

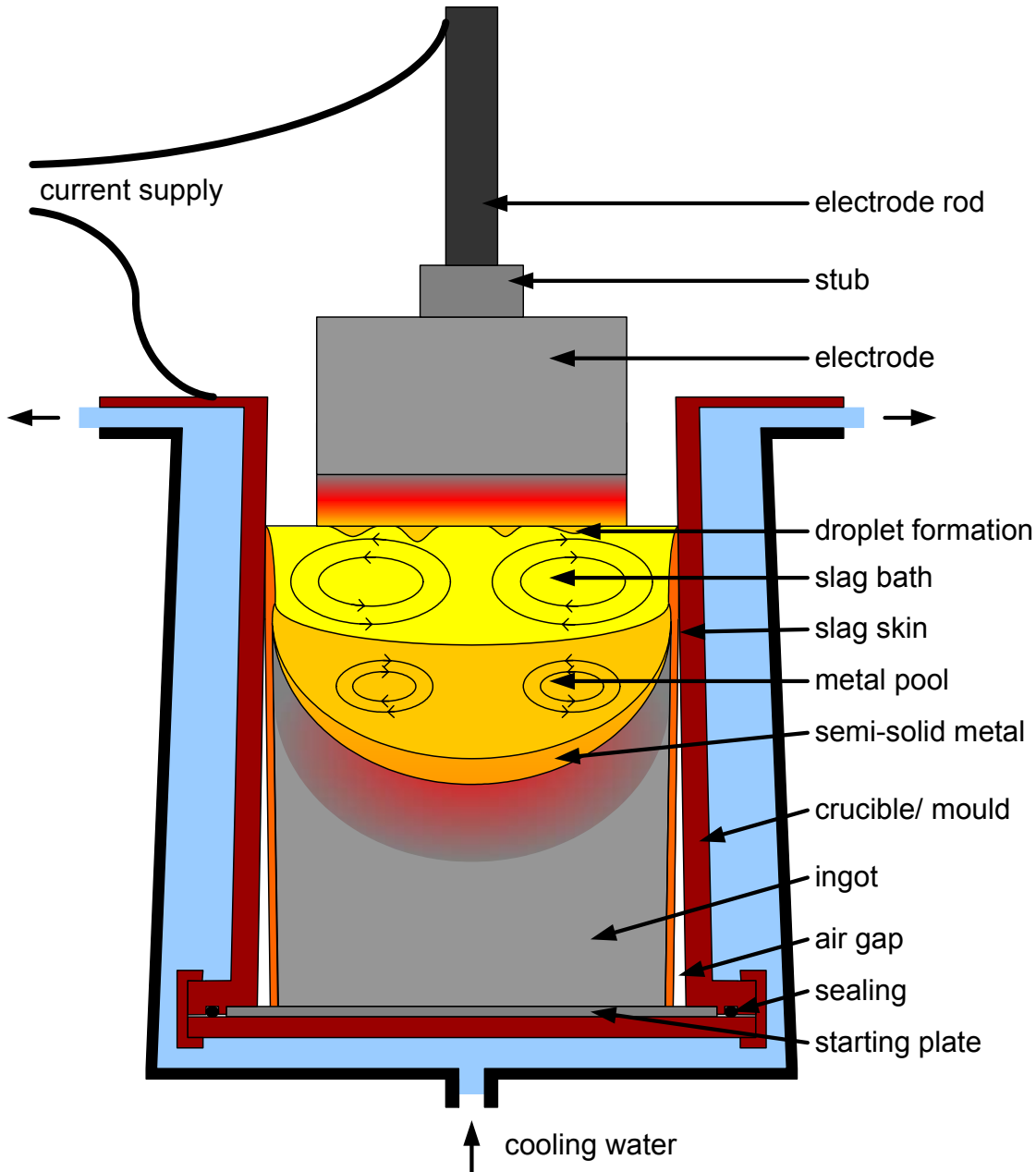


# **Kinetics of the calcium evaporation from active $\text{CaF}_2$ -slags during pressure electro slag remelting**

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# Application of PESR with active slags at IME Aachen



active slag:

- $\text{CaF}_2 + \text{Ca-metal (+ CaO)}$
- no  $\text{Al}_2\text{O}_3$ ,  $\text{SiO}_2$ , etc.

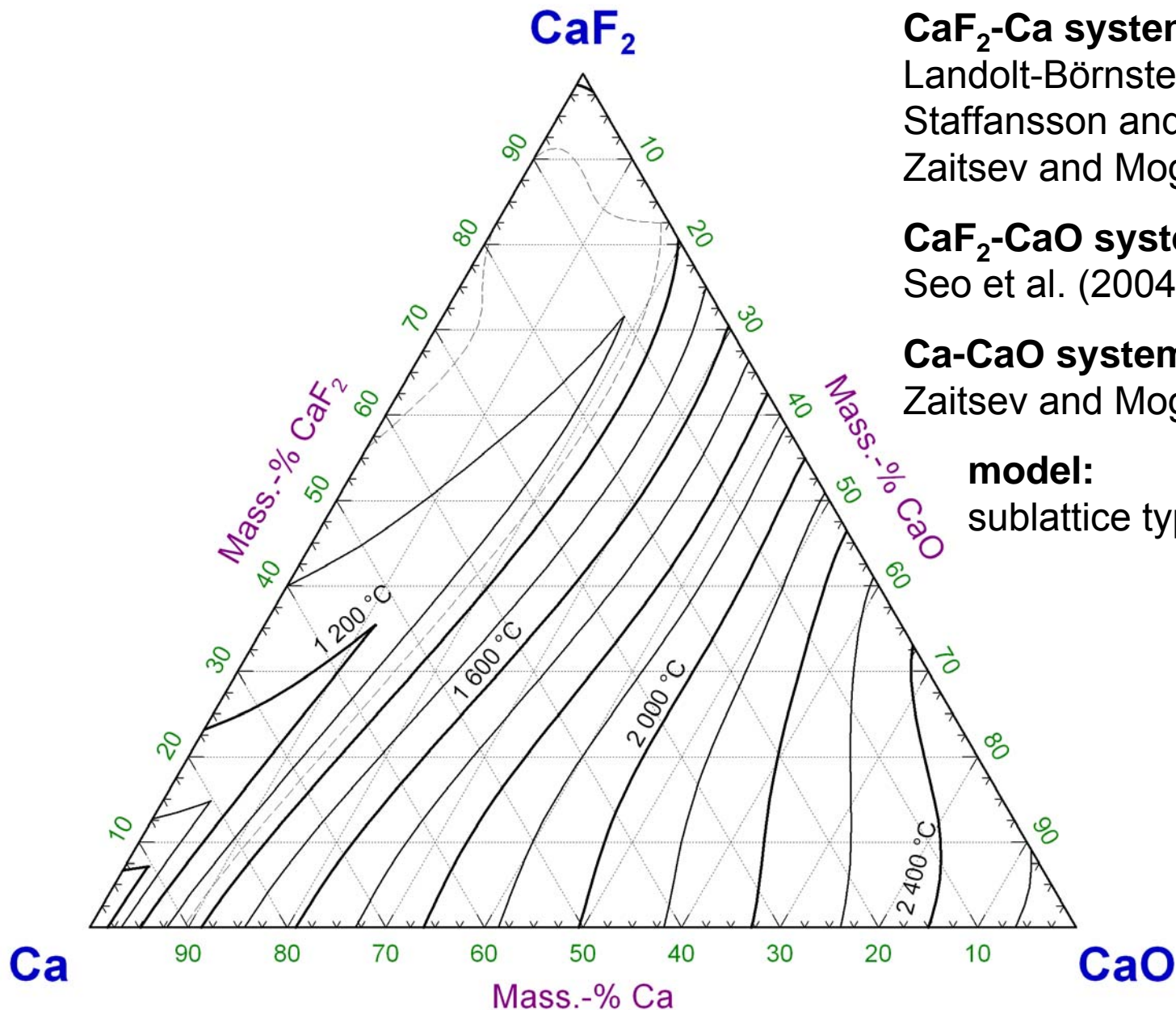
desoxidation of:

- Fe-Cr-alloys
- Ti-(Al)-alloys

preventing oxidation of:

- Ni-Fe-Be-alloy

# Ternary $\text{CaF}_2$ -Ca-CaO system modelled with OptiSage



**$\text{CaF}_2$ -Ca system:**

Landolt-Börnstein (1993),  
Staffansson and Sichev (1992),  
Zaitsev and Mogutnov (2001)

**$\text{CaF}_2$ -CaO system:**

Seo et al. (2004)

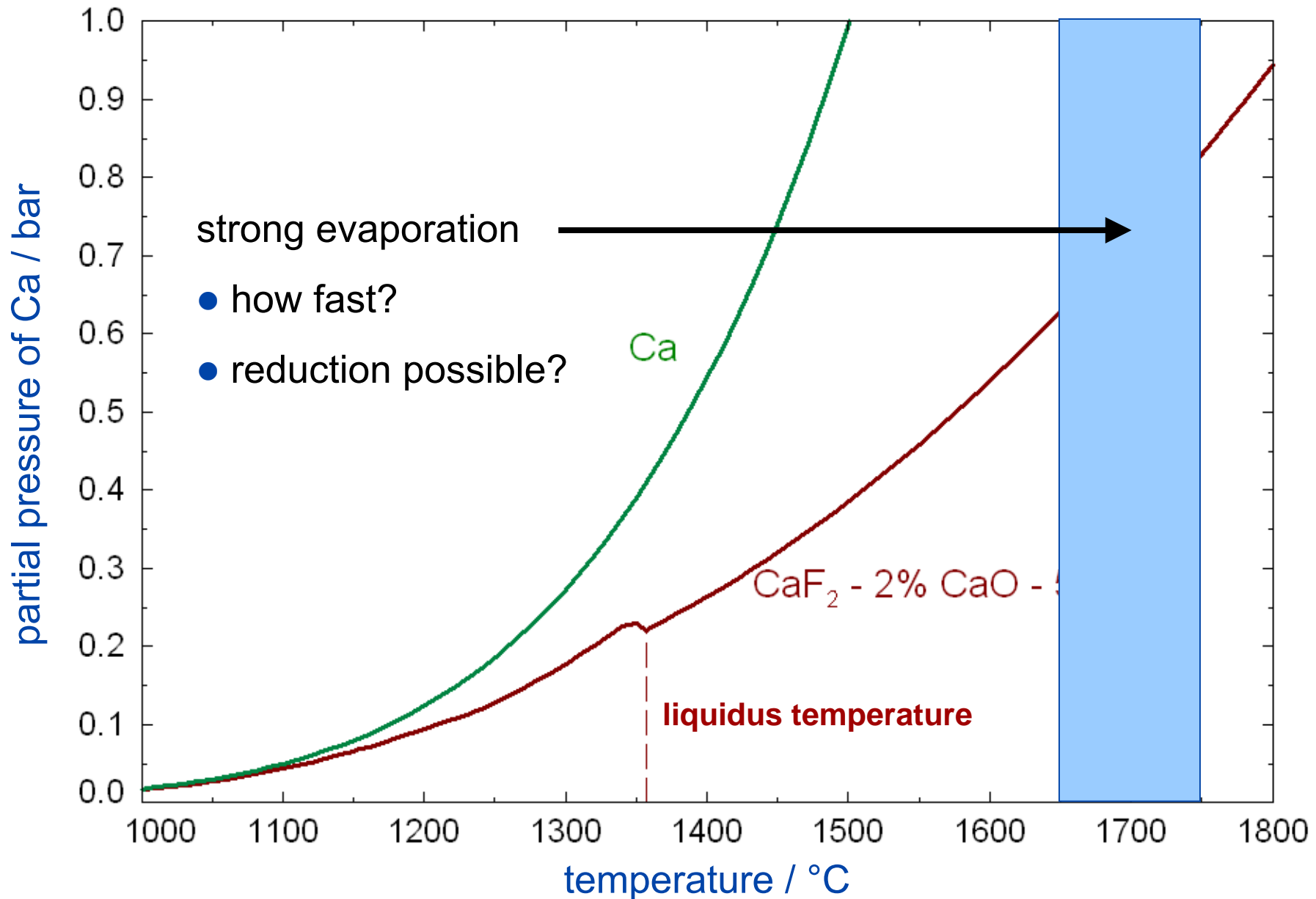
**Ca-CaO system:**

Zaitsev and Mogutnov (2001)

**model:**

sublattice type, Kohler/Toop

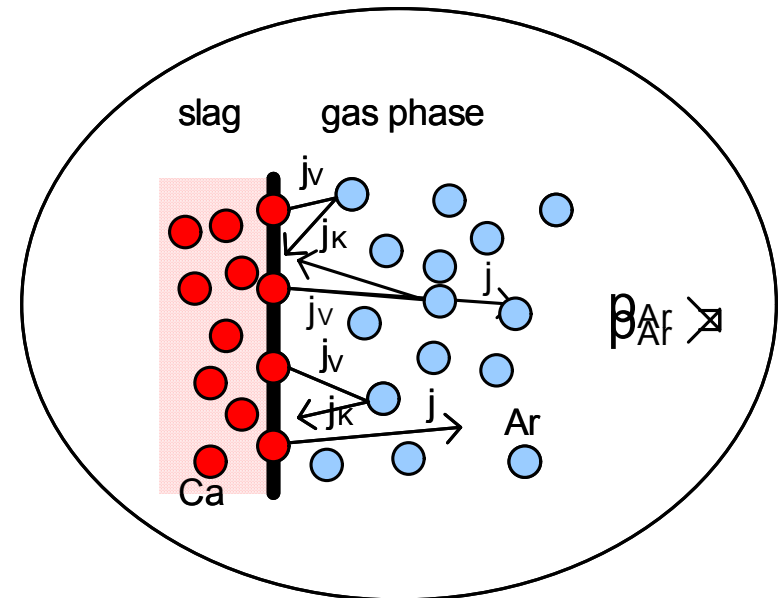
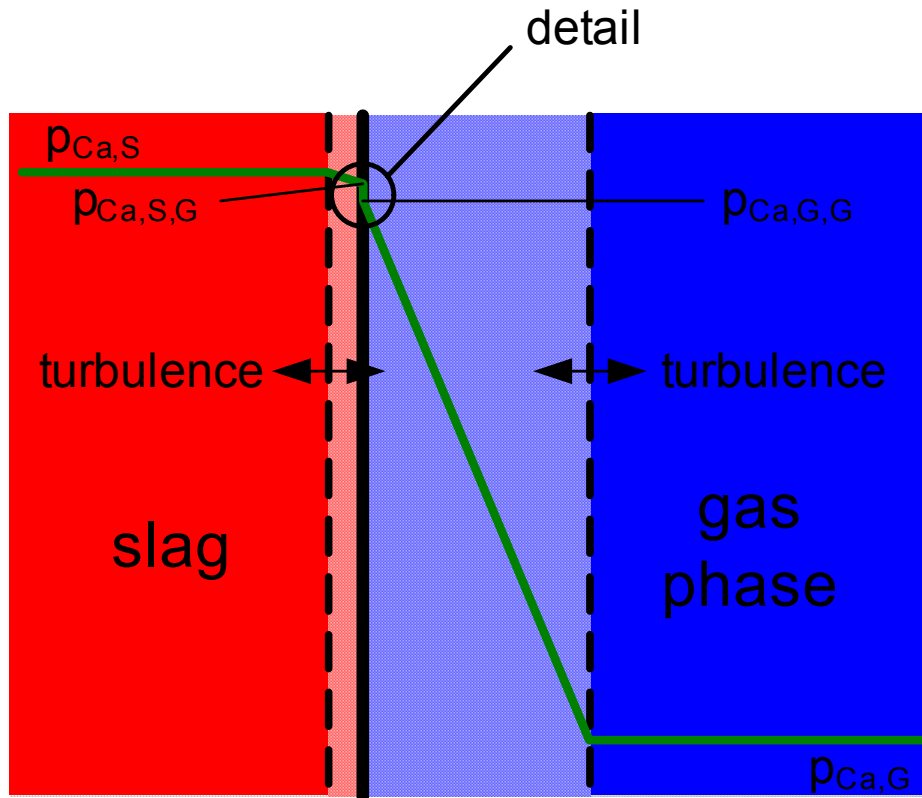
# Partial pressure of Ca in equilibrium



# Fundamentals of the Ca evaporation

$$[\text{Ca}]_{\text{slag}} \Leftrightarrow \{\text{Ca}\}_{\text{gas}} \quad \rightarrow \quad k = \frac{p_{\text{Ca}} / p^*}{x_{\text{Ca,slag}} \cdot f_{\text{Ca,slag}}}$$

→ thermochemical view: no system pressure dependency, if  $f_{\text{Ca}} = \text{const.}$



→ kinetical view: dependency from system pressure and gas turbulence!

# Kinetic of the evaporation step

Hertz-Knudsen:

$$j = j_V - j_K = \alpha_V \cdot \frac{1}{\sqrt{2\pi M_{Ca} R T}} \cdot p_{Ca,S,G} - \alpha_K \cdot \frac{1}{\sqrt{2\pi M_{Ca} R T}} \cdot p_{Ca,G,G}$$

Example:

- $\alpha_V = \alpha_K \approx 1$
  - $p_{Ca,G,G} = 0$  (Ca-transport in the gas phase is indefinitely fast)
  - $T = 1973 \text{ K}$
- $j = 1130 \text{ mol/m}^2\text{s}$  and  $16,8 \text{ mol/s}$  in IME-PESR-furnace, respectively
- The evaporation step would be nearly indefinitely fast.
- The mass transport in the gas phase must be the limiting step.

# Kinetic of the mass transport in the gas phase I

diffusion layer model (Fick's 1<sup>st</sup> Law):

$$j = -D \cdot \frac{\Delta c}{\Delta x} = -\frac{D}{\Delta x} \cdot \frac{p_{Ca,G,G}}{RT} \approx -\frac{D}{\Delta x} \cdot \frac{p_{Ca,S}}{RT}$$

calc. of the diffusion coefficient (kin. gas theory + med. free length of path) :

$$D = \frac{3}{16} \bar{v} \lambda = \frac{3}{16} \sqrt{\frac{8RT_S}{\pi \mu_{Ca-Ar}}} \cdot \frac{kT_S}{\sqrt{2} \sigma p} = \frac{3}{8} \sqrt{\frac{k^2 RT_S^3}{\pi \mu_{Ca-Ar} \sigma^2 p^2}} \sim \frac{1}{p}$$

calc. of the diffusion layer thickness:

$$\Delta x = \frac{L}{0,15 \cdot \sqrt[3]{Gr \cdot Sc \cdot f_2(Sc)}} = \frac{1}{0,15 \cdot \sqrt[3]{\frac{T_S - T_m}{T_m} \cdot \frac{g}{v \cdot D_m} \cdot f_2(Sc)}} \sim \frac{1}{p^{2/3}}$$

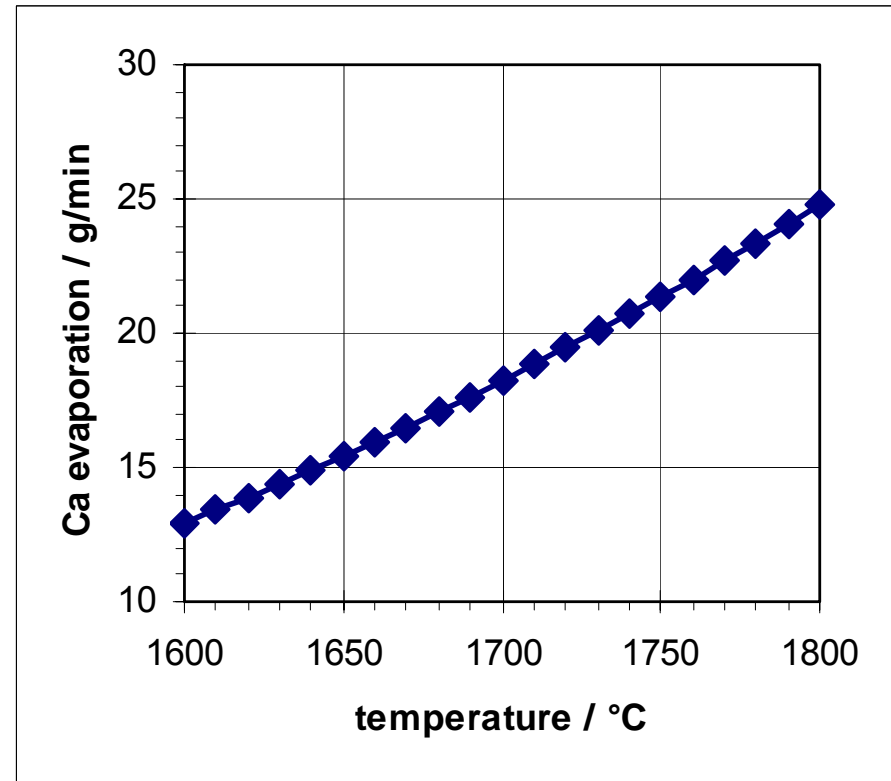
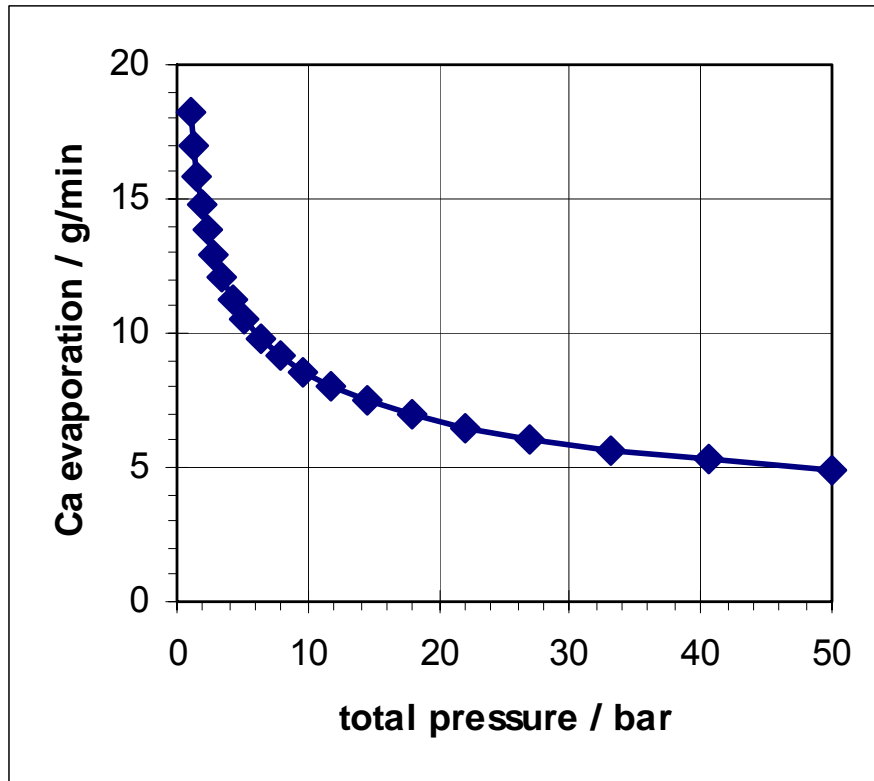
Sherwood's No. (Sh)

$$j \sim \frac{1}{\sqrt[3]{p}}$$

# Kinetic of the mass transport in the gas phase II

Example:

- $T_m = 100 \text{ }^\circ\text{C}$
- $\rightarrow \mu_{\text{Argon}} = 2,7 \times 10^{-5} \dots 2,8 \times 10^{-5} \text{ Pa s (1 ... 50 bar)}$
- $\rightarrow \nu_{\text{Argon}} = 2 \times 10^{-5} \dots 4,3 \times 10^{-7} \text{ m}^2/\text{s (1 ... 50 bar)}$





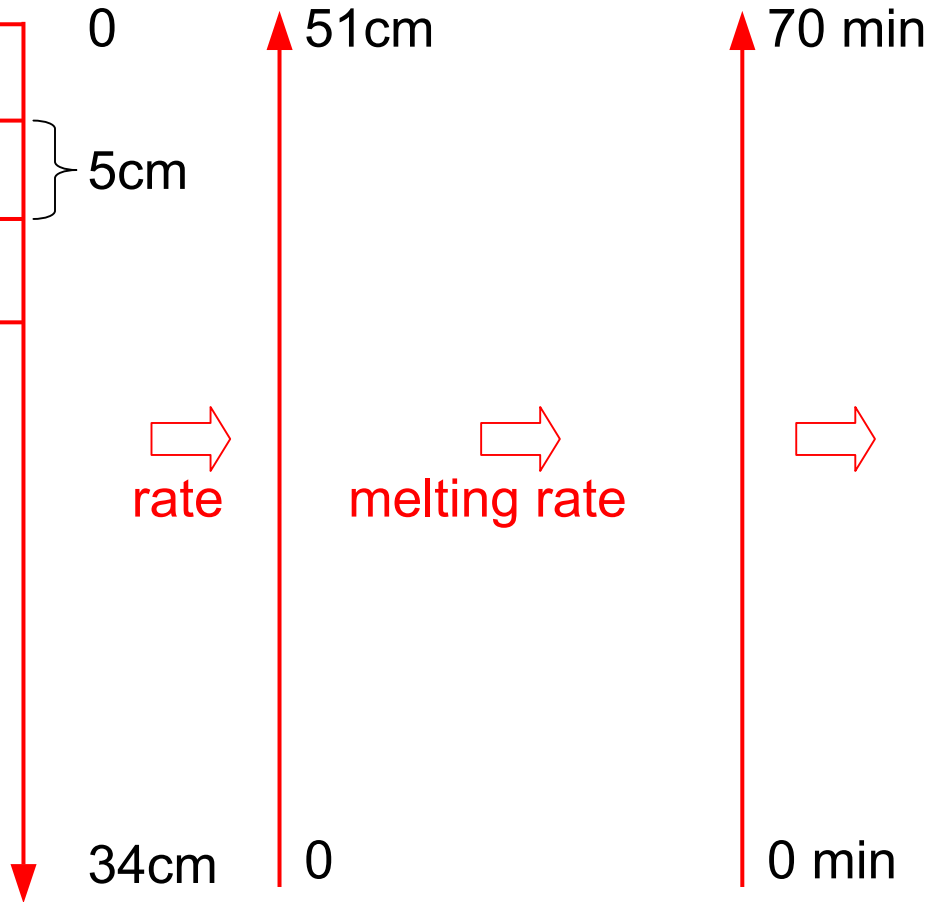
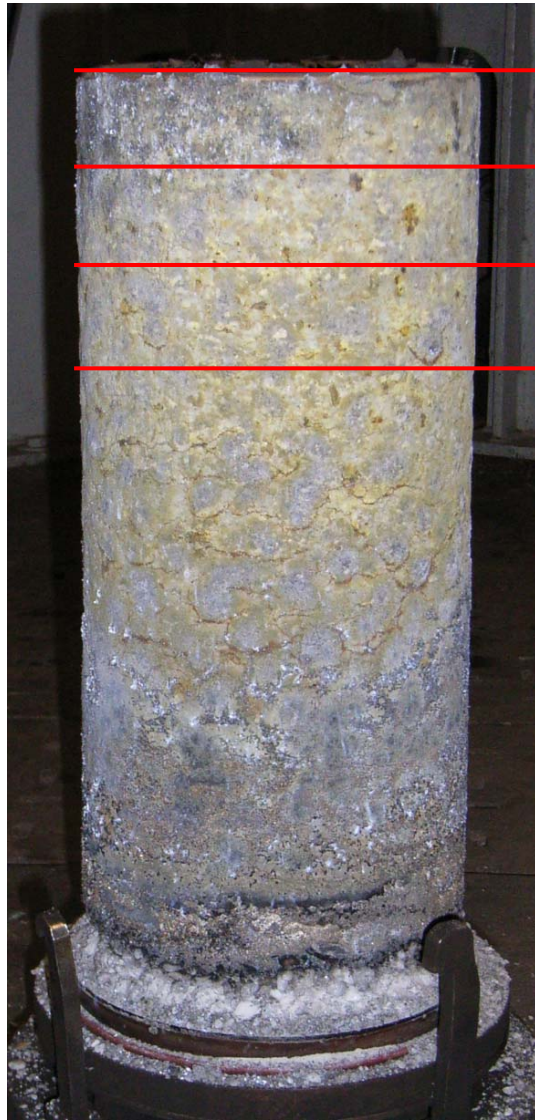
# Experimental examination

- 5 electrodes:
  - material: St 37
  - diameter: 100 mm
  - length: 1000 mm
- slag system:
  - 95 % CaF<sub>2</sub>-slag (Wacker 2052, > 97% CaF<sub>2</sub>, 1,2 % CaO)
  - 5 % Ca-metal
- shielding gas: Argon
- pressure: +1, +3, +7, +15 and +40 bar (over pressure).
- pressure increase during melting due to furnace temperature, blow off all 5 minutes
- side experiment:
  - temperature measurement with fibre optics and IR-pyrometer

# Experimental examination - results



# Experimental examination – evaluation I

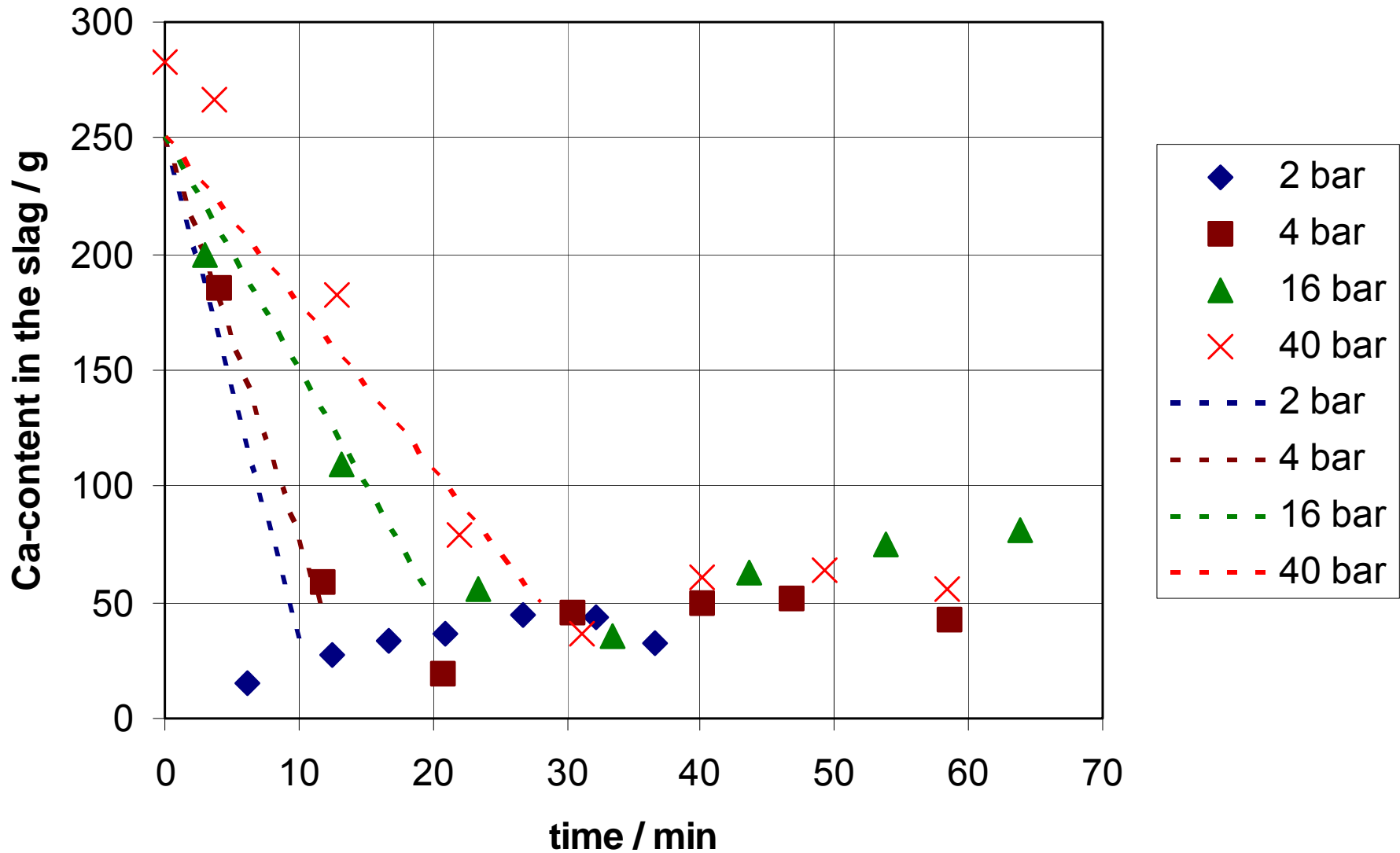


sample V03



t=25min  
c(Ca)=3,3%

# Experimental examination – evaluation II



# Summary and outlook

## Summary

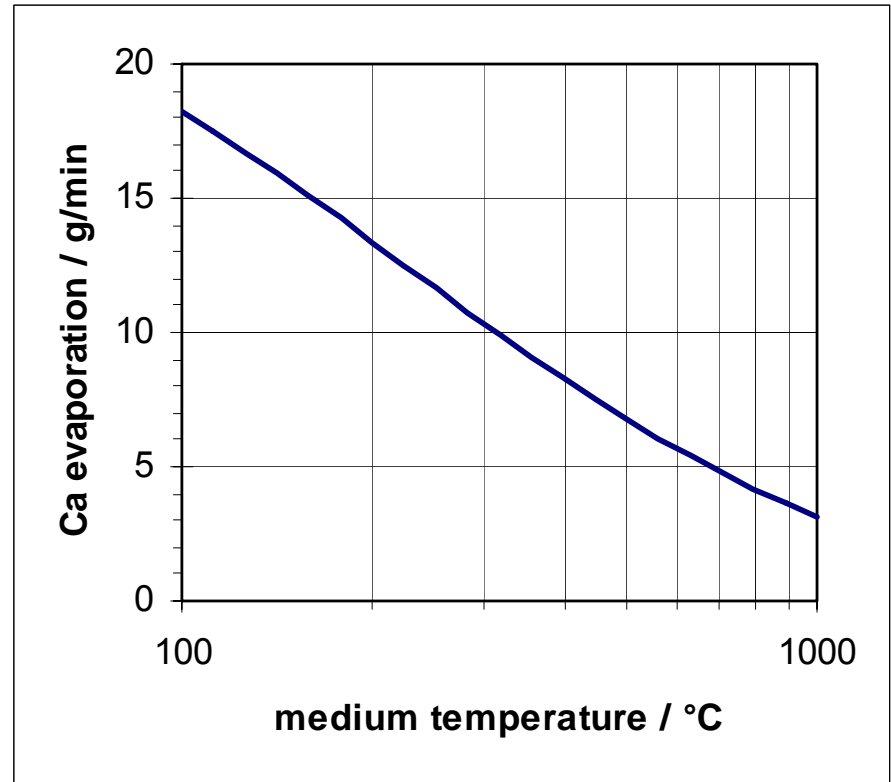
- Instead of the evaporation step (Hertz-Knudsen), the mass transport in the gas phase is relevant for the Ca losses.
- A kinetic model for calculation of the Ca losses was found using the similarity of heat and mass transfer:  
$$\text{Nu} = f(\text{Gr}, \text{Pr}) \rightarrow \text{Sh} = f(\text{Gr}', \text{Sc}).$$
- Increased pressure has low influence on the Ca losses (3<sup>rd</sup> root).

## Outlook

- Isolation of the mould top increases the medium gas temperature and decreases convection and Ca losses,

# Summary and outlook

$$\Delta x = \frac{1}{0,15 \cdot 3 \sqrt{\frac{T_s - T_m}{T_m} \cdot \frac{g}{v \cdot D_m} \cdot f_2(Sc)}}$$



## Outlook

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# Summary and outlook

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## Outlook

- Isolation of the mould top increases the medium gas temperature and decreases convection and Ca losses,
- Transfer of the model into other systems (Al-Mg, Al-Li, Ti-Al, ...).



**Thank you for your attention**

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