

10th Annual GTT-Technologies Workshop
Herzogenrath, Germany
June 4-6, 2008

Advances in Modelling Salt Stock Deposition of Nuclear Wastes

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GRS, Braunschweig, Germany

Content

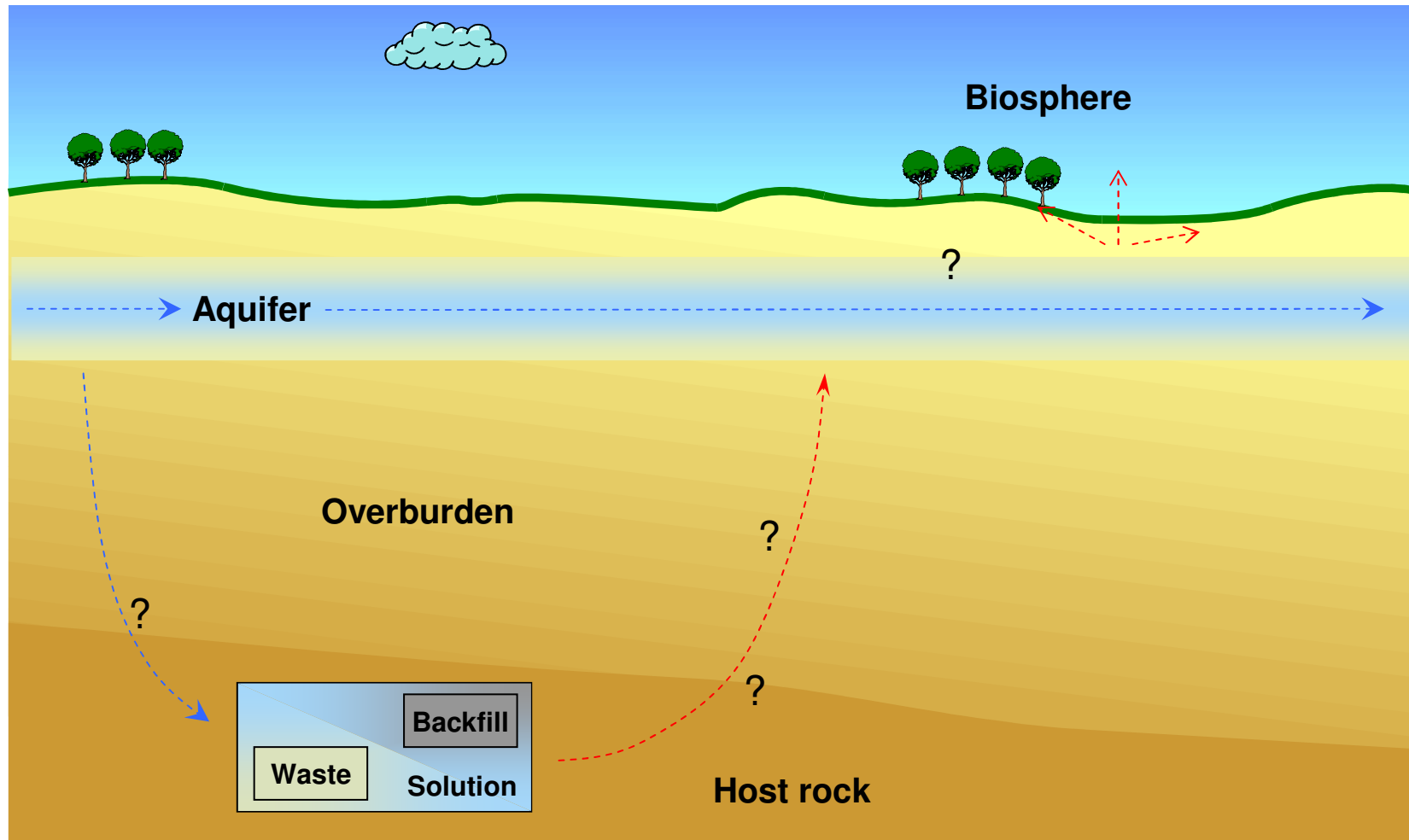


- Introduction
- Reactive Transport Modelling
- Reactions and Database
- Application – $\text{UO}_2(\text{s})$ dissolution and transport
- Outlook

Content



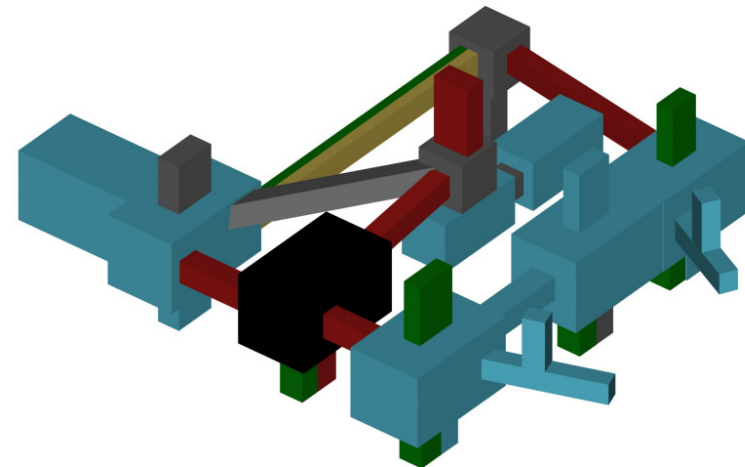
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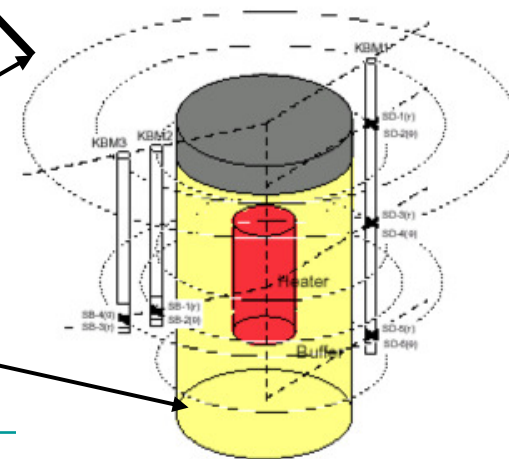
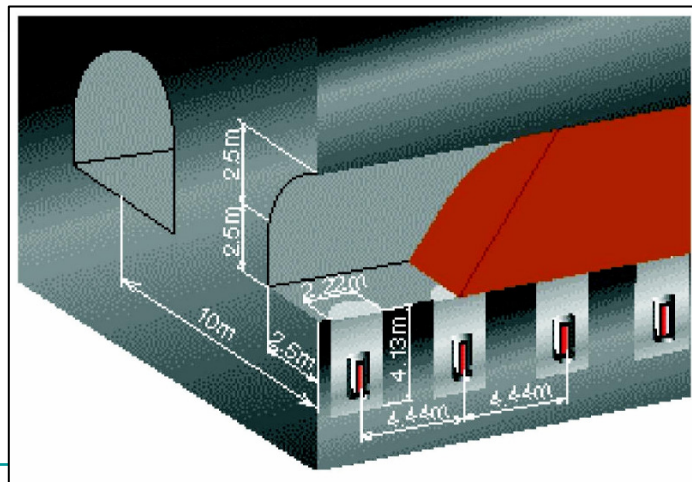
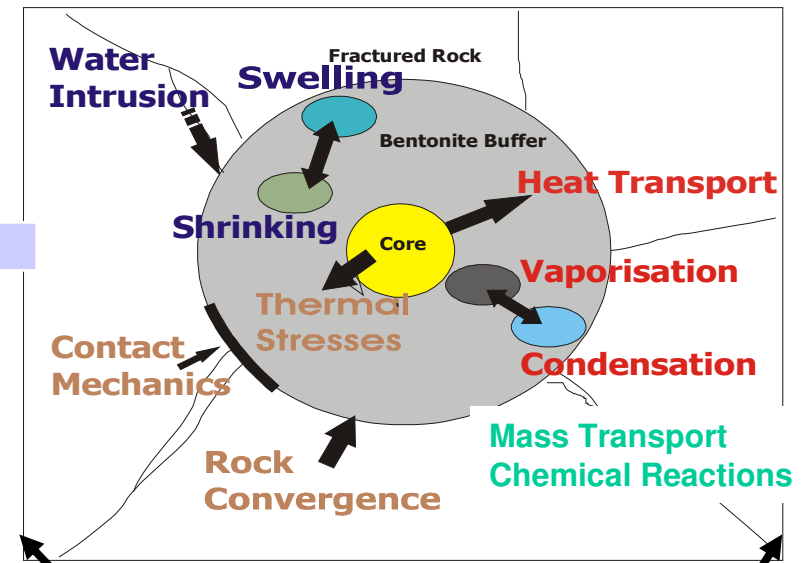
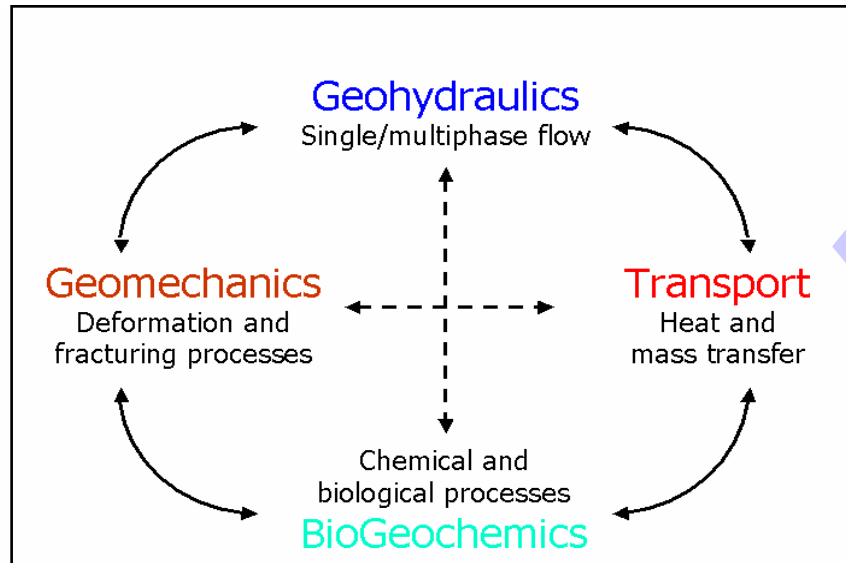
Of course, a real underground structure of a disposal site is much more complex...

This is just **ONE** base of an underground disposal site

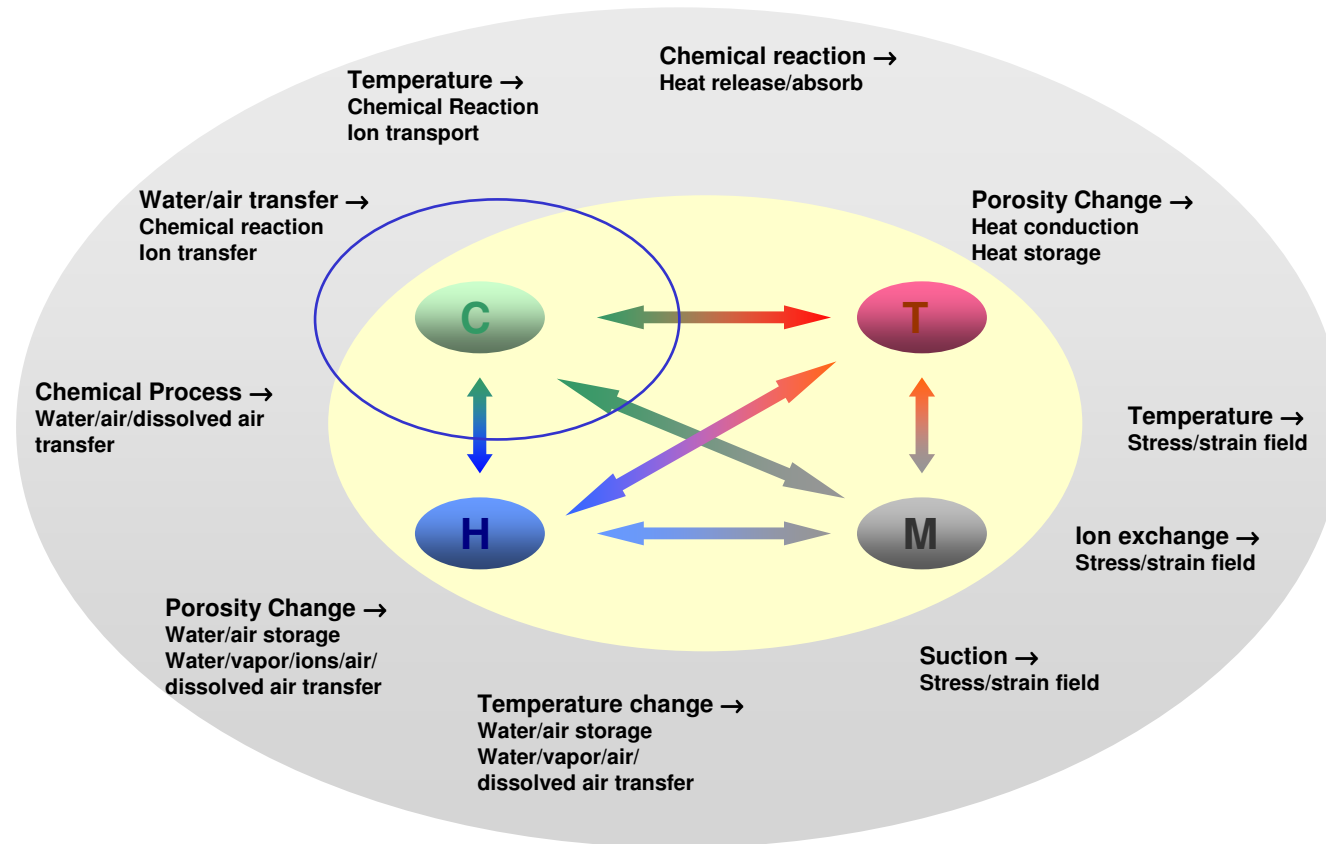
- **Red** = Barriers
 - **Green** = solid salt
 - **Blue** = crushed salt
 - **Black** = Disposal cavern
 - **Grey** = Excavation-disturbed zone
-
- Up to 15 bases possible



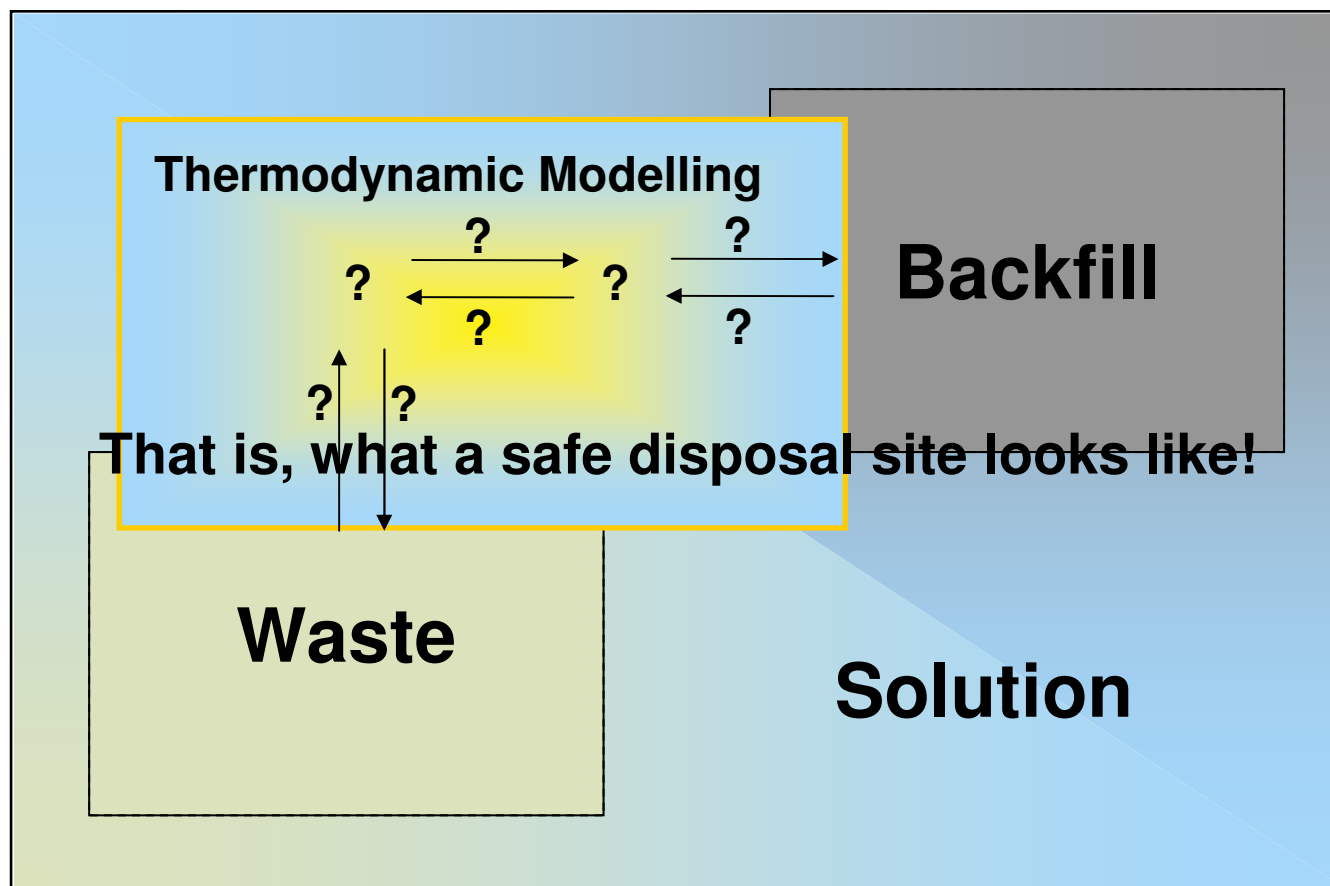
Coupled Processes in Geotech Systems



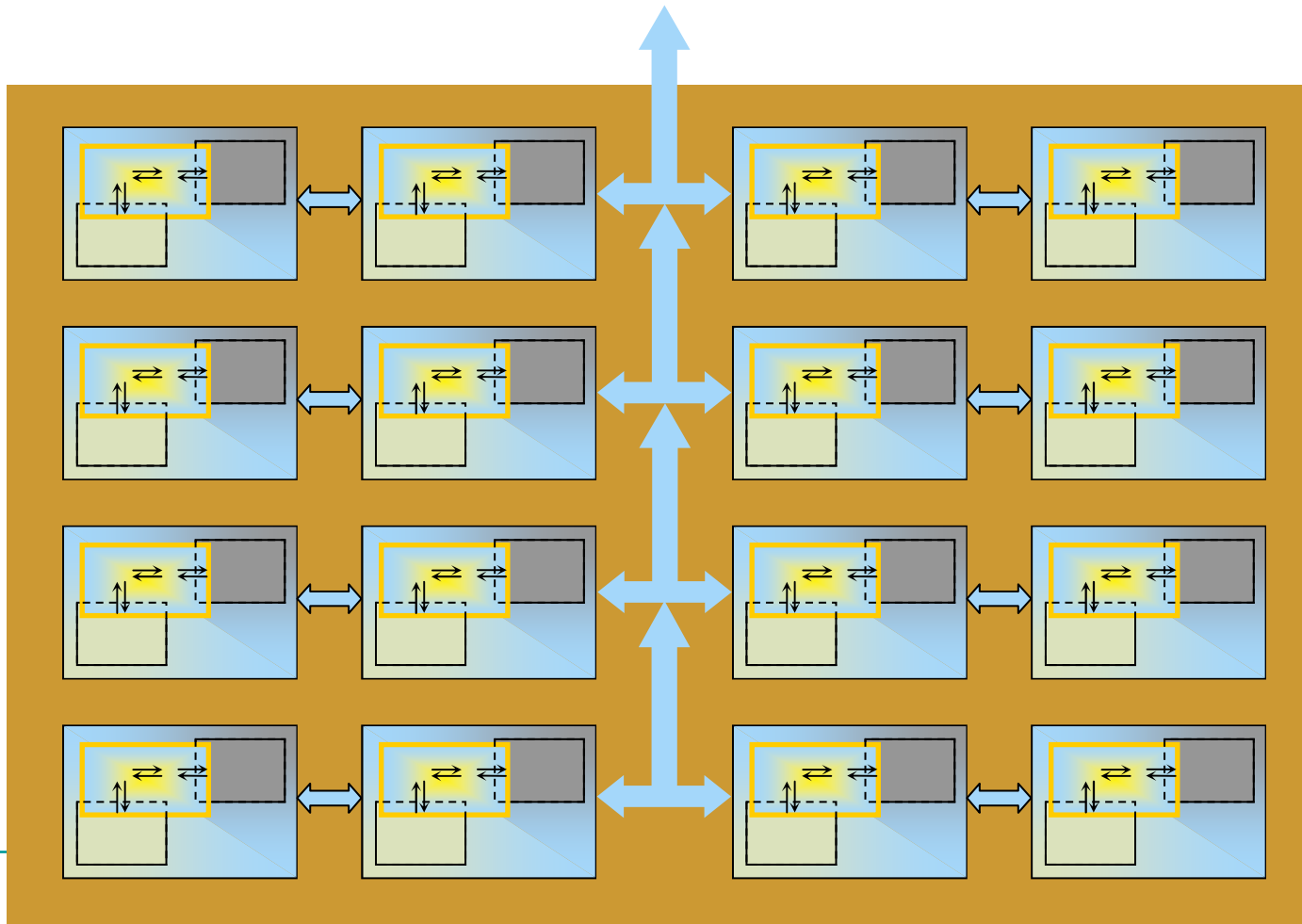
Concept of Coupled Processes



Disposal chamber for waste



Many caverns form one system...

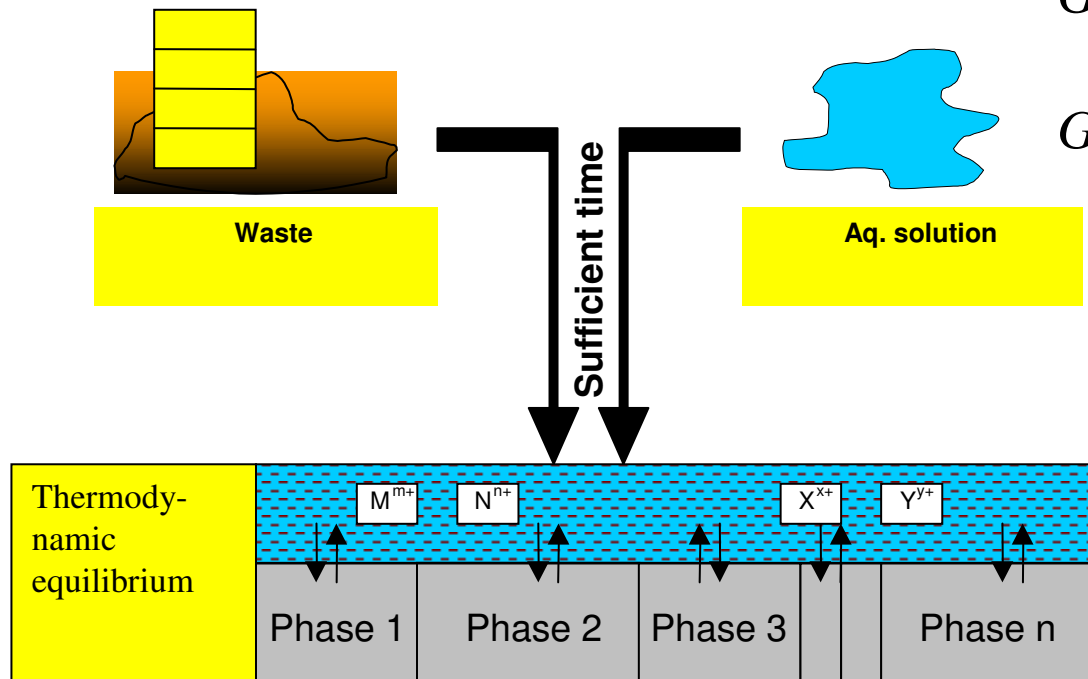


Interaction Waste - Solution

Phasecomposition:

$$G_{solids} = \sum_{\text{Phases } i} n_i \cdot G_{f,i}^{\otimes}$$

$$G_{solution} = \sum_i n_i (G_{f,i}^{\otimes} + RT(\ln m_i + \ln \gamma_i))$$

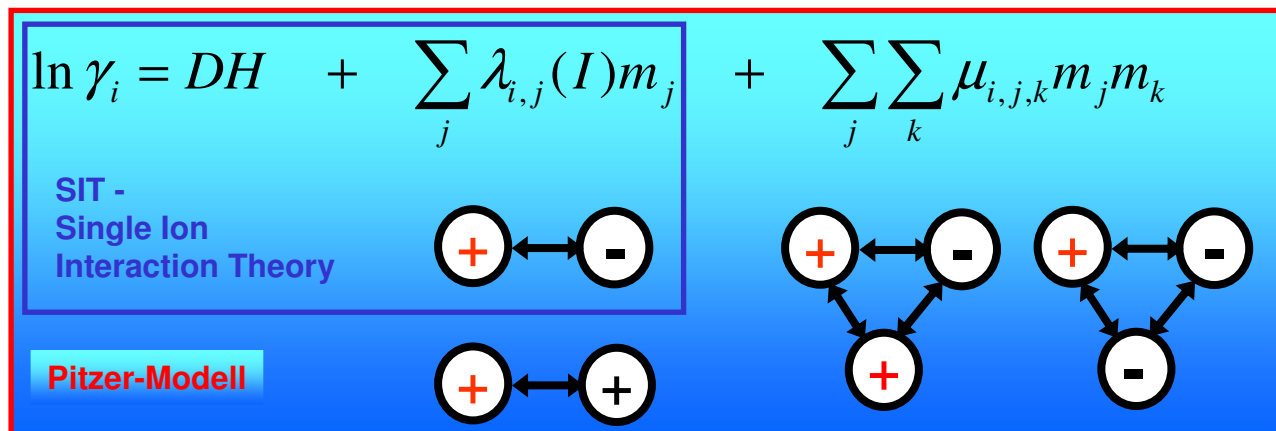


Equilibrium

$$K = \prod_j a_j^{\nu_j} = \prod_j m_j^{\nu_j} \cdot \gamma_j^{\nu_j}$$

Modells for the calculation of activity coefficients

- Debye-Hückel (1923): purely electrostatic interactions
- Extensions to the DH-equation...
- Approaches considering specific ionic interactions ...



- Material microstructure
- Dissolution/precipitation (C)

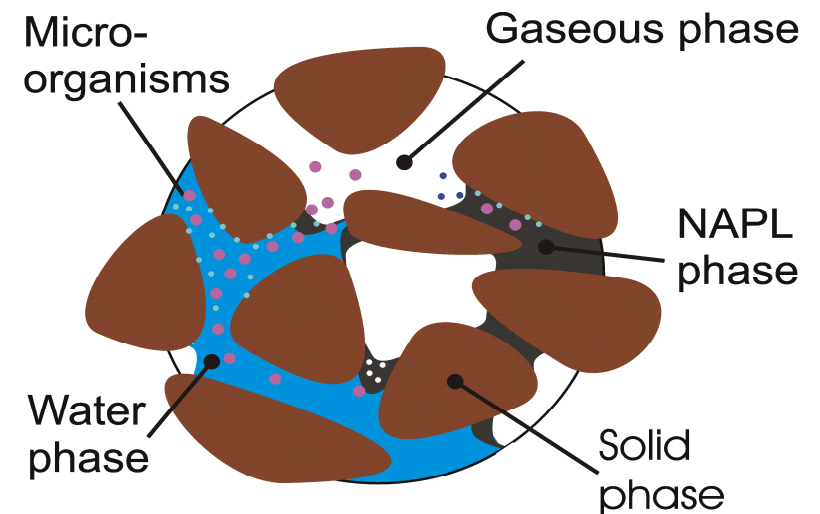
→ n_0

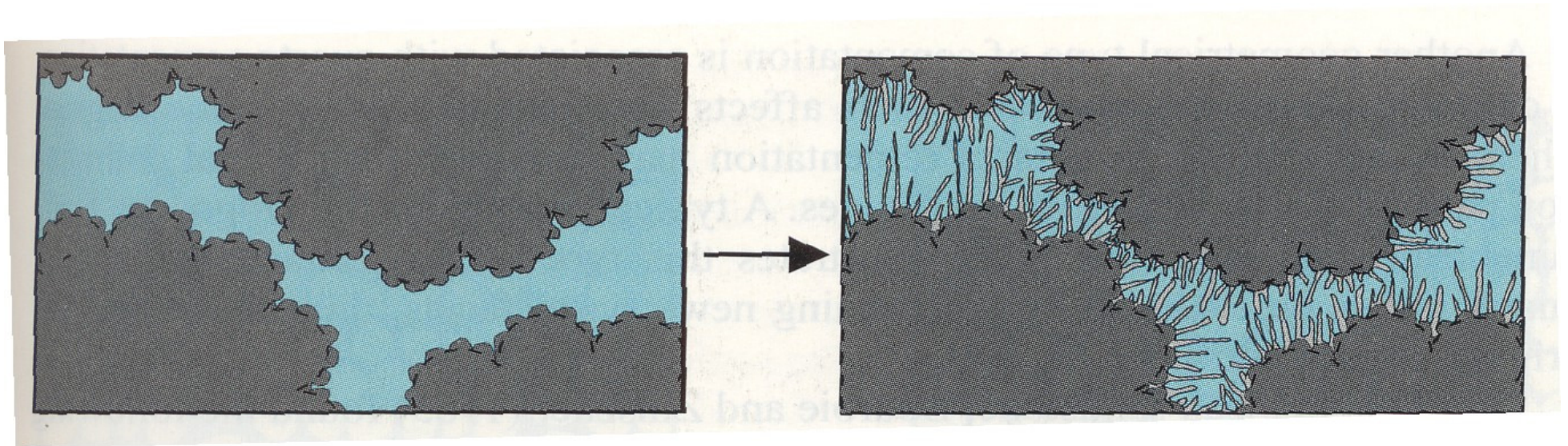
- $$n = n_0 - \sum_{j=1}^{nm} V_j M_j$$

- Swelling (bentonite)
 $n = n(\epsilon, \text{other factors})$

- Permeability $k=k(n)$

$$n_{IL} = (S^l)^\eta \cdot \beta \cdot n_{ILmax}$$



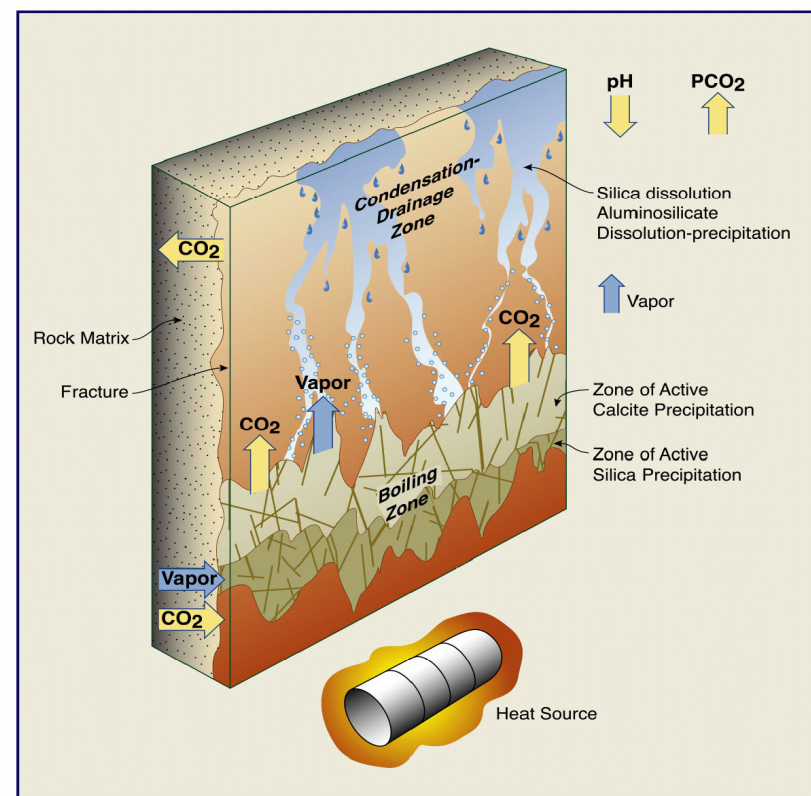


(Clauser 2003)

Geochemical processes



- Chemical evolution of waters, gases and minerals intimately coupled to TH processes
 - Drying concentrates aqueous species in remaining liquid phase
 - Boiling forces mineral precipitation
 - Dilute water in condensation zones promotes dissolution of minerals
- Mineral-water reactions limited by kinetics and water saturation
- pH affected by
 - CO_2 degassing and transport
 - Mineral dissolution/precipitation
- Mineral dissolution and precipitation
 - Porosity and permeability



THC Processes

(Sonnenenthal et al 2005)

Content

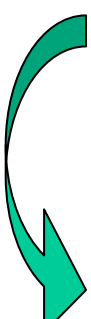


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Governing Equations



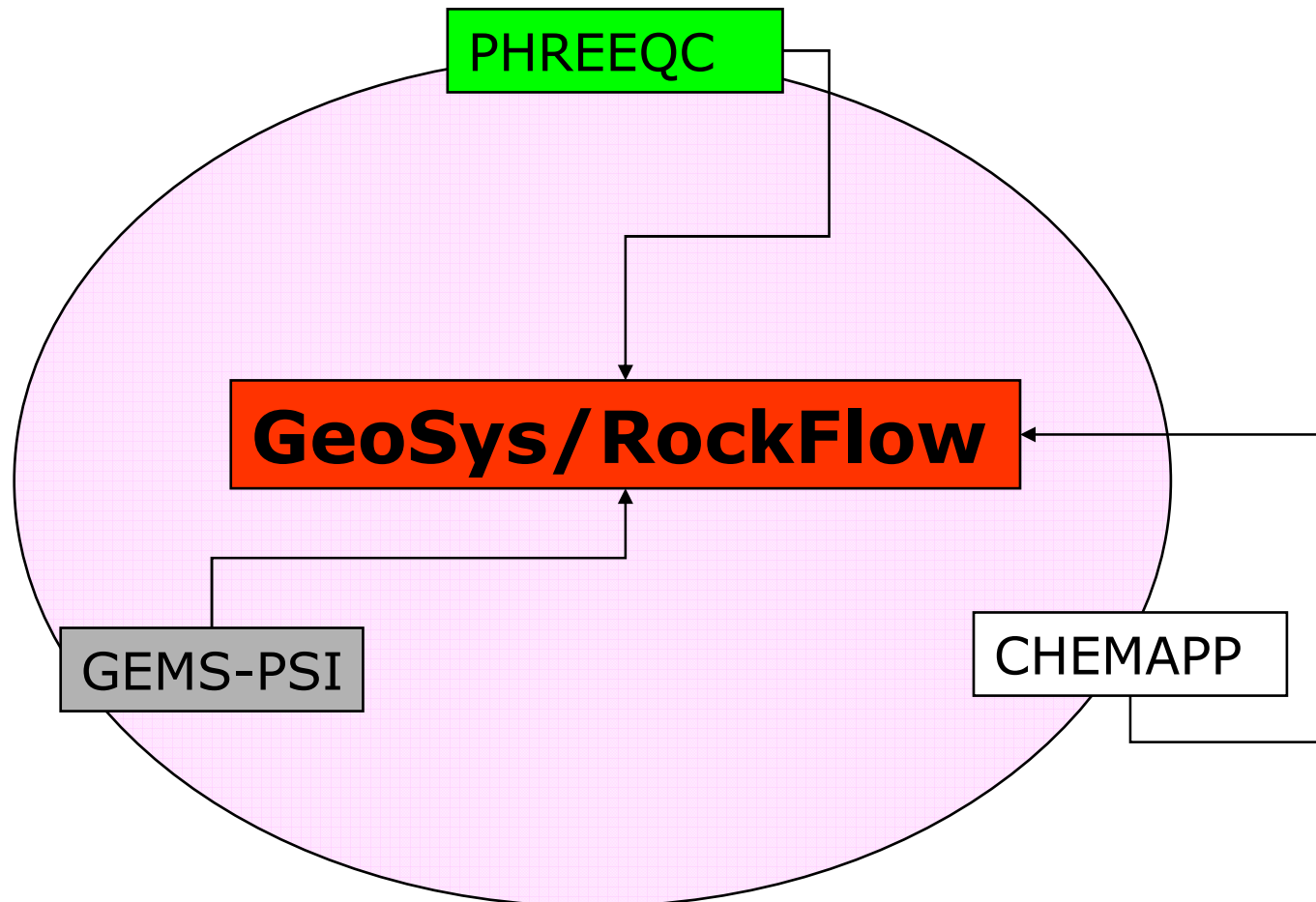
Saturated

$$\frac{\partial C_i}{\partial t} = \underbrace{-v_a \nabla C_i + \nabla \cdot (D \nabla C_i)}_{\text{n x conservative Transport}} + \underbrace{Q_{C_i} + Reakt(C_1, \dots, C_n)}_{\substack{\text{Chemical reactions with} \\ \text{PHREEQC, ChemApp or GEMS-PSI}}} \quad i=1, 2, \dots, n$$

$$\frac{\partial C_i}{\partial t} = -v_a \nabla C_i + \nabla \cdot (D \nabla C_i) + Q_{C_i}$$
$$\frac{\partial C_i}{\partial t} = Reakt(C_1, \dots, C_n)$$

Unsaturated

$$\frac{\partial(nS_{\gamma}C_{i,\gamma})}{\partial t} = -v_{\gamma}\nabla C_{i,\gamma} + \nabla(nS_{\gamma}D_{i,\gamma}\nabla C_{i,\gamma}) + nS_{\gamma}Q_{i,\gamma} + nS_{\gamma}\Gamma_{i,\gamma}(C_{1,\gamma}\dots C_{n,\gamma})$$

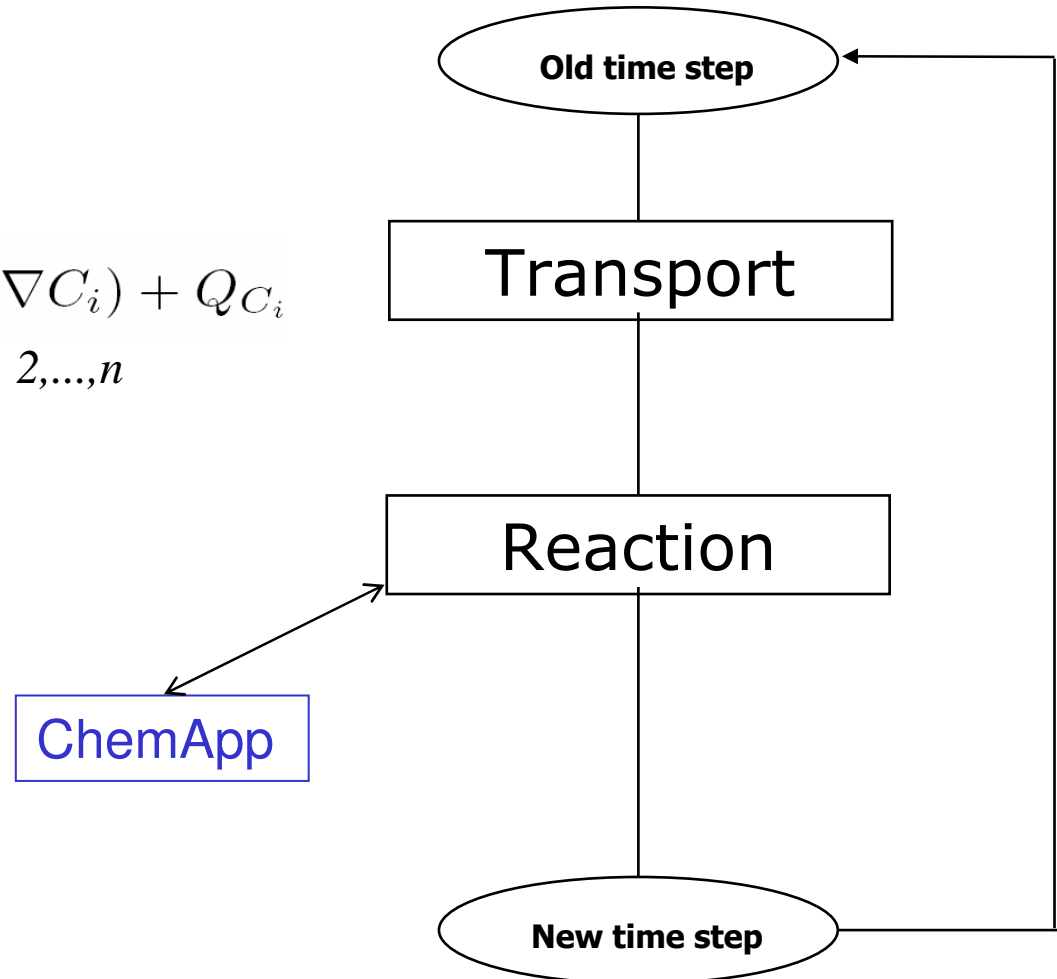
where $C_{i,\gamma}$ is the concentration of the i -th component of a n component system in phase γ , v_{γ} is the Darcy velocity of phase γ , S_{γ} is saturation of phase γ , D is the diffusion - dispersion coefficient of component i in phase γ , $Q_{i,\gamma}$ is the source/sink term and $\Gamma_{i,\gamma}(C_{1,\gamma}\dots C_{n,\gamma})$ is the source/sink term of component i in phase γ due to equilibrium chemical reactions with all other species in the same phase.



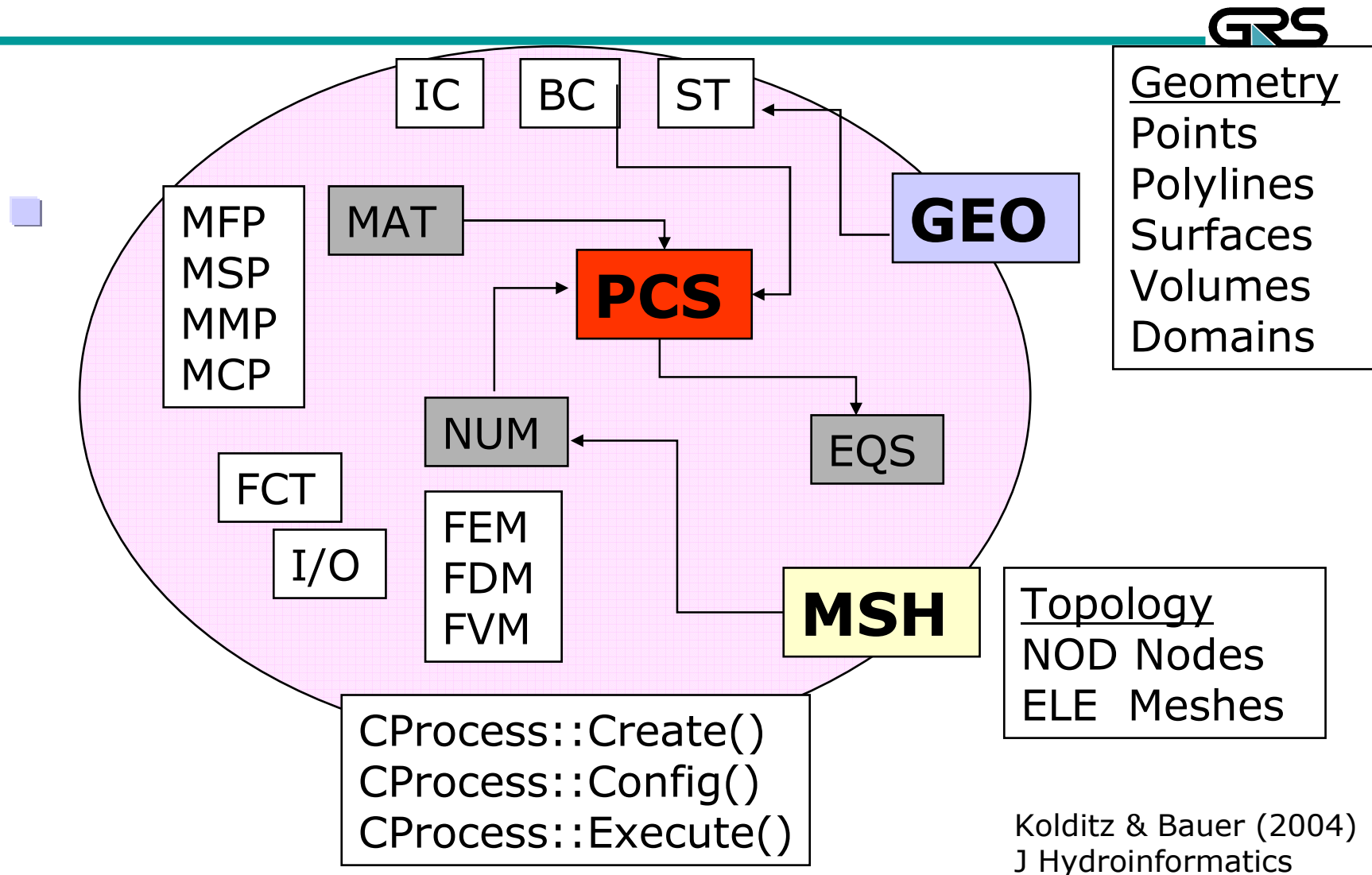
$$\frac{\partial C_i}{\partial t} = -v_a \nabla C_i + \nabla \cdot (D \nabla C_i) + Q_{C_i}$$

$i=1, 2, \dots, n$

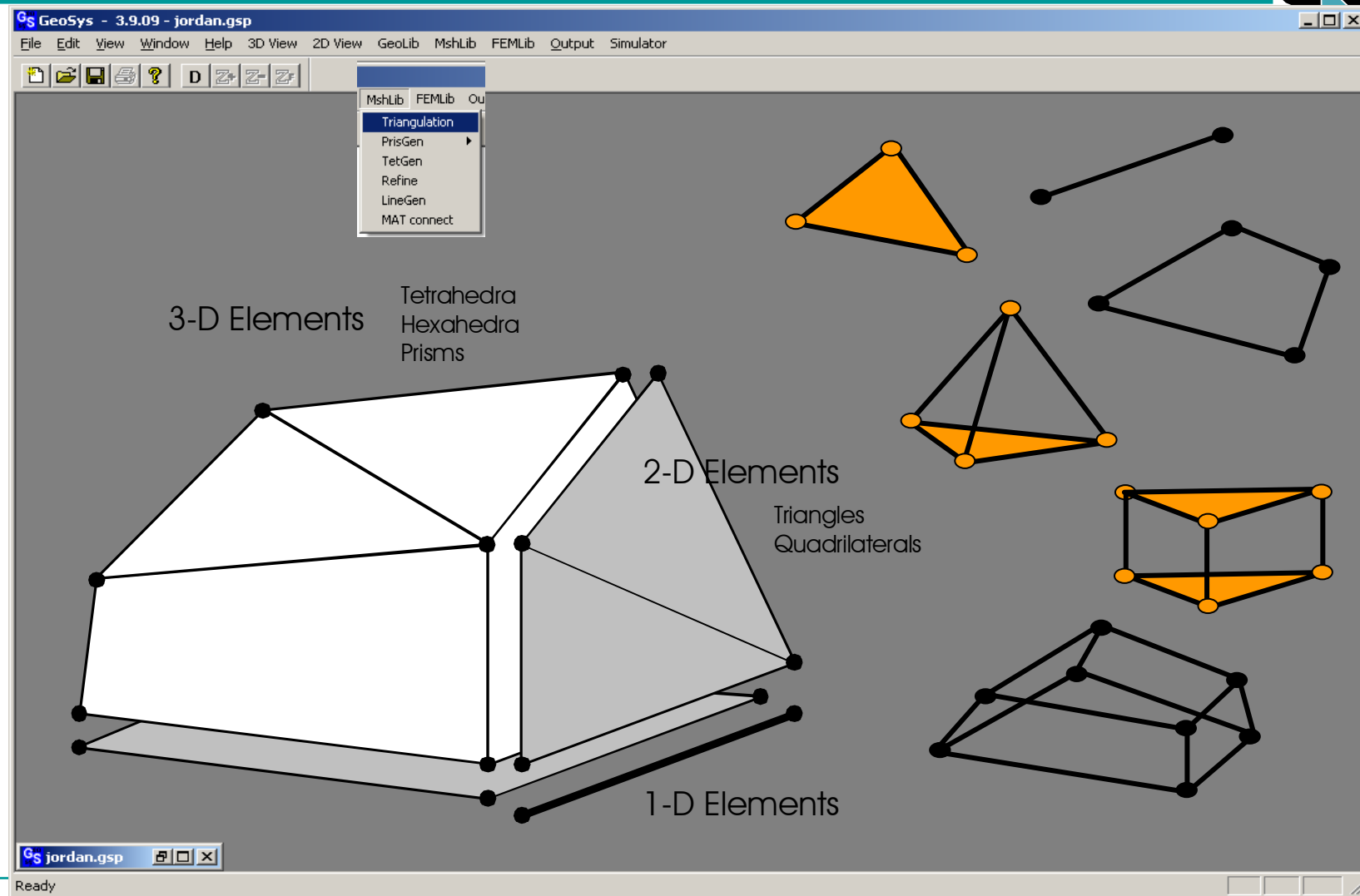
$$\frac{\partial C_i}{\partial t} = Reakt(C_1, \dots, C_n)$$



Object-Orientation:Multifield Problems



Geometric Element Types



Multi-Componental Systems



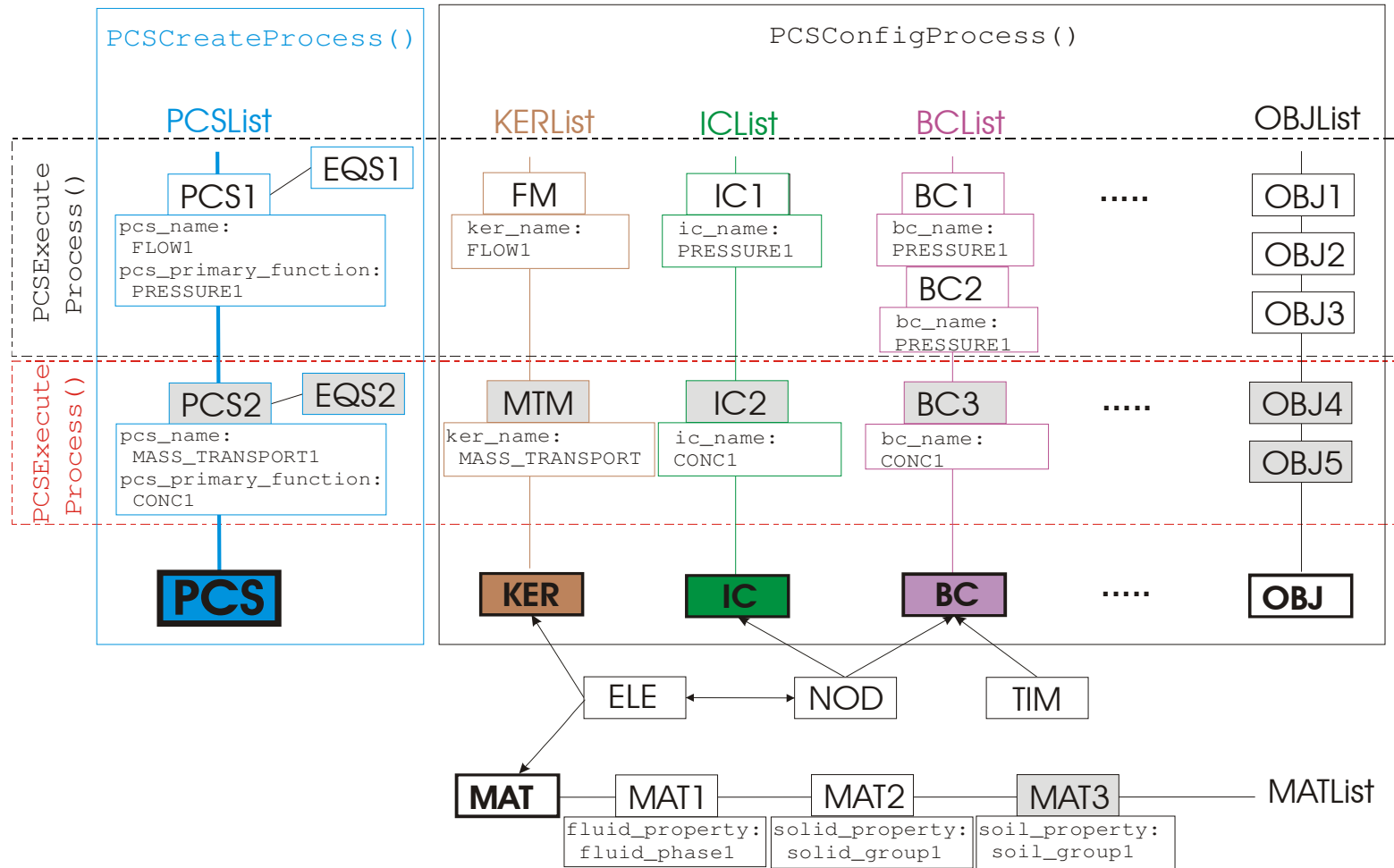
$$\begin{pmatrix}
 A_1 & B_{12} & B_{13} & \dots & B_{1n} \\
 B_{12} & A_2 & \cdot & B_{24} & \dots \\
 B_{13} & \cdot & A_3 & \dots & \dots \\
 & B_{24} & & A_4 & \dots & B_{4n} \\
 \dots & \dots & \dots & \dots & \dots & \dots \\
 B_{1n} & & & B_{4n} & \dots & A_n
 \end{pmatrix}
 *
 \begin{pmatrix}
 C_1 \\
 C_2 \\
 C_3 \\
 C_4 \\
 C_5 \\
 C_6
 \end{pmatrix}
 =
 \begin{pmatrix}
 R_1 \\
 R_2 \\
 R_3 \\
 R_4 \\
 \dots \\
 R_n
 \end{pmatrix}$$

Dimension: (number of grid nodes * number of components)²

For real world applications: $(10^5 * 20)^2 = 4 * 10^{12}$

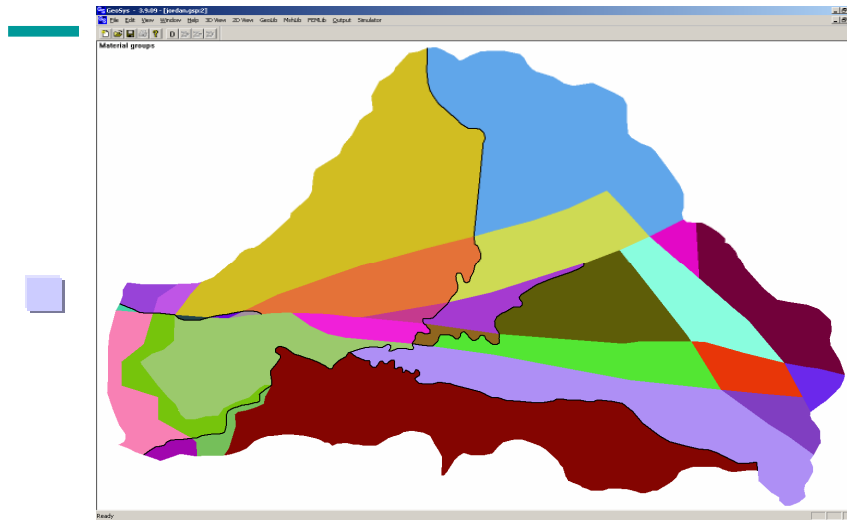
Memory requirement: $4 * 10^{12}$

PCS Implementation



Parallelization

High Performance Computing
Parallel Computing
Visualization



Nec SX-5

Parallel-
rechner



Cray T3E



Hitachi SR8000

In cooperation with HLRS Stuttgart

Verification example: Comparison with 1D PHREEQC

1D Transport and Cation exchange (Example 11, PHREEQC – User Instructions)

Flushing a 1D column with CaCl_2 .

Initial pore water: Na, K

Exchange: Ca-X2, Na-X, K-X

$$\text{Ca} = 6.0 \times 10^{-4}$$

$$\text{Cl} = 1.2 \times 10^{-3}$$

→
1 m/d

$$\text{Ca} = 0$$

$$\text{Cl} = 0$$

$$\text{K} = 2.0 \times 10^{-4}$$

$$\text{Na} = 1.0 \times 10^{-3}$$

$$\text{Ca-X2} = 0$$

$$\text{Na-X} = 5.493 \times 10^{-4}$$

$$\text{K-X} = 5.507 \times 10^{-4}$$

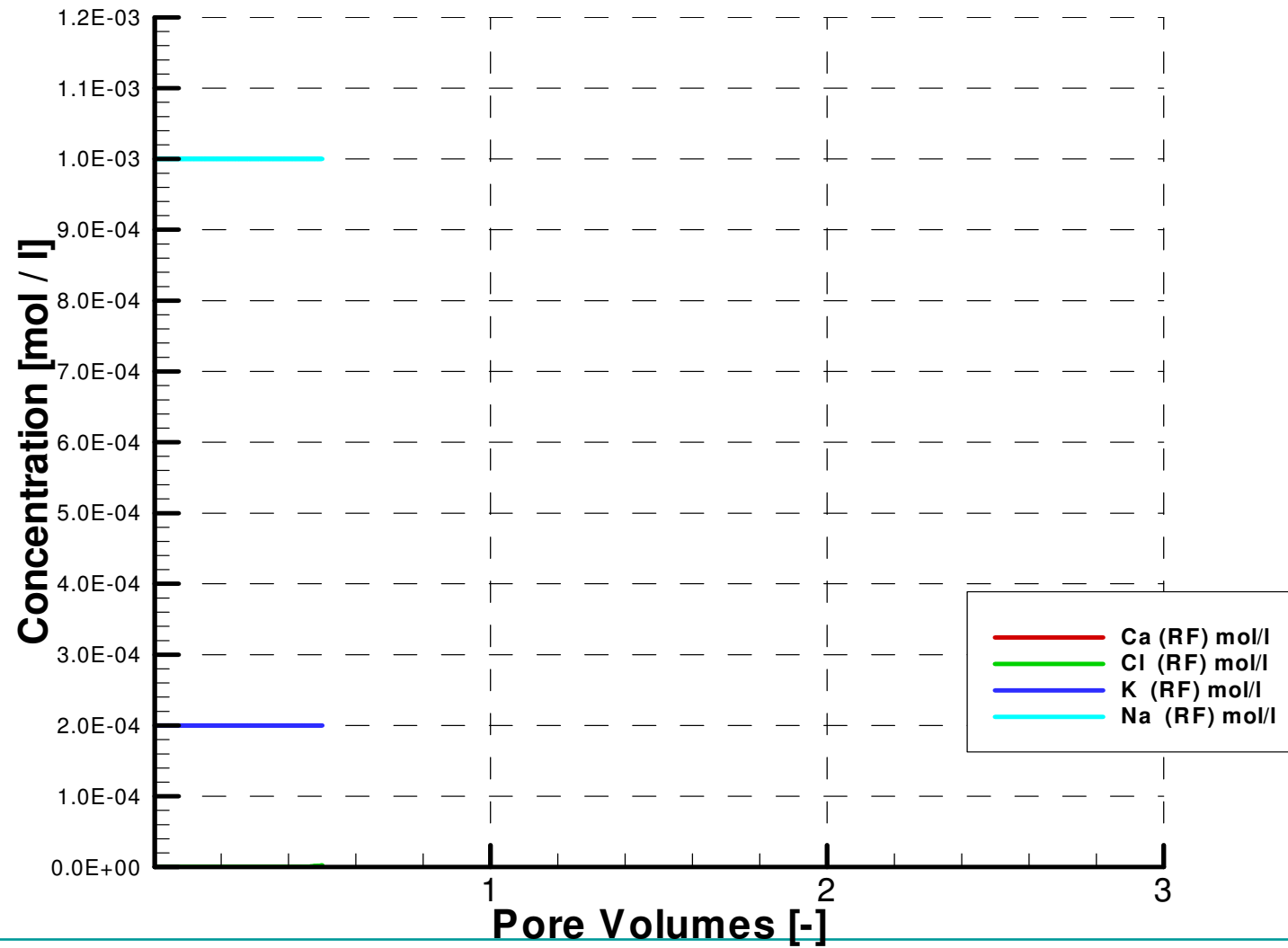
→
 C_{out}

0.08 m

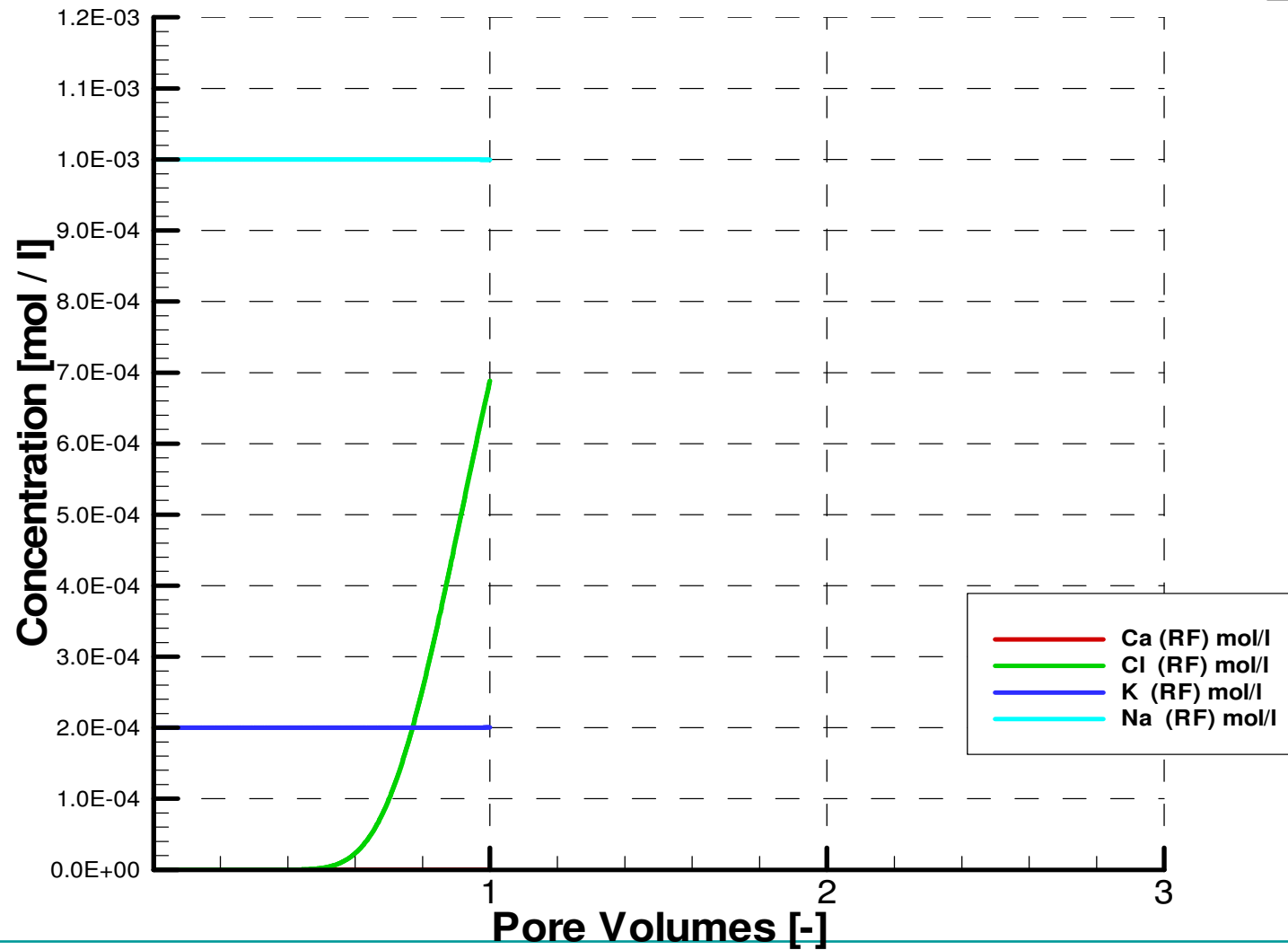
$D = 0.002 \text{ m}$, $n = 1.0$, $t = 0.24 \text{ d}$

C in mol/l

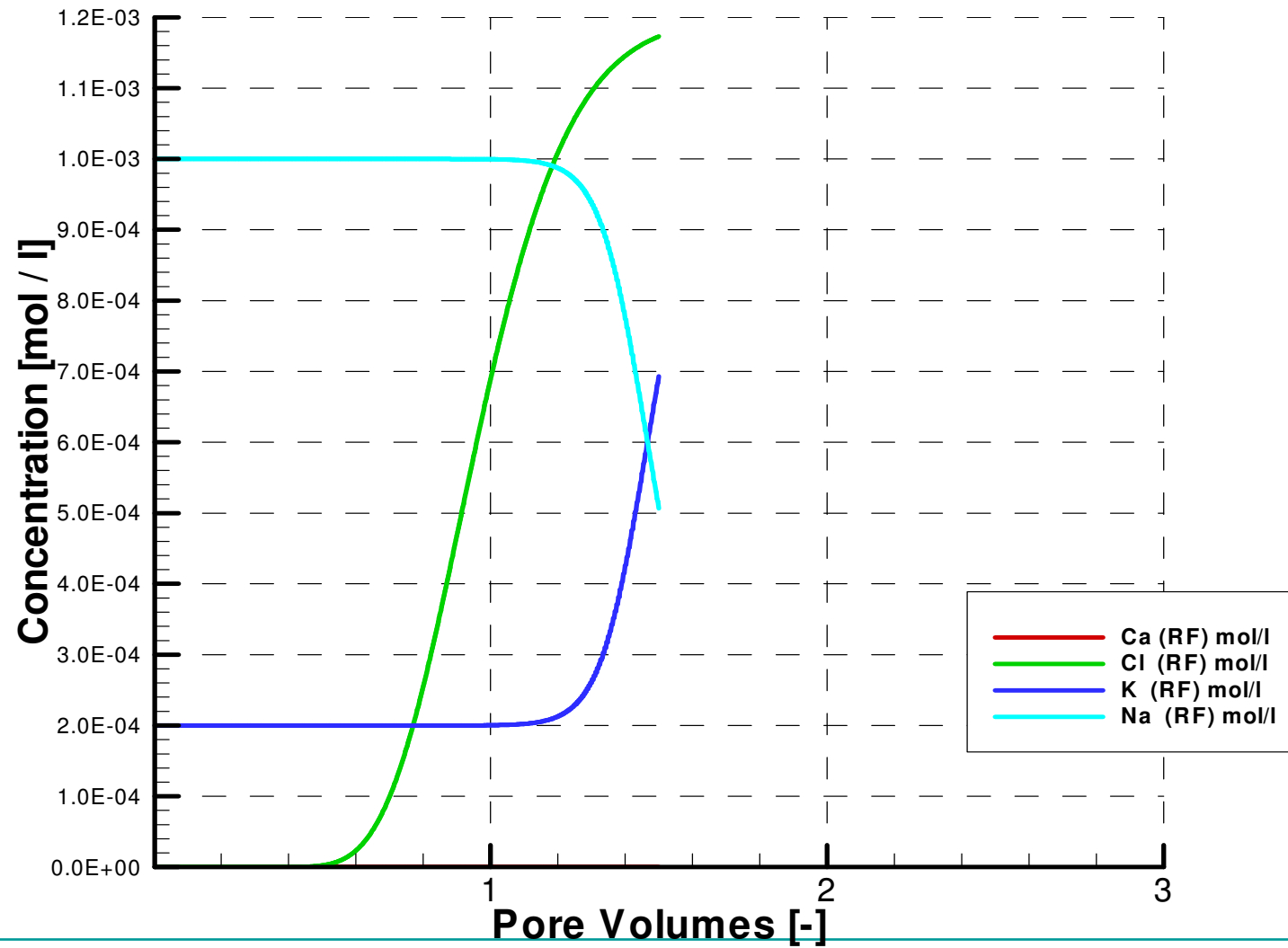
Verification Benchmark



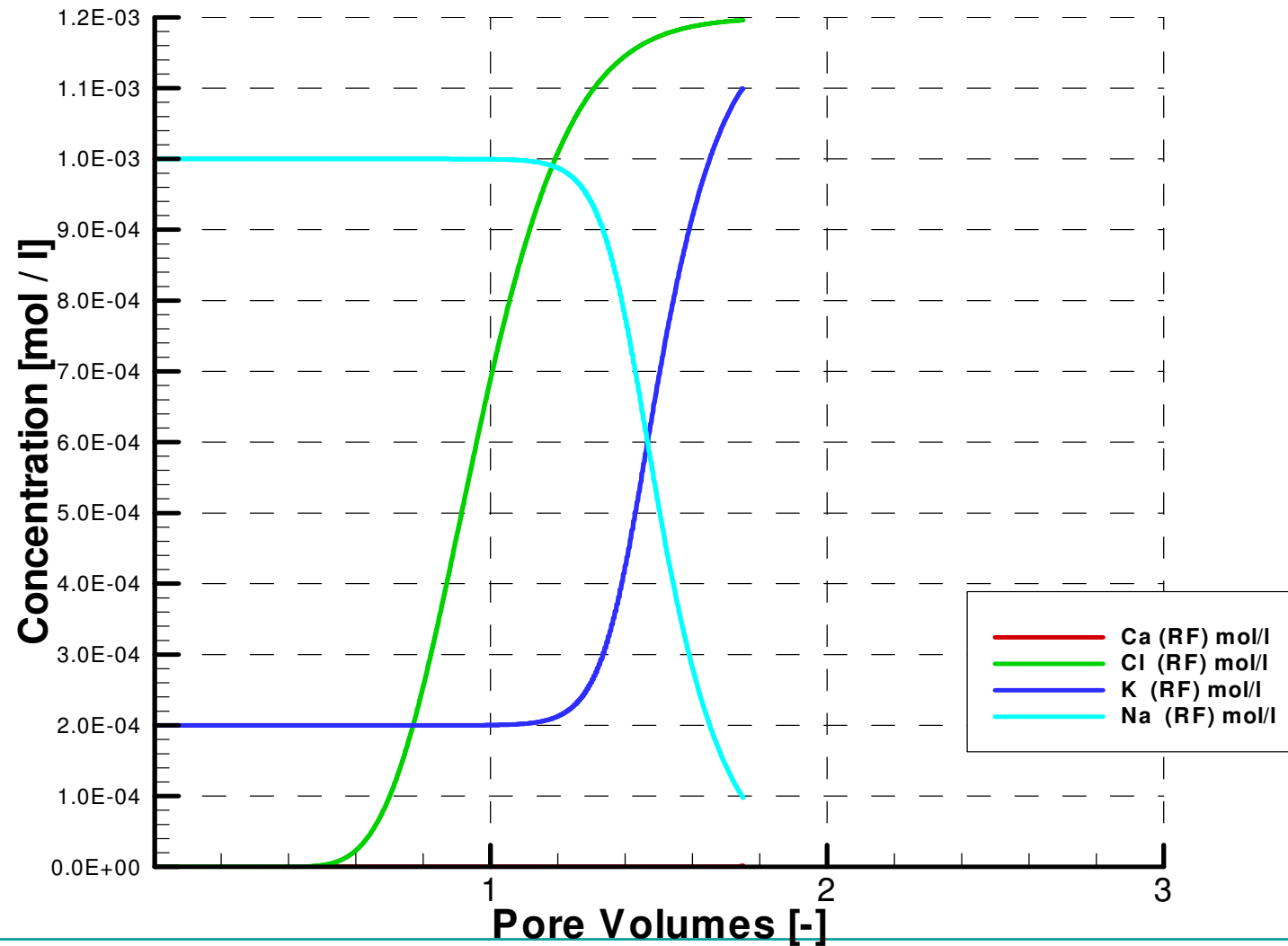
Verification Benchmark



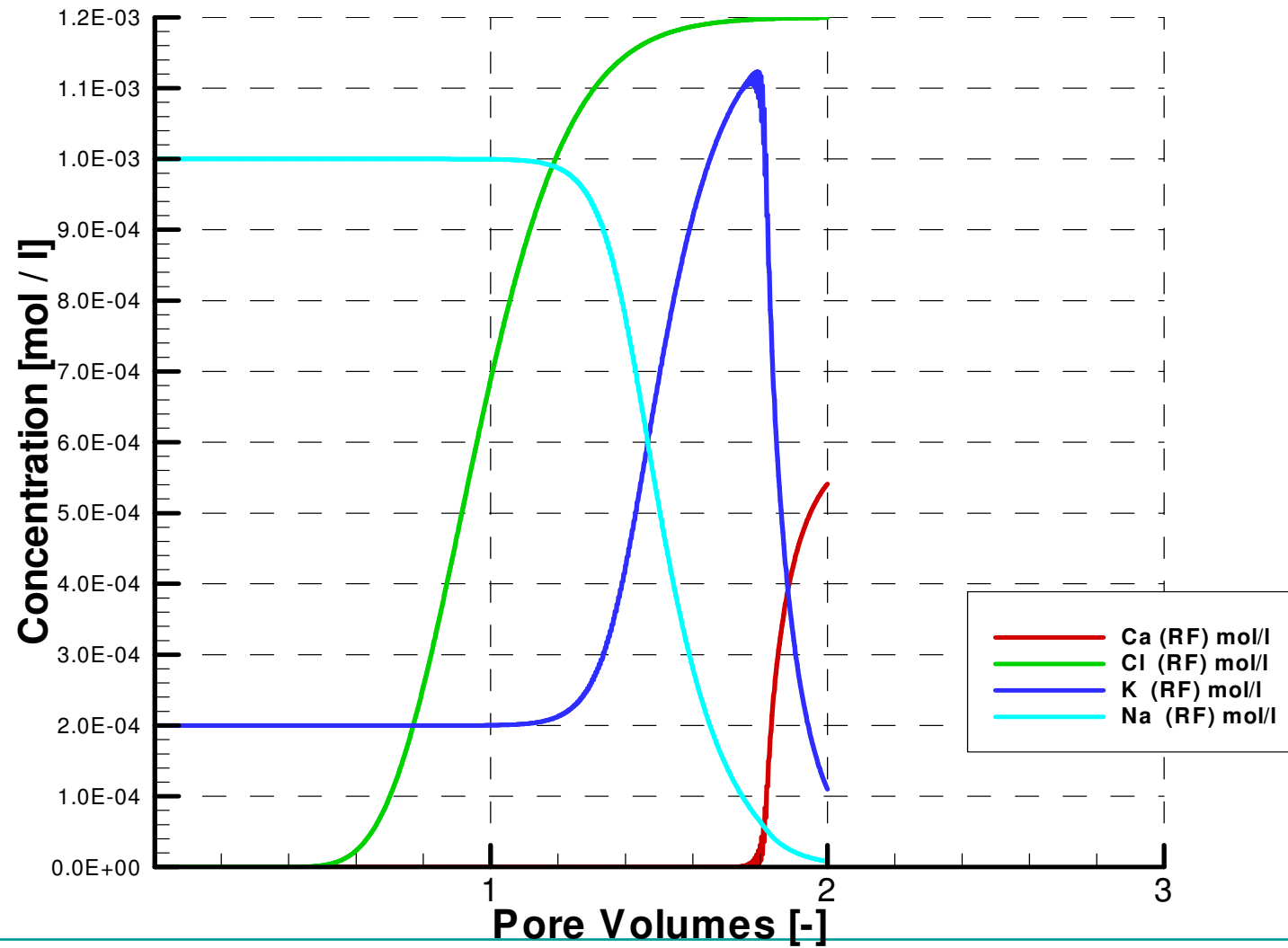
Verification Benchmark



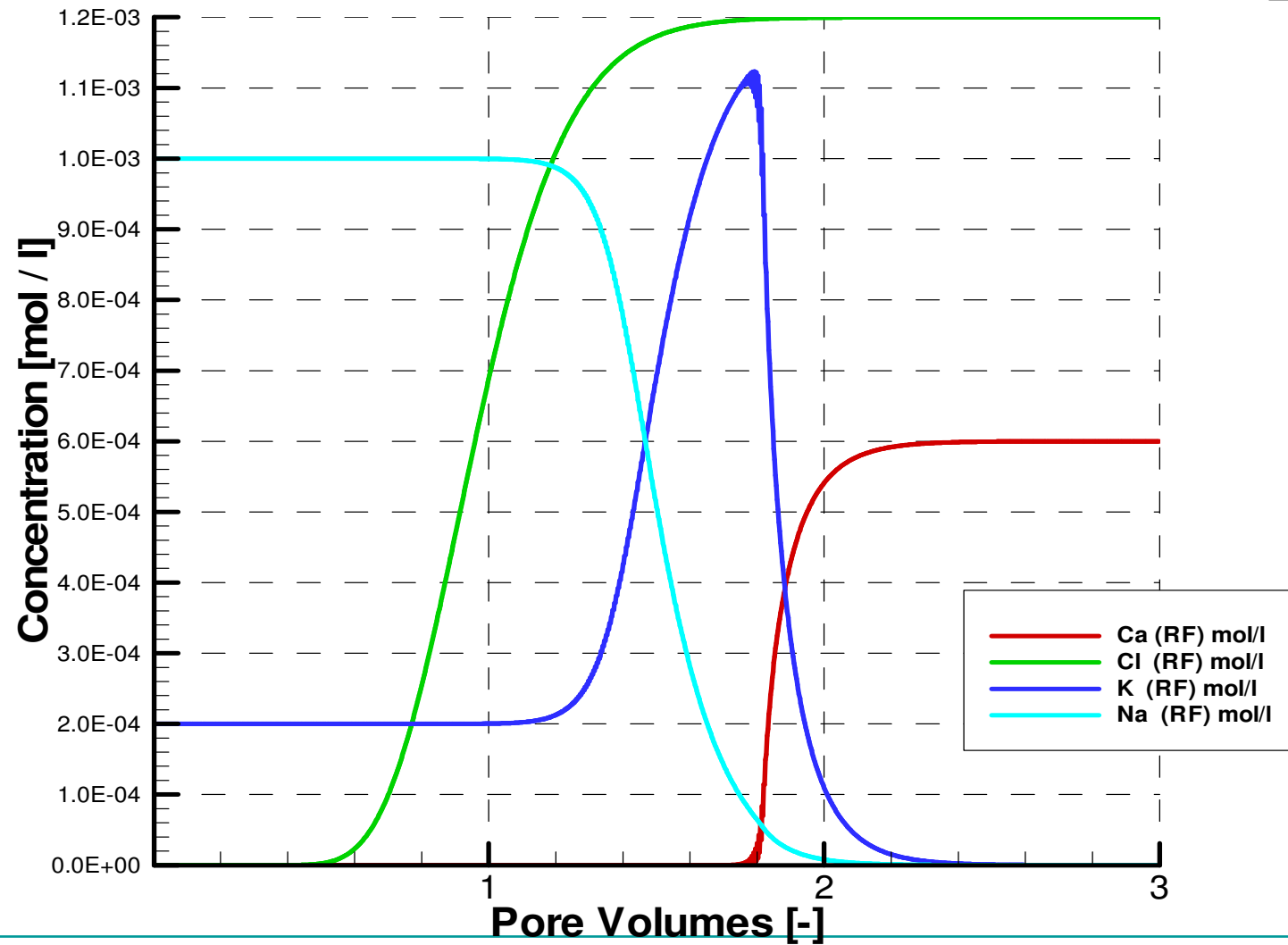
Verification Benchmark



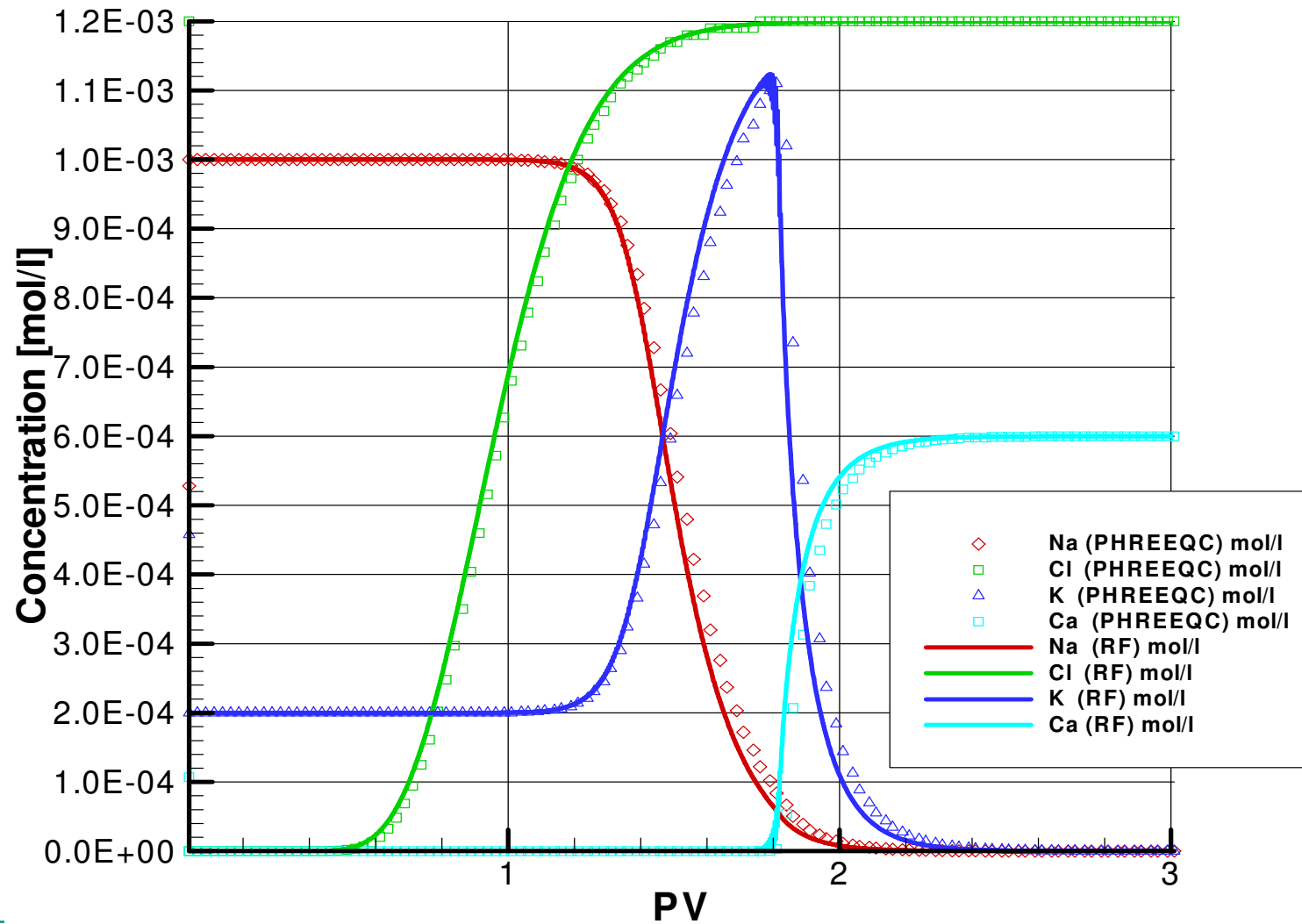
Verification Benchmark



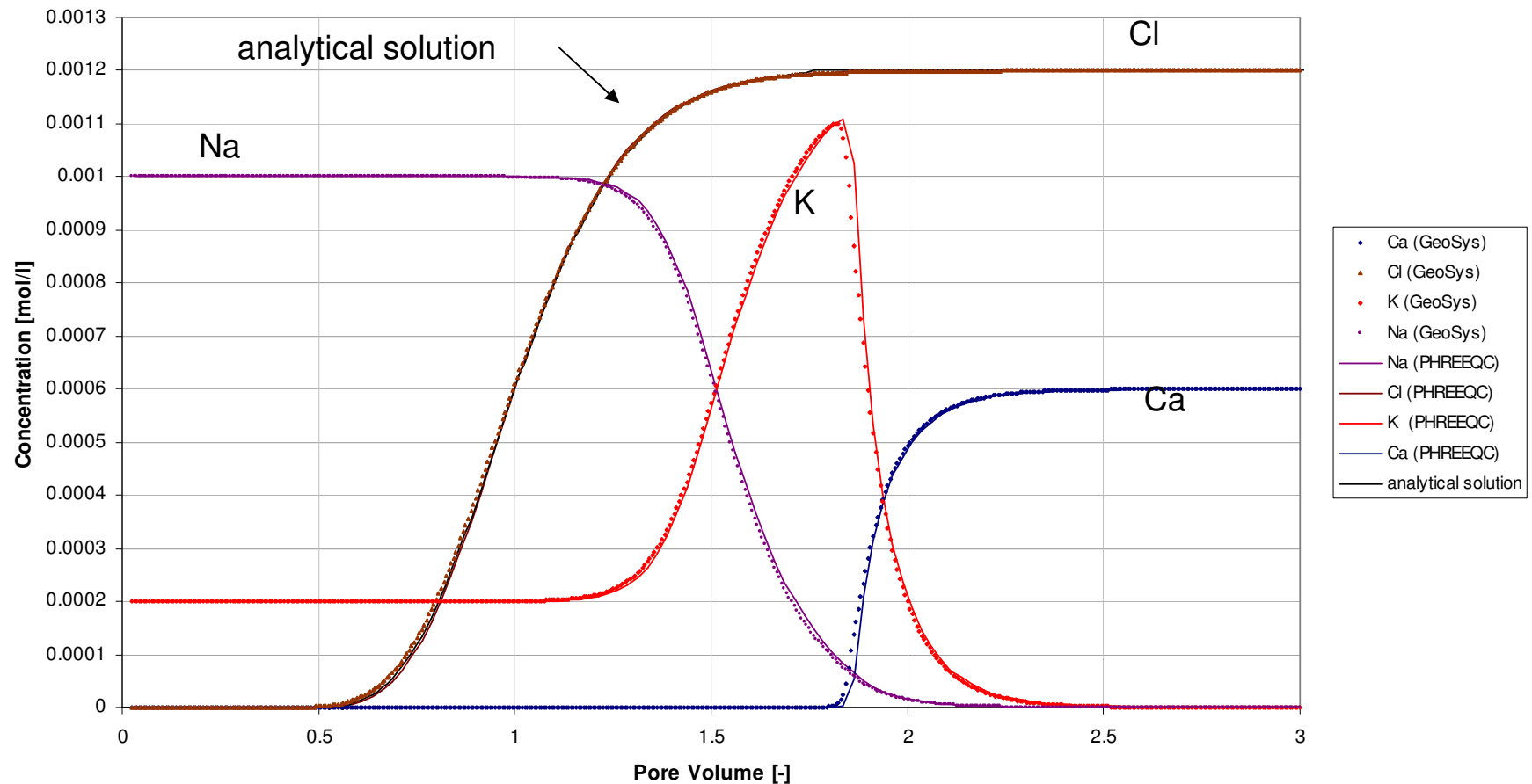
Verification Benchmark



Verification Benchmark



Concentrations at the column outlet



Content

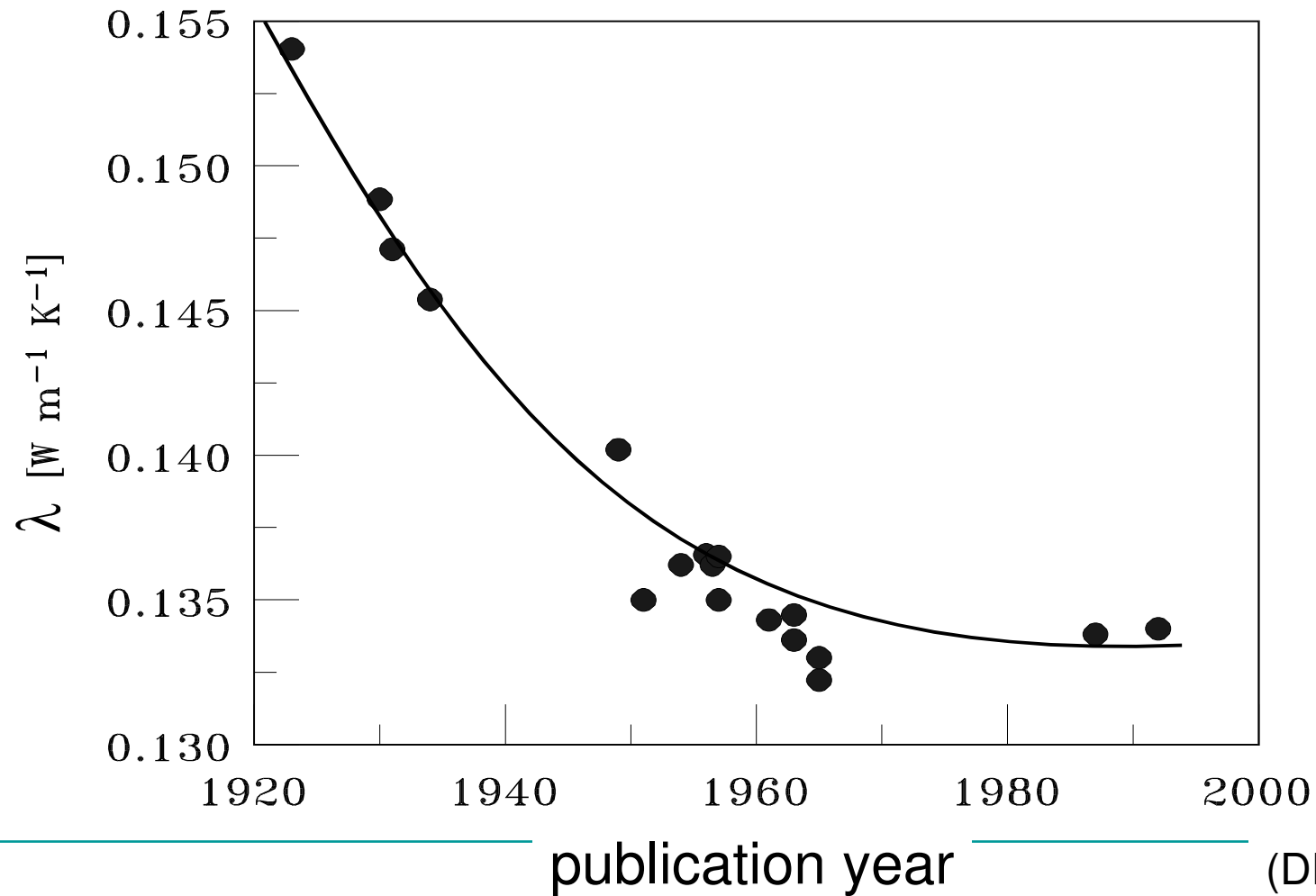


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Cause of Database Difference



Example: Thermal Conductivity λ of Liquid Toluene at 25°C

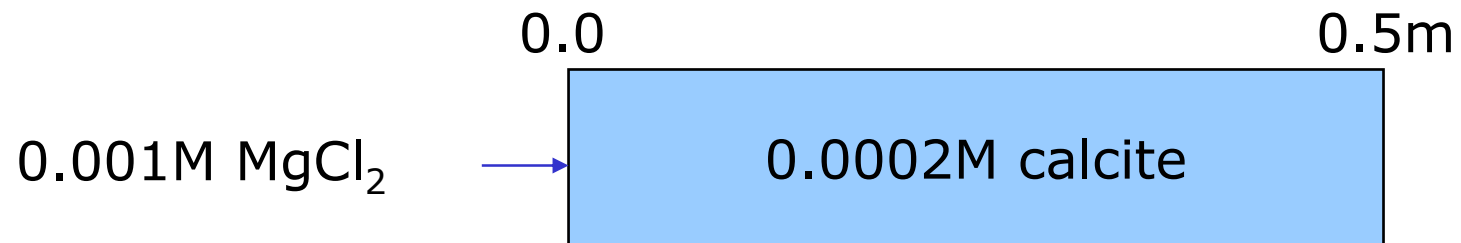


Verification Example

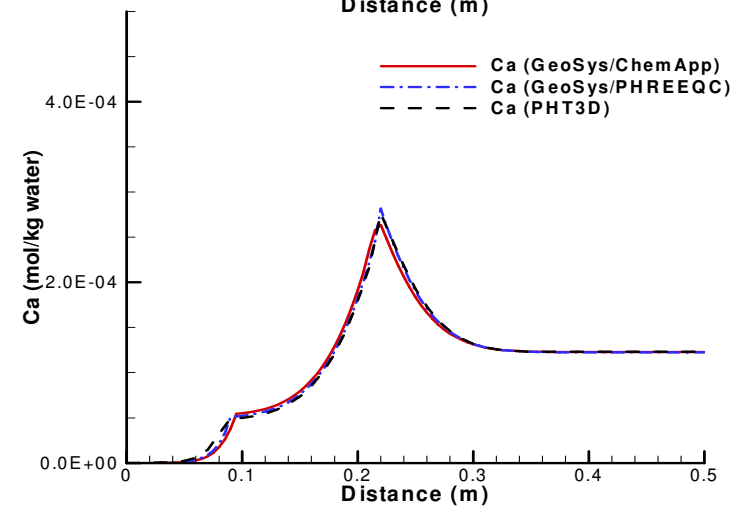
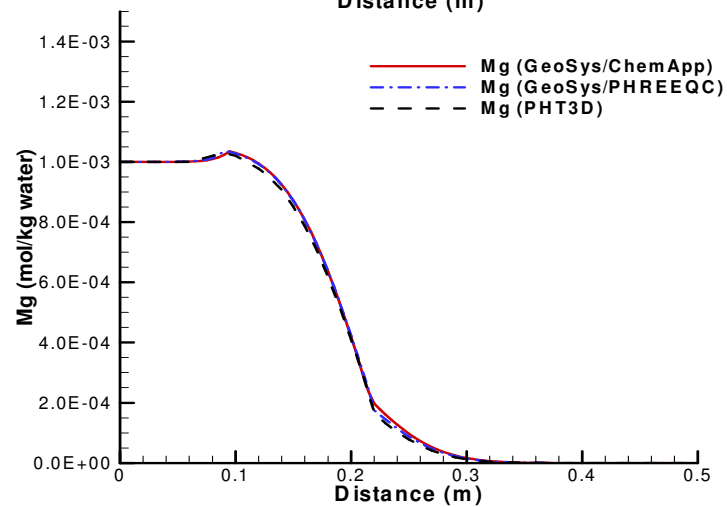
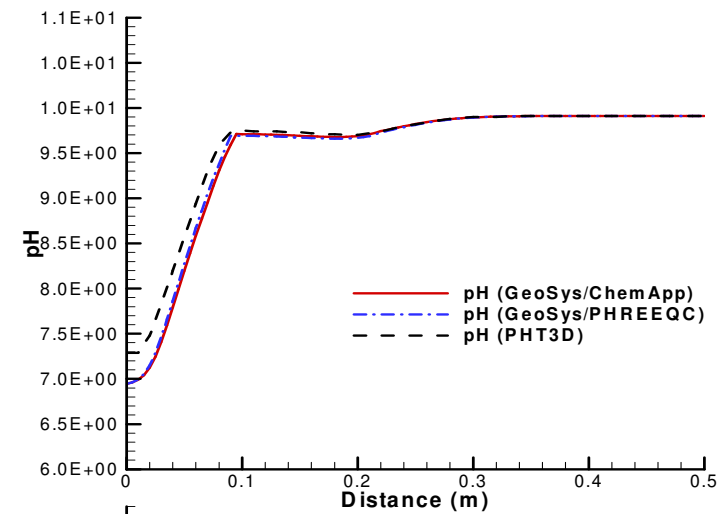
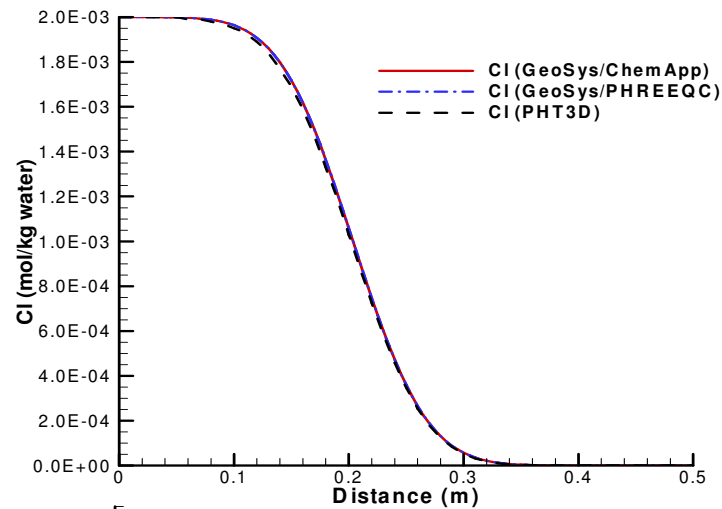
1D Transport and calcite dissolution

Simulated Program

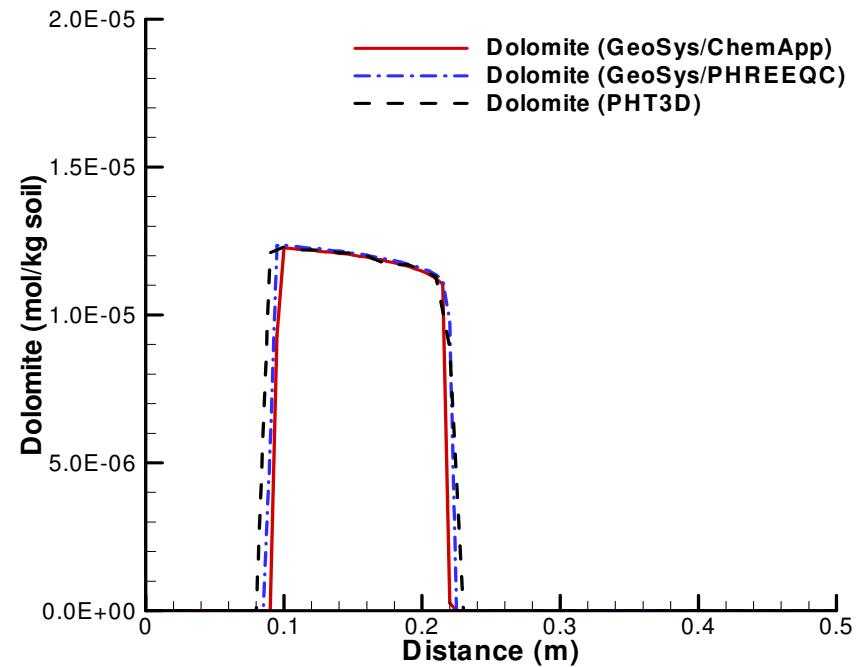
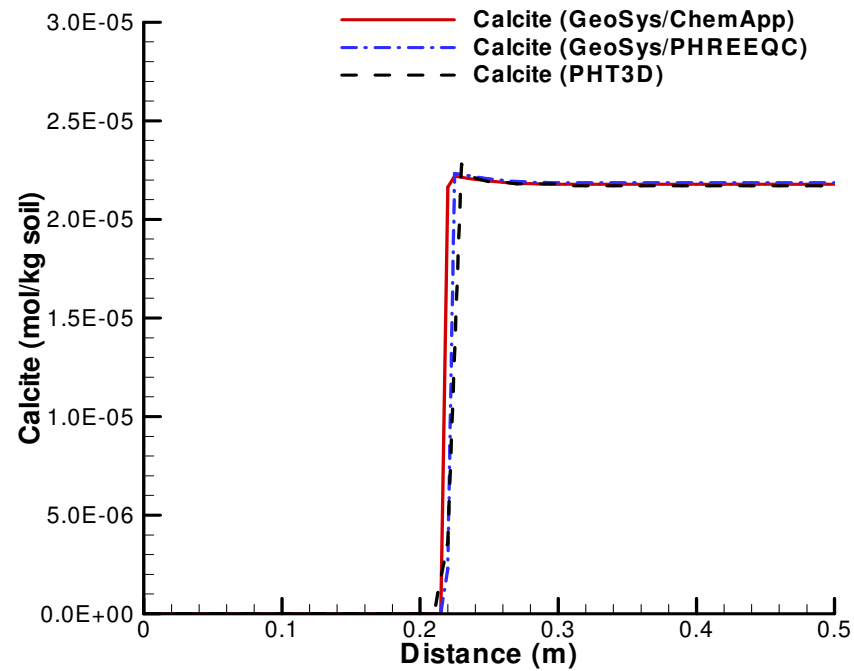
- MST1D (by Engesgaard and Kipp 1992)
- PHT3D (by Prommer 2002)
- GeoSys/PHREEQC (by Xie et al 2005)



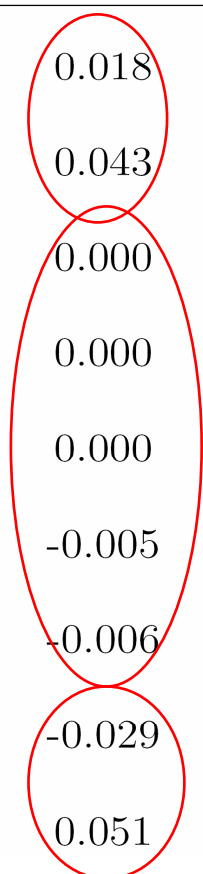
Simulation results comparison



Simulation results comparison



Database sensitivity analysis



Species	$\Delta_f G_m^0$ ($J \cdot mol^{-1}$)			Percentage
	YMF	NAGRA/PSI	Error	error (%)
H_2O	-237182.3302	-237140	-42.33015071	0.018
OH^-	-157297.7015	-157230	-67.70151593	0.043
Mg^{2+}	-455375	-455375	0	0.000
Ca^{2+}	-552806	-552806	0	0.000
Cl^-	-131217	-131217	0	0.000
$(HCO_3)^-$	-586845	-586875	30	-0.005
$(CO_3)^{2-}$	-527887.7684	-527917	29.23161984	-0.006
$(CO_2)^0$	-385878.4885	-385992	113.5115214	-0.029
$CaCO_3^0$	-1099684.997	-1099127	-557.9973053	0.051

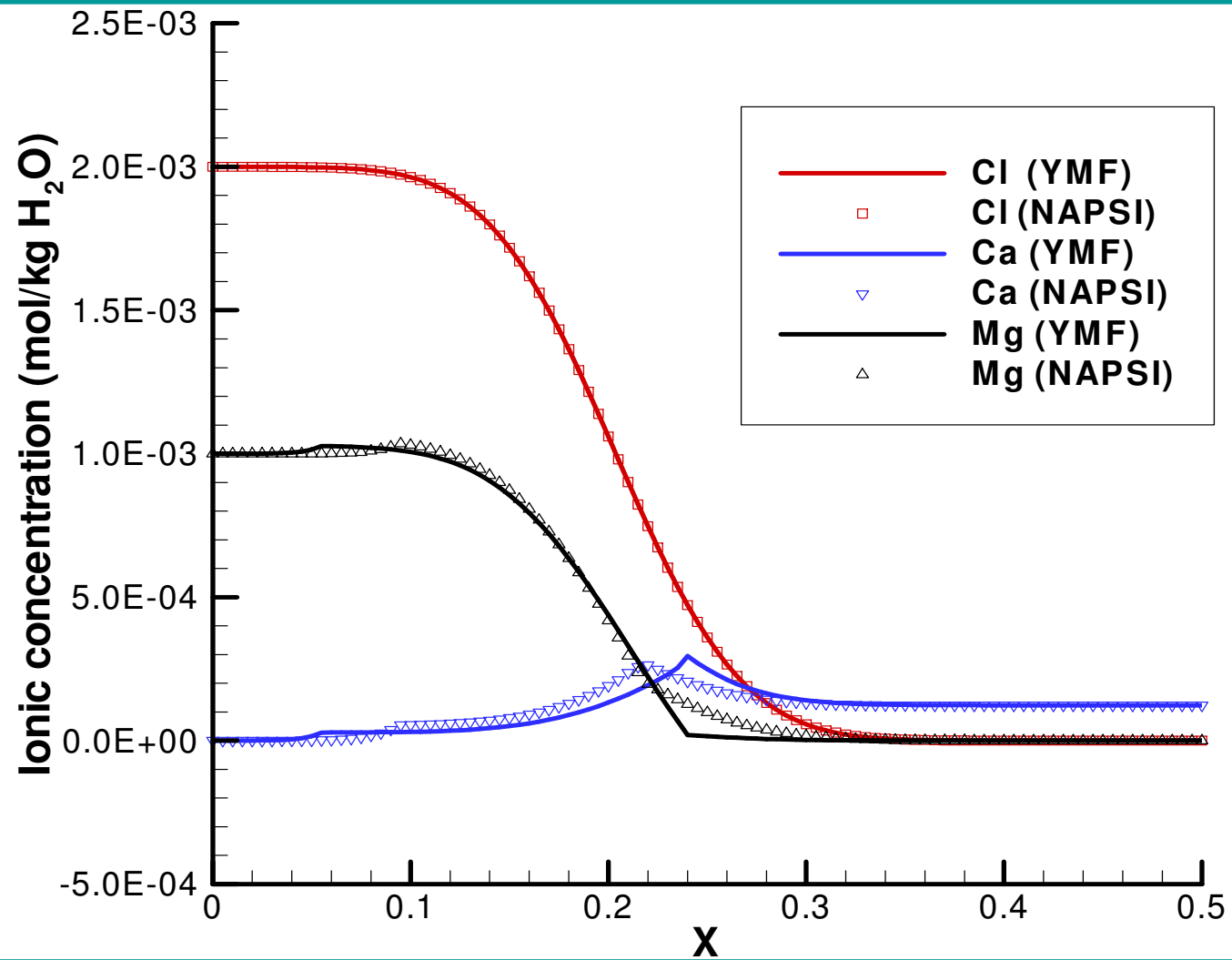
Database sensitivity analysis

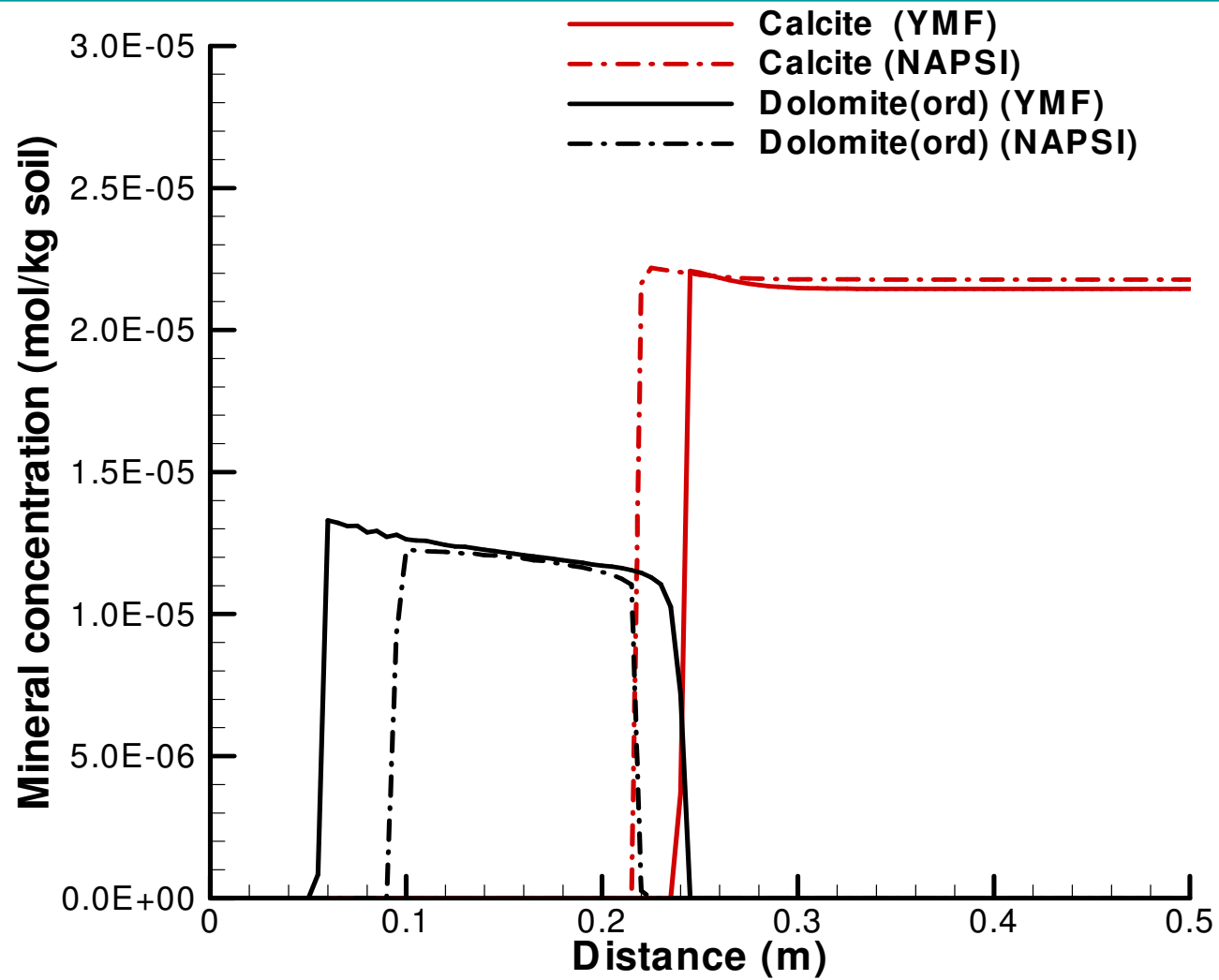
5

Species	$\Delta_f G_m^0$ ($J \cdot mol^{-1}$)		Percentage	
	YMF	NAGRA/PSI	Error	error (%)
$MgCO_3^0$	-1000266.457	-1000300	33.54316887	-0.003
$Mg(OH)^+$	-625873.1211	-627215	1341.878896	-0.214
$Mg(HCO_3)^+$	-1048131.82	-1048347	215.1801576	-0.021
$Ca(HCO_3)^+$	-1145625.608	-1145992	366.3916877	-0.032
$Ca(OH)^+$	-716735.3055	-716997	261.6944549	-0.036
$CaCO_3_Aragonite$	-1128274.3	-1128306	31.69994012	-0.003
$CaCO_3_Calcite$	-1129098.541	-1129127	28.45857172	-0.003
$CaMg(CO_3)_2_Dolomite$	-2167523.835	-2161565	-5958.83463	0.276

^a Nagra/PSI database [*Hummel et al.*, 2002].

^b Database based on EQ3/6, data0.ymf.





Content



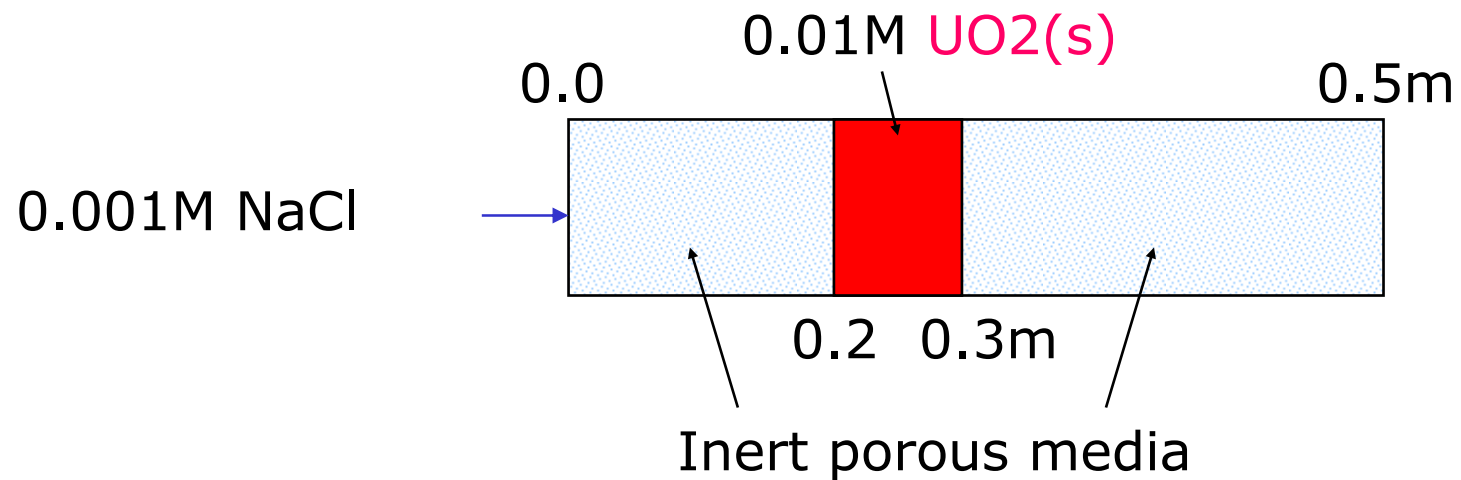
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Application Example

1D Transport and $\text{UO}_2(\text{s})$ dissolution

Simulated Program

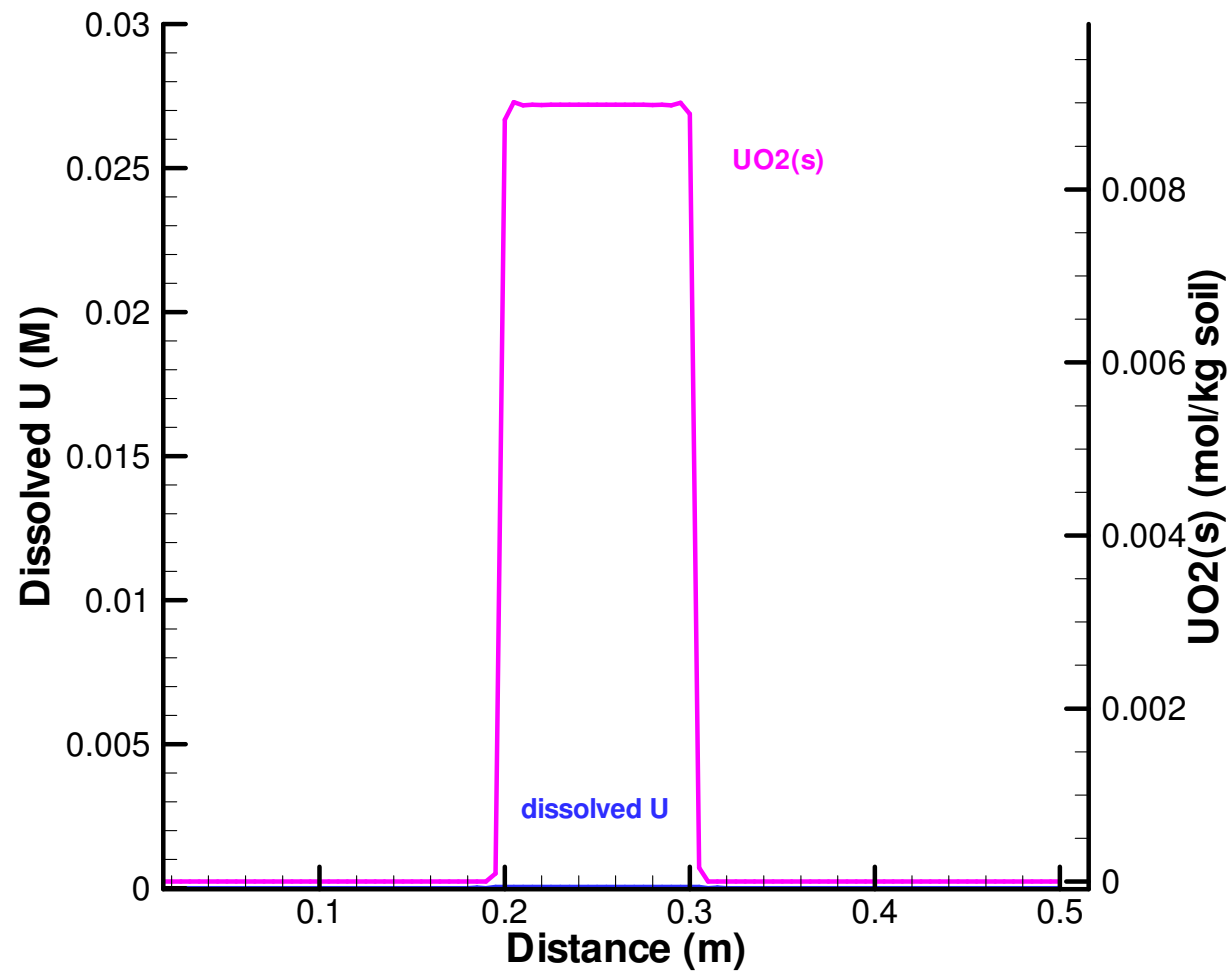
-- GeoSys/Rockflow+ChemApp (by Xie et al 2005)



UO₂(s) dissolution and transport



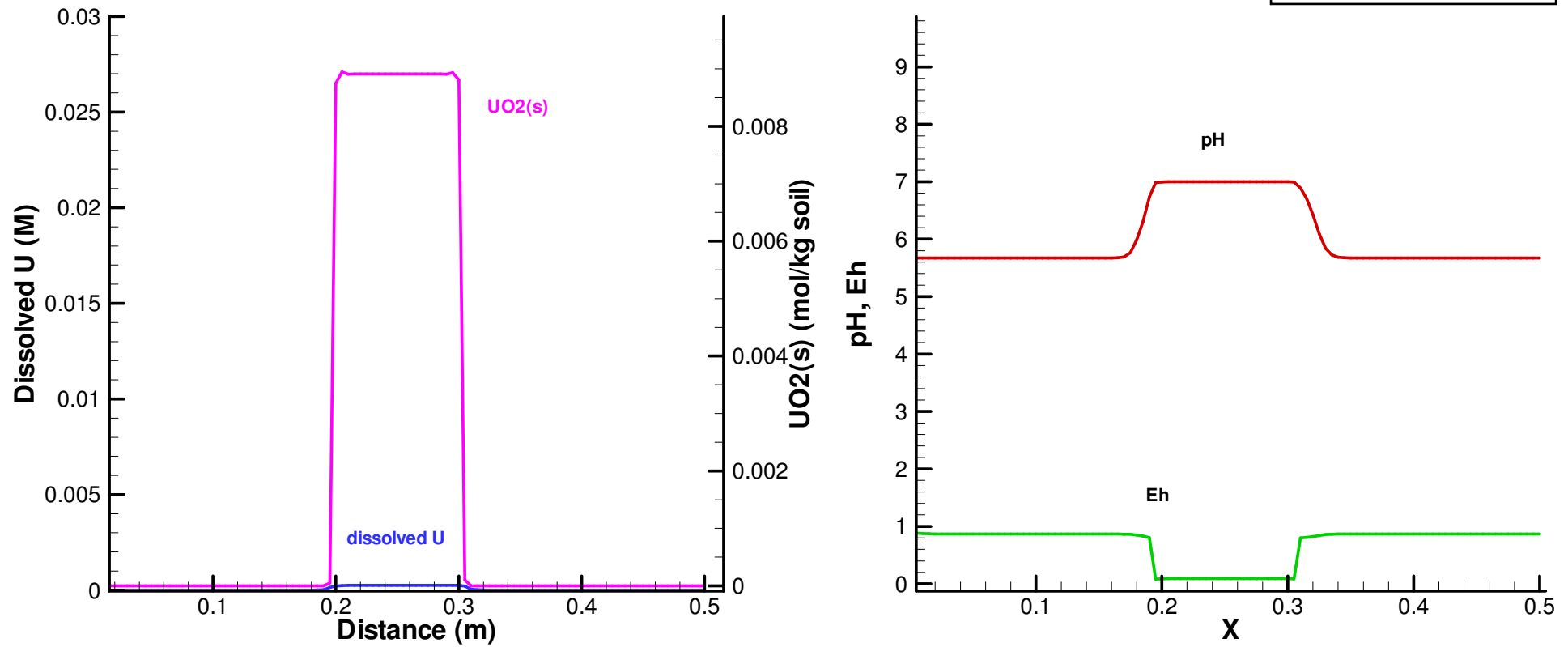
Initial



UO₂(s) dissolution and transport



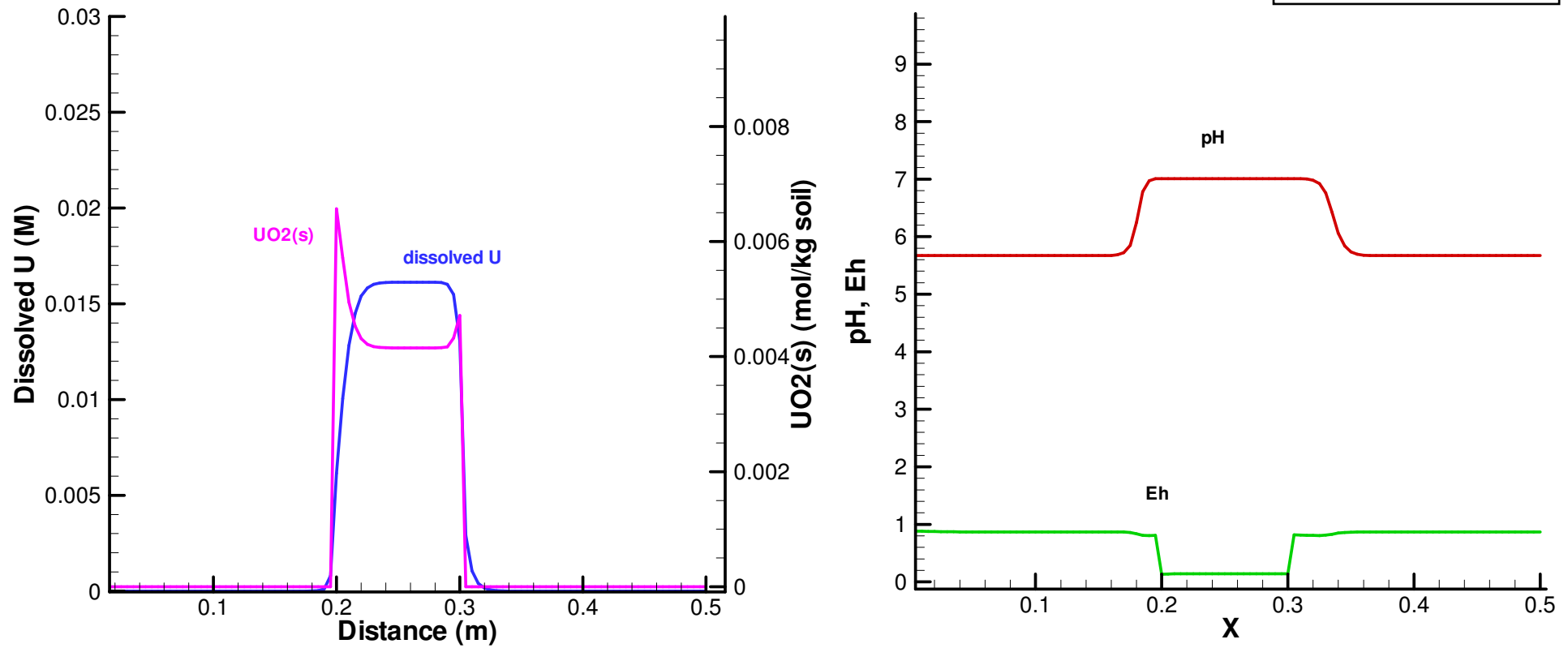
310 sec



UO₂(s) dissolution and transport



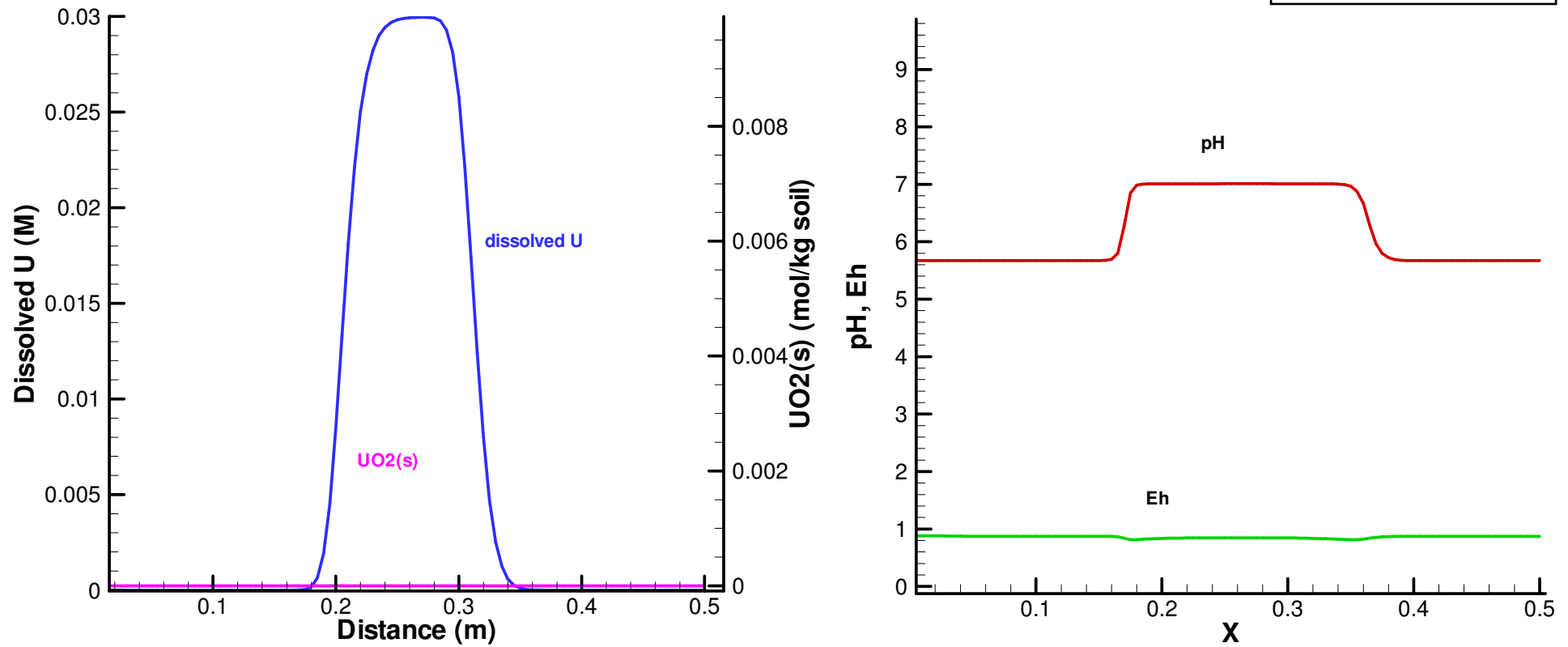
910 sec



UO₂(s) dissolution and transport



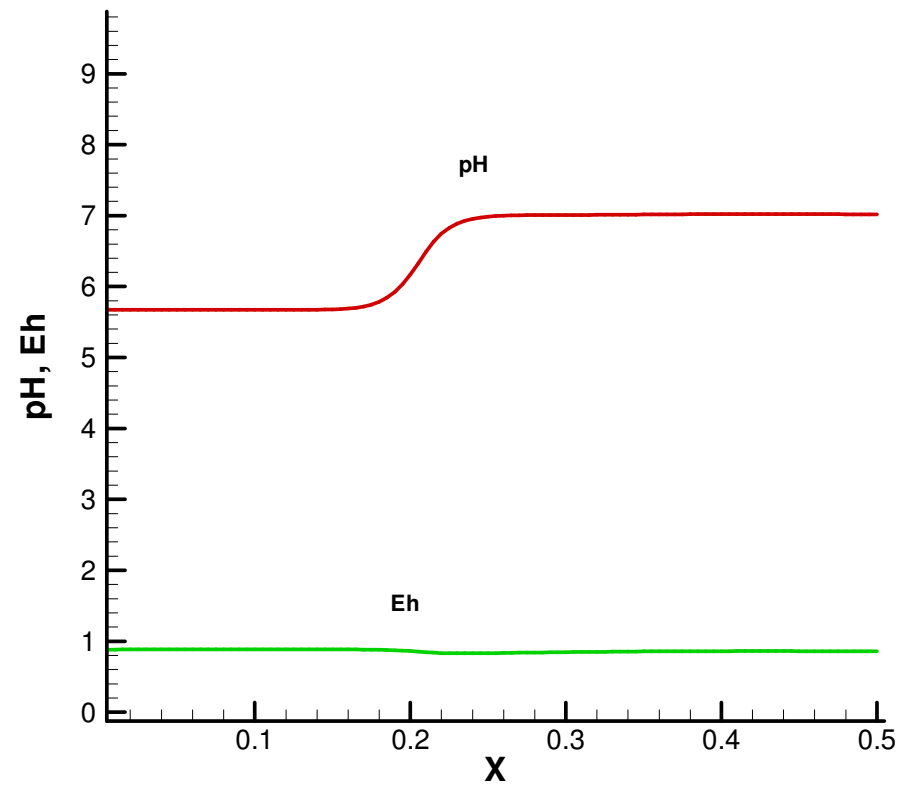
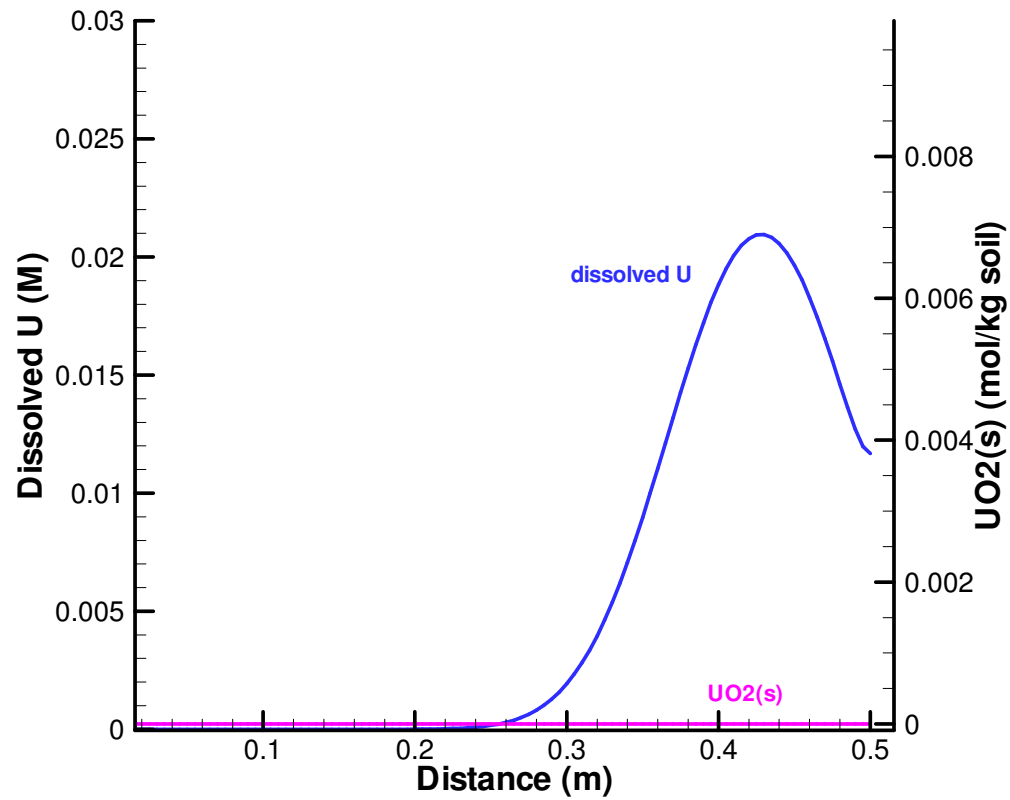
1110 sec



UO₂(s) dissolution and transport



2e4 sec



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Outlook

- Implementation of coupled effect of volumetric changes due to chemical reaction on HM-behaviour
- Corrosion of HLW container and gas production
- Performance assessment: Application to real systems
- Parallel computing