



Institute of Energy Process and
Chemical Engineering



Using SimuSage for the modelling of diverse processes in energy conversion

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- General steps in thermochemical modelling
- Slagging and fouling behaviour in a pulverized coal-fired boiler
- Slagging and fouling behaviour in pulverized coal-fired boiler for co firing of biomass
- Modelling of BGL-gasification processes - alkali metal cycle

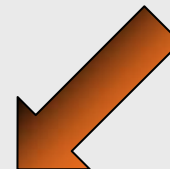
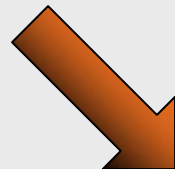
Why FactSage™ and SimuSage™ ?



- Thermochemical databases
- Data file



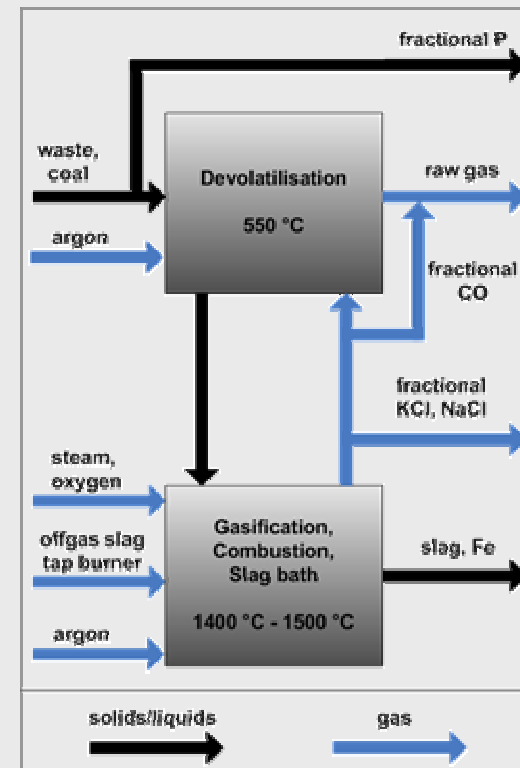
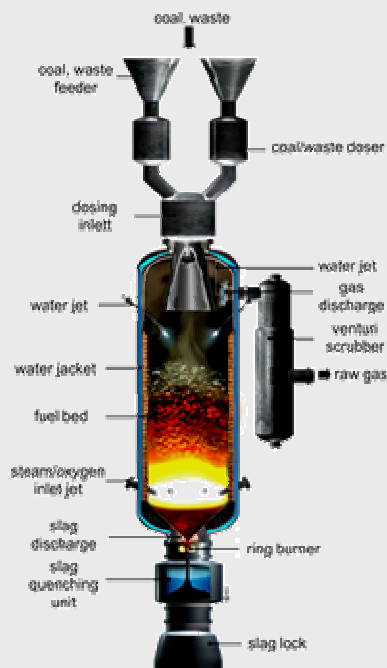
- local equilibrium stages
- material streams
- mixer, splitter, iterator
- interacting of single stages (recirculation, counter flow)
- Load/Save of interim results
- direct connecting to Excel™ (convenient result files, parameter calculations)



Thermochemical Model

Real process

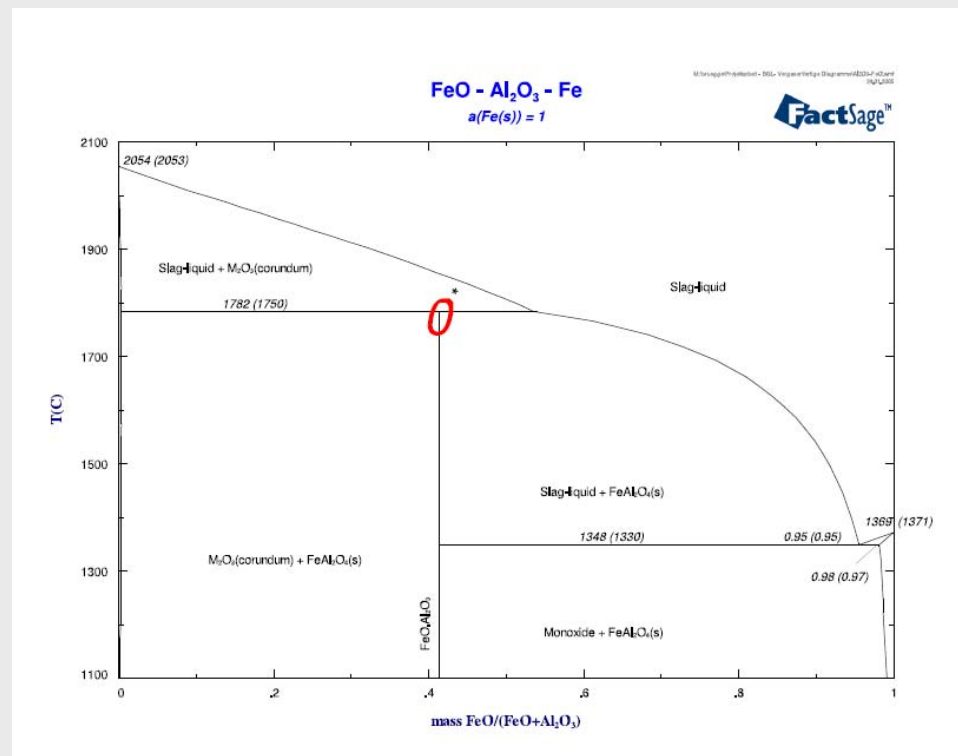
- Material balance, process parameters (as much information as possible, XRF, XRD...)
- Flow sheet for Stage Model
 - assembling of equilibrium units
 - isothermal/isenthalpic/isochoric?
 - definition of material flows
 - Equilibrium ?





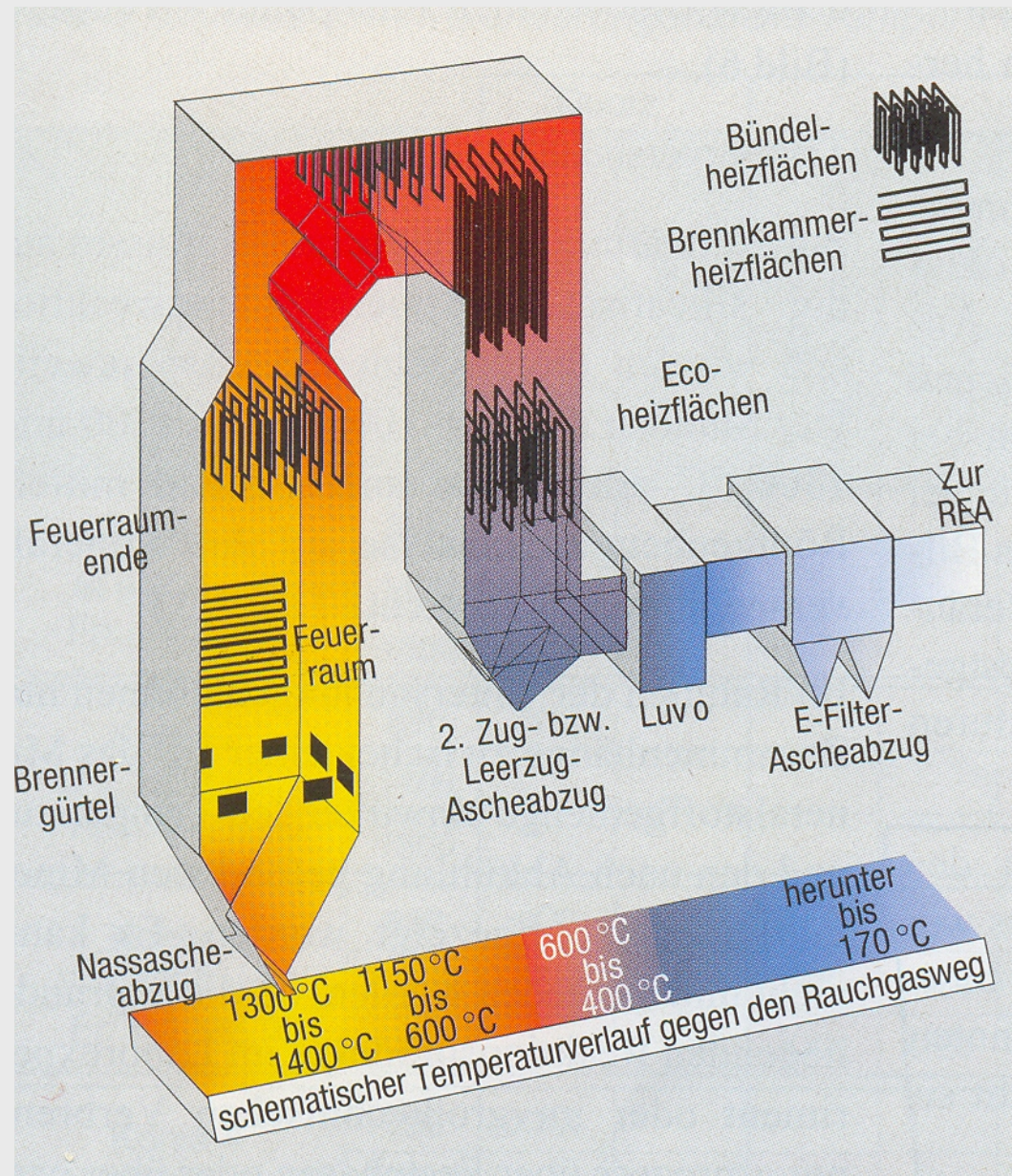
- selection of elements and possible products (solution phases!)
- rough calculation (reducing product list, equilibrium?)
- check thermodynamic data (calculation of binary and ternary systems, comparison to literature)

➤ data file





- definition of equilibrium stages
- definition of input and material flows
- adjusting equilibrium stages to non-equilibrium conditions (bypass, eliminated phases)
- evaluation with process data/samples (HT-XRD)
- application of the validated model

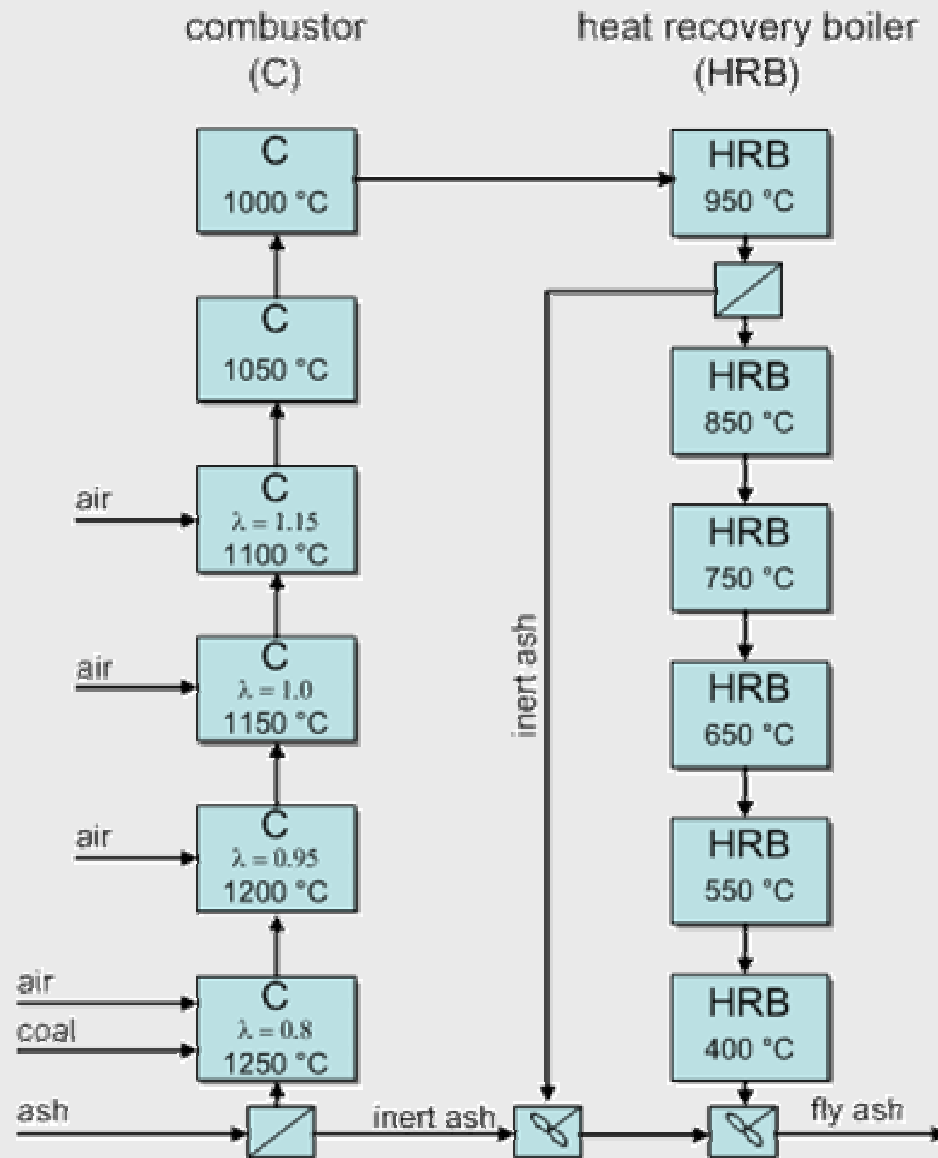


Model of pulverized coal-fired boiler (Dr. Muhammadieh)

- estimation of slagging and fouling for different coal mixtures
- kinetic inhibition for ash components is considered
- evaluated with HT-XRD of coal ashes and process samples
- development of classification numbers for the estimation of the slagging and fouling behaviour of new coal mixtures

Reference: M. Muhammadieh; 2007, "Beitrag zur Ermittlung des Ansatzbildungspotenzials von Braunkohlen in Dampferzeugern"; Dissertation TU-Freiberg [1]

Slagging and fouling behaviour in a pulverized coal-fired boiler

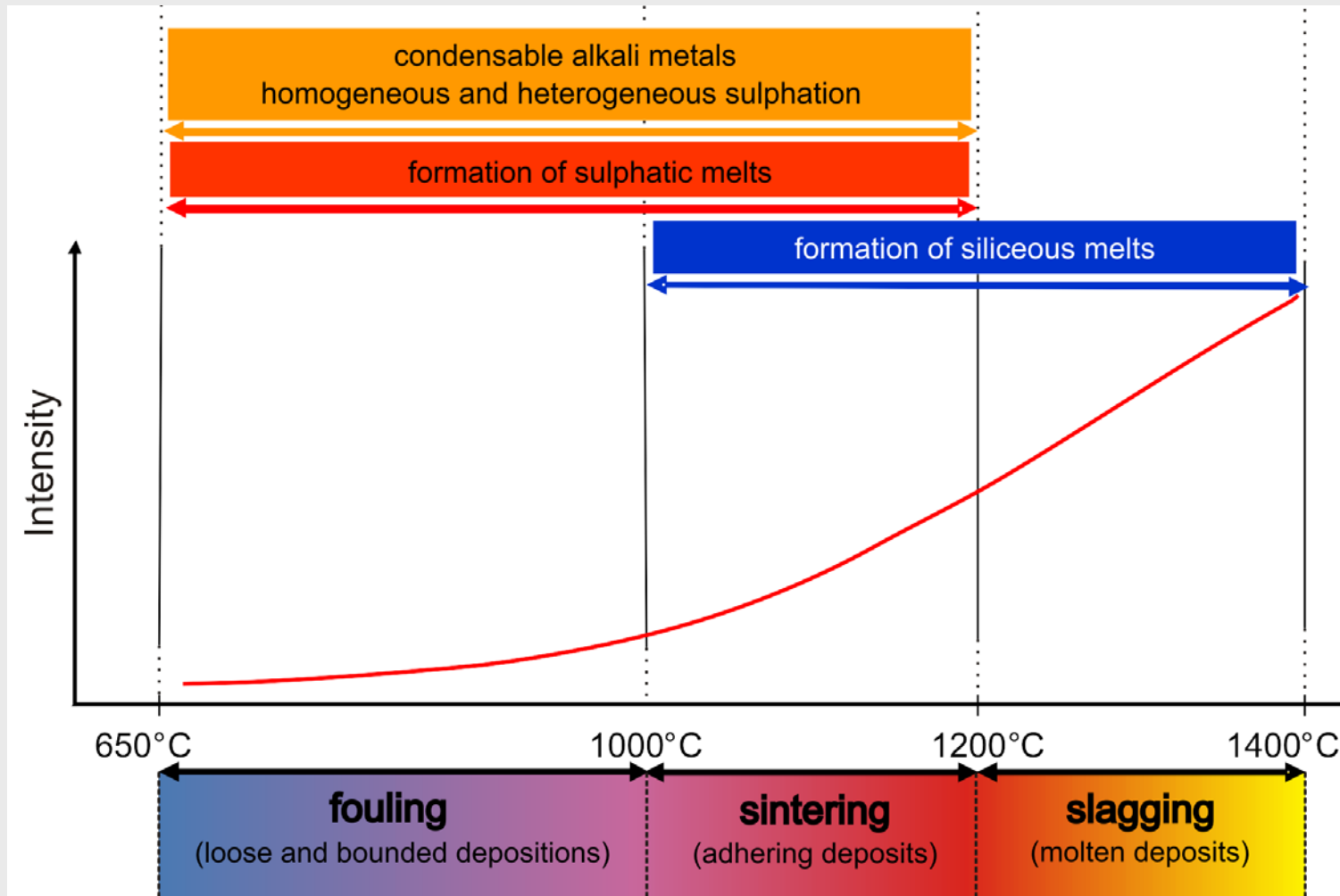


Reference: [1]

Definition of inert ash:

- fractionation of raw ash
- analysis of ash fraction (XRF, HT-XRD, AFT)
- definition of particle-size-effects
 - coarse ash fraction (quartz, layered silicates, siderite) as inert ash
 - fine-grained fraction (silt, clay) as reactive ash

Slagging and fouling behaviour in a pulverized coal-fired boiler



Reference: [1]

Classification numbers:

Slagging potential (T) = Fraction of siliceous melts * Ash fraction in coal

Fouling potential (T) = Fraction of sulfatic melts * Ash fraction in coal

Model of pulverized coal-fired boiler and estimation of the co-combustion of biomass on the slagging and fouling behaviour (Dr. Schreiner)

actual state: pulverized coal-fired boiler (hard coal – mixtures)

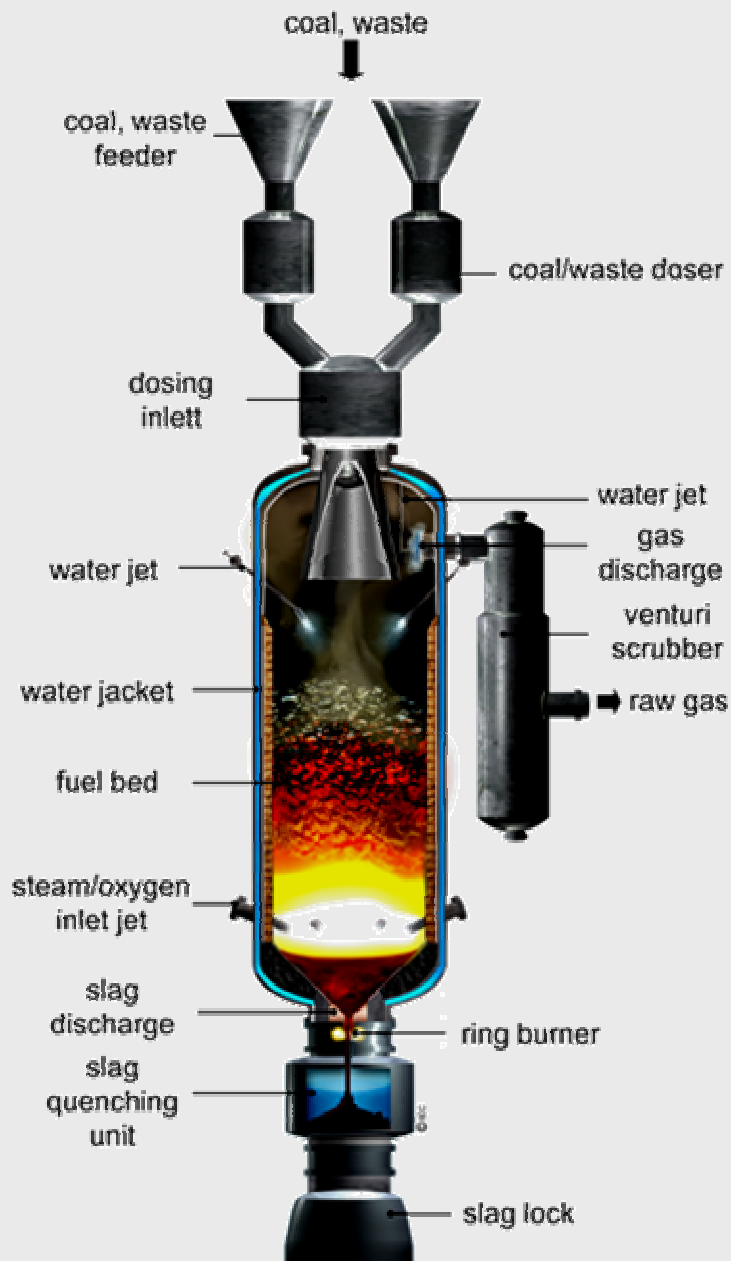
additional biomass feeding:

- external pyrolysis of wheat straw
- gaseous pyrolysis products to combustor
 - low alkali metal input

Model development:

- modelling of the hard-coal combustion, based on the previous shown model
- validating of the model
- implementing the gaseous pyrolysis products into the model
 - amount and composition (K, Na, Cl, S) from laboratory tests and test facility
- estimation of the slagging and fouling behaviour for the biomass feeding

- Motivation: deposit in the British Gas-Lurgi gasifier of the Sustec-Schwarze Pumpe-GmbH linked to alkali metal condensation
 - description of alkali metal volatilisation and condensation
- related problems in processes with reducing atmosphere:
 - deposit at raw gas heat exchangers (Shell/Texaco)
 - reduced efficiency
 - pressure drop
 - accumulation of alkali metals in blast furnaces
 - coke-stability
 - deposit reduce fix bed diameter
 - evaporation/condensation affects energy distribution



- operating pressure: 24 bar

- raw gas temperature

- at discharge: 550 °C

- after scrubber: 200 °C

In:

- MSW + coal: 24 - 30 t/h

- oxygen: 4000 - 6000 m³/h STP

- steam: 3.2 - 4.8 t/h

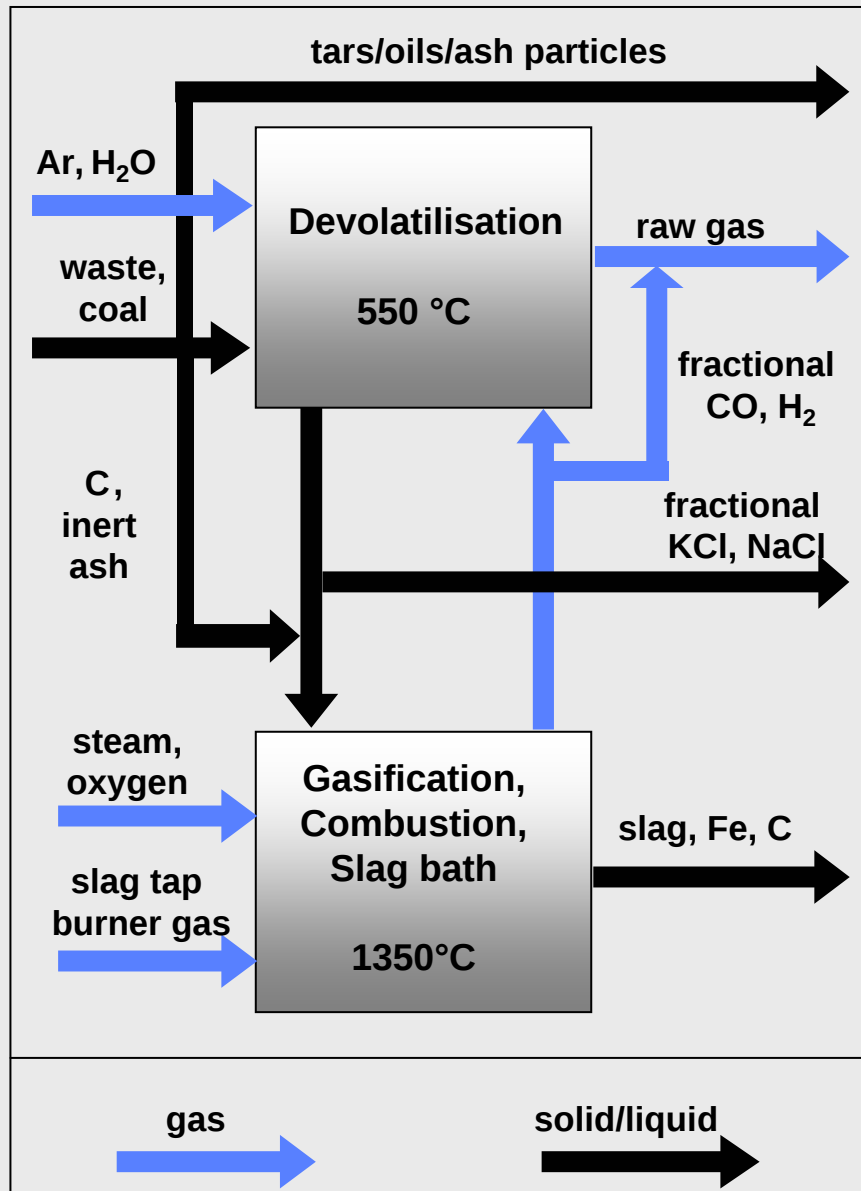
- steam-

- oxygen ratio: 0.8 – 1.2 kg/m³ STP

Out:

- raw gas: 35000 - 44000 m³/h STP, wf.

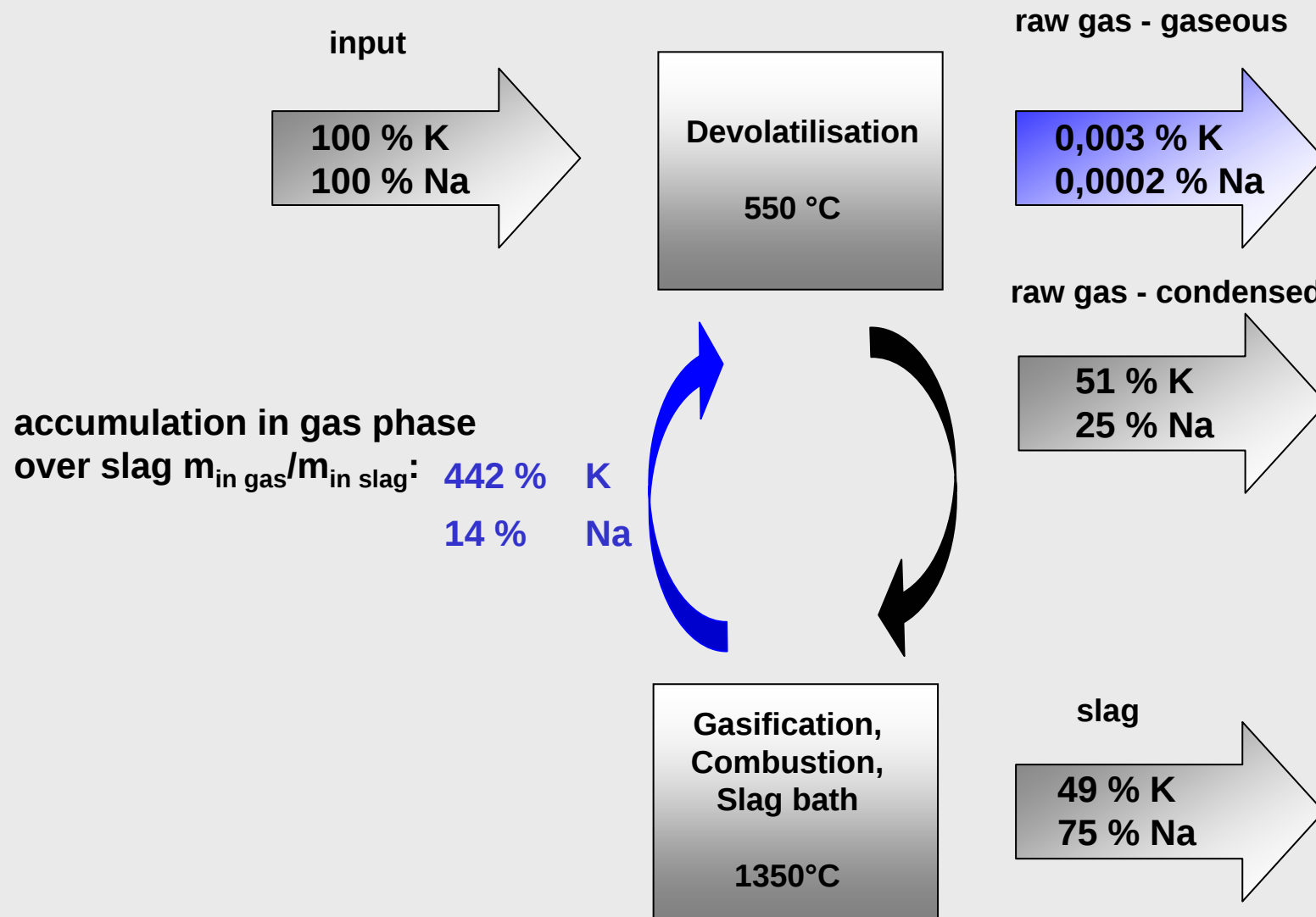
- slag: 3 – 5 t/h



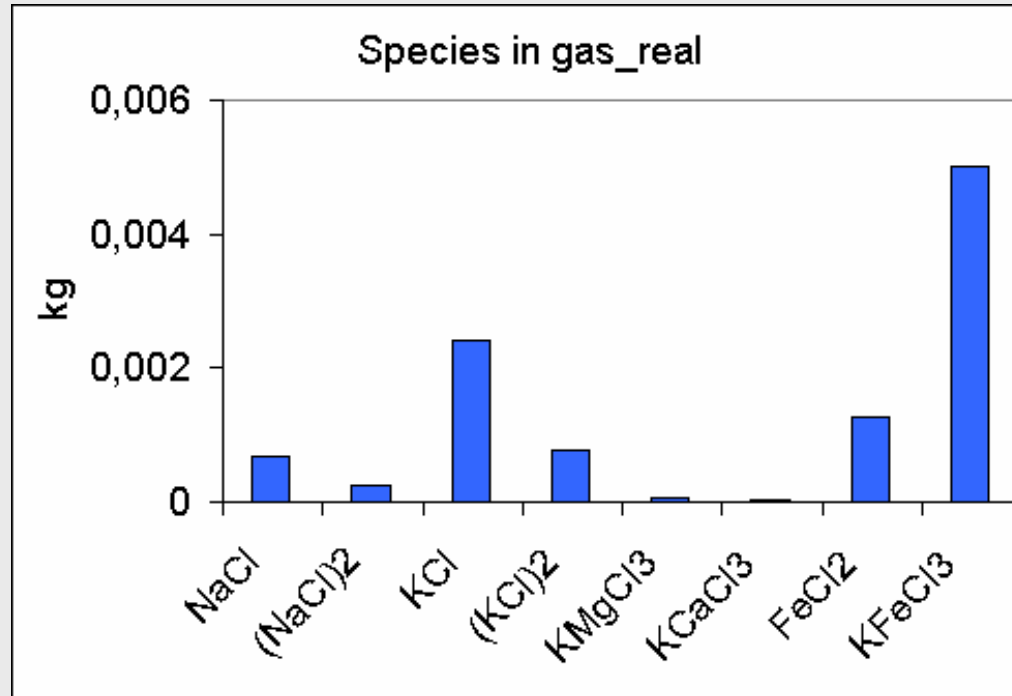
- kinetic inhibitions for permanent gases in cold stage: bypass for CO, H₂ and elimination of graphite, compensation with argon for constant partial pressures
- direct C-Input for hot stage
- bypass for tars and oils, ash of non-volatiles (material balance of process samples)
- condensed volatile ash components

$$m_{i \text{ kond. inTÖF}} = m_{i,IN} - m_{i \text{ in slag}} - m_{i \text{ in gas}}$$
- kinetic inhibitions for non-volatile ash components

- Distribution of K and Na on outlet streams and accumulation in alkali cycle:



- Gaseous and condensed volatiles in raw gas:



	mg/m ³ STP
K-Species gaseous	0.22
Na-Species gaseous	0.023
KCl condensed	4003
NaCl condensed	3774

- Composition of the slag stream (amount in kg):

ASlag-liq	5187
MgO	151
FeO	26
(Na ₂ O):2.000	152
SiO ₂	2251
TiO ₂	72
CaO	1585
(Al ₂ O ₃):2.000	789
(K ₂ O):2.000	54
MgS	3
CaS	32
FeS	1
(Na ₂ S):2.000	3
(K ₂ S):2.000	1
NaCl	5
KCl	1
CaCl ₂	50
MgCl ₂	6
FeCl ₂	1

Fe-liq	271
Fe	226
C	9
Cu	19
Al	5,E-06
N	1,E-02
P	11
S	1,E-02
Si	1,E-03
Ti	7,E-05
O	1,E-03
SiO	3,E-06
FeS	6
C_graphite(s)	216

- Composition of the gas phase in the hot stage:

Spezies K	kg
KCl	330
(KCl) ₂	55
KCaCl ₃	13
KMgCl ₃	3.E-01
KFeCl ₃	2.E-01
KCN	2.E-01
K	1.E-01
KOH	2.E-02
KH	8.E-04
KAlCl ₄	2.E-04
(KCN) ₂	3.E-06

Spezies Na	kg
NaCl	39
(NaCl) ₂	1
NaCN	1.E-01
Na	5.E-02
NaMgCl ₃	8.E-03
NaOH	2.E-03
NaH	7.E-04
Na ₂ MgCl ₄	2.E-04
NaAlCl ₄	2.E-05
NaFeCl ₄	1.E-05
(NaCN) ₂	3.E-06

- partial pressure K-species: 0.127 bar
- partial pressure Na-species: 0.018 bar

➤ concentration of alkali metal species as information for corrosion mechanisms of refractory lining

Thank you for your attention!

Questions?

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