



Fachbereich 11

Institut für Werkstofftechnik  
Lehrstuhl für Materialkunde und Werkstoffprüfung  
Prof. Dr.-Ing. H.-J. Christ



# An Extension of the Data-file for the System Co-Re-Cr-C-O: Sources and Restrictions of the Applicability

B. Gorr and H.-J. Christ



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## Content

- ✓ Introduction/Motivation
- ✓ Theoretical Background
- ✓ Development of the database
- ✓ Perspectives/Conclusions



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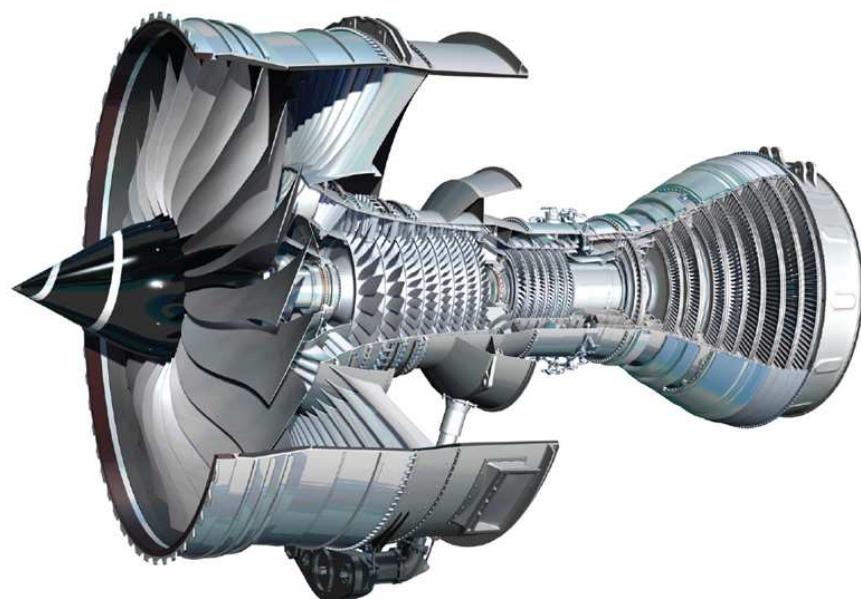
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## Content

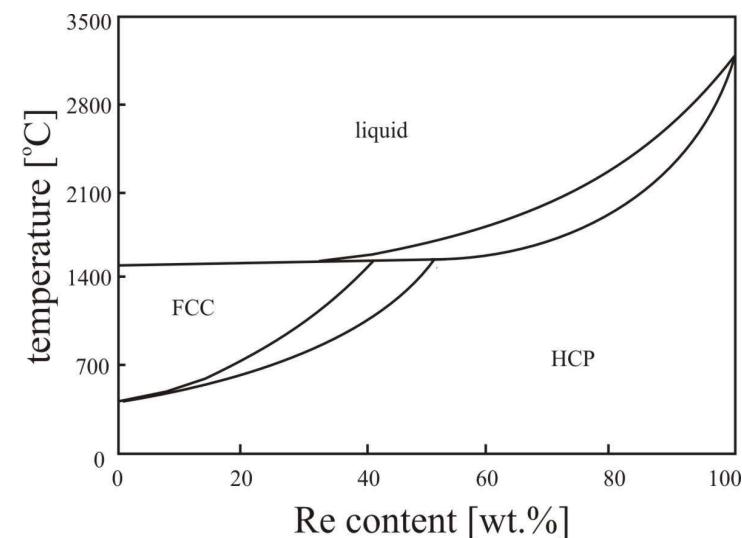
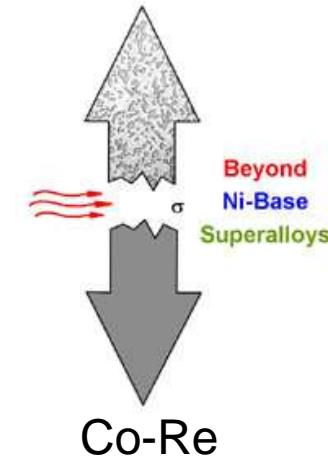
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# Introduction



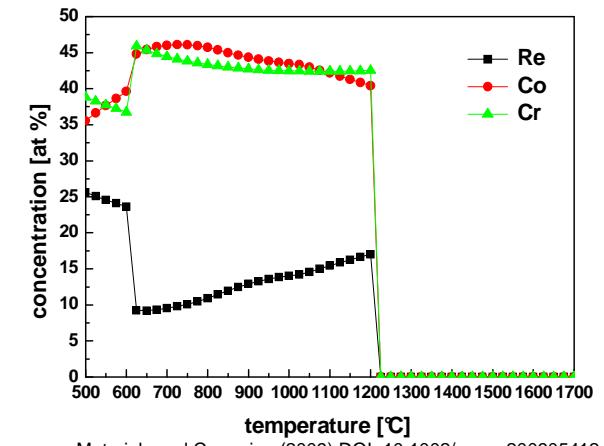
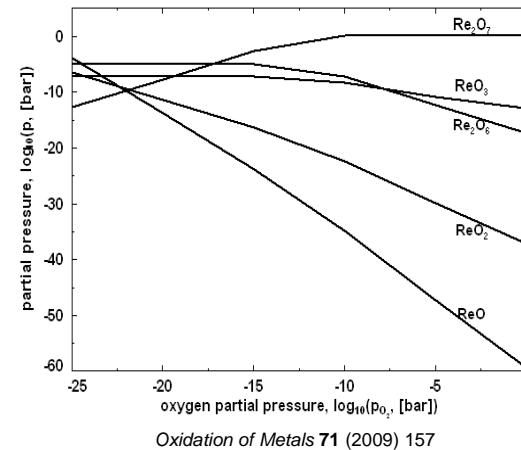
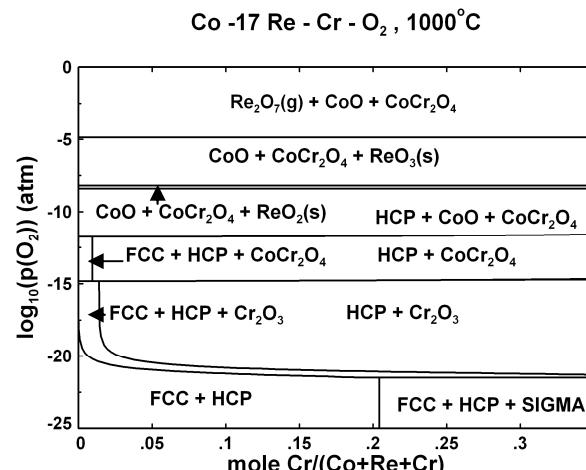
Jet Engine Trent XWB (Rolls-Royce)

Co-Re-based Alloys



## Motivation

- Previous history: ordering of the data-file Co-Re-Cr-C-O by GTT-Technologies



- Current task – addition of Si to the existing data-file
- Strategy:
  - understanding of the thermodynamic basics
  - understanding of the main modelling principles
  - comprehension of the data-file construction
  - literature research



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# Theoretical Background

Elements and stoichiometric compounds

$$C_p = -C - 2DT - 2ET^{-2} - 6FT^2$$

$$H(T) = H(T_0) + \int_{T_0}^T C_p dT = A - CT - DT^2 + 2ET^{-1} - 2FT^3$$

$$S(T) = S(T_0) + \int_{T_0}^T \frac{C_p}{T} dT = -B - C(1 + \ln(T)) - 2DT + ET^{-2} - 3FT^2$$

$$G = H - TS \quad (\text{Gibbs-Helmholz})$$

$$G(T) = A + BT + CT \ln T + DT^2 + FT^3 + ET^{-1}$$

Regular solution (liquid phases)      Phases with sublattices (bcc,fcc,..)

$$^{ex}G^\Phi = x_A x_B \sum_{v=0}^n v L(T) \cdot (x_A - x_B)^v.$$

(Redlich-Kister polynomial)



Compound energy formalism

$$G^\Phi = ^{ref}G^\Phi + ^{id}G^\Phi + ^{ex}G^\Phi$$

$$(A, B)_p (B, A)_q$$

## Compound energy formalism

$$G^\Phi(T, x) - H^{SER}(298, 15K) =$$

$$\begin{aligned}
& \stackrel{\circ}{G}_{A:B}^\Phi \cdot (1 - y_B^{'}) y_B^{''} \\
& + \stackrel{\circ}{G}_{A:A}^\Phi \cdot (1 - y_B^{'}) (1 - y_B^{''}) \\
& + \stackrel{\circ}{G}_{B:B}^\Phi \cdot y_B^{' } y_B^{''} \\
& + \stackrel{\circ}{G}_{B:A}^\Phi \cdot y_B^{' } (1 - y_B^{''}) \\
\\
& + RT [ p((1 - y_B^{'}) \ln(1 - y_B^{'}) + y_B^{' } \ln y_B^{'}) \\
& + q((1 - y_B^{''}) \ln(1 - y_B^{''}) + y_B^{'' } \ln y_B^{''}) ] \\
\\
& + \stackrel{\circ}{L}_{A,B:B}^\Phi \cdot (1 - y_B^{'}) y_B^{' } y_B^{''} \\
& + \stackrel{\circ}{L}_{A,B:A}^\Phi \cdot (1 - y_B^{'}) y_B^{' } (1 - y_B^{''}) \\
& + \stackrel{\circ}{L}_{A:B,A}^\Phi \cdot (1 - y_B^{'}) y_B^{'' } (1 - y_B^{''}) \\
& + \stackrel{\circ}{L}_{B:B,A}^\Phi \cdot y_B^{' } y_B^{'' } (1 - y_B^{''}) \\
\\
& + {}^1 L_{A,B:B}^\Phi \cdot (1 - y_B^{'}) y_B^{' } (1 - 2y_B^{'}) y_B^{''} \\
& + {}^1 L_{A,B:A}^\Phi \cdot (1 - y_B^{'}) y_B^{' } (1 - 2y_B^{'}) (1 - y_B^{''}) \\
& + {}^1 L_{A:B,A}^\Phi \cdot (1 - y_B^{'}) y_B^{'' } (1 - y_B^{''}) (1 - 2y_B^{''}) \\
& + {}^1 L_{B:B,A}^\Phi \cdot y_B^{' } y_B^{'' } (1 - y_B^{''}) (1 - 2y_B^{''}) \\
& + ...
\end{aligned}$$

$\left. \right\} ref G^\Phi$   
 $\left. \right\} id G^\Phi$   
 $\left. \right\} ex G^\Phi$



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## Construction of the FactSage data-files

9151b16g.dat - Editor

Datei Bearbeiten Format Ansicht ?

Ar-Al-Cr-Ni-Ti-O See commentary below ! GTT 2.7.2004

7 12 37 5 4 4 4 8 12 4 8 4 4 2 39

Ar Al Cr  
N Ni Ti  
O

39.9480 26.9815 51.9960 14.0067 58.6900 47.8800

15.9994

6 1 2 3 4 5 6  
4 1 2 3 4

GAS  
IDMX  
Cr

4 6 0.0 0.0 1.0 0.0 0.0 0.0 0.0  
800.00000 391905.70 65.023778 -20.786100 0.00000000  
0.00000000 0.00000000 0.0 0.00000000 0.0  
3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0  
1200.0000 391703.80 69.012778 -21.428800 0.82355800E-03  
-.18278500E-06 11071.900  
3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0  
2200.0000 401183.50 10.950778 -13.833600 -.10803500E-02  
-.22069200E-06 -1931730.0  
3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0  
3600.0000 393019.00 -2.4932223 -10.996000 -.44812700E-02  
0.11658000E-06 3710580.0  
3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0  
4800.0000 304527.70 256.69648 -55.864800 0.53938000E-02  
-.28363300E-06 35390400.  
3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0  
6000.0000 853670.90 -1195.0162 115.37800 -.18385300E-01  
0.33669000E-06 -.29543200E+09  
3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0

N2

4 3 0.0 0.0 0.0 2.0 0.0 0.0 0.0  
950.00000 -7501.3500 -18.908500 -25.563800 -.35337200E-02  
0.53620000E-08 -64748.000  
3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0  
3350.0000 -14717.700 34.400600 -32.739800 -.13021400E-02  
0.60194000E-07 1126140.0  
3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0  
6000.0000 -32785.600 100.52000 -40.939000 0.47950800E-03  
-.16666000E-07 9192750.0  
3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0

O2

4 3 0.0 0.0 0.0 0.0 0.0 0.0 2.0  
1000.0000 -6961.7400 -51.006076 -22.272000 -.10197776E-01  
0.13236920E-05 -76730.000



# Construction of the FactSage data-files

HEADER

DATA BLOCK(S) FOR MIXTURE PHASES

- Mixture Phase 1
- Mixture Phase 2
- 
- 
- Mixture Phase n

DATA BLOCK(S) FOR STOICHIOMETRIC CONDENSED PHASES

- Stoichiometric Condensed Phase 1
- Stoichiometric Condensed Phase 2
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- 
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COMMENTARY BLOCK

# Construction of the FactSage data-files

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15.9994

6 1 2 3 4 5 6

4 1 2 3 4

6000.0000	853670.90	-1195.0162	115.37800	-.18385300E-01
0.33669000E-06	-.29543200E+09			
3 0.00000000	0.0 0.00000000	0.0 0.00000000	0.0	
N2				
4 3 0.0 0.0 0.0 2.0 0.0 0.0 0.0	-7501.3500	-18.908500	-25.563800	-.35337200E-02
0.53620000E-08	-64748.000			
3 0.00000000	0.0 0.00000000	0.0 0.00000000	0.0	
3350.0000	-14717.700	34.400600	-32.739800	-.13021400E-02
0.60194000E-07	1126140.0			
3 0.00000000	0.0 0.00000000	0.0 0.00000000	0.0	
6000.0000	-32785.600	100.52000	-40.939000	0.47950800E-03
-.16666000E-07	9192750.0			
3 0.00000000	0.0 0.00000000	0.0 0.00000000	0.0	
O2				
4 3 0.0 0.0 0.0 0.0 0.0 0.0 2.0	-6961.7400	-51.006076	-22.272000	-.10197776E-01
0 132369200E-05	-76730.000			

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0.00000000 0.00000000  
3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0  
1200.0000 391703.80 69.012778 -21.428800 0.82355800E-03  
-.18278500E-06 11071.900

3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0  
3350.0000 -14717.700 34.400600 -32.739800 -.13021400E-02  
0.60194000E-07 1126140.0  
3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0  
6000.0000 -32785.600 100.52000 -40.939000 0.47950800E-03  
-.16666000E-07 9192750.0  
3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0  
O2  
4 3 0.0 0.0 0.0 0.0 0.0 2.0  
1000.0000 -6961.7400 -51.006076 -22.272000 -.10197776E-01  
0 132369270E-05 -76730.000

## Construction of the FactSage data-files

9151b16g.dat - Editor

Datei Bearbeiten Format Ansicht ?

7 3 0.0 0.0 0.0 0.0 0.0 1.0 0.0
473715.00 180.30099
1800.0000 23.453600
- .52357102E-02 0.29020700E-05 202914.00
0.00000000
4500.0000 2.2478800
0.10953800E-01 -.66014599E-06 11891000.
0.00000000
10000.0000 26.551601
0.22540100E-02 22106600E-06 16024100E-00

LIQUID

RKMP

AI

4 3 0.0 1.0 0.0 0.0 0.0 0.0 0.0
700.00000 3028.8790 125.25117 -24.367198 -.18846620E-02
-.87766400E-06 74092.000
3 0.79337000E-19 7.0 0.00000000 0.0 0.00000000 0.0
933.47000 -271.21100 211.20658 -38.584430 0.18531982E-01
-.57642270E-05 74092.000
3 0.79337000E-19 7.0 0.00000000 0.0 0.00000000 0.0
2900.0000 -795.99600 177.43018 -31.748192 0.00000000
0.00000000 0.00000000
3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0

4 2 0.0 0.0 0.0 0.0 1.0 0.0 0.0

1728.0000 11235.527 108.45700 -22.096000 -.48407000E-02

0.00000000 0.00000000

3 -.38231800E-20 7.0 0.00000000 0.0 0.00000000 0.0

3000.0000 -9549.7750 268.59800 -43.100000 0.00000000

n nnnnnnnn n nnnnnnnn

## Construction of the FactSage data-files

9151b16g.dat - Editor

Datei Bearbeiten Format Ansicht ?

3	1	2	4	1	-7567.0000	-1.1800000	0.00000000	0.00000000
3	2	3	4	1	-7567.0000	-1.1800000	0.00000000	0.00000000
BCC_A2								
SUBLM								
1.00000 0.400000								
Al:N								
16 1 0.0 1.0 0.0 3.0 0.0 0.0 0.0								
299.15000 0.00000000 0.00000000 0.00000000 0.00000000								
0.00000000 0.00000000								
3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0								
0.000000 0.000000								
Al:Va								
16 3 0.0 1.0 0.0 0.0 0.0 0.0 0.0								
700.00000 2106.8500 132.28004 -24.367198 -.188466								
0.90291000E-07 1689210.0								
3 -.28852600E+33 -9.0 0.00000000 0.0 0.00000000 0.0								
6000.0000 227822.26 524.08000 -111.40850 0.71926200E-03								
-.24999000E-07 13789125.								
3 -.28852600E+33 -9.0 0.00000000 0.0 0.00000000 0.0								
-311.500 -.800000E-02								
Cr:Va								
16 2 0.0 0.0 1.0 0.0 0.0 0.0 0.0								
2180 00000 -.8856 94000 157 48000 -.76 908000 0 18943500E-02								

# Construction of the FactSage data-files

HEADER

## DATA BLOCK(S) FOR MIXTURE PHASES

- Mixture Phase 1
- Mixture Phase 2
- 
- 
- Mixture Phase n

## DATA BLOCK(S) FOR STOICHIOMETRIC CONDENSED PHASES

- Stoichiometric Condensed Phase 1
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- 
- 
- Stoichiometric Condensed Phase n

COMMENTARY BLOCK

## Construction of the FactSage data-files

9151b16g.dat - Editor

Datei Bearbeiten Format Ansicht ?

```
Cr2Ti_LAVES_PHASES
4 1 0.0 0.0 2.0 0.0 0.0 1.0 0.0
299.15000 0.00000000 0.00000000 0.00000000 0.00000000
0.00000000 0.00000000
3 0.00000000 0.0 0.00000000 0.0 0.00000000 0.0

AIN
7 4 0.0 1.0 0.0 1.0 0.0 0.0 0.0
-317984.00 20.150000
500.00000 -56.592800 0.32205901 -.27721500E-03 1363820.0
0.00000000
1300.0000 43.973801 0.11811900E-01 -.50007202E-05 -2010330.0
0.00000000
1900.0000 21.656799 0.23793099E-01 -.53751801E-05 10454100.
0.00000000
3000.0000 55.534199 -.24074300E-02 0.41902800E-06 -7645010.0

Cr2Ni104
7 1 0.0 0.0 2.0 0.0 1.0 0.0 4.0
-1374000.0 120.74600
```

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- Stoichiometric Condensed Phase 1
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- 
- 
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COMMENTARY BLOCK

## Construction of the FactSage data-files

9151b16g.dat - Editor

Date : 07.04.1997  
Originator : KH  
Serial No : 9151B17G.DAT  
Quality Status : B  
ChemSage Vers. : 3.0

Temperatures : Below liquidus of the metallic subsystem  
Compositions : Ni-rich  
Applications : Oxidation and nitride formation

Sources of data

Unary : 945GT, 95Hac (for Ni<sub>3</sub>Al and Ni<sub>3</sub>Ti)  
Binary : 925GT, 95dup (for Ti in solid Ni)

NOTE: The elementary components contained in the set of Stoichiometric Condensed Phases are given to simplify input of the system composition. They are suppressed from the equilibrium calculations by use of the exclamation mark in the names. Do not change the "!".

System components:

1: Ar	2: Al	3: Cr
4: N	5: Ni	6: Ti
7: O		

Phases:

1: GAS	2: LIQUID	3: AL <sub>3</sub> Ni <sub>2</sub>
4: Ti <sub>3</sub> Al	5: TIAL	6: BCC_A2
7: FCC_A1	8: ALNI_B2	9: HCP_A3
10: (Cr,Ti)N	11: (Cr,Ni)2N:2	12: M <sub>2</sub> O <sub>3</sub> _alpha
13: Cr <sub>12</sub> .8Ni <sub>7</sub> .2N4_PI	14: Al <sub>1.8667</sub> Cr <sub>1.333</sub> _A	15: Al <sub>1.8</sub> Cr <sub>2</sub> _AL4CR
16: Al <sub>1.616</sub> Cr <sub>3.84</sub>	17: Al <sub>1.692</sub> Cr <sub>3.08</sub> _h	18: Al <sub>1.692</sub> Cr <sub>3.08</sub> _l
19: Al <sub>1.333</sub> Cr <sub>6.67</sub>	20: Al <sub>1.769</sub> Al <sub>0.077</sub> Cr <sub>1.154</sub>	21: Al <sub>1.75</sub> Ni <sub>1.25</sub> _AL3NI
22: Al <sub>1.68</sub> Ti <sub>1.32</sub>	23: Al <sub>1.667</sub> Ti <sub>1.333</sub>	24: Al <sub>1.75</sub> Ti <sub>1.25</sub>
25: Ti <sub>2</sub> N_Ti <sub>2</sub> N	26: Cr <sub>2</sub> Ti_LAVES_PHASE	27: Al <sub>1</sub> N
28: Al <sub>1</sub> Ni <sub>3</sub>	29: Al <sub>1</sub> Cr <sub>3</sub>	30: Al <sub>1</sub> O <sub>3</sub>

## Construction of the FactSage data-files

$$G(T) = A + BT + CT \ln T + DT^2 + FT^3 + ET^{-1}$$

System Re-Co-Cr-O-C									
5	8	20	4	6	6	6	4	2	6 30
Re				Co					Cr
O				C					
186.207000				58.933200					51.996100
15.999400				12.011000					
6	1	2	3	4	5	6			
6	1	2	3	4	5	6			
gas_ideal									
IDMX									
O2									
	4	5	0.0	0.0	0.0	2.0	0.0		
$\Delta T_1$	900.00000	-6960.6927		-51.183147		-22.258620		-10238670E-01	
	0.13399470E-05	-76749.550							
$\Delta T_2$	3700.0000	-13136.017		24.743297		-33.557260		-12348985E-02	
	0.16694333E-07	539886.00							
$\Delta T_3$	9600.0000	14154.646		-51.485458		-24.479780		-26347590E-02	
	0.60154433E-07	-15120935.							
$\Delta T_4$	18500.000	-314316.63		515.06804		-87.561430		0.25787245E-02	
	-.18787650E-07	0.29052515E+09							
$\Delta T_5$	20000.000	-108797.18		288.48302		-63.737000		0.14375000E-02	
	-.90000000E-08	0.25153895							
	1 0.00000000	0.00							

## Sources of thermochemical data-files

### 1). SGTE, SGUN Pure Substances and Solution databases



## Compound.txt - Editor

Datei Bearbeiten Format Ansicht ?

si Units: P(bar) Energy(J)  
Name: si

$$G(T) = A + BT + CT \ln T + DT^2 + FT^3 + ET^{-1}$$

G(T) J/mol - 1 bar

	G(T)	G(T)	G(T)	T(K)
S1	1 - 8162.60806			
S1	1 + 176667.000	T <sup>A-1</sup>	+ 137.236860 T - 1.912904000E-03 T <sup>A 2</sup>	298 - 1687
S1	2 - 9457.63976		- 3.552000000E-09 T <sup>A 3</sup> - 22.8317530 T ln(T)	298 - 1687
S1	2 - 27.1960000	T ln(T)	+ 167.281369 T - 4.203690000E+30 T <sup>A-9</sup>	1687 - 3600
S2	3 38837.3909		+ 114.736860 T - 1.912904000E-03 T <sup>A 2</sup>	298 - 1687
S2	3 + 176667.000	T <sup>A-1</sup>	- 3.552000000E-09 T <sup>A 3</sup> - 22.8317530 T ln(T)	298 - 1687
S2	4 37542.3592		+ 144.781369 T - 4.203690000E+30 T <sup>A-9</sup>	1687 - 3600
S2	4 - 27.1960000	T ln(T)	+ 116.859860 T - 1.912904000E-03 T <sup>A 2</sup>	1687 - 3600
S3	5 42045.3909		- 3.552000000E-09 T <sup>A 3</sup> - 22.8317530 T ln(T)	298 - 1687
S3	5 + 176667.000	T <sup>A-1</sup>	+ 146.904369 T - 4.203690000E+30 T <sup>A-9</sup>	298 - 1687
S3	6 40750.3592		+ 116.859860 T - 1.912904000E-03 T <sup>A 2</sup>	1687 - 3600
S3	6 - 27.1960000	T ln(T)	- 3.552000000E-09 T <sup>A 3</sup> - 22.8317530 T ln(T)	1687 - 3600
S4	7 39116.3909		+ 146.904369 T - 4.203690000E+30 T <sup>A-9</sup>	298 - 1687
S4	7 + 176667.000	T <sup>A-1</sup>	+ 116.859860 T - 1.912904000E-03 T <sup>A 2</sup>	298 - 1687
S4	8 37821.3592		- 3.552000000E-09 T <sup>A 3</sup> - 22.8317530 T ln(T)	1687 - 3600
S4	8 - 27.1960000	T ln(T)	+ 146.904369 T - 4.203690000E+30 T <sup>A-9</sup>	1687 - 3600
S5	9 42837.3909		+ 115.436860 T - 1.912904000E-03 T <sup>A 2</sup>	298 - 1687
S5	9 + 176667.000	T <sup>A-1</sup>	- 3.552000000E-09 T <sup>A 3</sup> - 22.8317530 T ln(T)	298 - 1687
S5	10 41542.3592		+ 145.481369 T - 4.203690000E+30 T <sup>A-9</sup>	1687 - 3600
S5	10 - 27.1960000	T ln(T)	+ 116.436860 T - 1.912904000E-03 T <sup>A 2</sup>	1687 - 3600
S6	11 41037.3909		- 3.552000000E-09 T <sup>A 3</sup> - 22.8317530 T ln(T)	298 - 1687
S6	11 + 176667.000	T <sup>A-1</sup>	+ 146.481369 T - 4.203690000E+30 T <sup>A-9</sup>	298 - 1687
S6	12 39742.3592		+ 116.436860 T - 1.912904000E-03 T <sup>A 2</sup>	1687 - 3600
S6	12 - 27.1960000	T ln(T)	- 3.552000000E-09 T <sup>A 3</sup> - 22.8317530 T ln(T)	1687 - 3600
S7	13 - 038.3909		+ 146.481369 T - 4.203690000E+30 T <sup>A-9</sup>	298 - 1687
S7	14 A 176667.000	T <sup>A-1</sup>	+ 116.436860 T - 1.912904000E-03 T <sup>A 2</sup>	298 - 1687
S7	14 - 743.3592		- 3.552000000E-09 T <sup>A 3</sup> - 22.8317530 T ln(T)	1687 - 3600
S7	14 - 27.1960000	T ln(T)	+ 46.481369 T - 4.203690000E+30 T <sup>A-9</sup>	1687 - 3600
L	15 427533.7506		+ 107.137420 T - 1.912904000E-03 T <sup>A 2</sup>	298 - 1687
L	15 + 176667.000	T <sup>A-1</sup>	- 3.552000000E-09 T <sup>A 3</sup> + 2.093070000E-21 T <sup>A 7</sup>	298 - 1687
L	15 - 22.8317530	T ln(T)	+ 137.722299 T - 27.1960000 T ln(T)	298 - 1687
L	16 40370.5233			1687 - 3600



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## Sources of thermochemical data-files

- 1). SGTE, SGUN Pure Substances and Solution databases (thermochemical data for pure substances in the system Co-Re-Cr-O-C-Si)
- 2). Ready-made data-files (thermochemical data for compounds, solutions, and interaction coefficients between constituents in the system Co-Cr-O-C-Si, without Re!)
  - FRAN (Co, Cr, Si, C O)
  - MoSi (Si, Cr, O)
- 4). Phase diagrams
- 3). Literature (Re,Si)



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# Sources of thermochemical data-files



Intermetallics 9 (2001) 1063–1068

Intermetallics

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## Thermodynamic analysis of the Re–Si system

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### Abstract

The Re–Si system is assessed thermodynamically, using the CALPHAD method. The calculated phase diagram and thermodynamic properties are in good agreement with available experimental data. Calculated enthalpies and entropies of fusion are compared with available data for other transition metal silicides, against melting points, showing good agreement with the general trends. This is a useful approach for thermodynamic assessment of alloy systems, where experimentally measured thermodynamic data are limited. The stability of the amorphous phase in this system has also been discussed. © 2001 Elsevier Science Ltd. All rights reserved.

**Keywords:** A. Silicides, various; B. Phase diagram; B. Thermodynamic and thermochemical properties

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### 1. Introduction

this phase is  $\text{Re}_2\text{Si}$  [4]. The latest version of the Re–Si phase diagram [5,6] is redrawn and shown in Fig. 1. The

## Sources of thermochemical data-files

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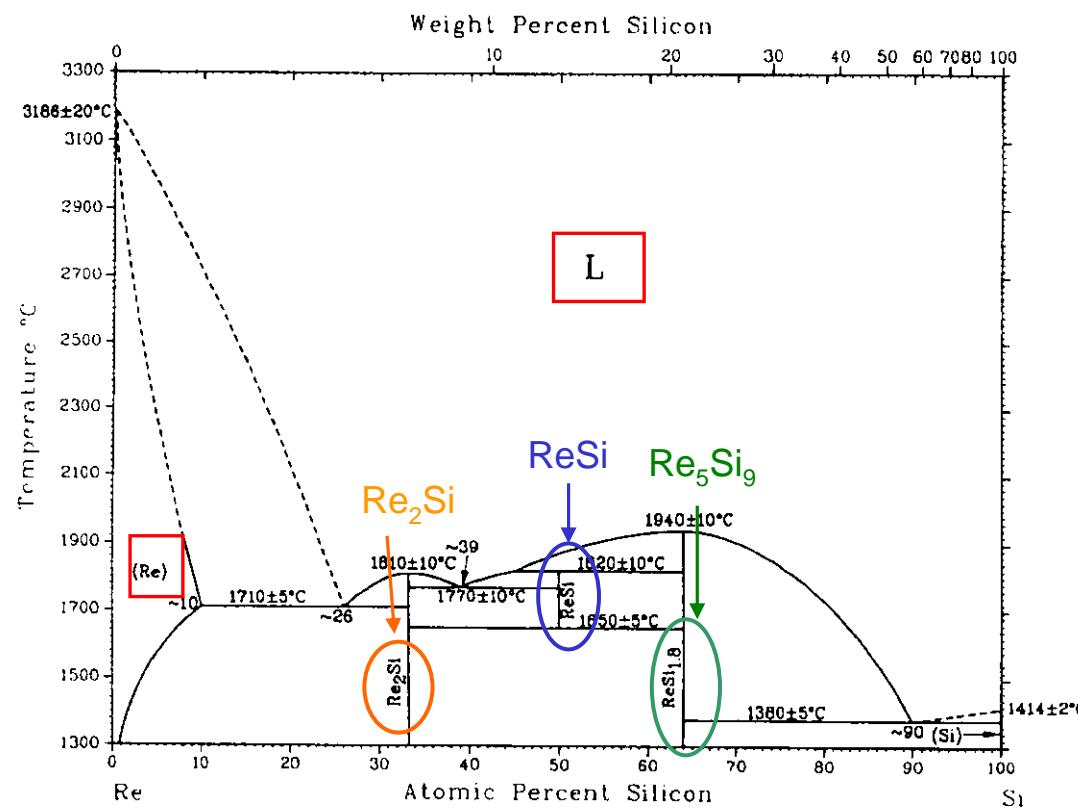
G. Shao *Intermetallics* 9 (2001) 1063-1068

Fig. 1. Experimentally determined Re-Si phase diagram redrawn from Refs. [5,6].

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shown in Fig 7 in dotted lines, indicating the difficulty in reaching stable metastable equilibrium, as extensive diffusion has to be involved. This explains why other stable phases such as Si and Re<sub>2</sub>Si could not coexist with the amorphous phase in the indicated composition range. Local equilibrium at the Am/Re<sub>2</sub>Si<sub>x</sub> interface is unlikely to be achieved, as the metastable equilibrium Re content in the amorphous Si(Re) is very low as well.

#### 4. Conclusions

The Re-Si system is assessed thermodynamically. The calculated phase diagram and thermodynamic properties are in good agreement with available experimental data. Calculated enthalpies as well as entropies, of fusion, are compared with reported values of various transition metal silicides, showing good agreement with the general trends. The approach of this work is useful for thermodynamic assessment of alloy systems, with limited experimentally measured data. The stability of the amorphous phase in this system has also been discussed.

#### Appendix

Summary of the optimised thermodynamic parameters for the Re-Si systems. Values are given in SI units and correspond to one mole of atoms.

Phase liquid  
description: (Re, Si)

$$L_{\text{Re}, \text{Si}}^{\text{liq}} = -96700 - 45000(x_{\text{Re}} - x_{\text{Si}}) - 60000(x_{\text{Re}} - x_{\text{Si}})^2$$

Data for amorphization stabilization in this work are:

$$\begin{aligned} T_g^{\text{Re}} &= 865 \text{ K} & \alpha^{\text{Re}} &= 2.839 \\ T_g^{\text{Si}} &= 1266 \text{ K} & \alpha^{\text{Si}} &= 3.59 \\ \Delta_0^{\text{Re}, \text{Si}} &= -2.5 & \Delta_1^{\text{Re}, \text{Si}} &= -2.2 \end{aligned}$$

Phase hep  
description: (Re, Si)

$$L_{\text{Re}, \text{Si}}^{\text{hep}} = -48000 - 3000(x_{\text{Re}} - x_{\text{Si}})$$

Phase Re<sub>2</sub>Si  
description: (Re)<sub>0.667</sub>(Si)<sub>0.333</sub>

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$$G_{\text{Re}, \text{Si}} = 0.667 G_{\text{Re}}^0 - 0.333 G_{\text{Si}}^0 = -22700 - 1.86 T$$

Phase ReSi  
description: (Re)<sub>0.5</sub>(Si)<sub>0.5</sub>

$$G_{\text{ReSi}} = 0.5 G_{\text{Re}}^0 - 0.5 G_{\text{Si}}^0 = -21480 - 5 T$$

Phase ReSi<sub>1.8</sub>  
description: (Re)<sub>0.357</sub>(Si)<sub>0.643</sub>

$$G_{\text{ReSi}_{1.8}} = 0.357 G_{\text{Re}}^0 - 0.643 G_{\text{Si}}^0 = -31200 - 2.1 T$$

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### Phase hep

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description: (Re)<sub>0.667</sub>(Si)<sub>0.333</sub>

$$G_{\text{Re}_2\text{Si}} = 0.667 G_{\text{Re}}^0 - 0.333 G_{\text{Si}}^0 = -22700 - 1.86 T$$

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Phase ReSi<sub>1.8</sub>  
description: (Re)<sub>0.357</sub>(Si)<sub>0.643</sub>

$$G_{\text{ReSi}_{1.8}} = 0.357 G_{\text{Re}}^0 - 0.643 G_{\text{Si}}^0 = -31200 - 2.1 T$$

# Sources of thermochemical data-files

## Liquid

Phase liquid

description: (Re, Si)

$$L_{\text{Re}, \text{Si}}^{\text{liq}} = -96700 - 45000(x_{\text{Re}} - x_{\text{Si}}) - 60000(x_{\text{Re}} - x_{\text{Si}})^2$$

$${}^{ex}G^{\Phi} = x_A x_B \sum_{\nu=0}^n {}^{\nu}L(T) \cdot (x_A - x_B)^{\nu}.$$

## Re<sub>2</sub>Si

Phase Re<sub>2</sub>Si

description: (Re)<sub>0.667</sub>(Si)<sub>0.333</sub>

$$G_{\text{Re}_2\text{Si}} = 0.667 G_{\text{Re}}^0 + 0.333 G_{\text{Si}}^0 = -22700 + 1.86 T$$

$$G = H - TS$$

$$A_{\text{Re}_2\text{Si}} = 2A_{\Delta T_1}^{\text{Re}} + 1A_{\Delta T_1}^{\text{Si}} + H^{\text{Re}_2\text{Si}} = \\ 2(-7695,27) + 1(8162) + 3(-22700) = -91653$$

2				
4	5	3		
-96700.000	0.00000000	0.00000000	0.00000000	
0.00000000	0.00000000			
-45000.000	0.00000000	0.00000000	0.00000000	
0.00000000	0.00000000			
-60000.000	0.00000000	0.00000000	0.00000000	
0.00000000	0.00000000			
0				

Re2Si_re2si(s)						
4	7	2.0	0.0	0.0	1.0	0.0
1200.0000	-91653.167				388.50004	-71.527753
0.38208400E-06	242497.00					.69830040E-02
1687.0000	-107814.60				520.99171	-90.003753
-56722200E-06	2929207.0					0.25783960E-02
2400.0000	-109109.63				551.03622	-94.368000
-56367000E-06	2752540.0					0.44913000E-02

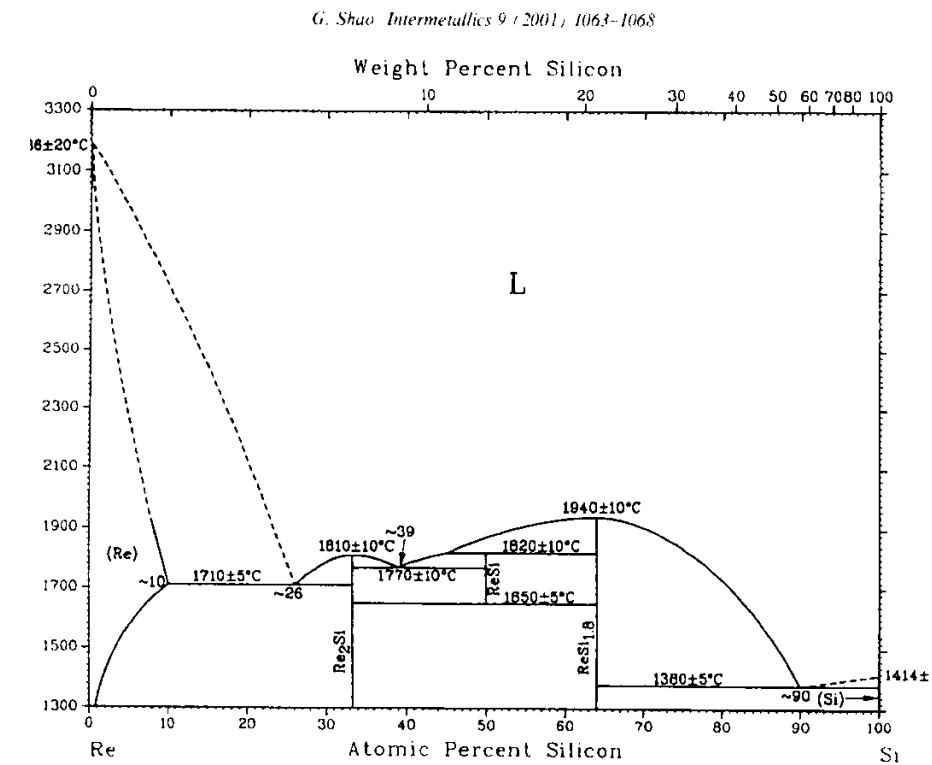
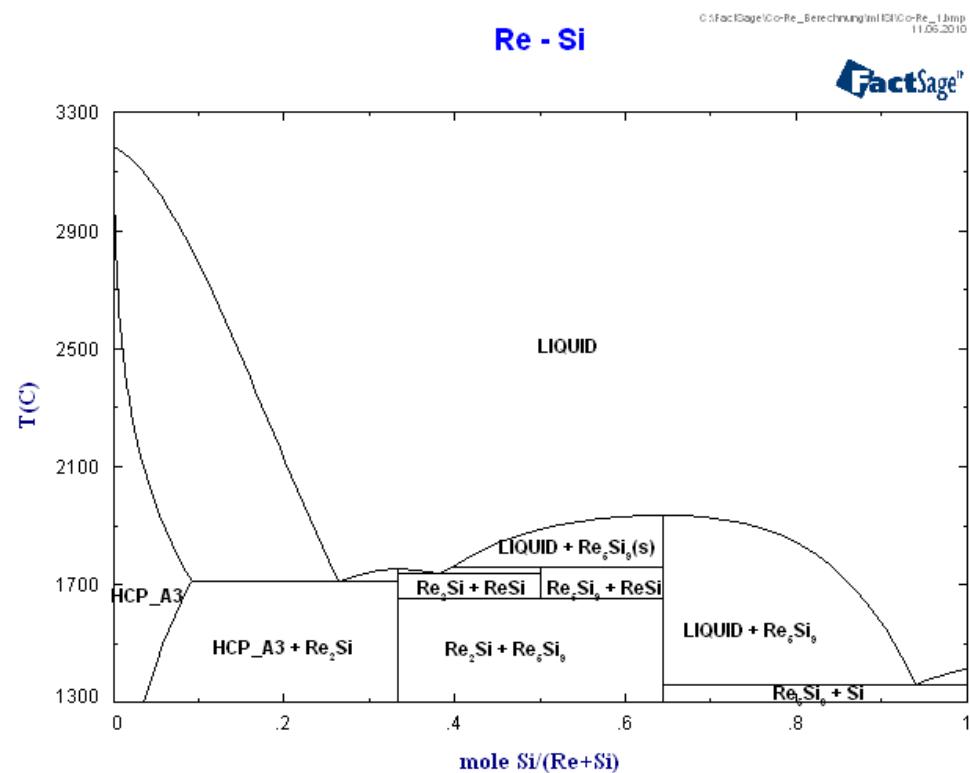


Fig. 1. Experimentally determined Re-Si phase diagram redrawn from Refs. [5,6].



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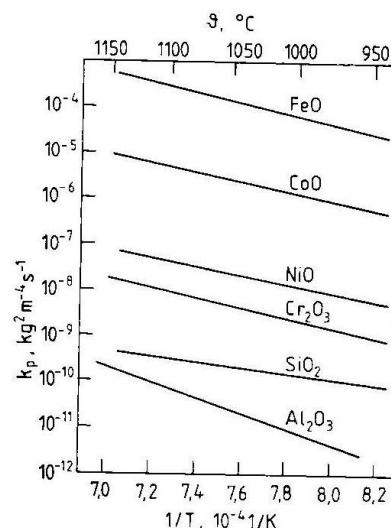
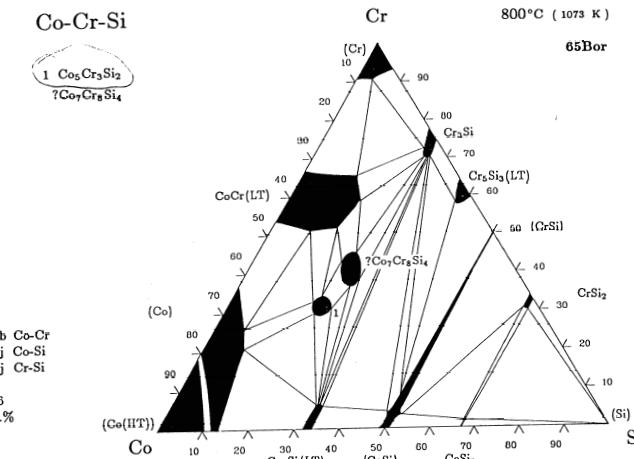
## Content

- ✓ Introduction/Motivation
- ✓ Theoretical Background
- ✓ Development of the database
- ✓ Perspectives/Conclusions

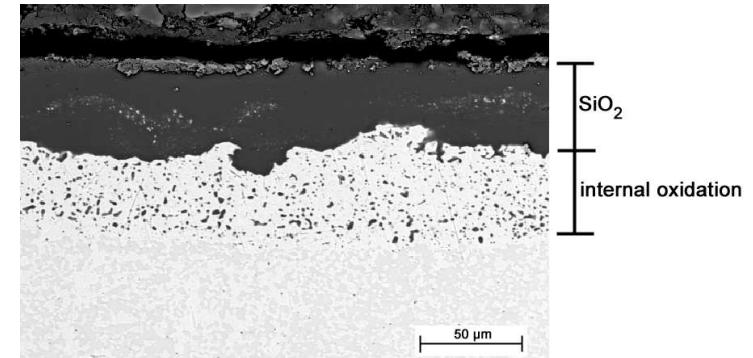
# Perspectives: An Extension of the Data-file

## Goals/Perspectives

- Modelling of further phases (primarily in the Co-Cr-Si system)
- Addition of Al to the Co-Re-Cr-C-O-Si data-file
- Addition of B and N to the Co-Re-Cr-C-O-Si data-file
- Literature research
- Critical analysis of calculations



R. Bürgel: Hochtemperaturwerkstofftechnik,  
Vieweg, Braunschweig, 1998



Mo-9Si-8B, air, 1300°C, 72h

S. Burk et al., Oxidation of Metals, 73 (2010) 163

## Conclusions

- There is an urgent need for the development of alloys for temperatures beyond the application range of Ni-based superalloys. Experimental Co-Re-based alloys are potential high-temperature alloys of the new generation.
- Theoretical background of equilibria for stoichiometric reactions and complex systems was presented.
- Models for pure substances and solution phases as well as a basic construction of the FactSage data-files and main sources of the thermochemical data were discussed.
- Perspectives and goals in the further extension of the existing data-files were determined. Al and B should be added to the data-file.

*Thank you for your attention!*