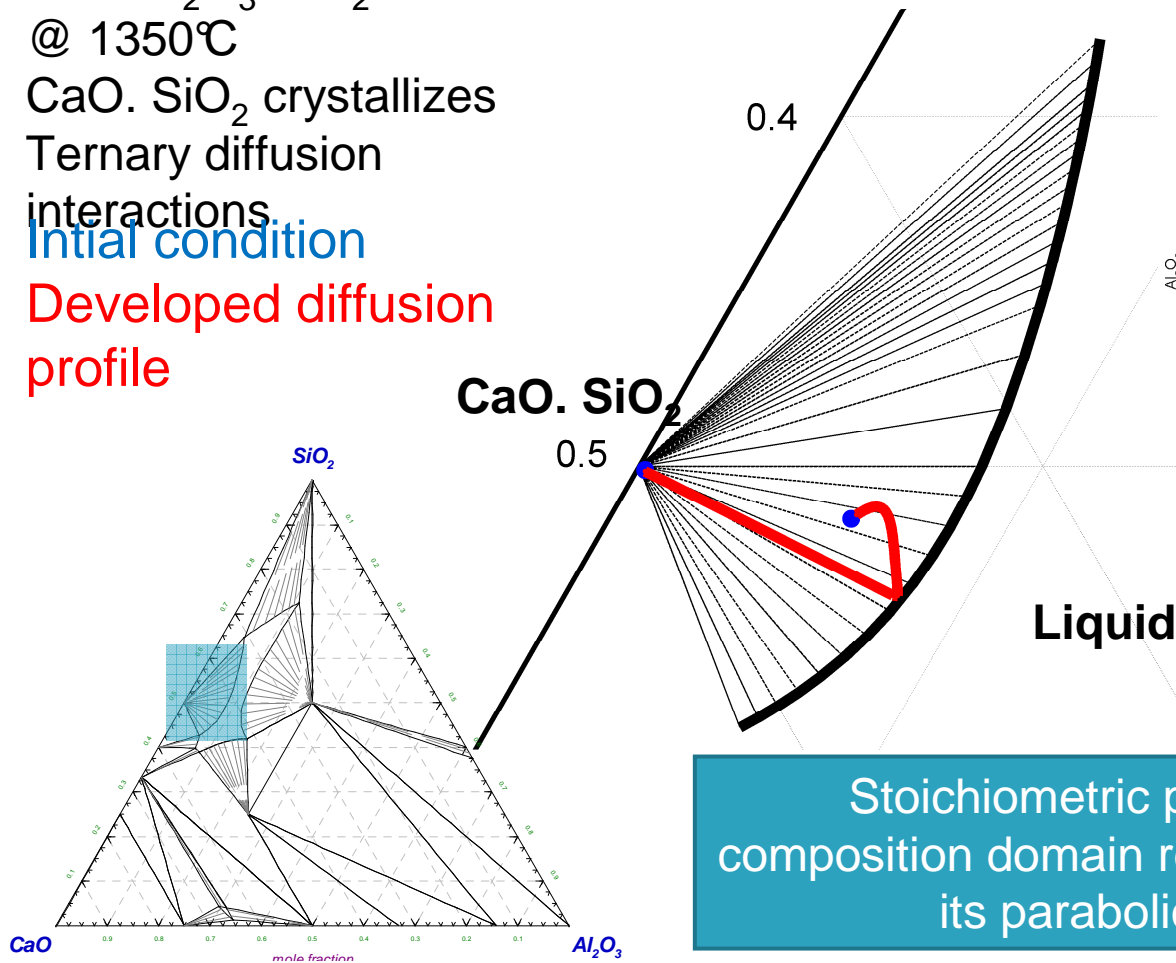
Uehara T, Sekerka RF, Journal of Crystal Growth 254, 2003

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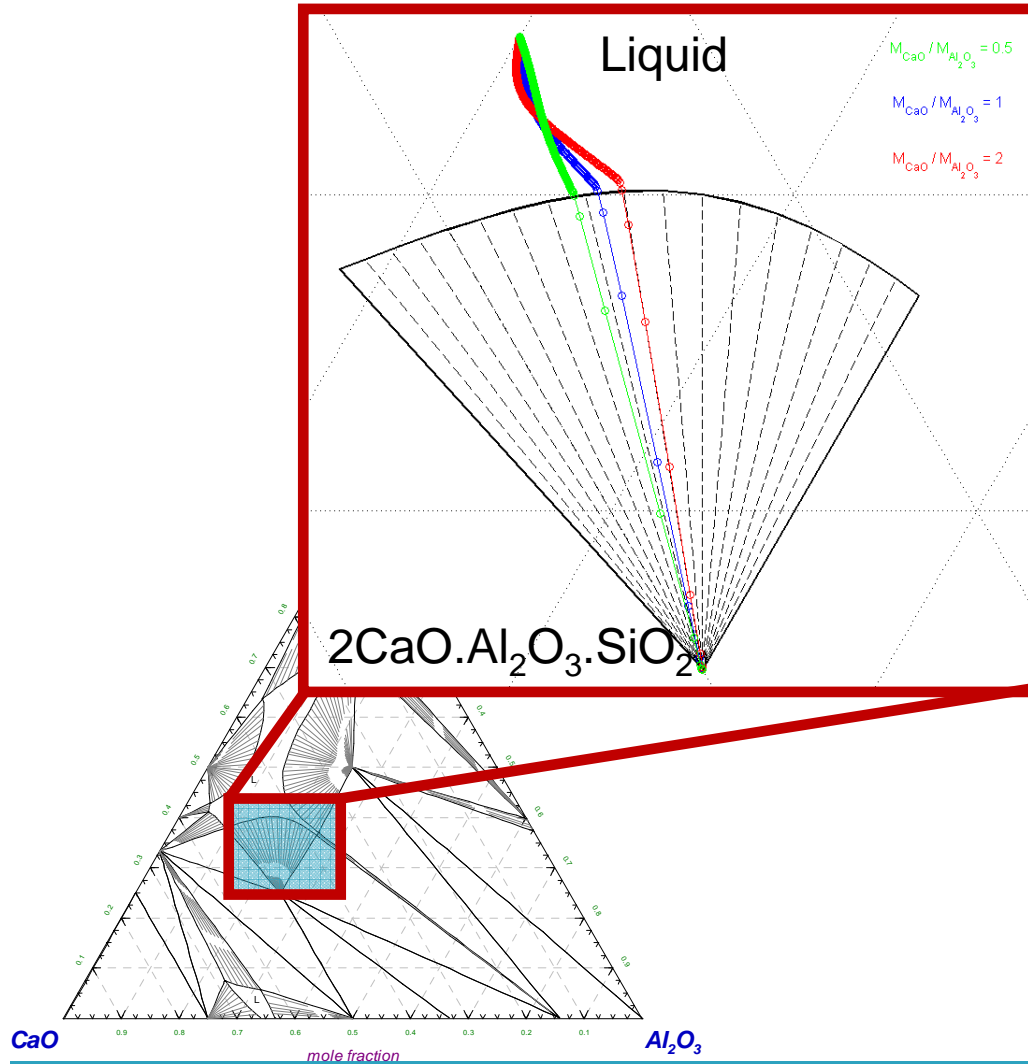
Isothermal mineral crystallization

CaO-Al₂O₃-SiO₂
 @ 1350°C
 CaO. SiO₂ crystallizes
 Ternary diffusion
 interactions.
 Initial condition
 Developed diffusion
 profile

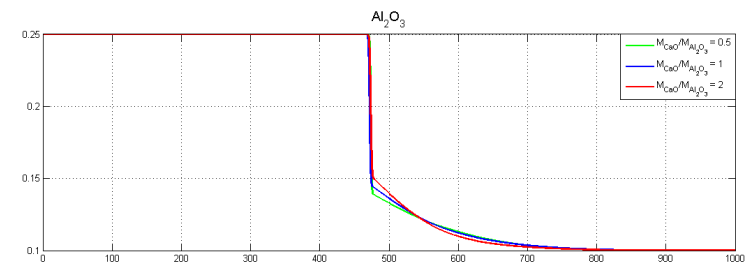
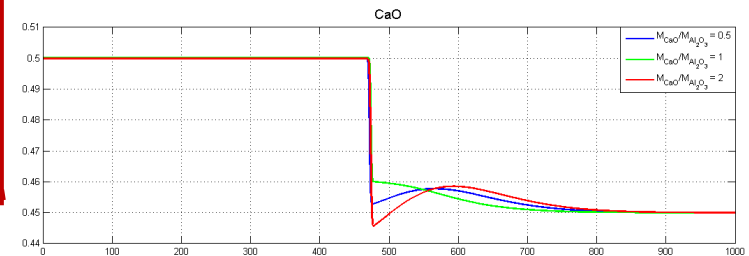


Stoichiometric phase at boundary of composition domain requires careful selection of its parabolic approximation.

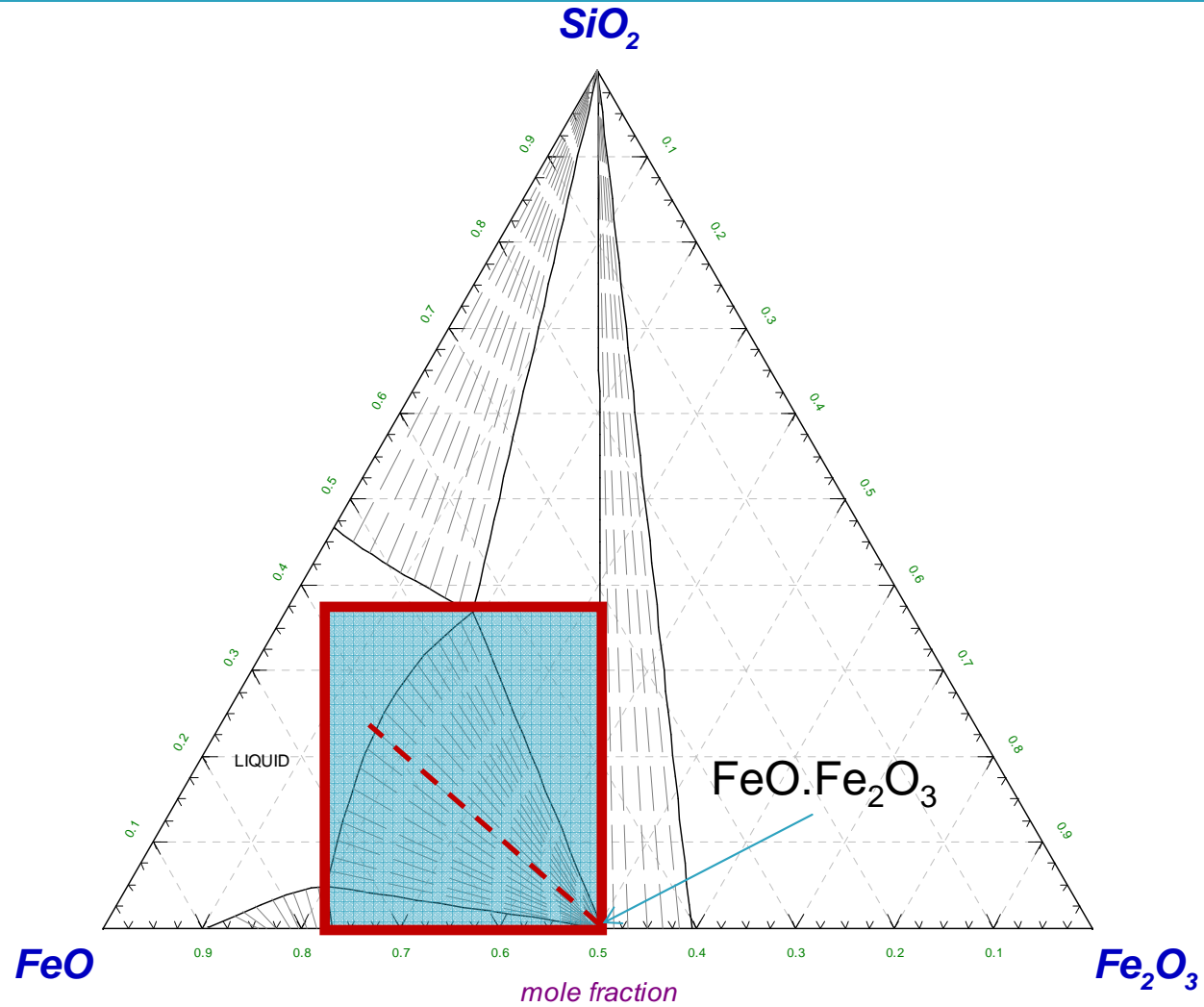
Ternary diffusion paths in slags



CaO-Al₂O₃-SiO₂
 @ 1400°C
 Liquid and
 2CaO·Al₂O₃·SiO₂
**Different tie-line
 selection**

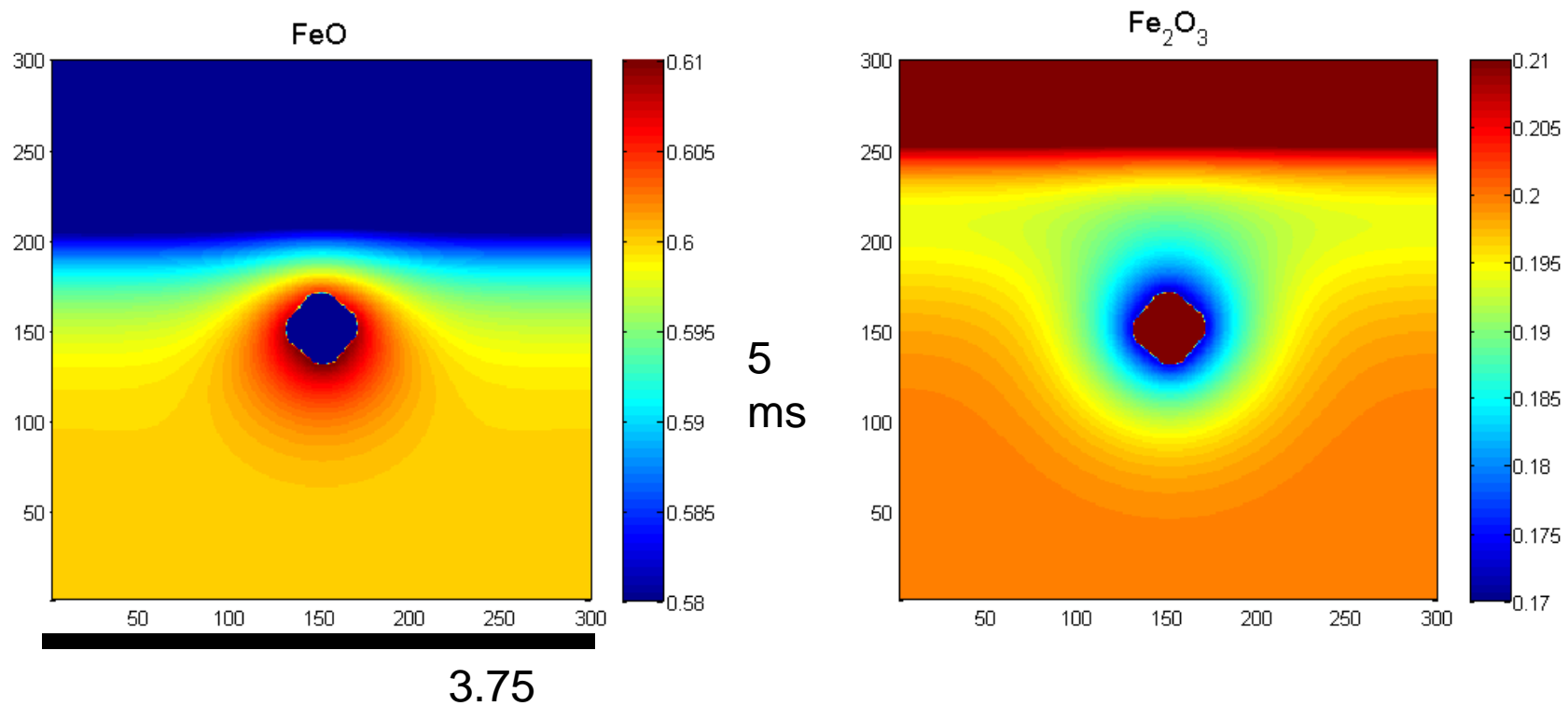


FeO-Fe₂O₃-SiO₂ system at 1400°C



Open boundary in CO / CO_2 / SiO_2

- Initial slag is in equilibrium with $p_{\text{O}_2} = 2.4\text{E-}5$
- Upper boundary has $p_{\text{O}_2} = 1.5\text{E-}3$



Conclusions

- Phase field model linked with FACT database
 - ▣ Gibbs energies and diffusion potentials are retrieved
 - ▣ Stoichiometric phases → parabolic Gibbs energies
 - ▣ Faceted growth with cusp function in mobility
- Case studies of simulations
 - ▣ Mineral growth and diffusion path calculations
 - Stoichiometric phase in contact with liquid
 - ▣ Mineral growing with varying oxygen potential
 - Two competing diffusion fields